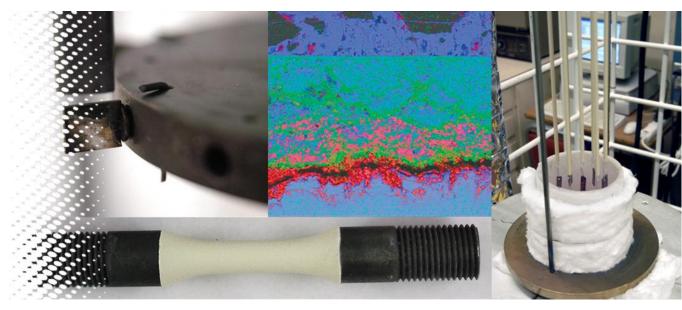


NATIONAL ENERGY TECHNOLOGY LABORATORY



Oxy-Combustion Environment Characterization: Fire- and Steam-Side Corrosion in Advanced Combustion

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Outline

Introduction

- Goals
- Project Background

Research Progress

- Long-term oxy-combustion fireside corrosion tests
- Effects of pressure—update on A-USC steam autoclave

Summary

Goals

DOE Office of Clean Coal goal for pulverized coal boilers

 Achieve 90% CO₂ capture at no more than a 35% increase in levelized cost of electricity of post-combustion capture for new and existing conventional coal-fired power plants

Project goals

- Provide high-temperature corrosion information to aid in materials development and selection for oxy-fuel combustion (fireside corrosion) and A-USC steam conditions (steam oxidation)
- Identify corrosion mechanism and behavior differences between airand oxy-firing

Project Background

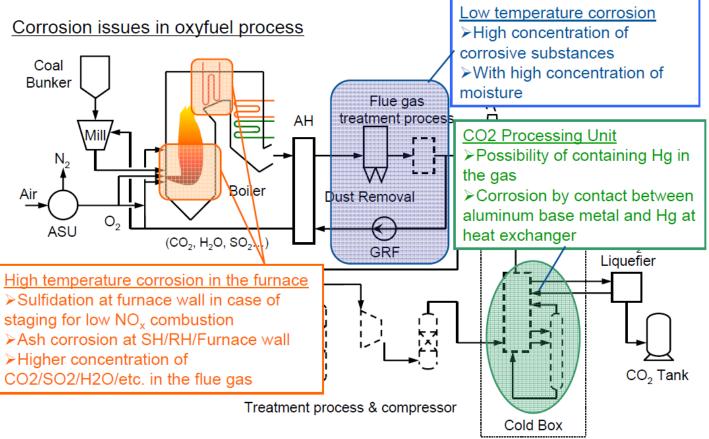
Fireside Corrosion

- Long-term oxy-combustion fireside corrosion tests
- Short-term oxy-combustion fireside corrosion tests
 - Jerry Meier's presentation
- Field exposures in collaboration with JCOAL and IHI
- Post economizer flue gas corrosion (oxy-firing leading to lower dew points)—Laboratory and field tests
- Use of TBCs for protection in oxy-combustion environments

Steam Side Oxidation

- Effects of pressure—update on A-USC autoclave
- Chromia evaporation in steam
- Round robin study on T92 in atmospheric pressure steam (US-UK collaboration)
- Examination of oxide spallation comparing flat and whole tube section samples
- Hydrogen transport as a by-product of steam oxidation
 - Jerry Meier's presentation

Fireside Corrosion Associated with Oxy-Combustion



- Main corrosion areas in changing from air- to oxy-firing. In the boiler this project considers
 - Waterwall (WW) corrosion—reducing conditions
 - Waterwall (WW) corrosion—oxidative conditions
 - Superheater/Reheater (SH/RH) corrosion—oxidative conditions
 - 3 different flue gas recycle choices

Fireside Corrosion Associated with Oxy-Combustion

Oxy-combustion is quite complex to simulate. Challenge is to combine different tests to understand the ramifications of oxy-firing.

- Long term tests with step differences in gas phases approximating air- and 3 oxy-firing cases
- Short term tests to examine other variables without the time and equipment availability issues of the long term tests
- Field exposures in an oxy-firing test facility
 - Exposure samples would see all the different combustion trials, thus correlation with environment is difficult
 - Electrochemical sensors offer instantaneous corrosion measurements, but with not exact correlation with section loss

Laboratory Test Issues

Ash Phase

- Wigley and Goh (2009)—oxy ash particles similar in size, more rounded, more sintering
- Brzozowska et al (2011)—more sulfur in oxy ash
- Hjörnhede et al (2010)—increased oxy ash deposition
- Ash phase complications differences between air- and oxyfiring not considered in long-term tests. Could be addressed in short-term tests

Heat Flux and Temperature Gradients

- Refit boilers use flue gas recirculation to match heat rate, so not much of an issue
- New boiler designs like will have higher heat rates and so this could be a concern
- Heat flux complications between air- and oxy-firing not considered

Laboratory Test Issues

Gas Phase

- Not constant even in air-firing
- Long-term tests bin the gas phase into 3 locations in the boiler and representing 1 airfiring case and 3 oxy-firing cases
- Short-term tests examine more varieties of gases
- Use Pt catalyst to form SO₃(g)

Alloys

- There is an extensive variety of candidate alloys.
 We narrowed the focus to a few types of alloys
- Commercial alloys (T22, T91, T92, TP347H, IN617)
- Model alloys (Fe-Cr, Fe-Cr-Ni, Ni-Cr)

Alloys and Deposits

Model Alloys (wt%)

- Fe-10Cr, Fe-13.5Cr, Fe-22Cr (ferritic/martensitic)
- Fe-12Ni-18Cr, Ni-22Cr (austenitic)

Commercial Alloys (wt%)

Alloy	Fe	Cr	Ni	Co	Mo	C	Si	Al	Mn	W	Nb	V	Cu	N	Other
T22	Bal	2.07	0.19		0.91	0.10			0.50						
T91	Bal	8.48	0.16		0.99	0.10	0.35		0.41			0.20	0.18	0.04	
T92	Bal	8.84	0.32		0.32	0.12	0.28		0.29	1.83				0.14	
P92	Bal	8.90	0.23		0.38	0.07	0.30		0.43	1.20					
TP347	Bal	17.55	11.04	0.10	0.39	0.08	0.57		1.57	0.04	0.93	0.07	0.35		0.02 Ta
IN617	0.39	21.87	Bal	11.46	9.65	0.10	0.01	0.98	0.04		0.03		0.01		0.47 Ti

Ash and deposits (all wt% except for SCM)

- Deposit A: 50SiO₂-25Al₂O₃-12.5Fe₂O₃-12.5CaO (baseline)
- Deposit B: 49SiO₂-25Al₂O₃-12.5Fe₂O₃-12.5CaO-1K₂SO₄ (some variations with more K₂SO₄)
- Deposit C: 67% deposit A + 33% graphite
- Deposit D: 30SiO₂-30Al₂O₃-30Fe₂O₃-5Na₂SO₄-5K₂SO₄ [deposit used in long term tests]
- SCM: K₂SO₄, Na₂SO₄, Fe₂O₃ 1.5:1.5:1.0 molar ratio

Long Term Fireside Tests in SECERF

Severe Environment Corrosion Erosion Research Facility



Modular laboratory for safely examining hot-corrosion and wear of materials at temperatures to 1600°C in a mixture of any of the following gases: O₂, N₂, CO, CO₂, CH₄, H₂, H₂S, SO₂, HCl, He, Ar, dry air, and water vapor.

Environments (1 air- and 3 oxy-firing cases)

			Oxid	ative	Reducing					
ns	SH/RH	700	°C (T91, 7	ΓΡ347, IN	617)					
Conditions	ww	450) °C (T22,	T91, IN6	17)	450 °C (T22, T91, IN617)				
Sono				Оху			Оху			
	Air		FGD <h<sub>2O</h<sub>	FGD	wo FGD	Air	FGD <h₂o< td=""><td>FGD</td><td>wo FGD</td></h₂o<>	FGD	wo FGD	
Gas	N ₂	Bal	8	8	8	Bal	8	8	8	
	CO ₂	14	Bal	Bal	Bal	14	Bal	Bal	Bal	
	СО					5	5	5	5	
	H ₂ S					0.1	0.1	0.1	0.3	
	H ₂ O	9	9	2 0	20	9	9 -	2 0	20	
	O ₂	2.5	2.5	2.5	2.5					
	SO ₂	0.3	0.3	0.3	0.9	0.2	0.2	0.2	0.6	

Long Term Fireside Corrosion Tests

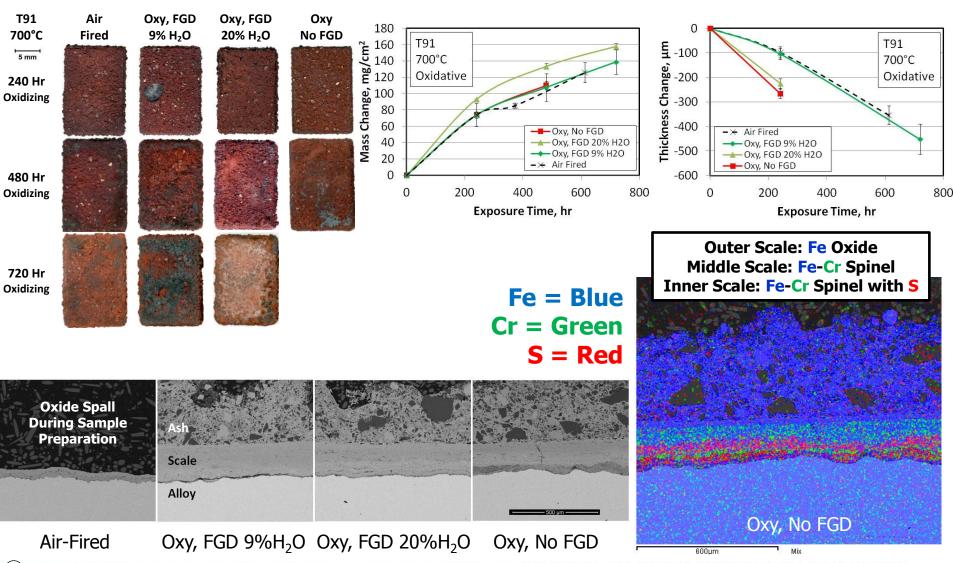
Plan is to run experiments for 1440 hours, in nominally 240 hr increments, then decide if further exposures are warranted

Section off part of one of the triplicate samples for each alloy after 240, 720, and 1440 hr for cross-section examination

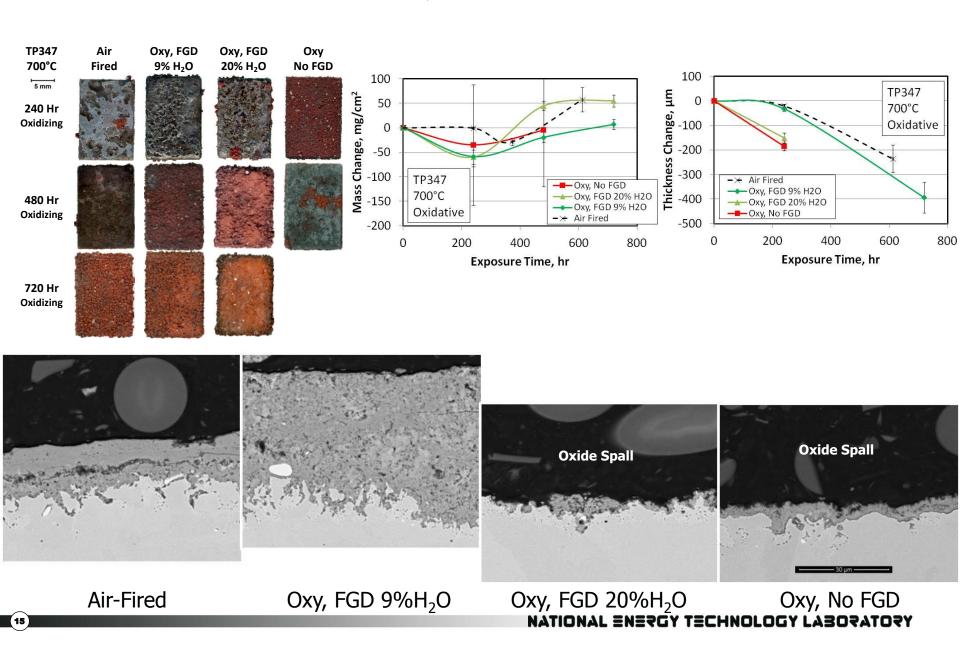
Test progress as of 3/31/2012:

Condition	Oxidative, 700°C	Oxidative, 450°C	Reducing, 450°C
Air-fired	60%	42%	17%
Oxy, FGD 9% H ₂ O	50%	50%	17%
Oxy, FGD 20% H ₂ O	50%	50%	17%
Oxy, No FGD	33%	50%	17%

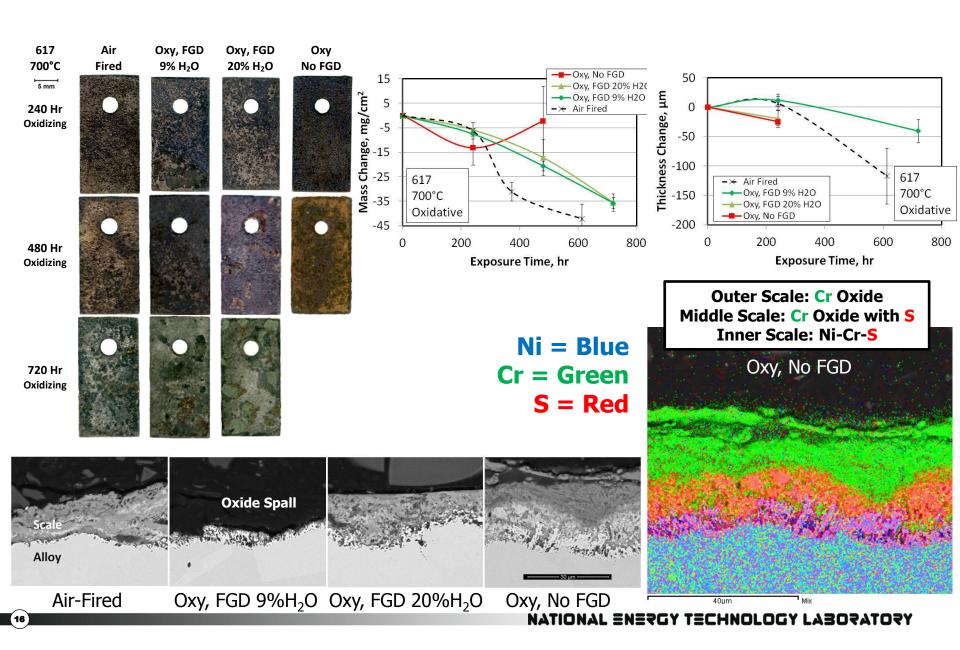
T91 at 700°C, Oxidative Conditions



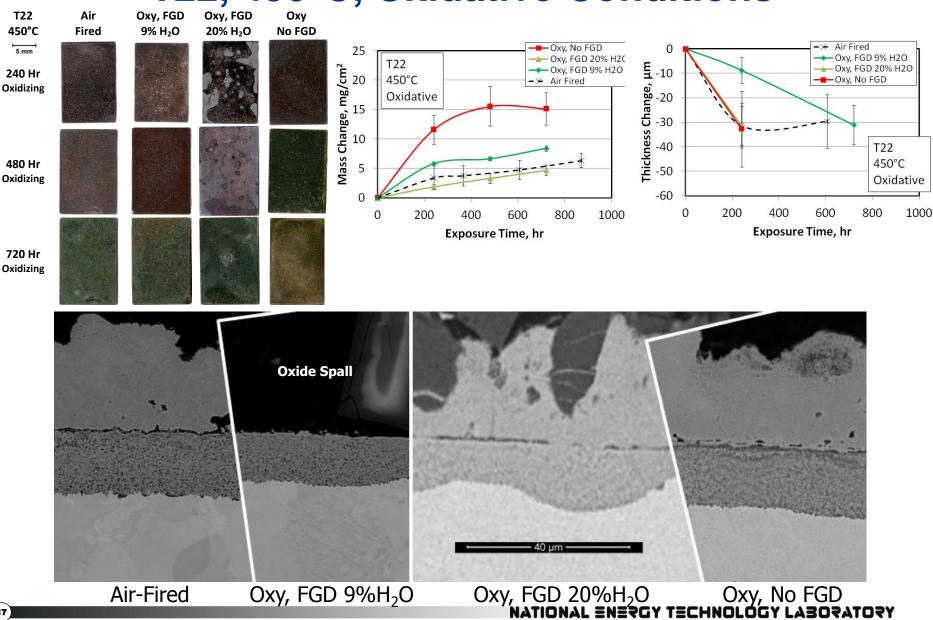
TP347H at 700°C, Oxidative Conditions



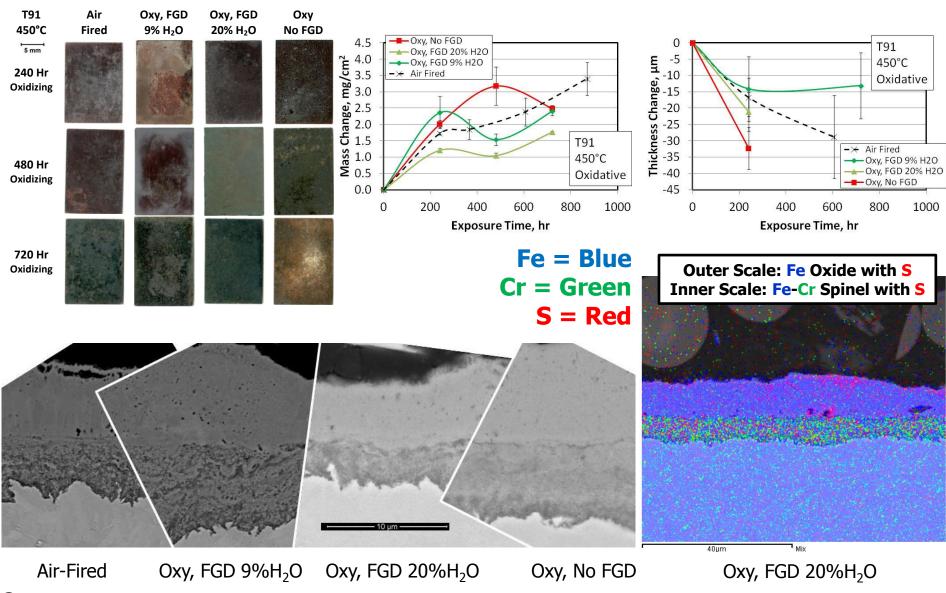
617 at 700°C, Oxidative Conditions



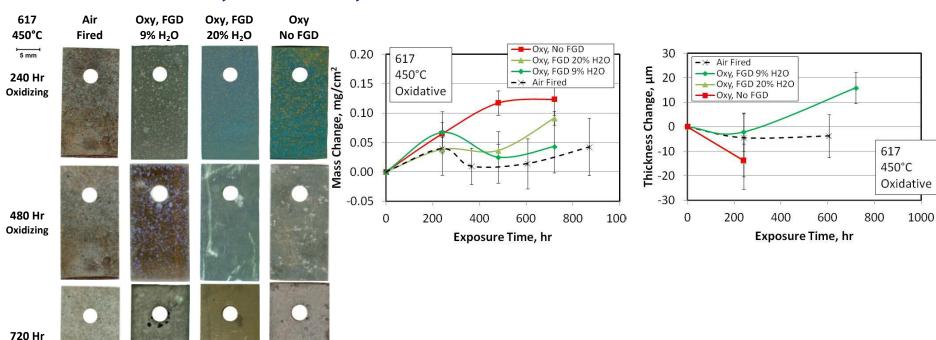
T22, 450°C, Oxidative Conditions



T91, 450°C, Oxidative Conditions



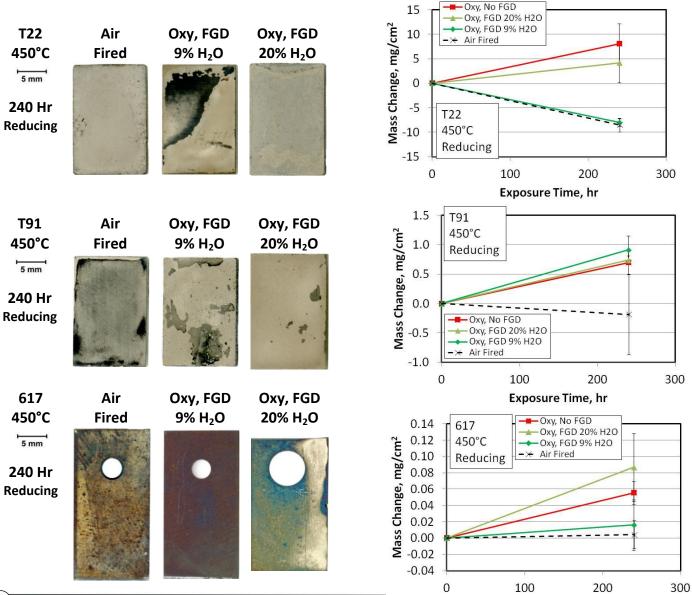
617, 450°C, Oxidative Conditions



Oxidizing

450°C, Reducing Conditions

Exposure Time, hr



Observation—Long Term Tests

Initial Section Loss Results

- At 700°C T91 had more section loss in the high water FGD with 20% H₂O and without FGD cases
- At 700°C TP347 had more section loss in the high water FGD with 20% H₂O and without FGD cases
- At 450°C (both oxidative and reducing) 617 is essentially free of corrosion in all cases
- No clear differentiation yet for other alloys and conditions

Corrosion Mechanism Possibilities

SH/RH Conditions (650-700°C, Oxidative Conditions)

SO₃ threshold (shown below in terms of SO₂)

- Between 100 & 1000 ppm SO₂ with SCM ash (Jerry Meier's talk)
- Between 100 & 3000 ppm SO₂ with 30-30-5-5 ash (deposit D)
- Could mean a large oxy-corrosion difference for some range of S in coals, and small difference in others

Fluxing mechanism for T91

- Fe oxide dissolving into ash
- Ash attachment as Fe deposits within ash
- Very thin Fe-oxide portion of scale
- Usually requires a molten phase
 - Na₂SO₄ and K₂SO₄ have too high of melting points
 - FeNaK tri-sufates have lower melting points (SCM composition)
 - Tri-sulfates require SO₃ in gas phase for stability—threshold tie-in?

Steam Side Oxidation Effects of pressure—update on A-USC autoclave

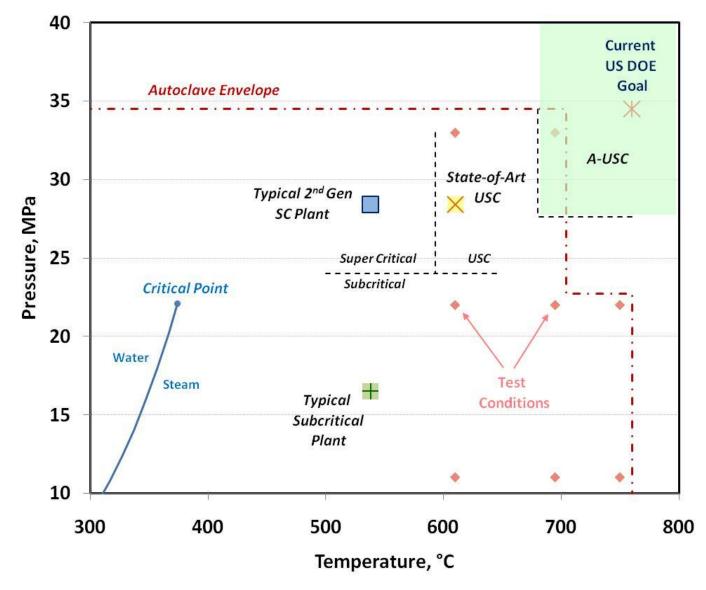
Overview of System and Plans

Shakedown Progress and Current Status

Coal-fired power plant nomenclature, conditions, and typical efficiency

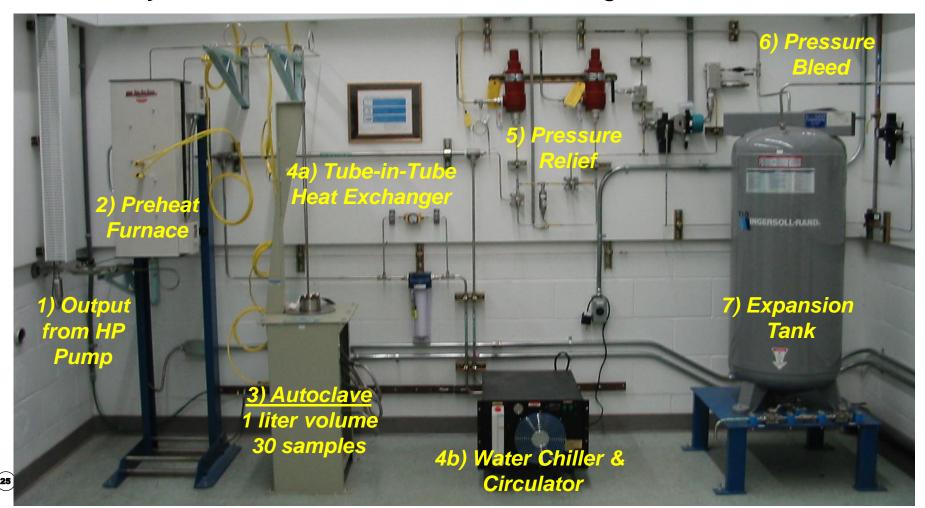
Nomenclature	Conditions	Net Plant Efficiency (%, HHV)		
Subcritical	16.5 MPa (2400 psi) 566°C /566°C (1050°F/1050°F)	35		
Supercritical (SC)	>24.8 MPa (3600 psi) 566°C /579°C (1050°F/1075°F)	38		
Ultra-supercritical (USC)	>24.8 MPa (3600 psi) 593°C /621°C (1100°F/1150°F)	>42		
Advanced Ultra-Supercritical (A-USC)	27.6-34.5MPa (4000-5000 psi) 704-760°C (1300-1400°F) main steam	>45		

Steam Oxidation at Pressure Test Conditions



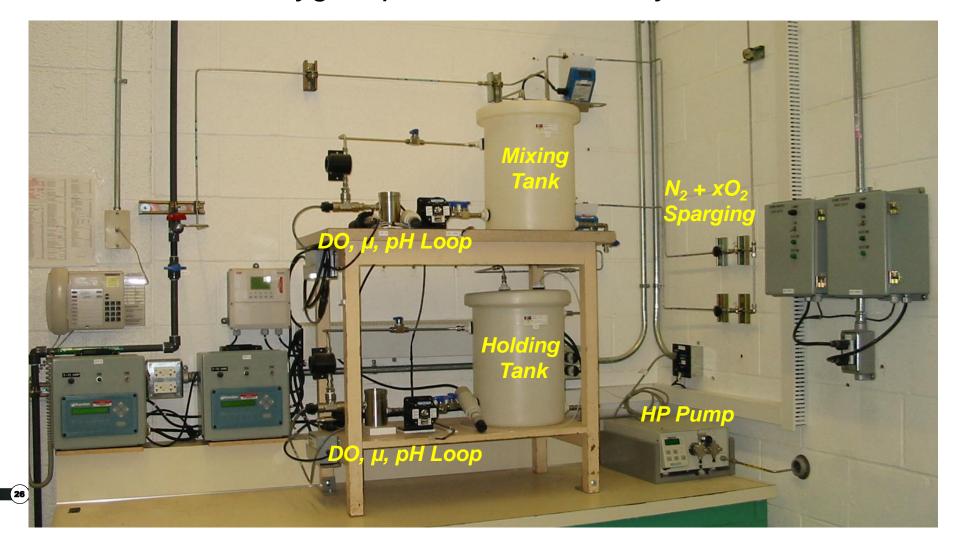
Dual Rated Flowing Steam A-USC Autoclave

- 5000 psig (34.5 MPa) at up to 704°C
- 3300 psig (22.7 MPa) at up to 760°C
- Haynes 230 used for autoclave and high T/P line material



A-USC Steam Autoclave Water Treatment

- Two tank system
- Dissolved oxygen, pH, and conductivity



Pressure Test Alloys

Alloy Group A—All pressures and temperatures

H230, H263, H282, IN740u

Alloy Group B—All pressures, 695 and 750°C

IN617, IN625, IN740, HR6W, U720Li, IN718

Alloy Group C—All pressures, 610 °C

- TP304H, TP347u
- T91, T92

Alloys with the "u" designation are alloys from the US-UK Phase I round robin tests

Pressures are 11, 22, and 33 MPa

Current Status of Shakedown Activates

Good control of pressure

• ±10 psi at 3100 psig

In the process of improving temperature control

Water chiller currently not working

awaiting repairs

Summary

Long-term oxy-combustion fireside corrosion tests

- Oxidative tests ~50% complete
- At 700°C T91 had more section loss in the high water FGD with 20% H₂O and without FGD cases
- At 700°C TP347 had more section loss in the high water FGD with 20% H₂O and without FGD cases
- At 450°C (both oxidative and reducing) 617 is essentially free of corrosion in all cases
- No clear differentiation yet for other alloys and conditions
- Probable SO₃ gas threshold at 650-700°C
- Evidence of fluxing mechanism for T91 at 700°C

Effects of pressure—update on A-USC autoclave

- USC steam conditions achieved
- Currently finishing shakedown tests