

Implementation and Refinement of a Comprehensive Model for Dense Granular Flows

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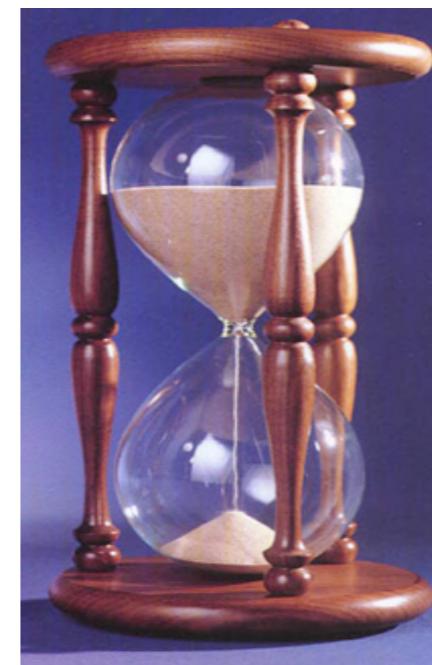


This work is supported by DOE-UCR
grant DE-FE0006932.



Motivation

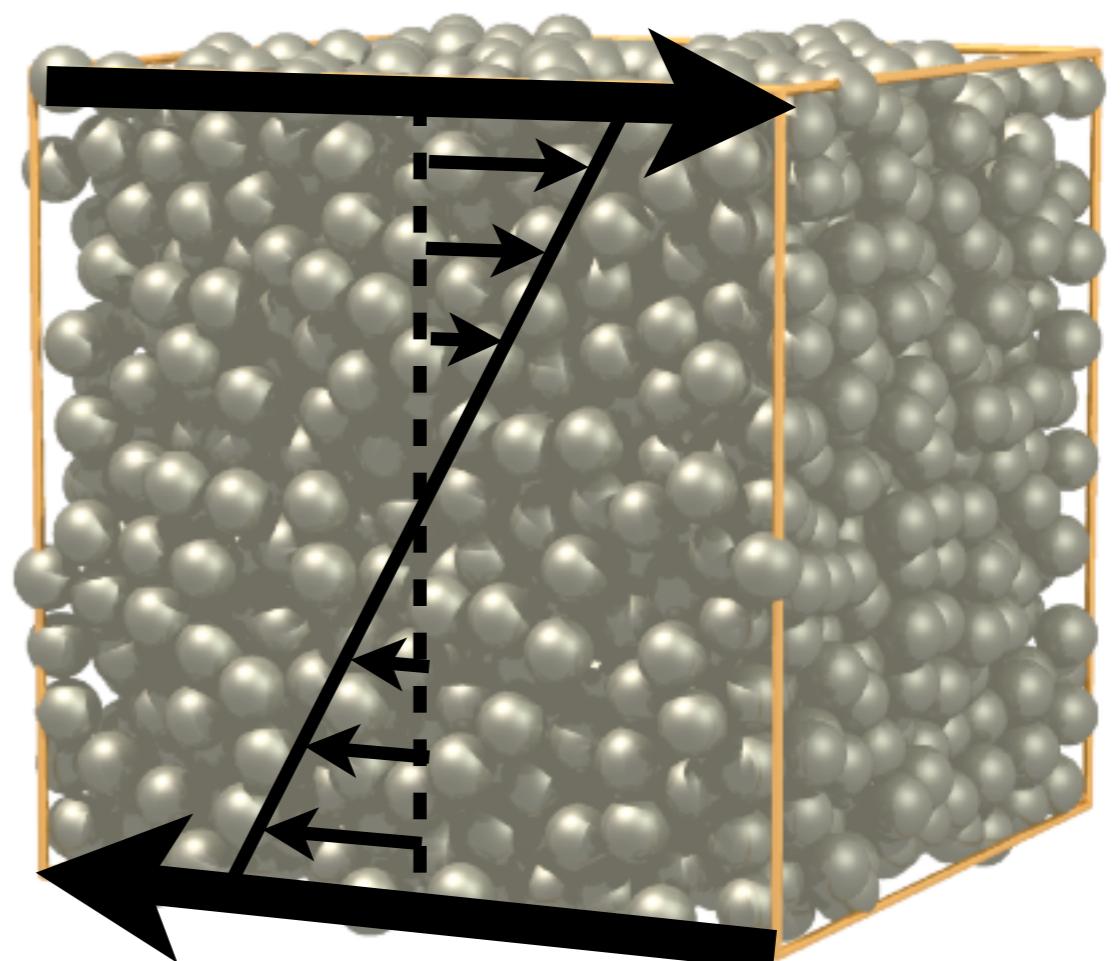
- Granular flows are ubiquitous in nature and in industry, e.g. avalanches and hopper discharge.
- Complex behavior: solid-, liquid-, or gas-like



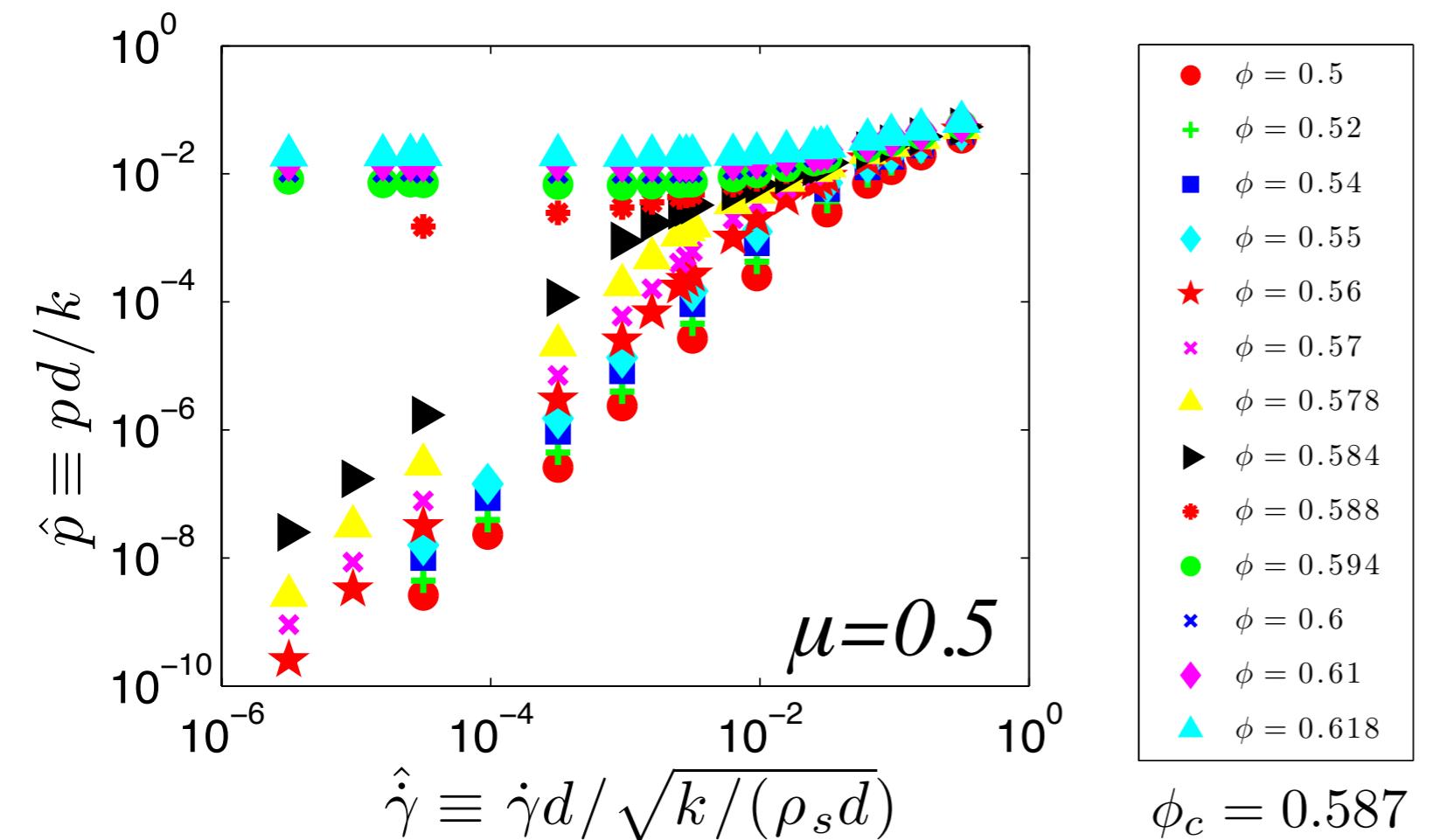
- Goal: To probe flow behavior computationally and develop general rheological models.

Computational methodology

- Simulate particle dynamics of homogeneous assemblies under simple shear using discrete element method (DEM).
 - ▶ Linear spring-dashpot with frictional slider.
 - ▶ 3D periodic domain without gravity
 - ▶ Lees-Edwards boundary conditions
- Extract stress and structural information by averaging.



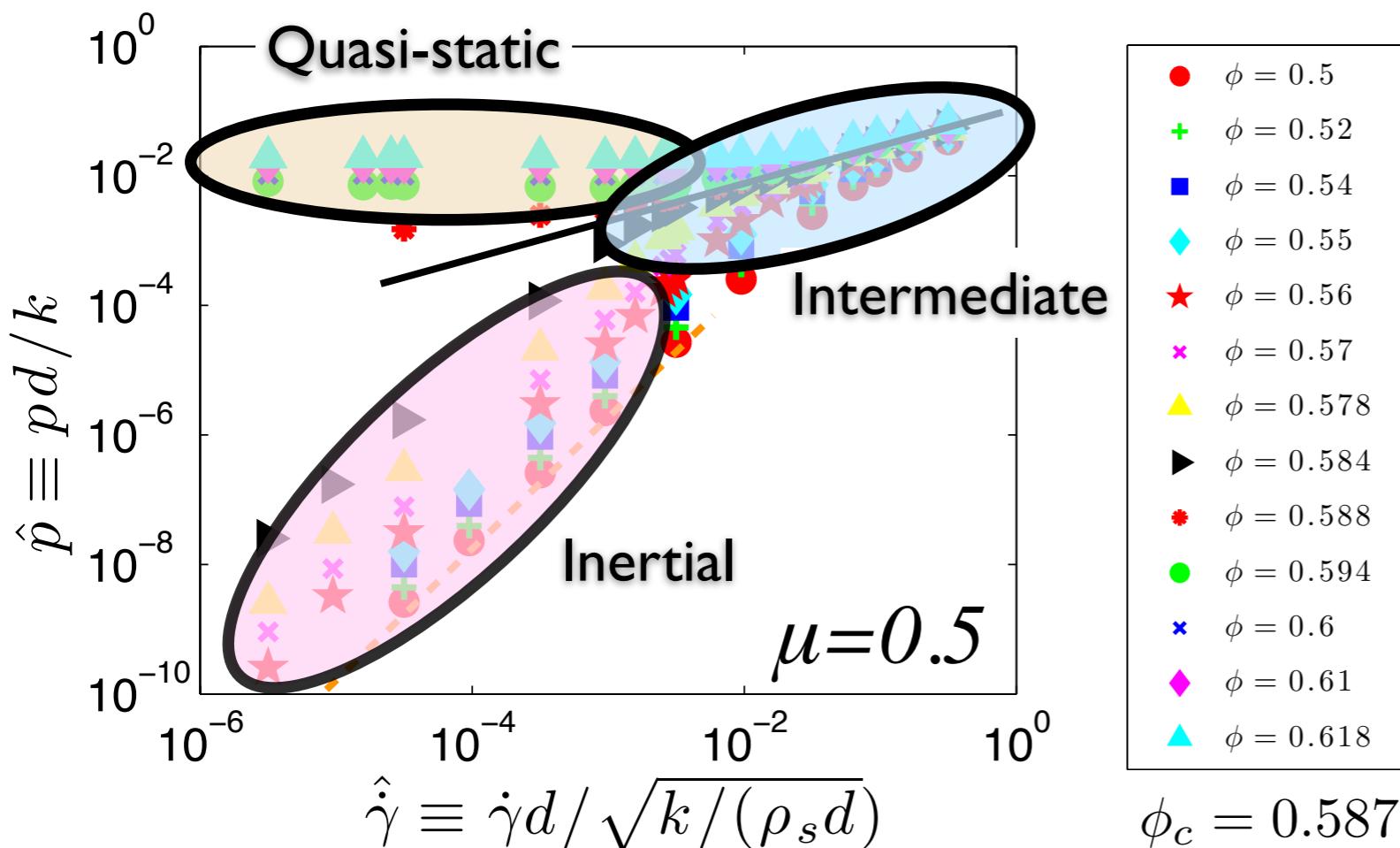
Flow map



Previous studies

- Computational
 - ▶ C. S. Campbell, J. Fluid Mech. 465, 261 (2002).
 - ▶ T. Hatano, J. Phys. Soc. Japan 77, 123002 (2008).
- Experimental
 - ▶ K. N. Nordstrom et al. Phys. Rev. Lett. 105, 175701 (2010).

Flow map



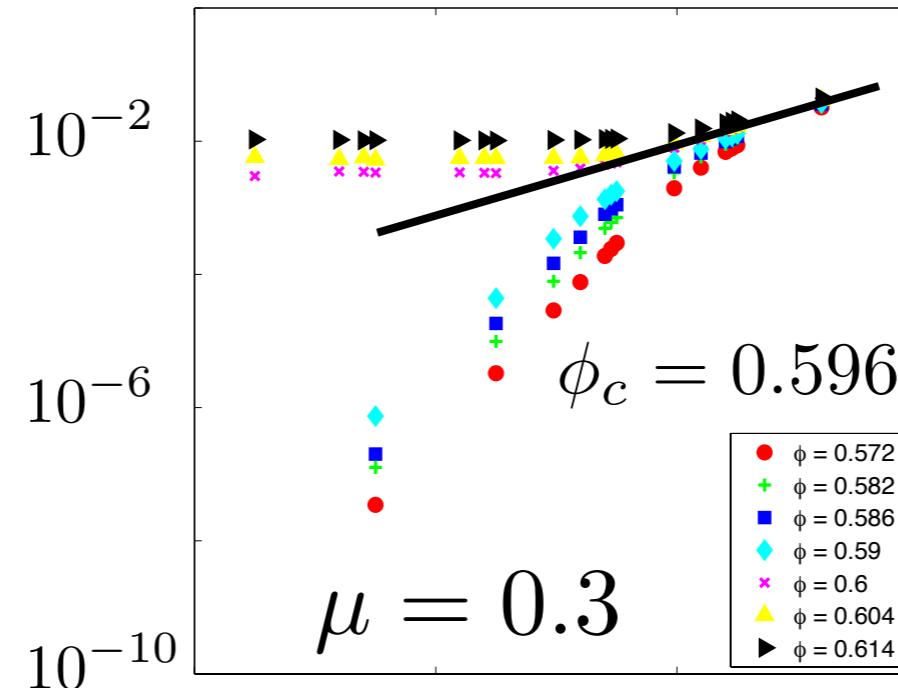
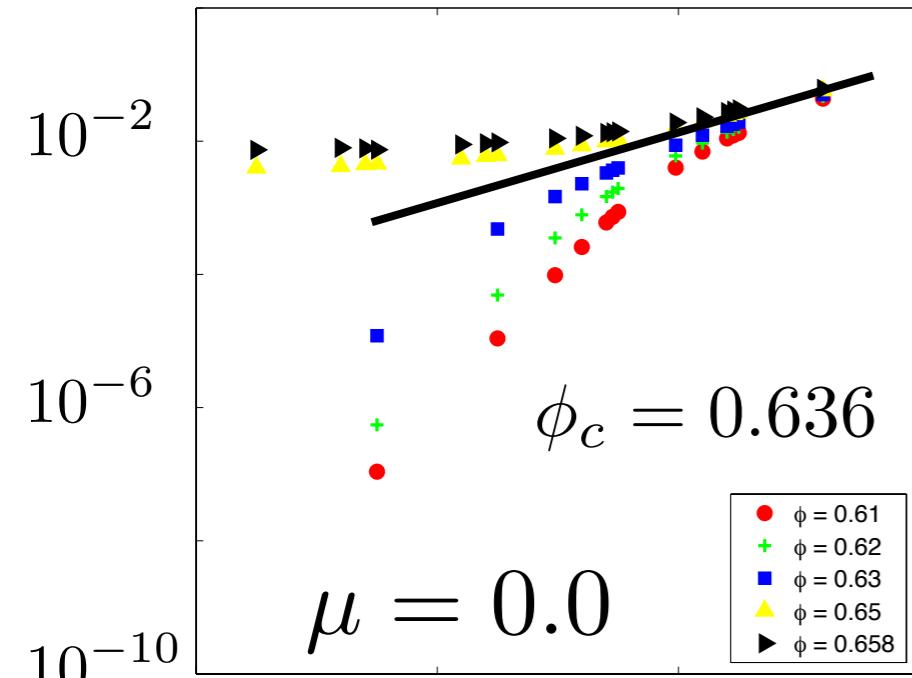
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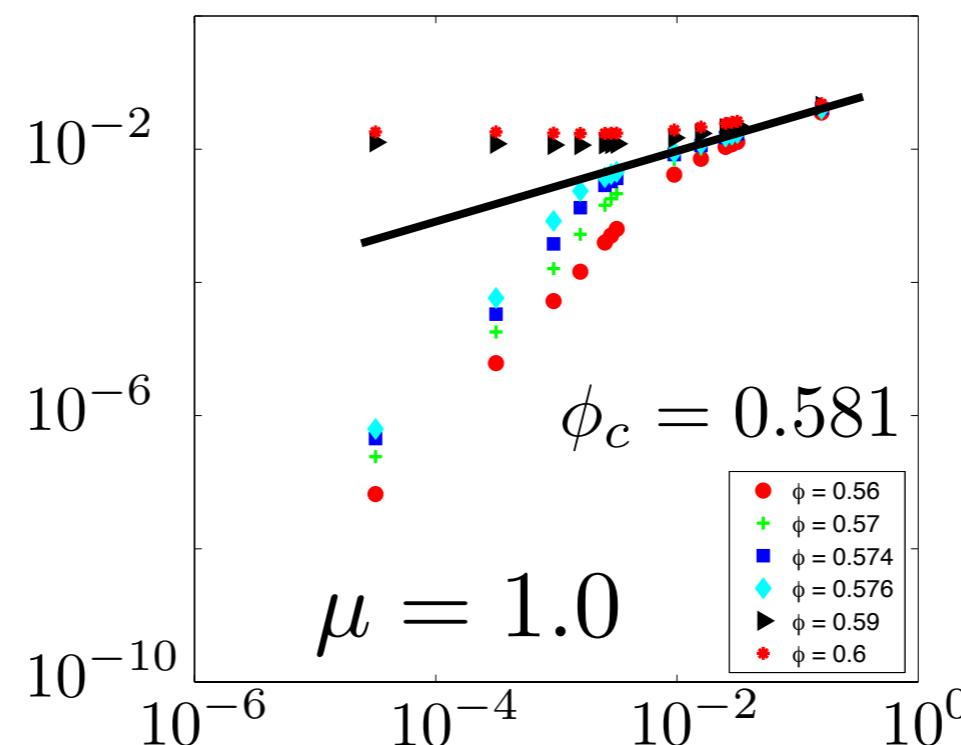
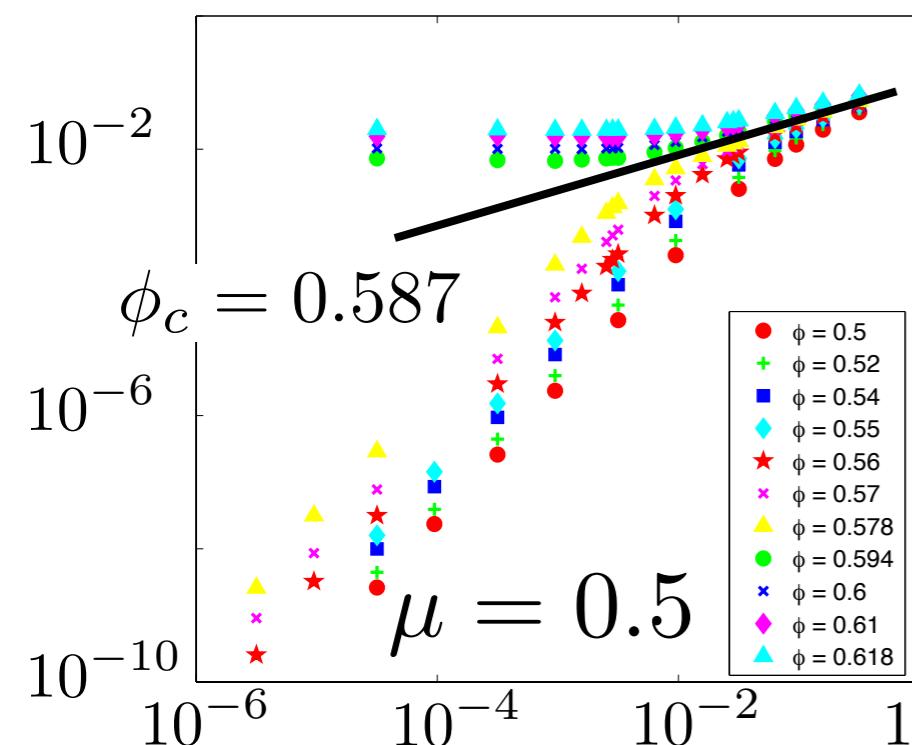
- Critical volume fraction ϕ_c and its flow curve $\hat{p} = \alpha \dot{\gamma}^m$ distinguish the three flow regimes.
- Role of particle softness:
 - Large $k \implies$ quasi-static or inertial regime
 - Small $k \implies$ intermediate regime

Effect of μ on pressure

\hat{p} vs. $\dot{\gamma}$

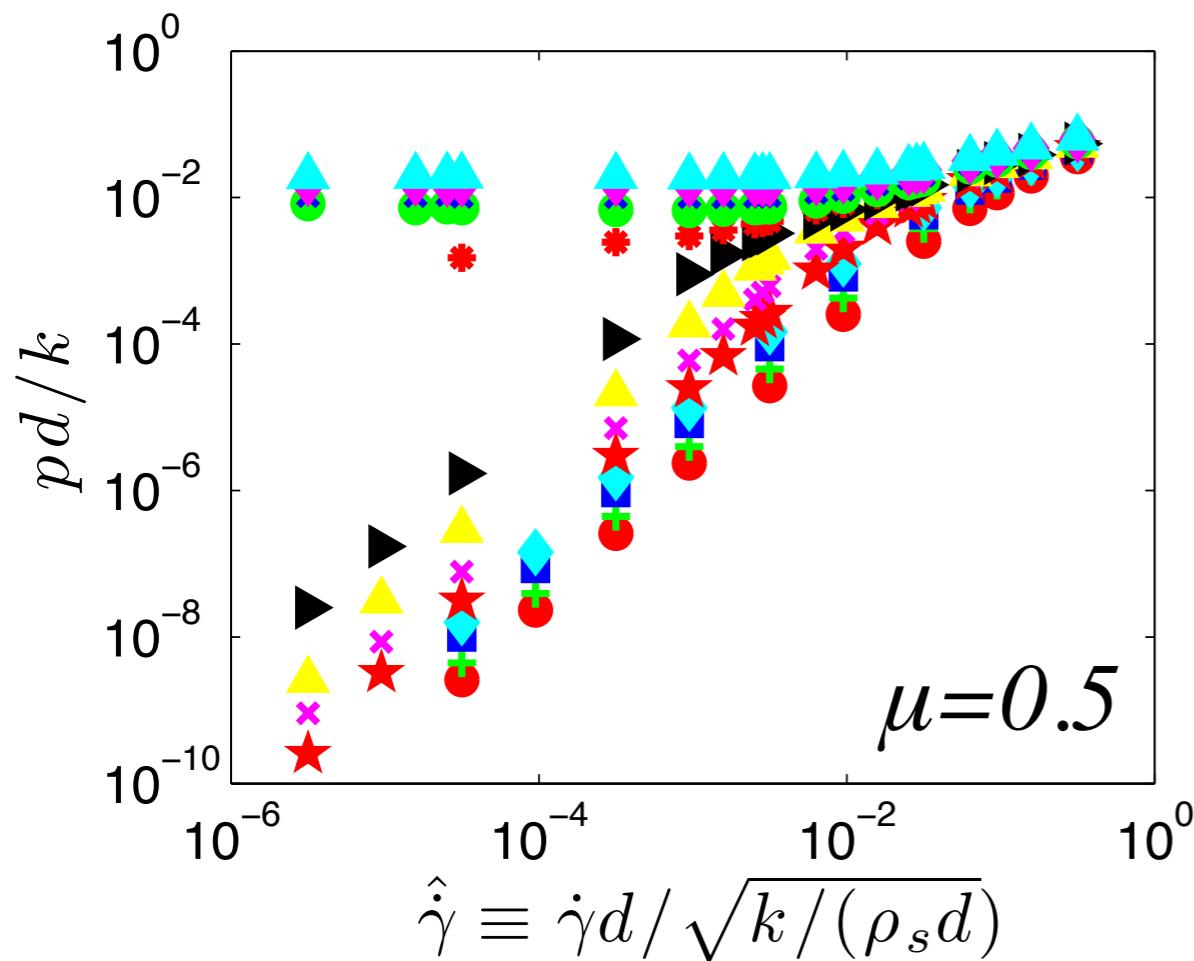


Intermediate asymptote
 $pd/k = \alpha \dot{\gamma}^{1/2}$
 independent of μ



Critical volume fraction
 $\phi_c = \phi_c(\mu)$

Pressure scalings for frictional particles

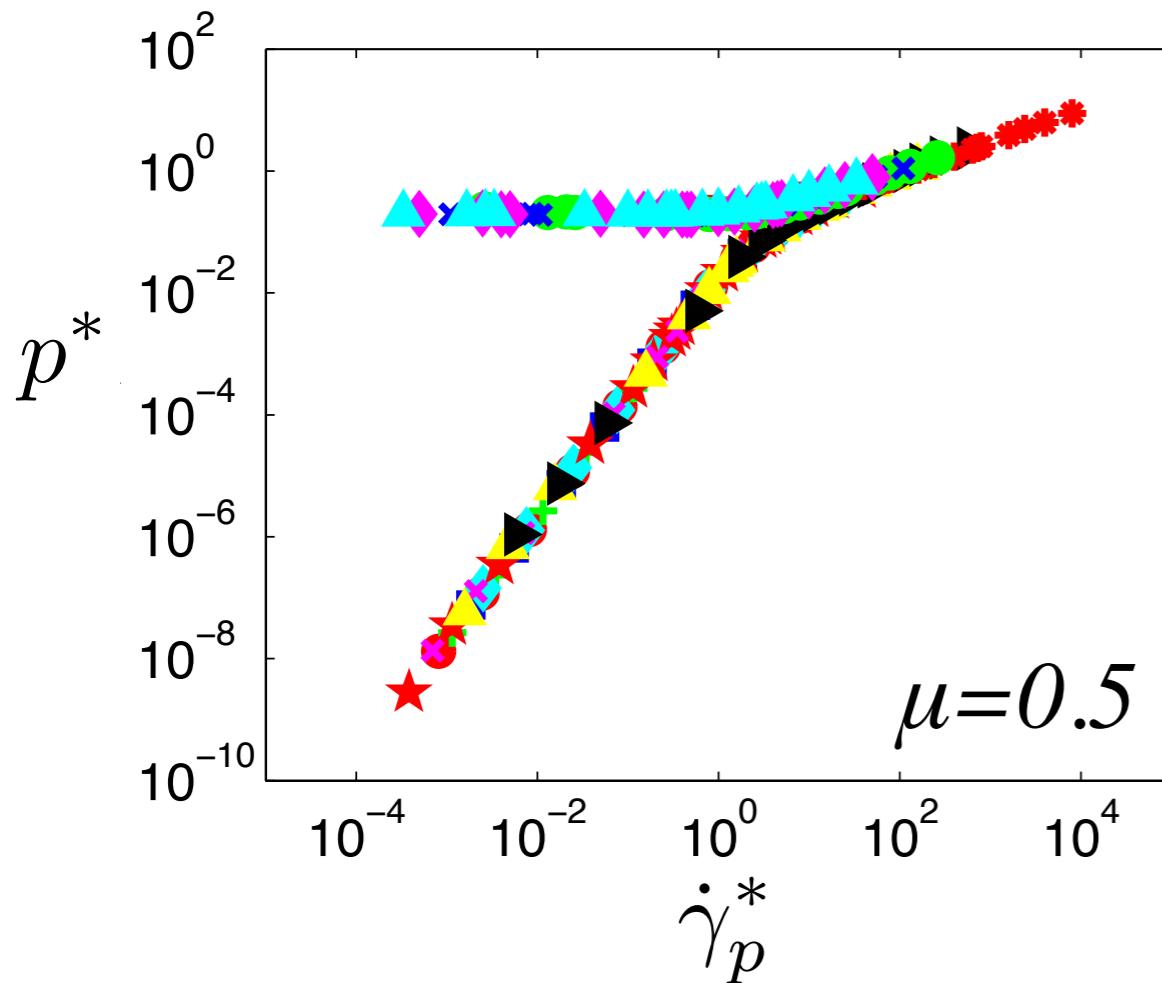


Scaled pressure and shear rate[†]:

$$p^* = \hat{p}/|\phi - \phi_c|^a$$

$$\dot{\gamma}^* = \hat{\dot{\gamma}}/|\phi - \phi_c|^b$$

Pressure scalings for frictional particles



- Three pressure asymptotes:

Scaled pressure and shear rate[†]:

$$p^* = \hat{p}/|\phi - \phi_c|^a$$

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Choose exponents:

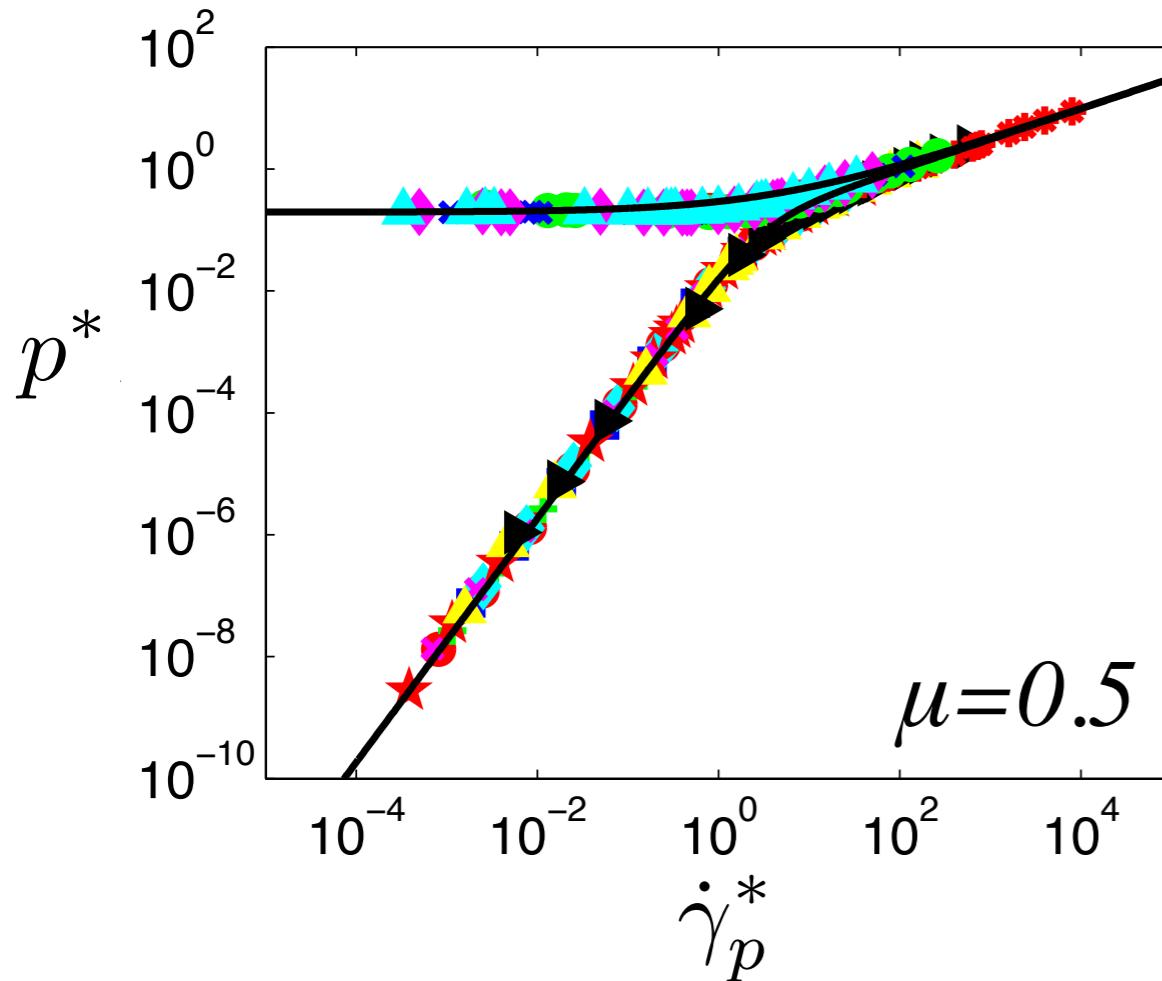
$$a = 2/3$$

$$b = 4/3$$

} Independent
of μ

$$\frac{p_i}{|\phi - \phi_c|^{2/3}} = \alpha_i \left[\frac{\dot{\gamma}}{|\phi - \phi_c|^{4/3}} \right]^{m_i}$$

Pressure scalings for frictional particles



- Three pressure asymptotes:

$$\frac{p_i}{|\phi - \phi_c|^{2/3}} = \alpha_i \left[\frac{\dot{\gamma}}{|\phi - \phi_c|^{4/3}} \right]^{m_i}$$

- Transitions between regimes captured with a blending function:

$$B(y_1, y_2) = (y_1^w + y_2^w)^{1/w}$$

- $w = +1$ for top curve
- $w = -1$ for bottom curve

Scaled pressure and shear rate[†]:

$$p^* = \hat{p}/|\phi - \phi_c|^a$$

$$\dot{\gamma}^* = \hat{\dot{\gamma}}/|\phi - \phi_c|^b$$

Choose exponents:

$$a = 2/3$$

$$b = 4/3$$

} Independent
of μ

Shear stress ratio

- Definition:

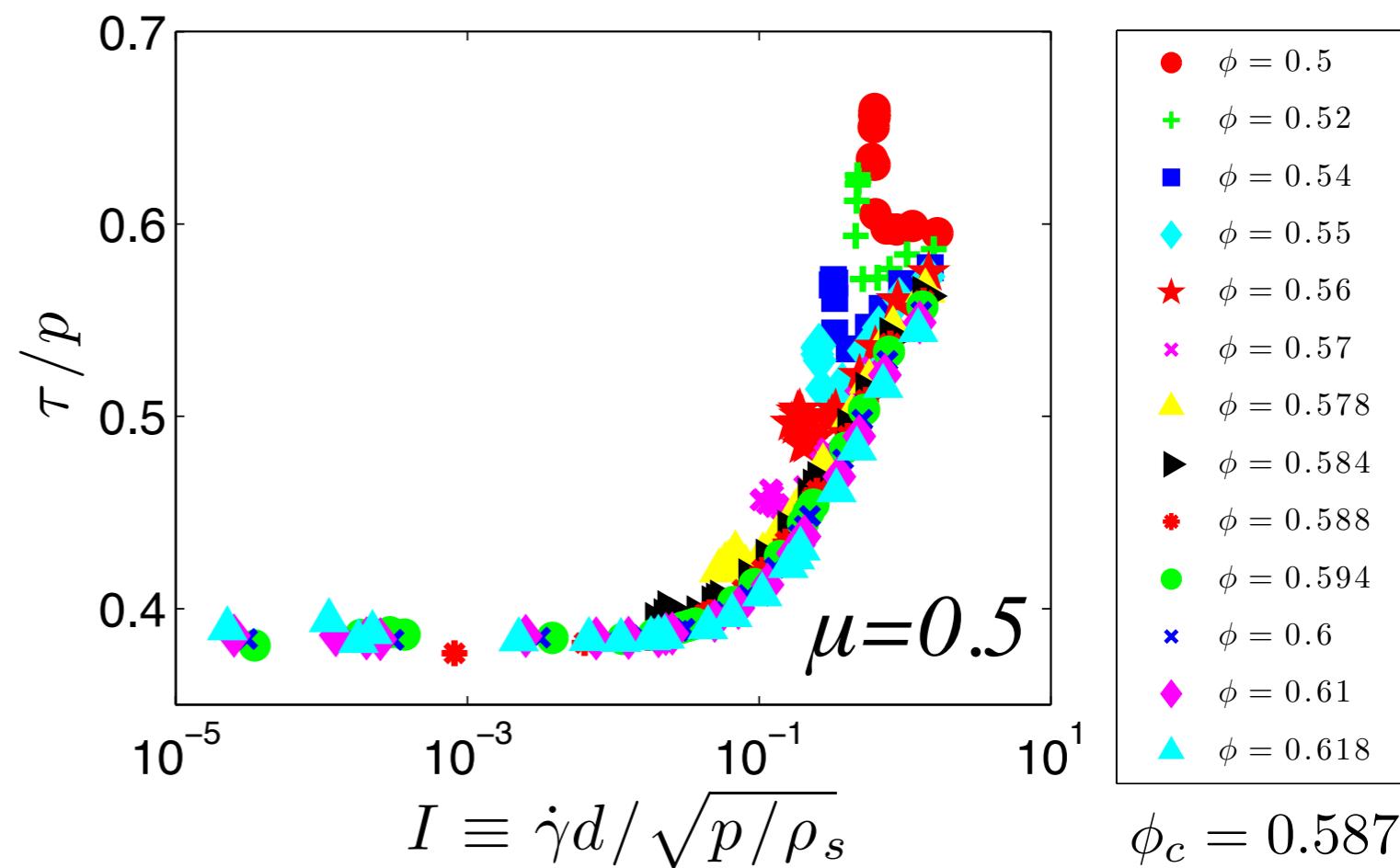
$$\eta \equiv \tau/p$$

- Inertial number†: $I \equiv \frac{\dot{\gamma}d}{\sqrt{p/\rho_s}} = \frac{\text{(timescale of particle rearrangement)}}{\text{(timescale of macroscopic deformation)}}$

- Existing hard-sphere models:

$$\eta = \eta(I)$$

- Scatter at large I due to particle softness



- G. D. R. Midi, Eur. Phys. J. E 14, 341 (2004).
- P. Jop, Y. Forterre, and O. Pouliquen, Nature 441, 727 (2006).
- F. da Cruz et al, Phys. Rev. E 72, 021309 (2005).

Contributions to shear stress ratio

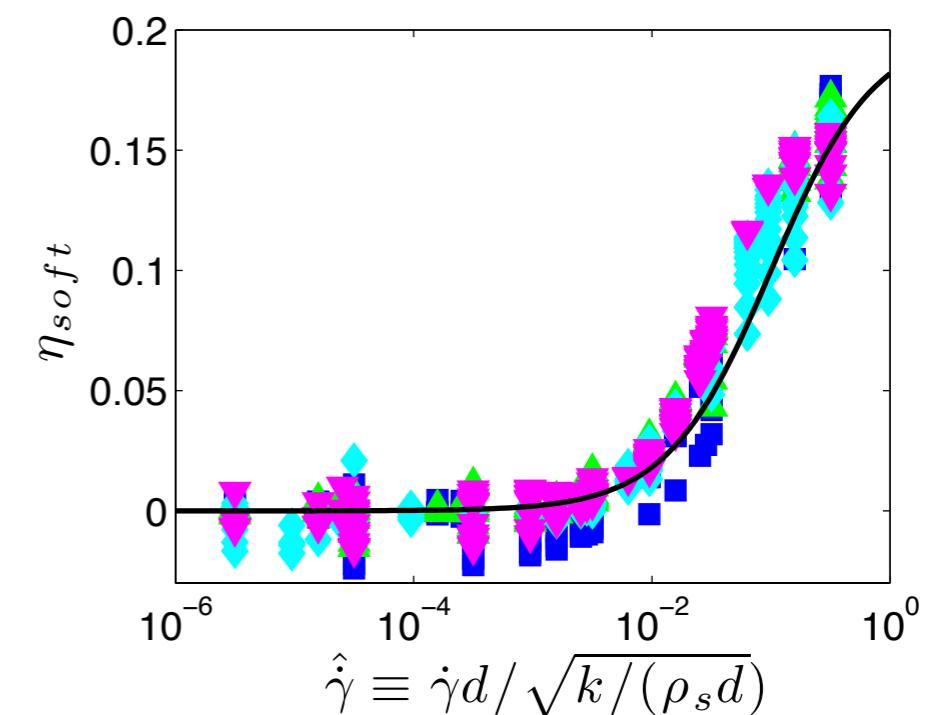
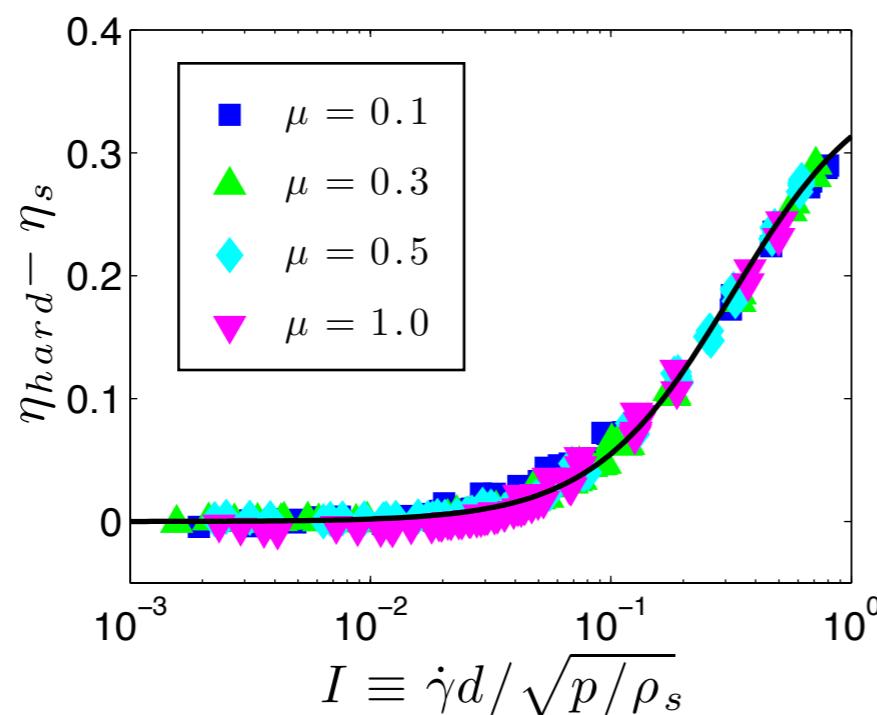
- Propose a model of the form:

$$\eta(I, \dot{\gamma}) = \eta_{\text{hard}}(I) + \eta_{\text{soft}}(\dot{\gamma})$$

- Can fit each contribution to DEM data:

$$\eta_{\text{hard}}(I) = \eta_s(\mu) + \frac{\alpha_1}{\left(\frac{I_0}{I}\right)^{\beta_1} + 1}$$

$$\eta_{\text{soft}}(\dot{\gamma}) = \frac{\alpha_2}{\left(\frac{\dot{\gamma}_0}{\dot{\gamma}}\right)^{\beta_2} + 1}$$



Contributions to shear stress ratio

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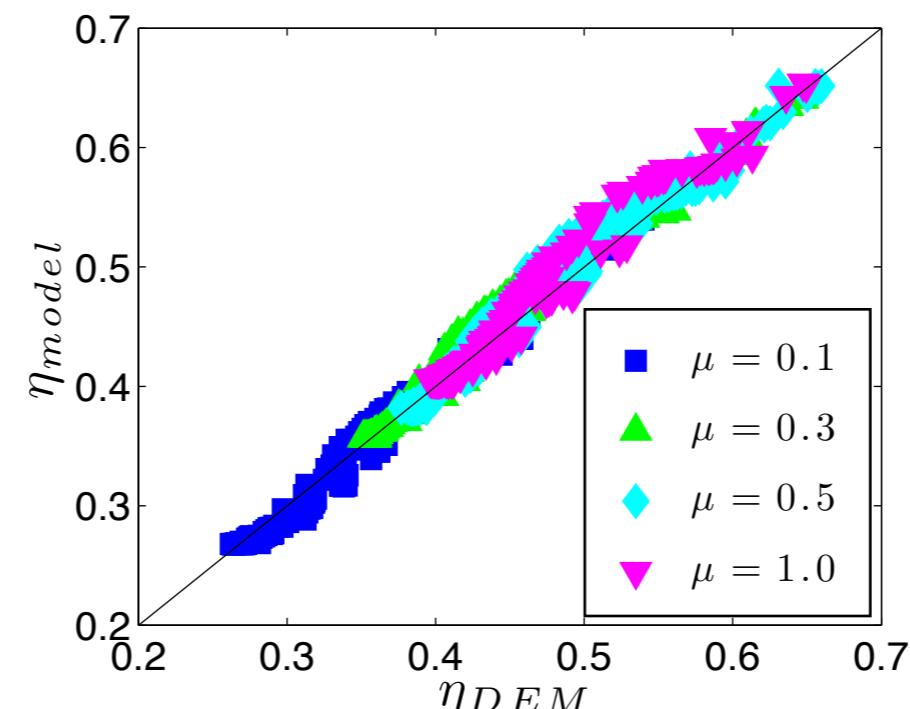
$$\eta(I, \dot{\gamma}) = \eta_{hard}(I) + \eta_{soft}(\dot{\gamma})$$

- Can fit each contribution to DEM data:

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$$\eta_{soft}(\dot{\gamma}) = \frac{\alpha_2}{\left(\frac{\dot{\gamma}_0}{\dot{\gamma}}\right)^{\beta_2} + 1}$$

- Model works well for $\mu \geq 0.1$





Model summary

$$p = \begin{cases} p_{QS} + p_{Int} & \text{for } \phi \geq \phi_c \\ (p_{Inert}^{-1} + p_{Int}^{-1})^{-1} & \text{for } \phi < \phi_c \end{cases}$$

$$\tau = \eta(I, \hat{\dot{\gamma}}) p = [\eta_{hard}(I) + \eta_{soft}(\hat{\dot{\gamma}})] p$$

- Model features:
 - ▶ Captures behavior in all three flow regimes.
 - ▶ Describes transitions between regimes.
 - ▶ Continuous in shear rate – no arbitrary cutoffs.
 - ▶ C⁰ continuous in volume fraction

$$p_{QS} = \alpha_{QS} |\phi - \phi_c|^{2/3}$$

$$p_{Int} = \alpha_{Int} \hat{\dot{\gamma}}^{1/2}$$

$$p_{Inert} = \frac{\alpha_{Inert} \hat{\dot{\gamma}}^2}{|\phi - \phi_c|^2}$$

$$\eta_{hard}(I) = \eta_s + \frac{\alpha_1}{\left(\frac{I_0}{I}\right)^{\beta_1} + 1}$$

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$$\tau = \eta(I, \hat{\dot{\gamma}}) p = [\eta_{hard}(I) + \eta_{soft}(\hat{\dot{\gamma}})] p$$

- Model features:
 - ▶ $\phi_c = \phi_c(\mu)$
 - ▶ Valid for $\mu \geq 0.1$
but can be extended to the frictionless case.

$$p_{QS} = \alpha_{QS} |\phi - \phi_c|^{2/3}$$

$$p_{Int} = \alpha_{Int} \hat{\dot{\gamma}}^{1/2}$$

$$p_{Inert} = \frac{\alpha_{Inert} \hat{\dot{\gamma}}^2}{|\phi - \phi_c|^2}$$

$$\eta_{hard}(I) = \eta_s + \frac{\alpha_1}{\left(\frac{I_0}{I}\right)^{\beta_1} + 1}$$

$$\eta_{soft}(\hat{\dot{\gamma}}) = \frac{\alpha_2}{\left(\frac{\hat{\dot{\gamma}}_0}{\hat{\dot{\gamma}}}\right)^{\beta_2} + 1}$$



Hard-particle limit

- As $k \rightarrow \infty$:

- ▶ $\dot{\gamma} \rightarrow 0 \implies$ No intermediate regime
- ▶ $\phi \geq \phi_c$ is possible only in static packings
- ▶ $\phi < \phi_c$ for sheared systems
- ▶ Model can be simplified to:

$$p = p_{\text{Inert}} \sim \dot{\gamma}^2$$

$$\tau = \eta_{\text{hard}}(I) p \sim \dot{\gamma}^2$$

- ▶ This form suggests a way to modify existing kinetic theories, e.g. Garzó-Dufy (1999)[†]

[†]Garzó, V., Dufty, J.W. Phys. Rev. E 59, 5895 (1999).



Kinetic theory equations

Garzó-Dufty kinetic theory for simple shear flow

Pressure

$$p = \rho_s \phi [1 + 2(1 + e)\phi g_0] T$$

Shear stress

$$\tau = \left(\frac{2J}{5\sqrt{\pi}} \right) \frac{pd\dot{\gamma}}{F\sqrt{T}}$$

Energy dissipation rate

$$\Gamma = \frac{12}{\sqrt{\pi}} \frac{\rho \phi g_0}{d} (1 - e^2) T^{3/2}$$

Steady-state energy balance

$$\Gamma - \dot{\gamma}\tau = 0$$

Important quantities:

$$F = F(e, \phi)$$

$$J = J(e, \phi)$$

- Radial distribution function at contact $g_0 = g_0(\phi)$

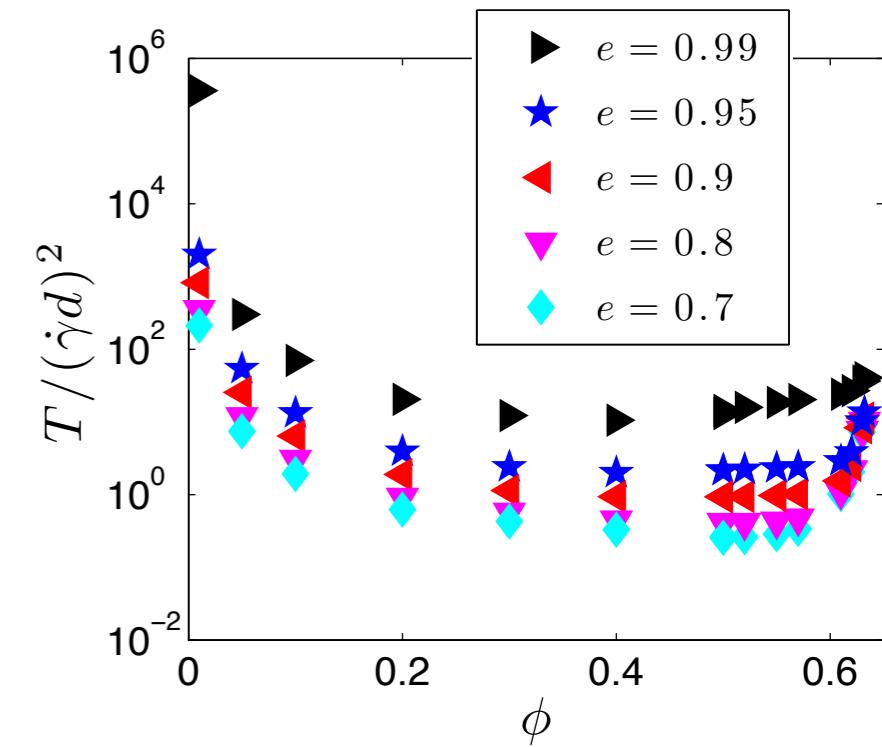
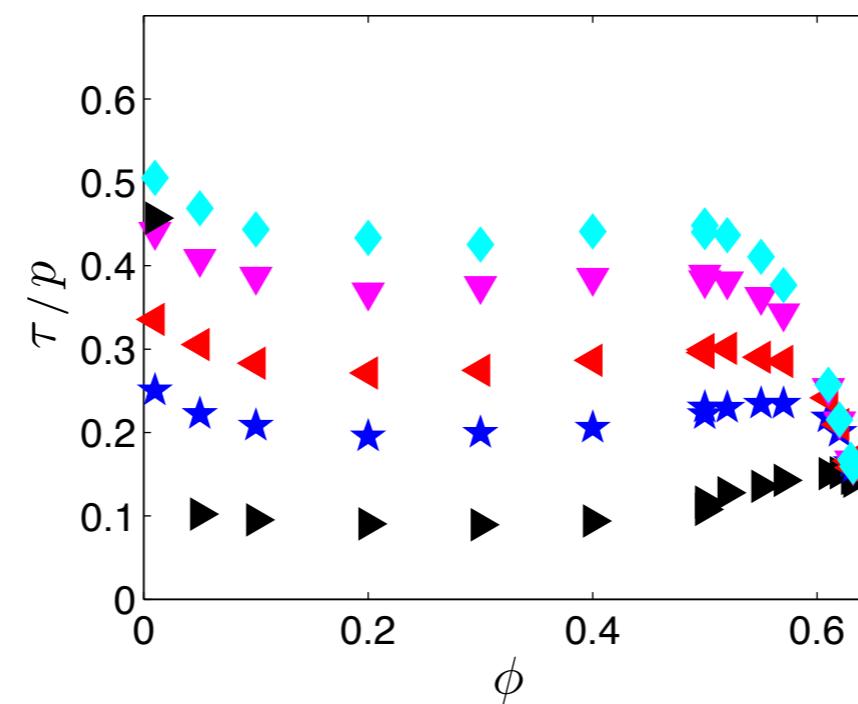
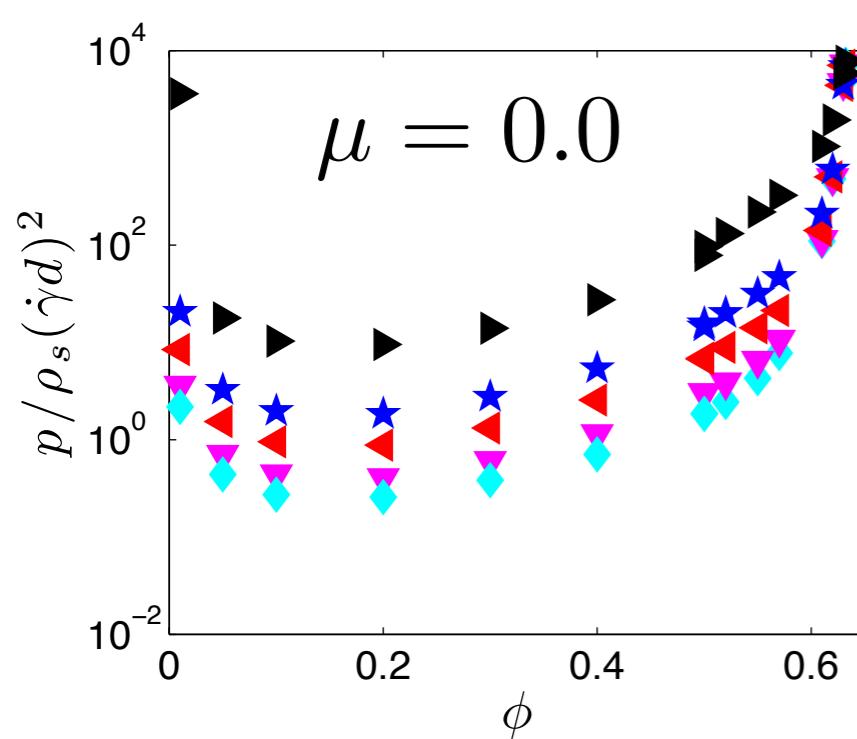
- ▶ Measure of packing
 - ▶ Diverges at random close packing

- Restitution coefficient e

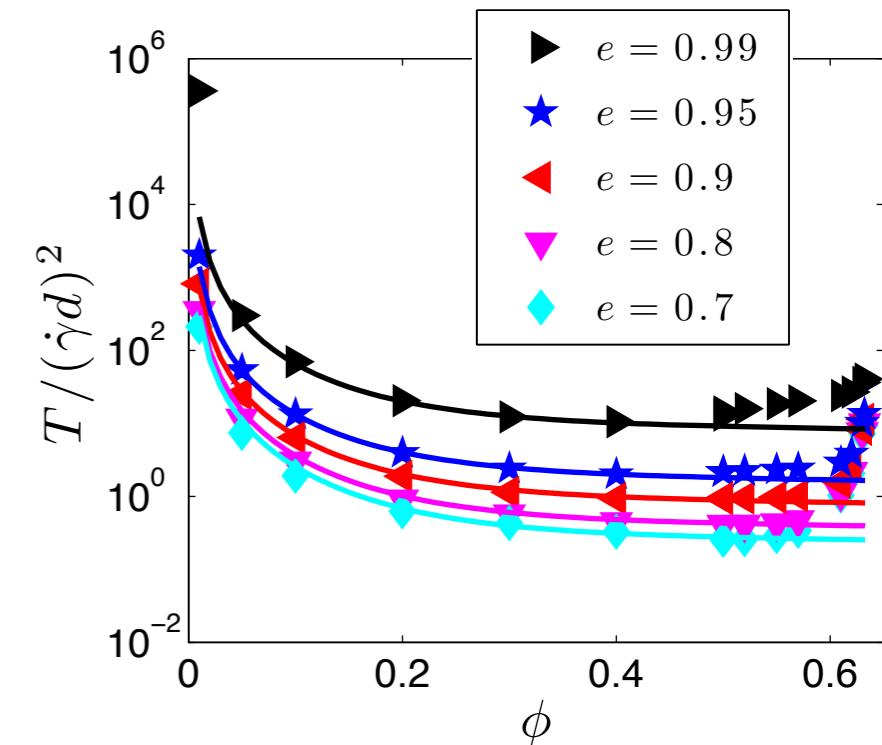
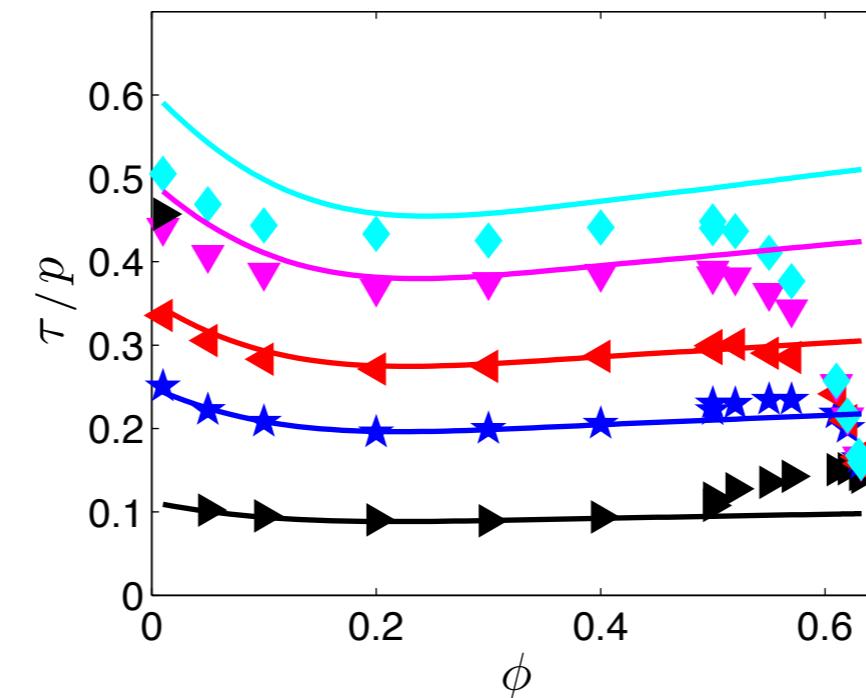
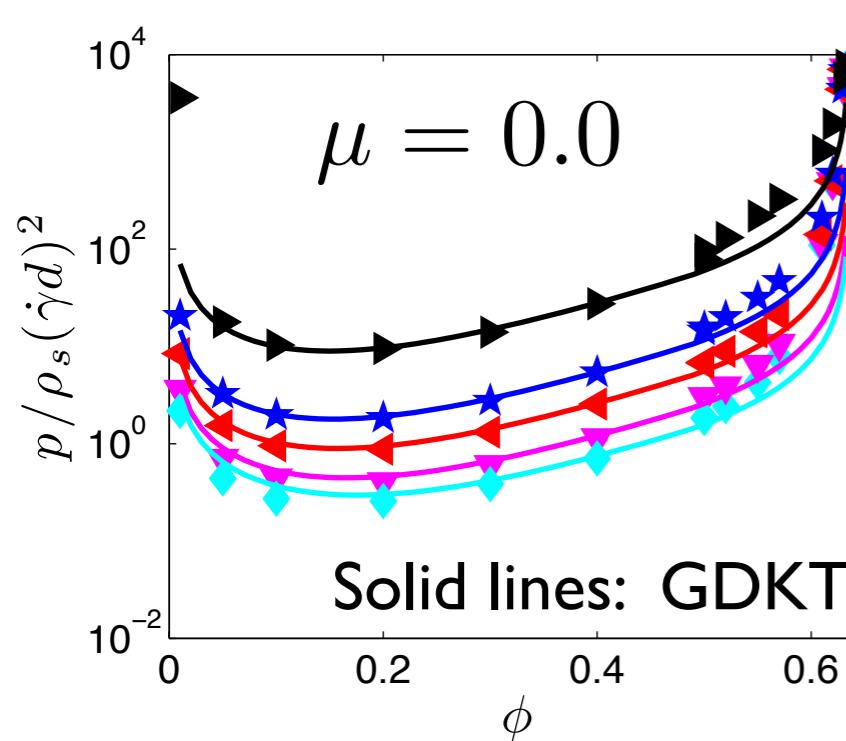
- ▶ Measure of dissipation

- ▶ Has strong effect on temperature

DEM results: without friction

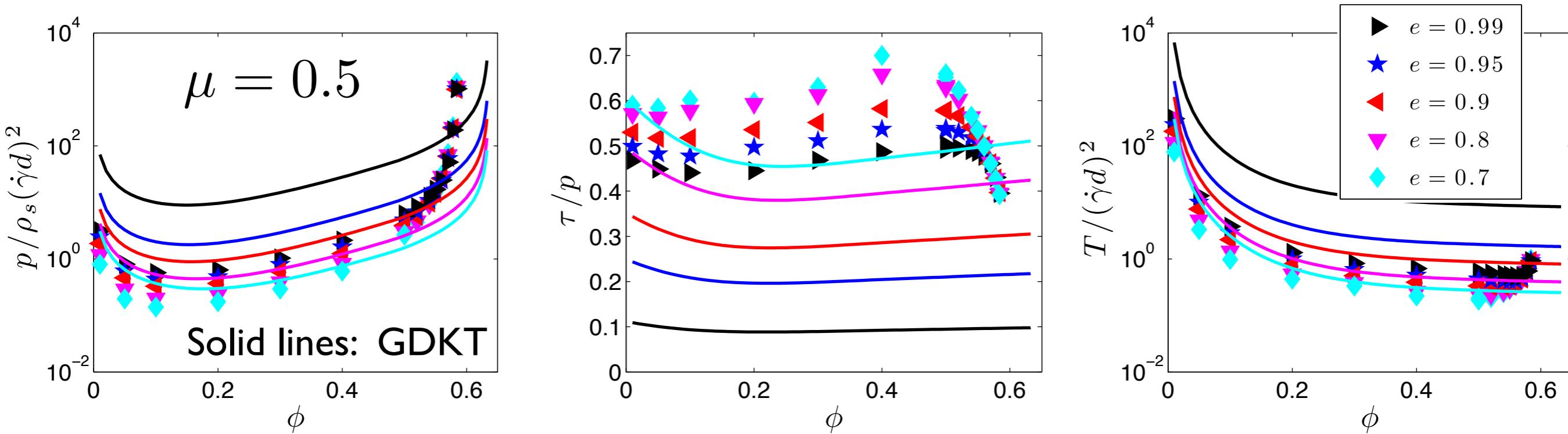


DEM results: without friction



- GD theory agrees with DEM results for dilute systems
- GD theory fails for dense systems
 - ▶ Predicts incorrect scaling of pressure with volume fraction
 - ▶ Cannot predict yield stress in close-packed limit
 - ▶ Derived from false assumption of uncorrelated, isotropically-distributed collisions

DEM results: with friction



- GD theory fails to capture DEM results for frictional particles
 - ▶ Increased collisional stress in dense regime
 - ▶ Increased dissipation in dilute regime
- Possible modifications
 - ▶ Modified RDF at contact $g_0 = g_0(\phi, e, \mu)$ $\longrightarrow p$
 - ▶ Effective restitution coefficient[†] $e_{\text{eff}} = e_{\text{eff}}(e, \mu)$ $\longrightarrow T$
 - ▶ Correction factors^{*} $\delta_i = \delta_i(\phi, e, \mu)$ $\longrightarrow \tau / p$

[†]Jenkins, J.T. and Zhang, C. Phys. Fluids 14, 1228 (2002).

^{*}Jenkins, J.T. and Berzi, D. Granul. Matter 12, 151 (2010).

Effective restitution coefficient

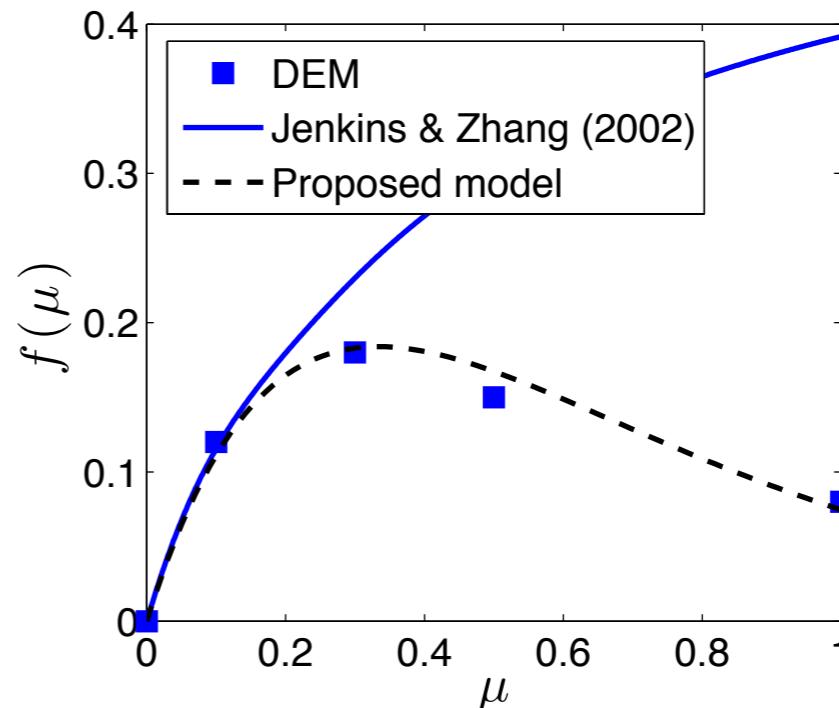
- Can use dilute regime temperature to calculate effective restitution coefficient

$$T = \frac{2J(\dot{\gamma}d)^2}{15(1 - e^2)} \implies e_{\text{eff}} = \sqrt{1 - \frac{2J(\dot{\gamma}d)^2}{15T}}$$

- Proposed form:

$$e_{\text{eff}} = e - f(\mu)$$

$$f(\mu) = 1.5\mu e^{-3\mu}$$



Effective restitution coefficient

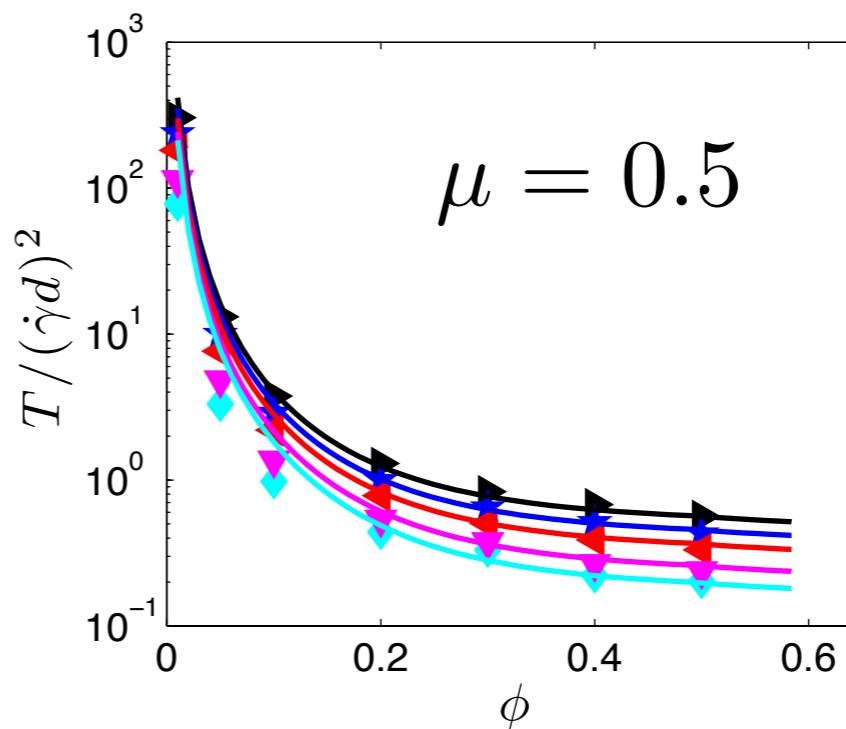
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- Proposed form:

$$e_{\text{eff}} = e - f(\mu)$$

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- Can capture temperature for frictional systems

Radial distribution function: no friction

- Pressure

$$p = \rho_s \phi [1 + 2(1 + e)\phi g_0] T$$

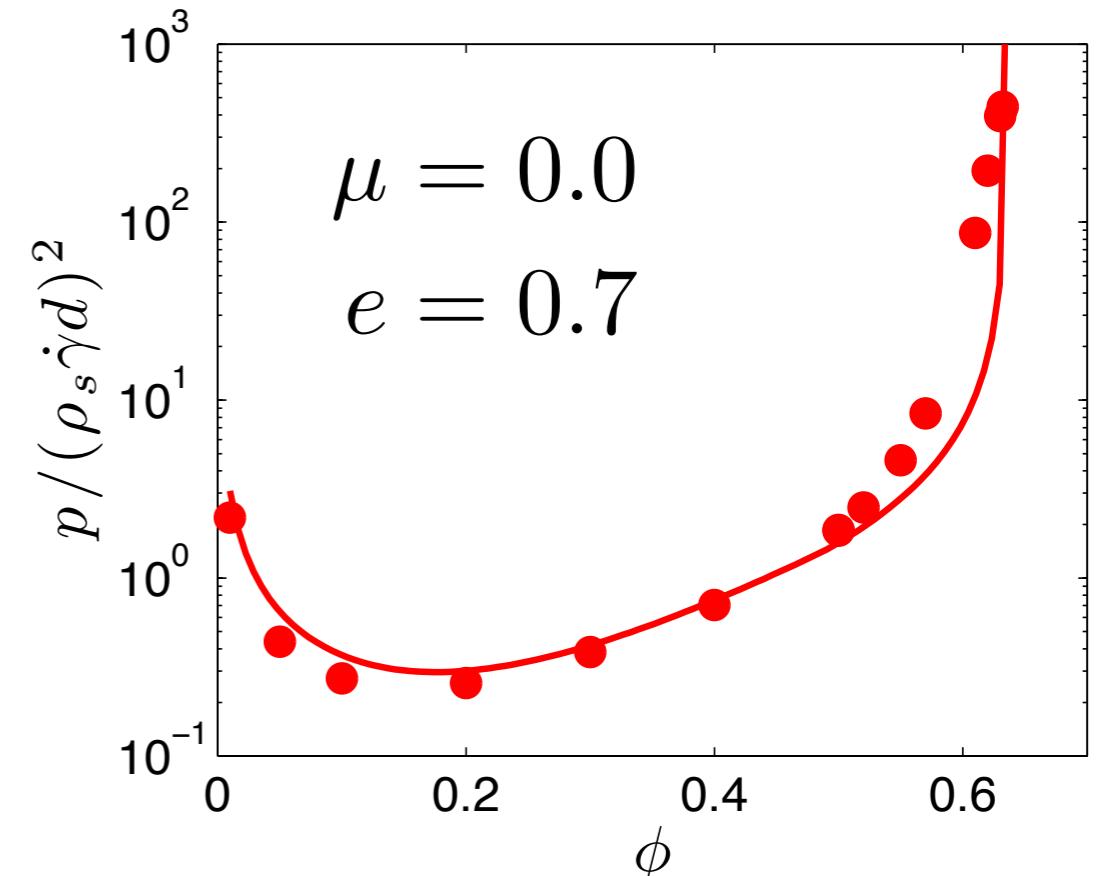
- Radial distribution function

- Carnahan-Starling[†]:

$$g_0^{CS} = \frac{1 - \phi/2}{(1 - \phi)^3}$$

- Torquato (1995)*:

$$g_0 = \begin{cases} g_0^{CS}(\phi), & \phi \leq \phi_f \\ g_0^{CS}(\phi_f) \frac{\phi_c - \phi_f}{\phi_c - \phi}, & \phi > \phi_f \end{cases}$$



[†]Carnahan, N.F., Starling, K.E.
J. Chem. Phys. 51, 635 (1969).

*Torquato, S. Phys. Rev. E 51, 3170 (1995).
15/19

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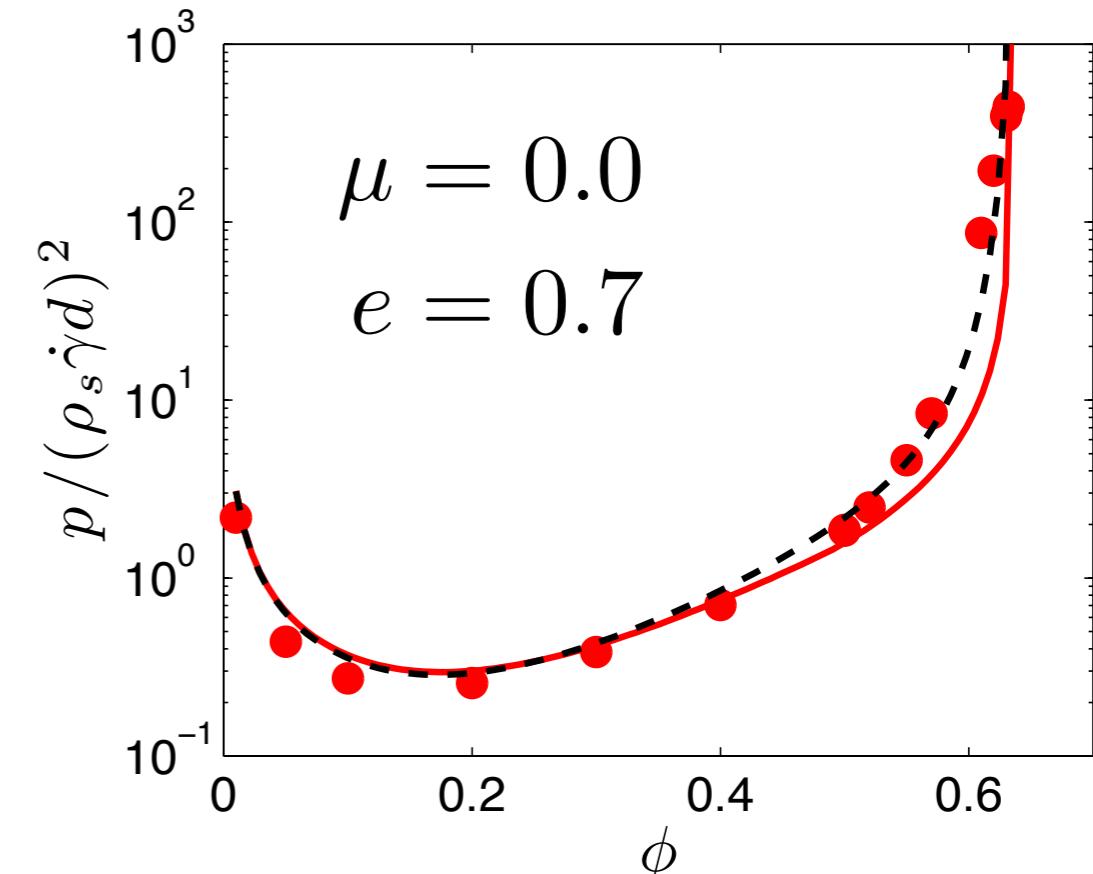
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- Proposed form:

$$g_0 = g_0^{CS} + \frac{\alpha(e, \mu)\phi^2}{(\phi_c - \phi)^2}$$



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Radial distribution function: friction

- Pressure

$$p = \rho_s \phi [1 + 4\eta \phi g_0] T$$

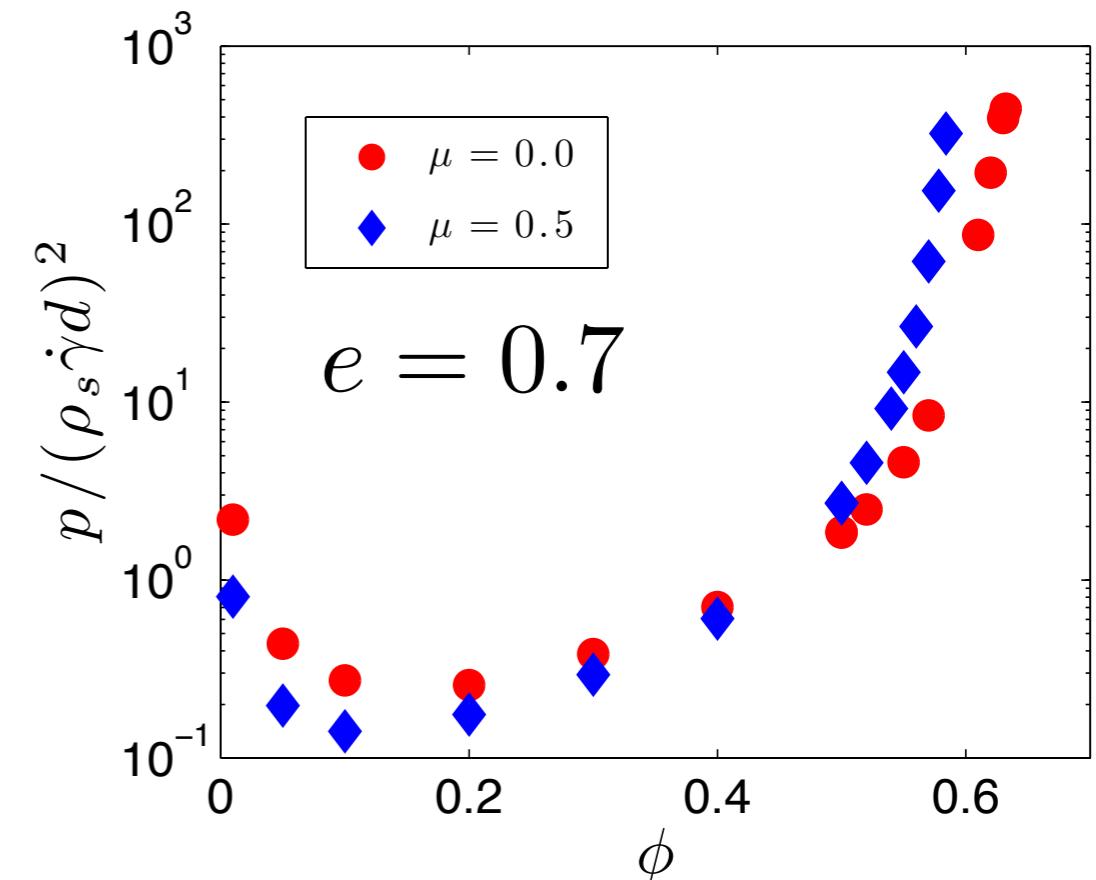
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$$g_0 = g_o^{CS} + \frac{\alpha(e, \mu)\phi^2}{(\phi_c - \phi)^2}$$



$$\phi_c = \phi_c(\mu)$$



Radial distribution function: friction

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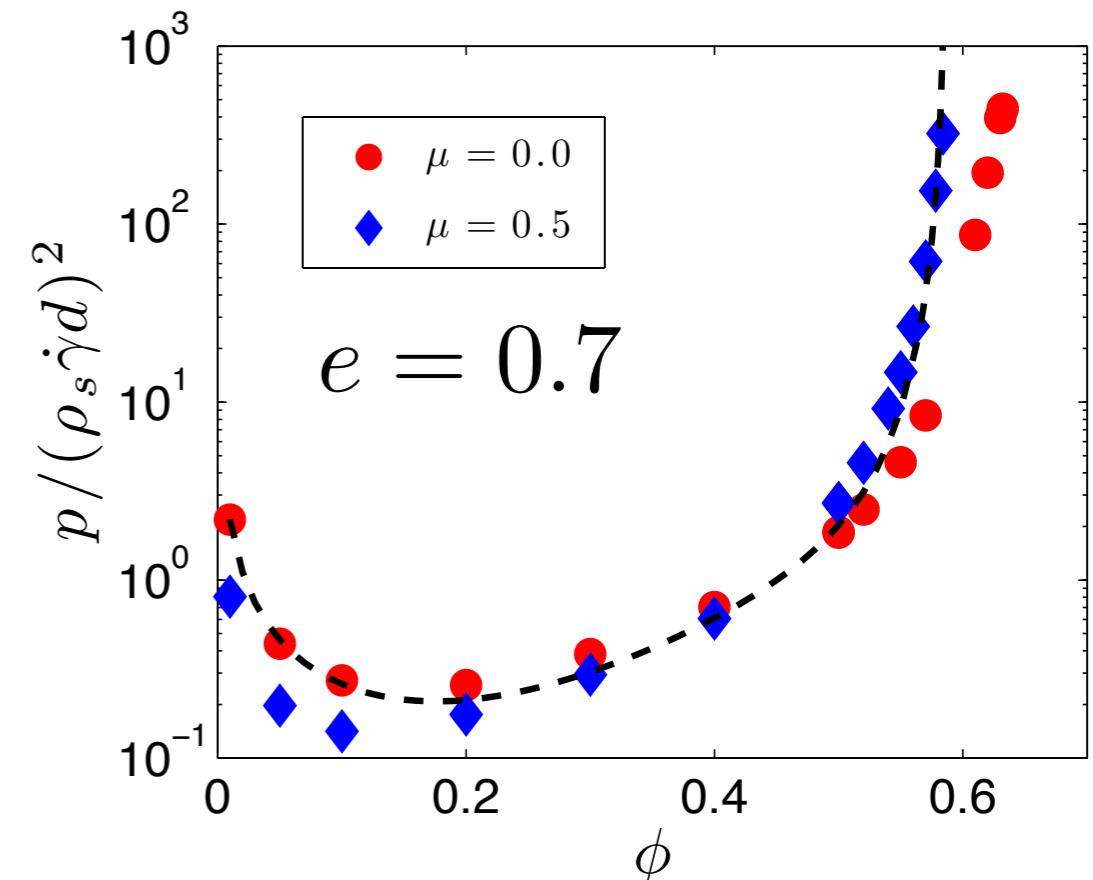
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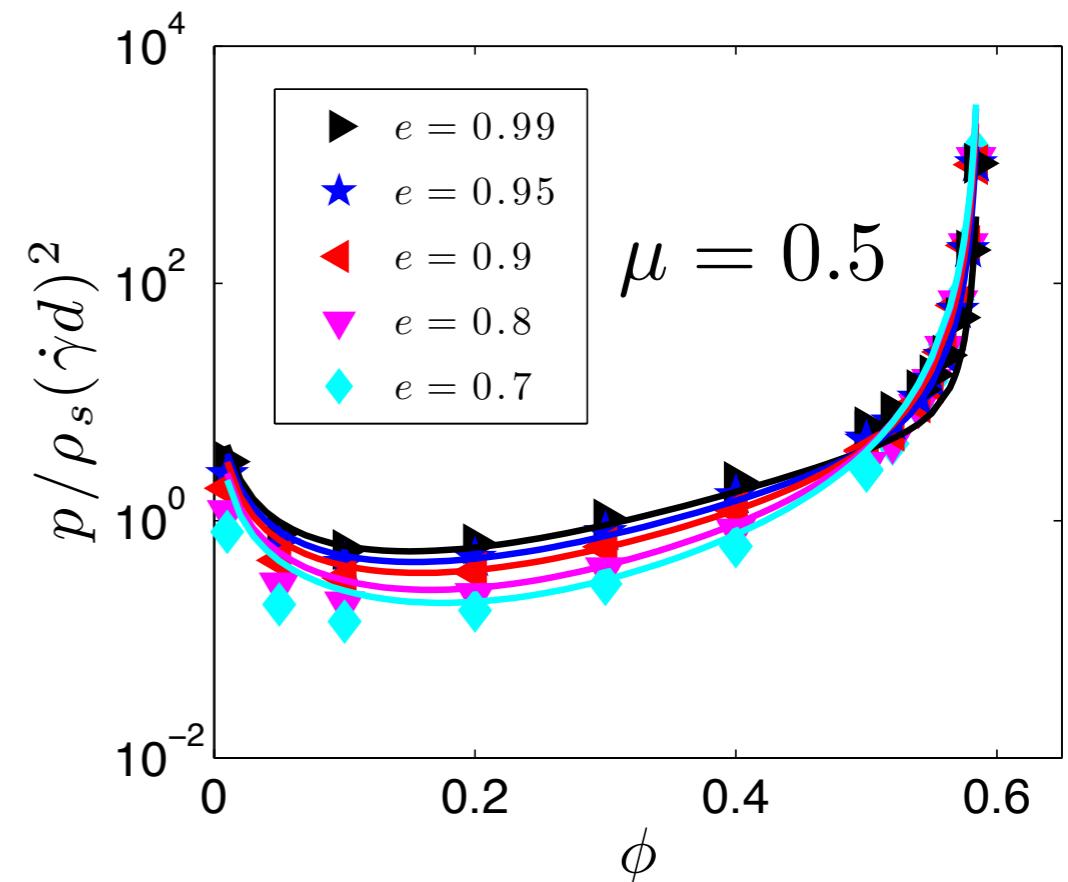
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$$\phi_c = \phi_c(\mu)$$



$$\alpha(e, \mu) = \left(\frac{1}{3} + \frac{3}{2}\mu \right) (1 - e)$$

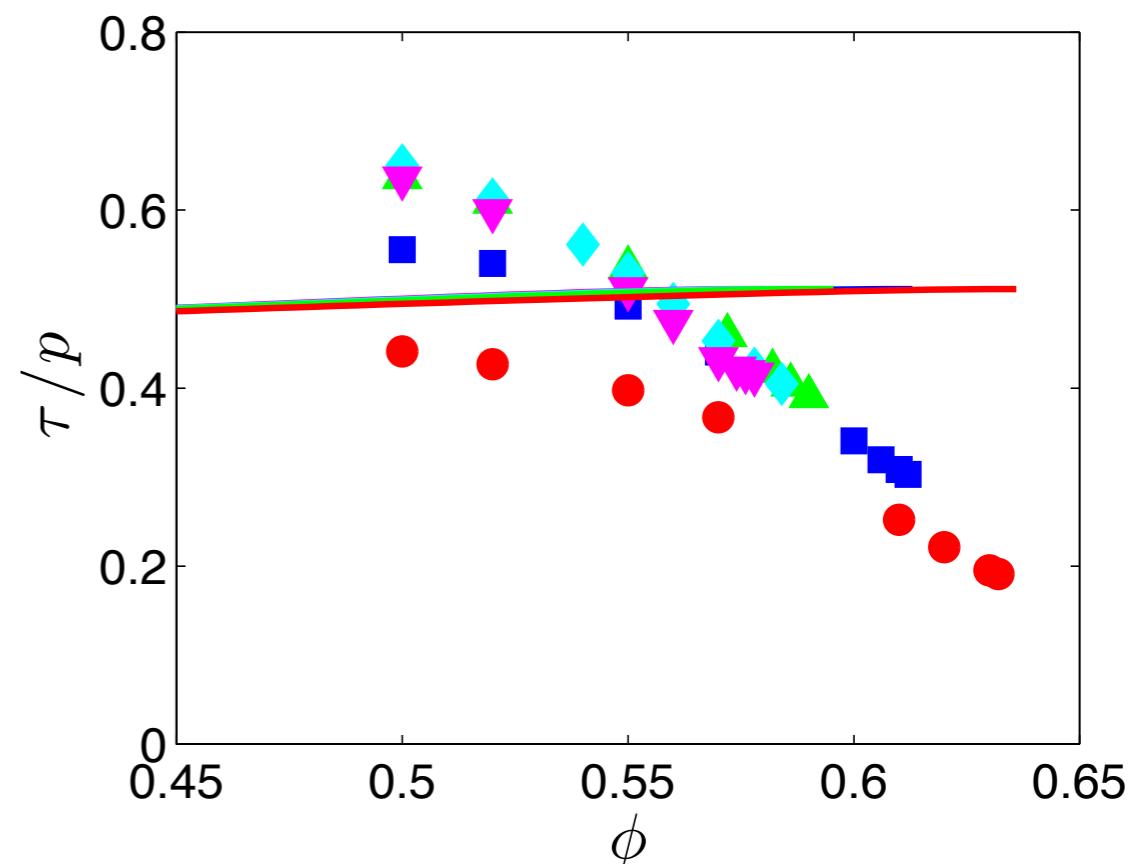
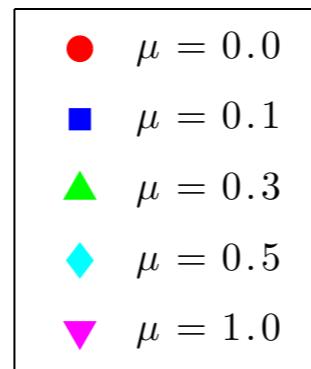
Shear stress ratio for dense regime

- Garzó-Dufty (1999)

$$p = \rho_s \phi [1 + 4\eta \phi g_0] T$$

$$\tau = \left(\frac{2J}{5\sqrt{\pi}} \right) \frac{pd\dot{\gamma}}{F\sqrt{T}}$$

$$\Gamma = \frac{12}{\sqrt{\pi}} \frac{\rho \phi g_0}{d} (1 - e^2) T^{3/2}$$



Shear stress ratio for dense regime

- Jenkins-Berzi (2010)

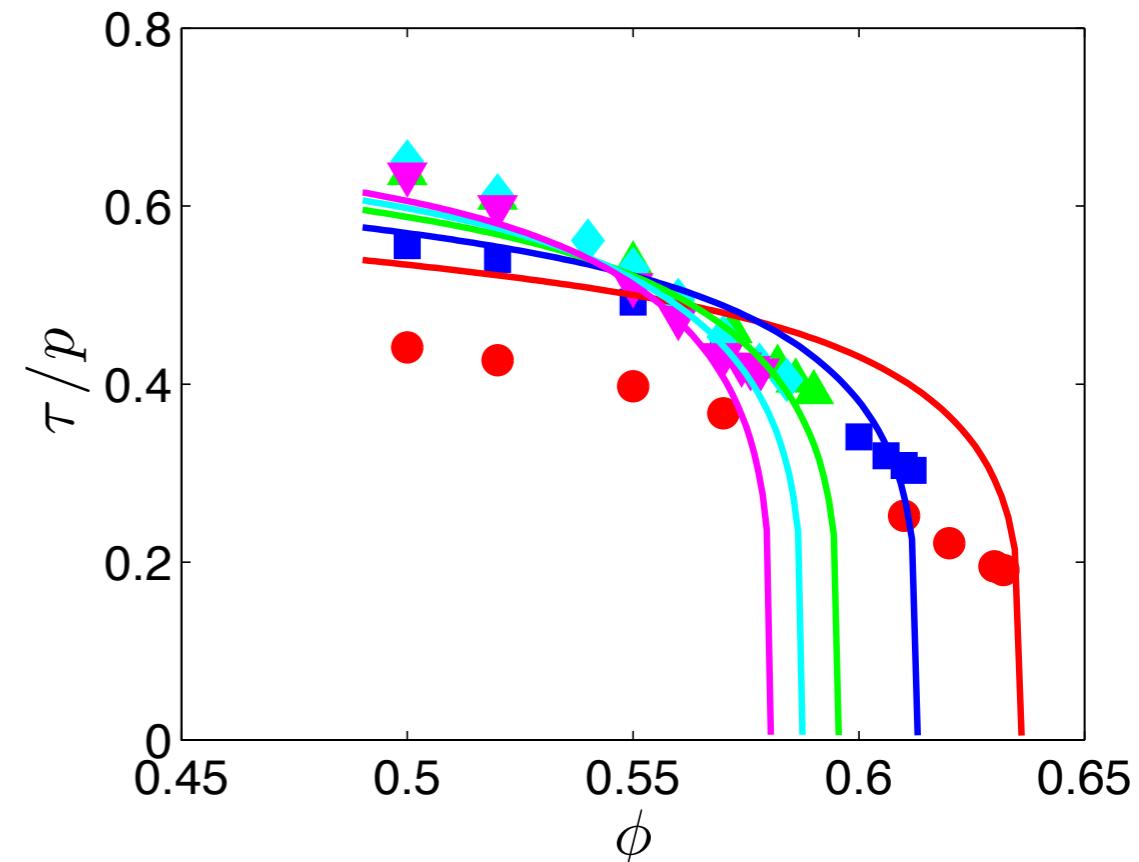
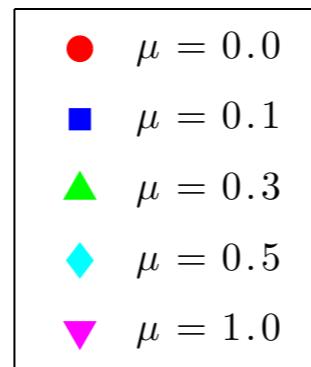
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$$\tau = \left(\frac{2J}{5\sqrt{\pi}} \right) \frac{pd\dot{\gamma}}{F\sqrt{T}}$$

$$\Gamma = \frac{12}{\sqrt{\pi}} \frac{\rho\phi g_0}{L} (1 - e^2) T^{3/2}$$

Length scale

$$\frac{L}{d} = \frac{1}{2} \hat{c} G^{1/3} \frac{\dot{\gamma} d}{\sqrt{T}}$$



- Undesirable features:

- Does not predict a yield stress ratio η_s
- Temperature diverges at ϕ_c



Modifications for dense regime

- Our proposed model:

$$p = \rho_s \phi [1 + 4\eta\phi g_0] T$$

$$\tau = \left(\frac{2J}{5\sqrt{\pi}} \right) \frac{pd\dot{\gamma}}{F\sqrt{T}} \delta_1 \longrightarrow \text{to match DEM stress ratio}$$

$$\Gamma = \frac{12}{\sqrt{\pi}} \frac{\rho\phi g_0}{d} (1 - e^2) T^{3/2} \delta_2 \longrightarrow \text{to retain temperature expression, i.e. leave T unaffected}$$

Steady-state:

$$\Gamma - \dot{\gamma}\tau = 0 \implies T = T \frac{\delta_1}{\delta_2} \implies \delta_1 = \delta_2 \equiv \delta$$

$$\eta = \eta(I) = \eta_s + \frac{\alpha_2}{\left(\frac{I_0}{I}\right)^{1.5} + 1} \implies \delta = \frac{\eta(I)}{\eta_{KT,SS}}$$

$$I \equiv \frac{\dot{\gamma}d}{\sqrt{p/\rho_s}}$$

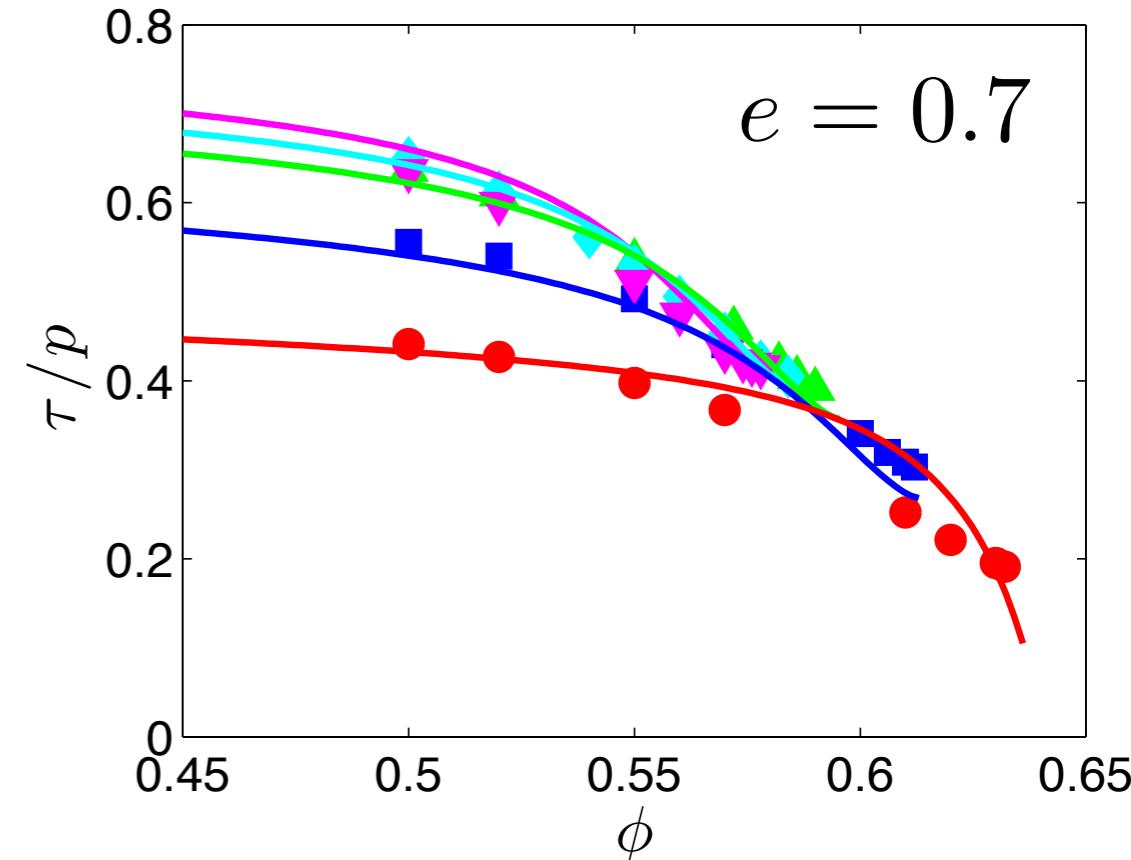
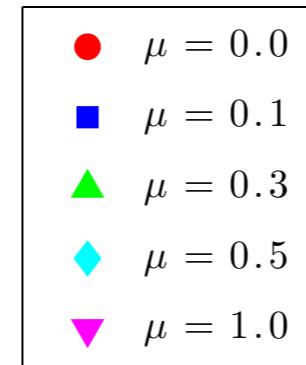
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Steady-state:

$$\Gamma - \dot{\gamma}\tau = 0 \implies T = T \frac{\delta_1}{\delta_2} \implies \delta_1 = \delta_2 \equiv \delta$$

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$$I \equiv \frac{\dot{\gamma}d}{\sqrt{p/\rho_s}}$$

Summary and future work



- Developed rheological model spanning three regimes of *dense* granular flow
- Proposed modified kinetic theory to capture rheological behavior for *dense and dilute* systems
- Will soon implement KT model into MFIX continuum solver for testing on process-scale flow problems