

Effects of Phosphorus and Arsenic on SOFC Anodes

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Outline

- ▶ Introduction / Summary of Previous Work
- ▶ Objectives / Experimental Approach
- ▶ Experimental Results
- ▶ Summary
- ▶ Future Work
- ▶ Acknowledgements



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Introduction

- ▶ Coals contain a wide variety of impurities.
- ▶ Different impurities lead to different types of interactions with SOFC anode.
- ▶ Anode performance degradation due to coal gas impurities is affected by various factors, such as concentration of contaminants, temperature, operation time, cell voltage, and fuel utilization.
- ▶ Previous studies at PNNL focused on effects of P, As, Sb, S, Se, Cl at ppm levels
- ▶ Current studies are focused effects of sub-ppm levels of P and/or As on anode chemistry/microstructure



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Anode–Phosphorus Interactions: Conclusions from Previous Work

- ▶ Strong interaction between Ni and P-containing contaminants in coal gas (PH_3 , PO_2 , etc.)
 - Nickel phosphide solid phases: Ni_3P , Ni_5P_2 , Ni_{12}P_5 , Ni_2P , etc.
 - Sharp boundary observed between reacted and un-reacted parts of the anode
- ▶ Degradation Mechanisms
 - Increased Ohmic resistance due to
 - Loss of electrical connectivity in the anode support due to phosphide formation (Ni depletion)
 - Micro-crack formation due to particle coalescence
 - Poisoning due to transport of phosphorus to the active interface (increased electrodic polarization)
 - P adsorbs on surface of Ni grains in unreacted anode (observed by XPS, ToF-SIMS)
- ▶ Effect of Contaminant Level
 - For $[\text{PH}_3] = 1\text{-}10$ ppm, both ohmic and electrodic losses in tested cells increased substantially during 1000 hours of testing

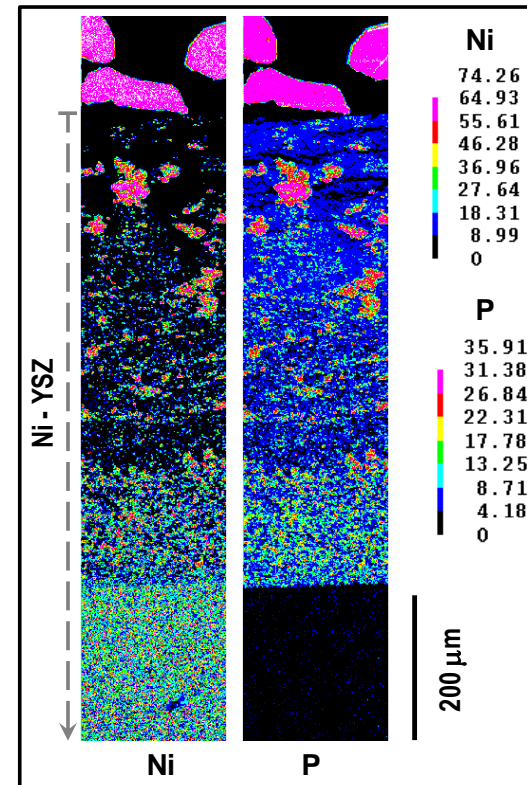
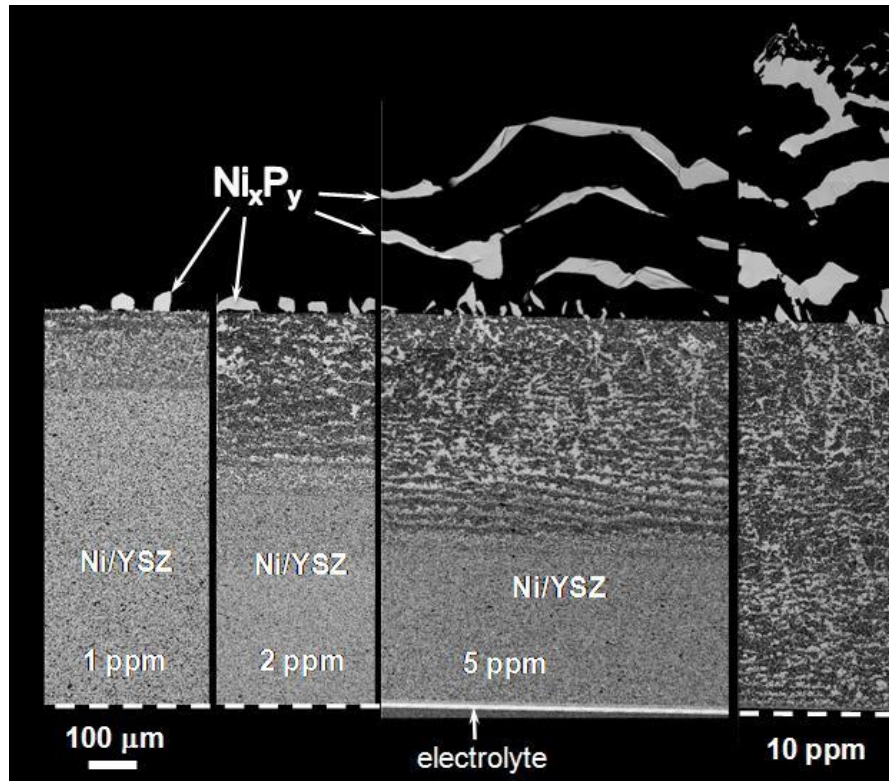


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Anode–Phosphorus Interaction

► SEM Analysis of anode-supported button cells after exposure



- ❑ Sharp boundary between reacted and unreacted anode
- ❑ WDS confirmed P is associated only with nickel, not zirconia.
- ❑ Micro-crack formation in reacted area: W. Liu et al., “Effect of Nickel-Phosphorus Interactions on Structural Integrity of Anode-Supported SOFC,” J. Power Sources, 195, 7140 (2010).



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Anode–Arsenic Interactions: Conclusions from Previous Work

- ▶ Strong interaction between Ni and As-containing contaminants in coal gas (AsH_3 , As_2 , etc.)
 - Nickel arsenide solid phases: Ni_5As_2 , $\text{Ni}_{11}\text{As}_8$, etc.
 - Sharp boundary observed between reacted and un-reacted parts of the anode
- ▶ Degradation Mechanisms
 - Loss of electrical connectivity in the anode support due to arsenide formation: Ni depletion (increased Ohmic resistance)
 - Abrupt failure after long-term operation upon loss of electrical percolation
 - Unlike case for P, poisoning effects due to adsorption of As at active anode interface were not observed
- ▶ For $[\text{AsH}_3] = 1 - 10$ ppm, substantial degradation of performance observed in 1000 hours or less

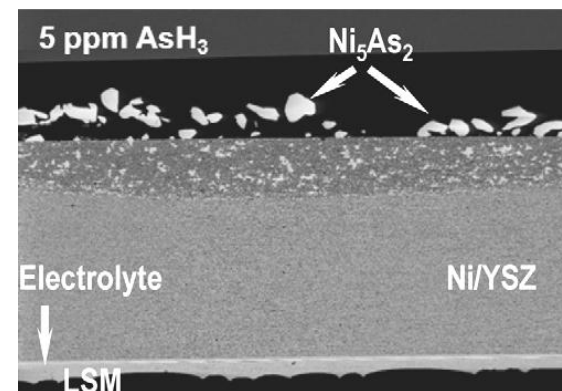
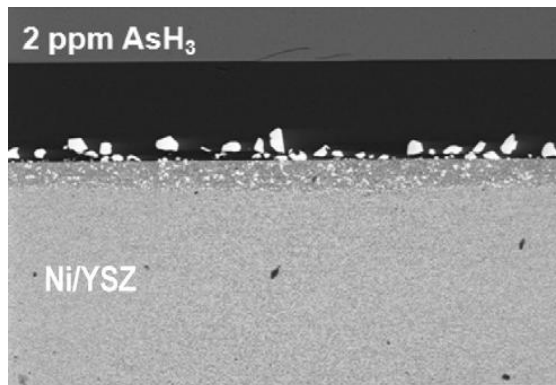
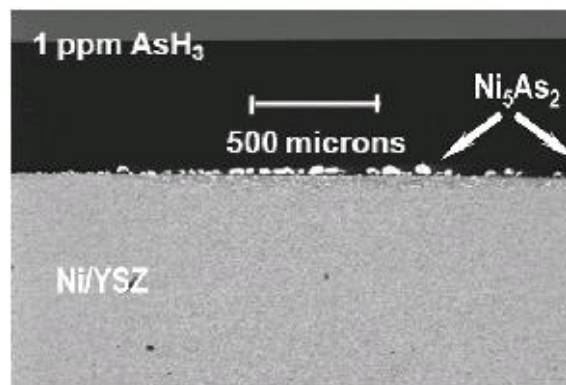


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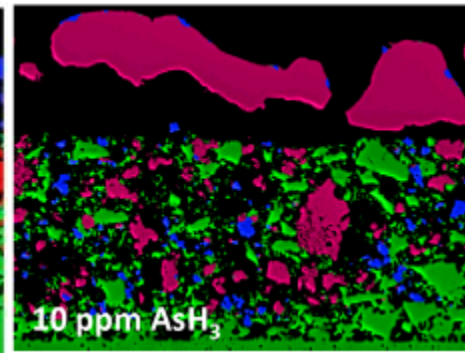
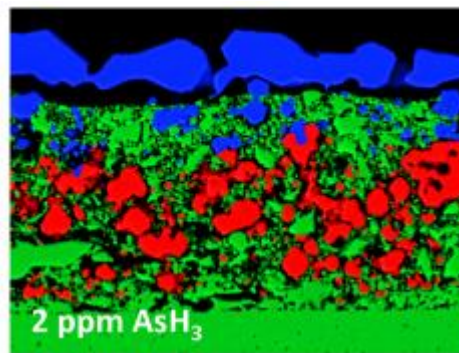
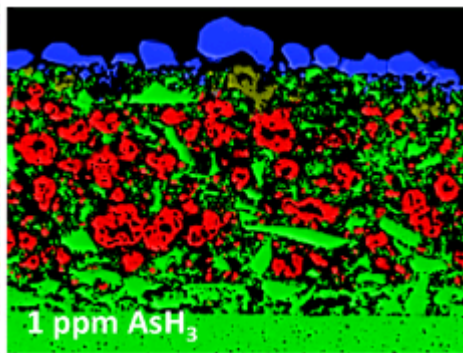
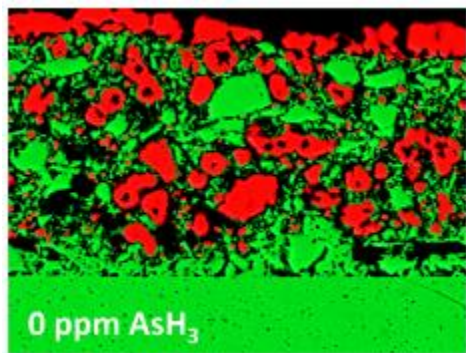
Anode-Arsenic Interaction

SEM Cross-Section Image (800°C, 500 hours)



□ AsH_3 Concentration \uparrow ~ Depth of Reaction \uparrow , Agglomeration \uparrow

Conversion of Nickel to Nickel Arsenide (Ni_5As_2 , $\text{Ni}_{11}\text{As}_8$)



• 700°C, 50 Hours

• Red: Ni, Dark Yellow: Ni-As Solid Solution, Green: YSZ, Blue: Ni_5As_2 , Magenta: $\text{Ni}_{11}\text{As}_8$

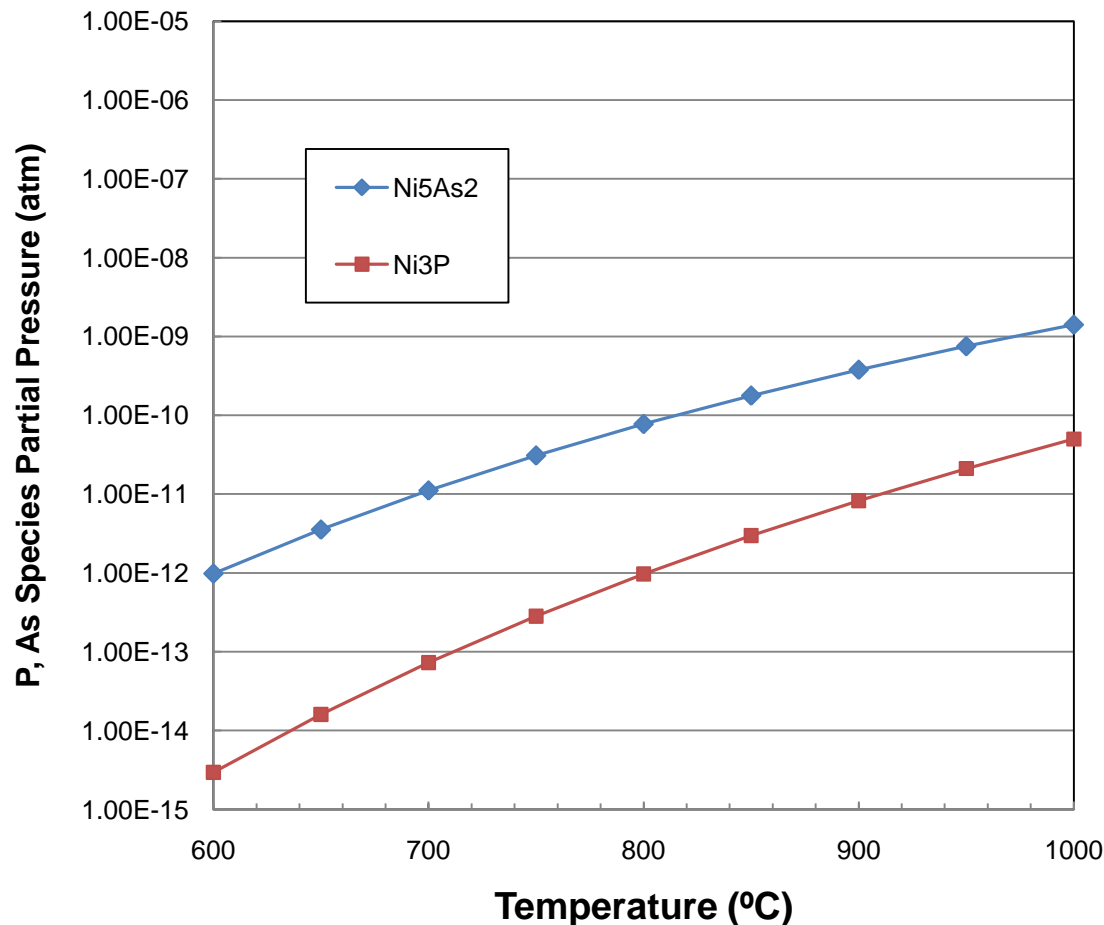


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Phosphide/Arsenide Formation

- ▶ Ni Phosphide / Ni Arsenide formation expected to occur even at sub-ppb contaminant levels:



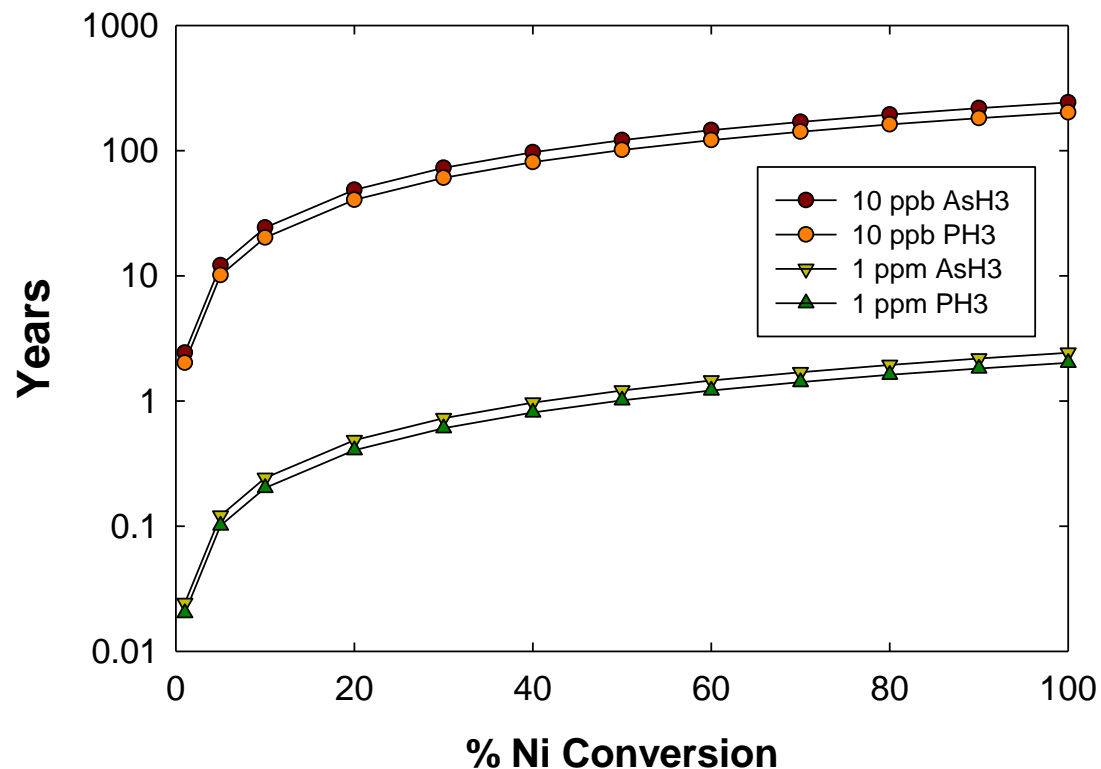
Effect of contaminant level on conversion rate

▶ Expect lower rate of reaction as contaminant level decreases due to lower contaminant delivery rate

▶ Calculated rates of Ni conversion

■ Assumptions:

- 50/50 vol% Ni/YSZ anode w/ 40% porosity; 500 microns thick
- 65% fuel utilization, 0.8 A/cm² current density
- Complete capture of contaminant by anode (worst-case scenario)
- Dominant phase formed:
 - ◆ P: Ni₃P
 - ◆ As: Ni₅As₂



Objective/Approach

- ▶ Objective: Study effects of sub-ppm levels of P, As on Ni/YSZ anode chemistry and microstructure
 - Coal gasification cleanup may reduce P, As levels to the level of ~10 ppb.
- ▶ Previous studies verified substantial reaction phase formation at ppm levels. Do the nature and extent of anode/contaminant interactions change as contaminant concentration decreases below 1 ppm?
- ▶ Approach:
 - Perform “flow-by” reaction tests over a range of contaminant levels (between 10 ppb and 1 ppm)
 - Adjust test time to deliver equivalent total dosage for all tests (concentration x time = constant)
 - Use surface and cross-section electron microscope analyses of tested samples to assess relationships between contaminant type, contaminant level, dosing time, and secondary phase formation

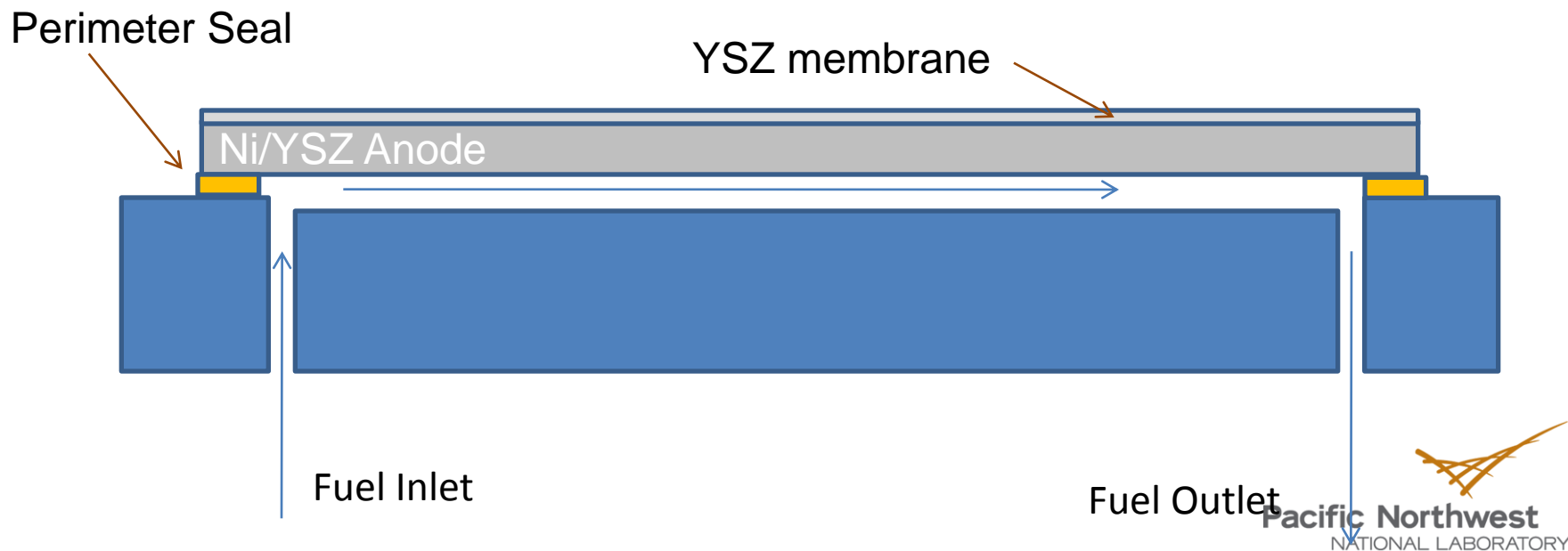


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“Flow-by” anode contaminant tests

- Flow rate: 200 sccm, corresponding to ~65% fuel utilization at 0.8 A/cm²
- Gas composition: Simulated coal gas (55% H₂; 45% CO₂)
- Contaminant: AsH₃ and/or PH₃
- Temperature: 700, 800°C



Experimental parameters

- ▶ Perform tests over a range of contaminant levels (between 10 ppb and 1 ppm)
 - Equivalent total dosage of contaminant (dosing rate x time = Constant)

Concentration	Time (h)	Total Moles Supplied
1.00 ppm	50	2.68×10^{-5}
0.50 ppm	100	2.68×10^{-5}
0.10 ppm (100 ppb)	500	2.68×10^{-5}
0.05 ppm (50 ppb)	1000	2.68×10^{-5}
0.01 ppm (10 ppb)	5000	2.68×10^{-5}



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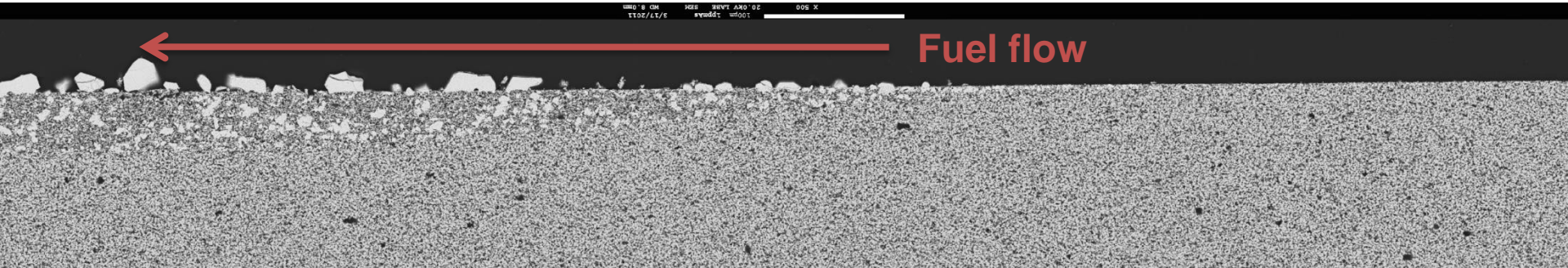
Experimental Results



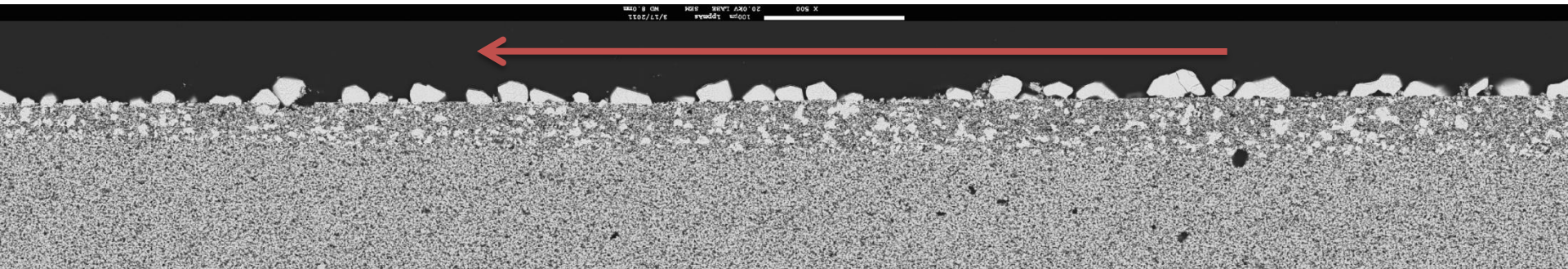
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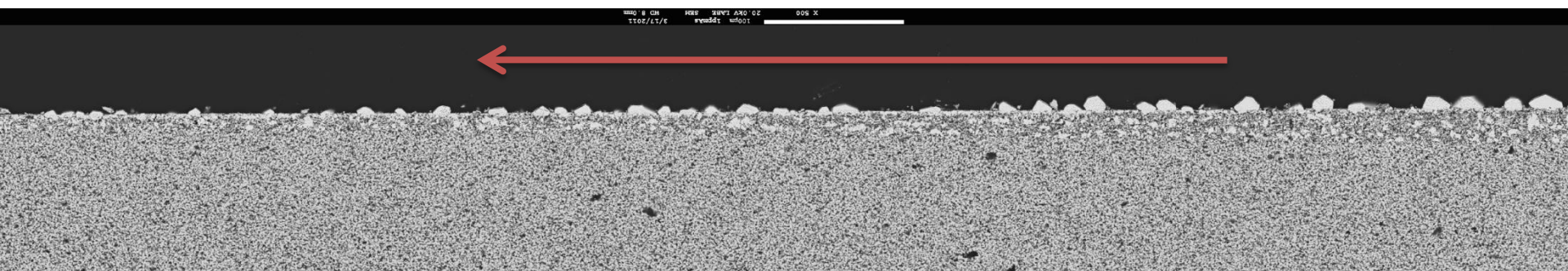
50 h, 1 ppm AsH₃ in simulated coal gas, 800°C



► Region 1 (inlet)

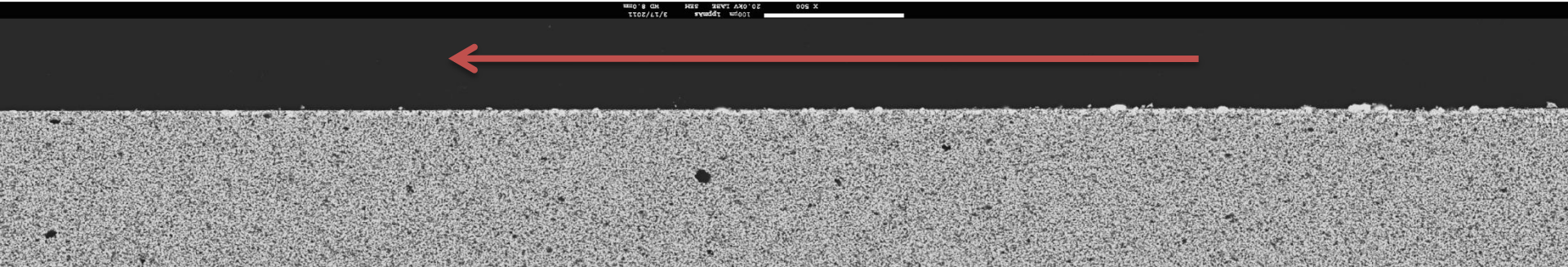


► Region 2

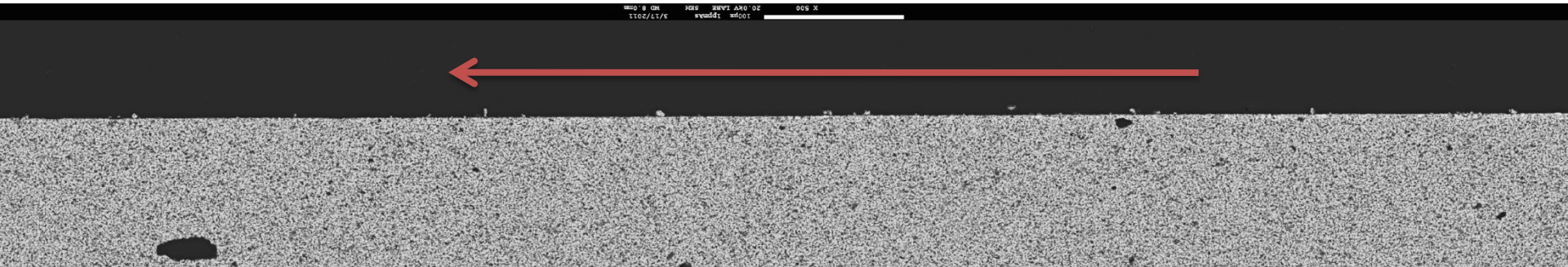


► Region 3

50 h, 1 ppm AsH₃ in simulated coal gas, 800°C

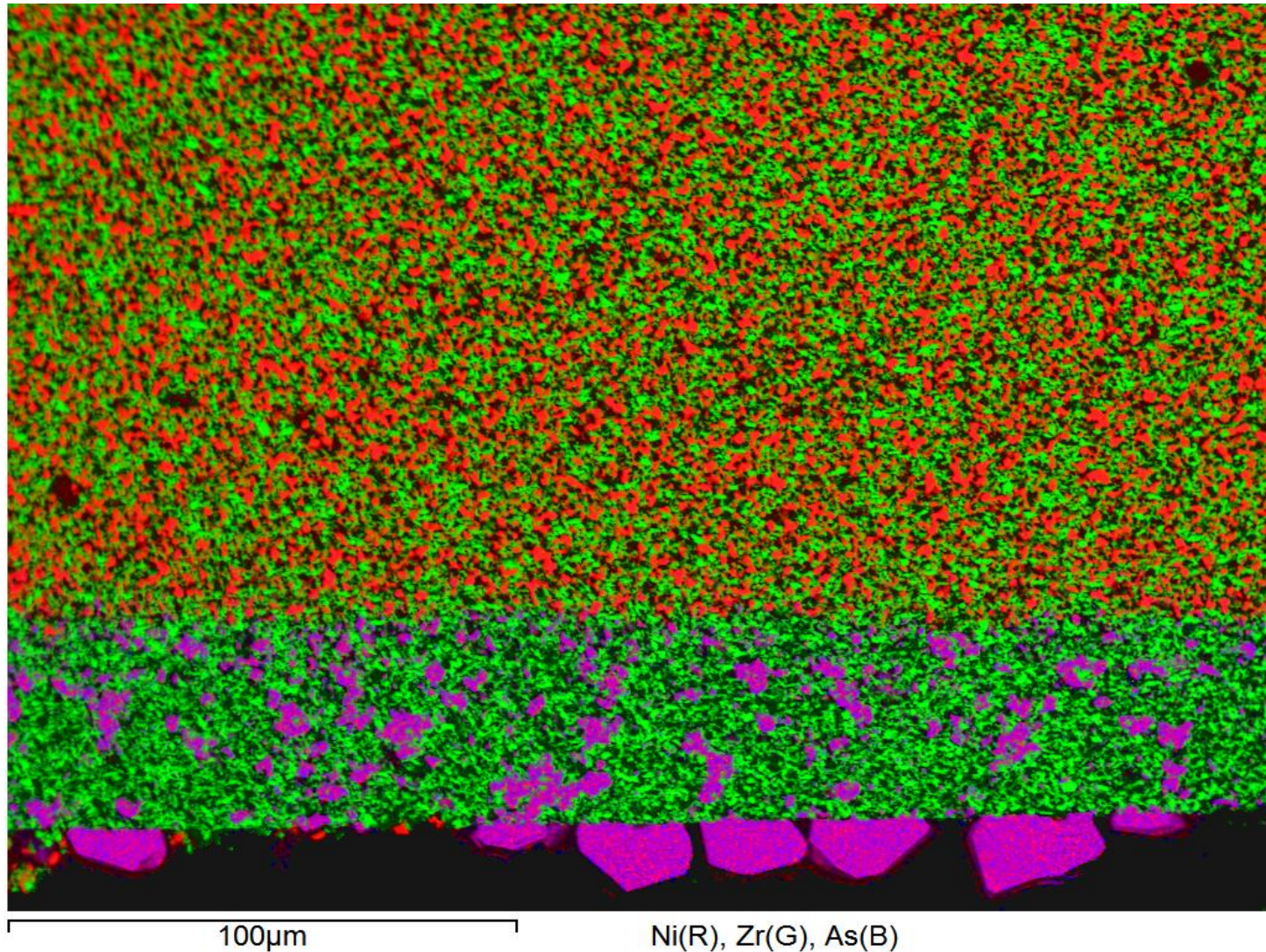


► Region 4



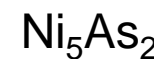
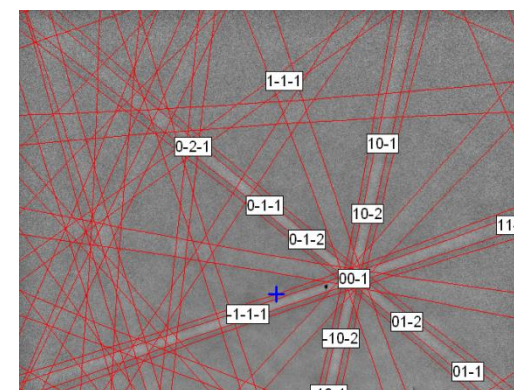
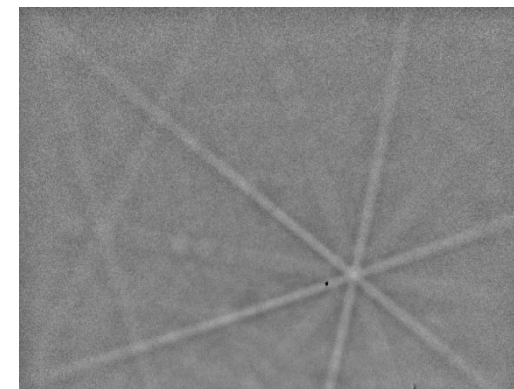
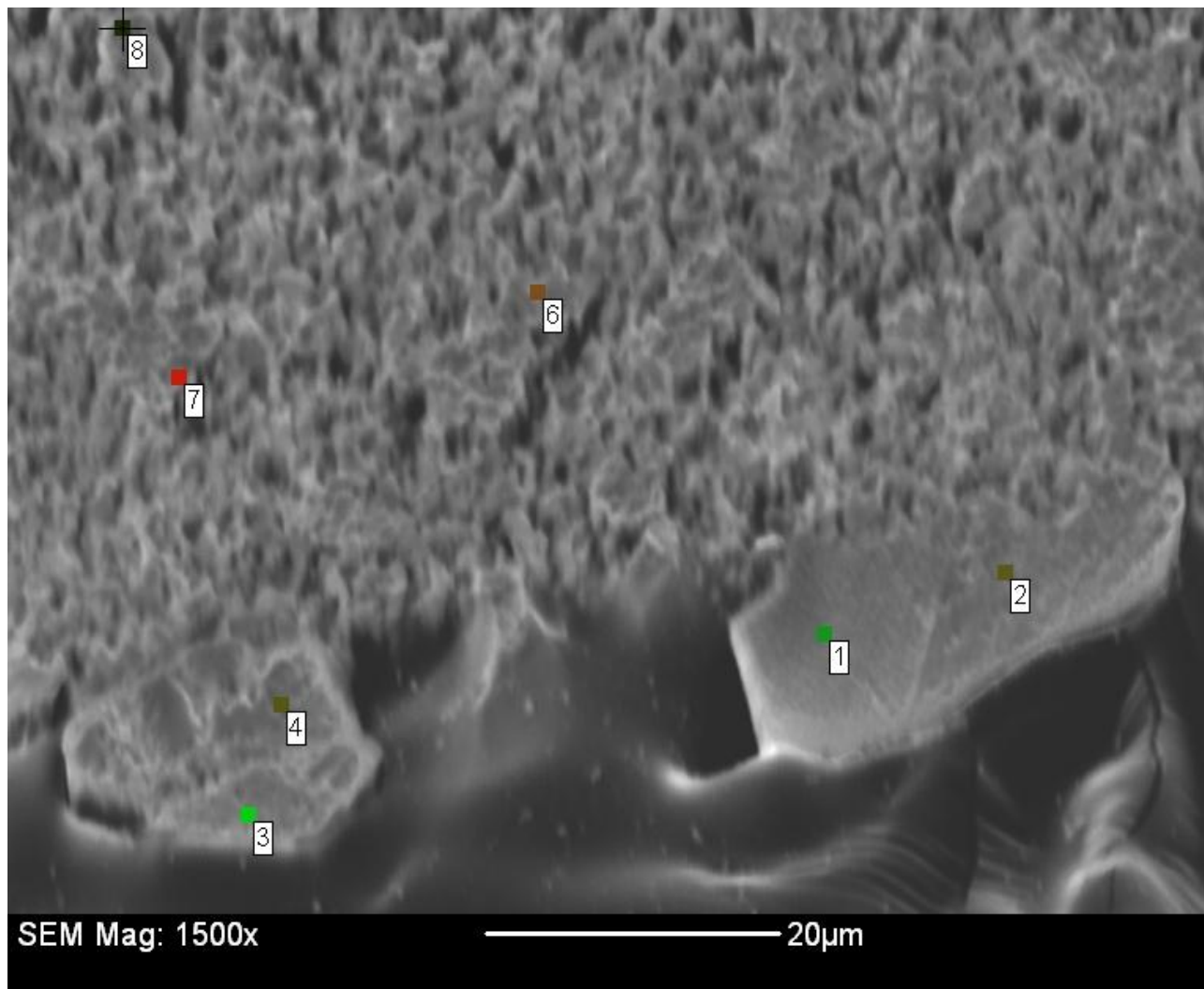
► Region 5

50 h, 1 ppm AsH_3 in simulated coal gas, 800°C : EDS Analysis



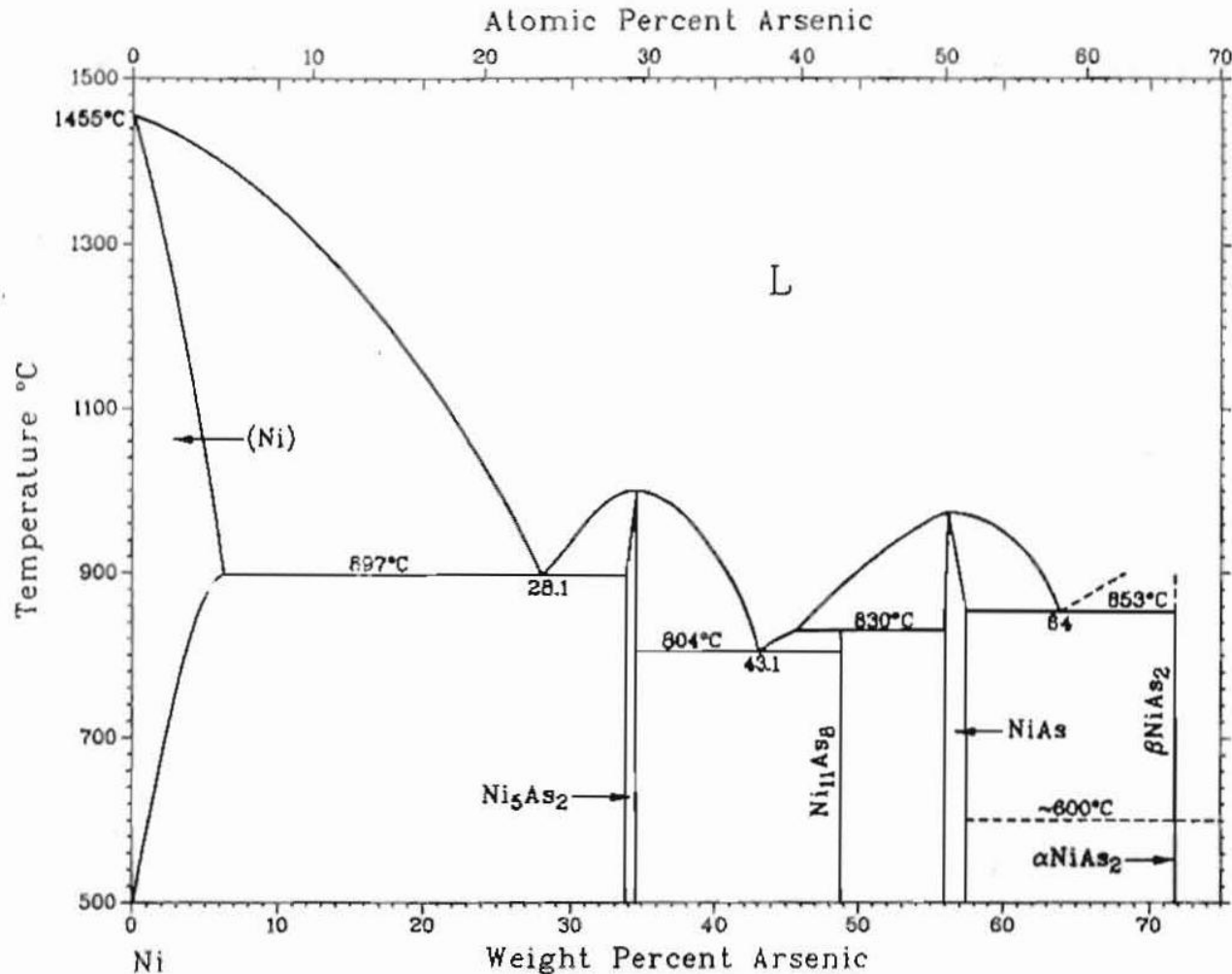
Purple is Ni_5As_2 phase

EBSD Analysis confirmed surface (points 1-4) and bulk reaction phase (point 8) to be Ni_5As_2



Arsenic – Nickel Phase Diagram

As-Ni

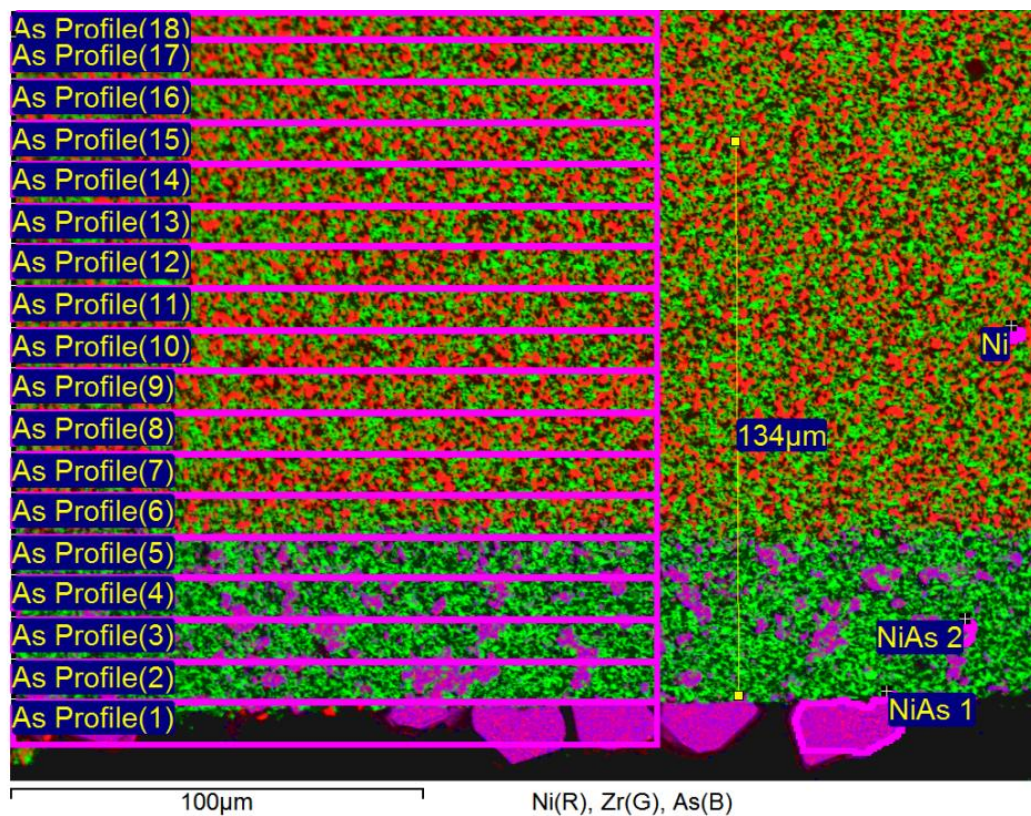


Note eutectics
at 897 and
804°C



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50 h, 1 ppm AsH₃ in simulated coal gas, 800°C: EDS area concentration profiles



Spectrum	O	Ni	As	Y	Zr
As Profile(18)	37.56	43.02	0	1.18	18.24
As Profile(17)	39.75	40.19	0	1.37	18.69
As Profile(16)	41.09	38.54	0	1.32	19.05
As Profile(15)	39.93	40.04	0.07	1.32	18.65
As Profile(14)	40.81	38.66	0.08	1.35	19.09
As Profile(13)	40.69	38.85	0	1.38	19.08
As Profile(12)	40.42	39	0.07	1.37	19.14
As Profile(11)	39.2	40.8	0	1.28	18.72
As Profile(10)	38.68	41.65	0.1	1.24	18.33
As Profile(9)	39.03	41.14	0.11	1.26	18.46
As Profile(8)	40.11	39.6	0.11	1.37	18.81
As Profile(7)	40.1	39.49	0.52	1.29	18.61
As Profile(6)	41.61	35.71	2.28	1.34	19.06
As Profile(5)	48.77	22.32	6.1	1.47	21.35
As Profile(4)	49.48	20.91	6.21	1.61	21.78
As Profile(3)	51.74	18.74	5.39	1.64	22.49
As Profile(2)	52.65	17.66	5.05	1.7	22.94
As Profile(1)	24.78	46.87	15.3	0.74	12.31

All results in atomic%

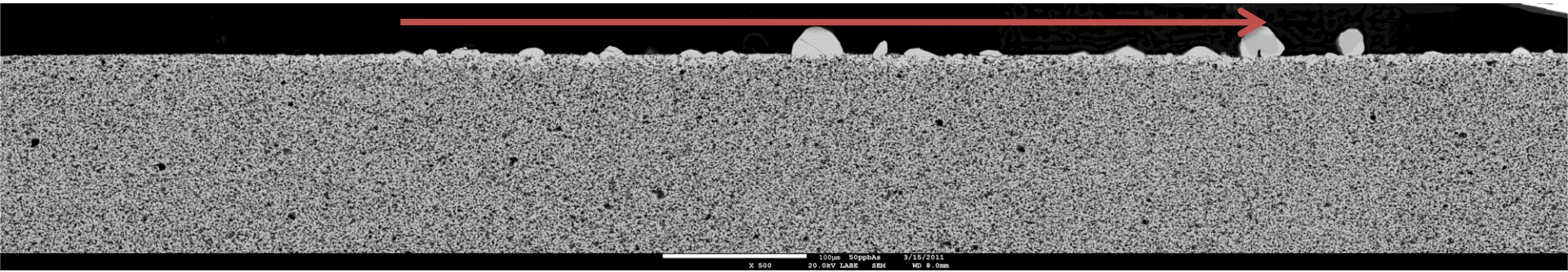
Profile height = 10µm



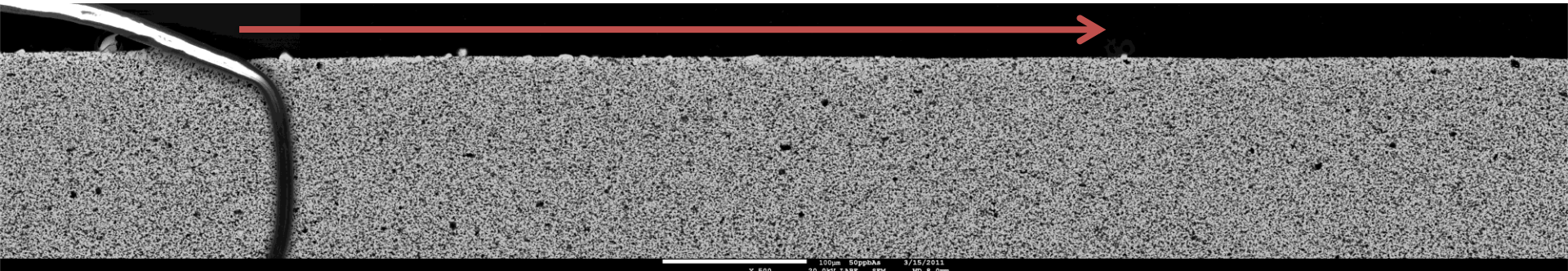
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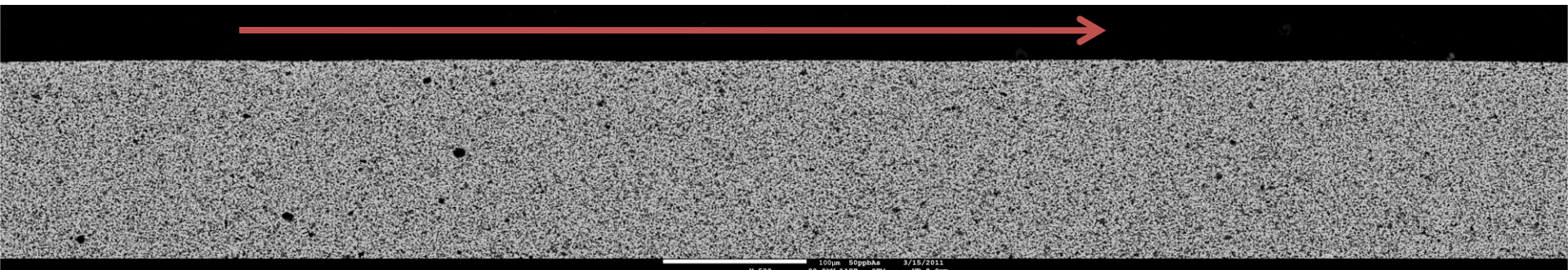
1000 h, 0.05 ppm AsH₃ in simulated coal gas, 800°C



▶ Region 1 (inlet)

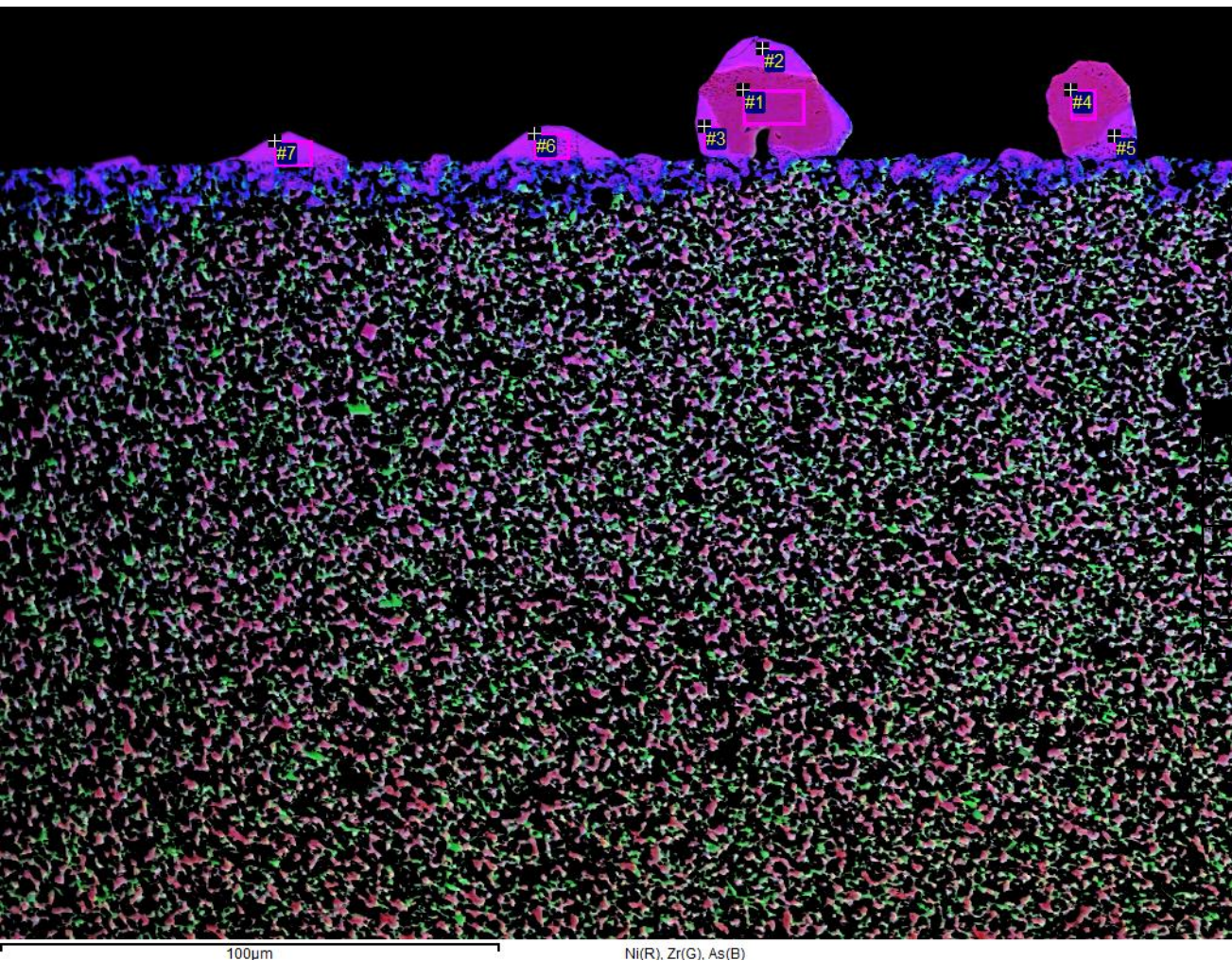


▶ Region 2



▶ Region 3

1000 h, 0.05 ppm AsH₃ in simulated coal gas, 800°C



Spectrum	O	Ni	As	Y	Zr
#1	2.42	89.41	8.16	0.00	0.00
#2	0.00	71.47	28.53	0.00	0.00
#3	0.00	71.64	28.36	0.00	0.00
#4	2.77	89.85	7.38	0.00	0.00
#5	7.19	67.45	25.36	0.00	0.00
#6	0.00	73.00	27.00	0.00	0.00
#7	3.65	68.93	25.95	0.00	1.48

All results in atomic%

Points 2,3,5,6,7 are Ni₅As₂

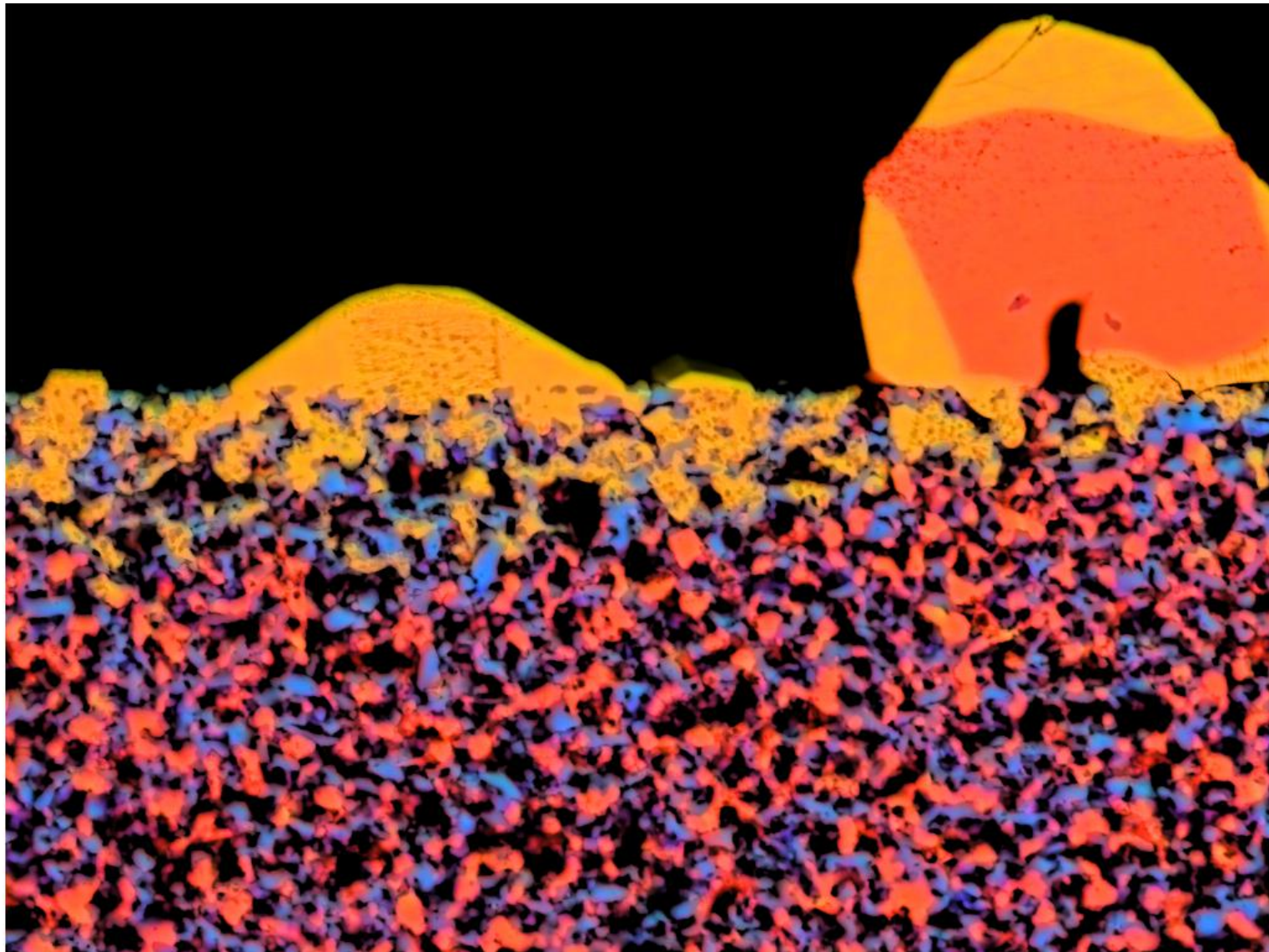
Ni (red); Zr (green); As (blue)



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1000 h, 0.05 ppm AsH_3 in simulated coal gas, 800°C



40μm

QuantMap Mix



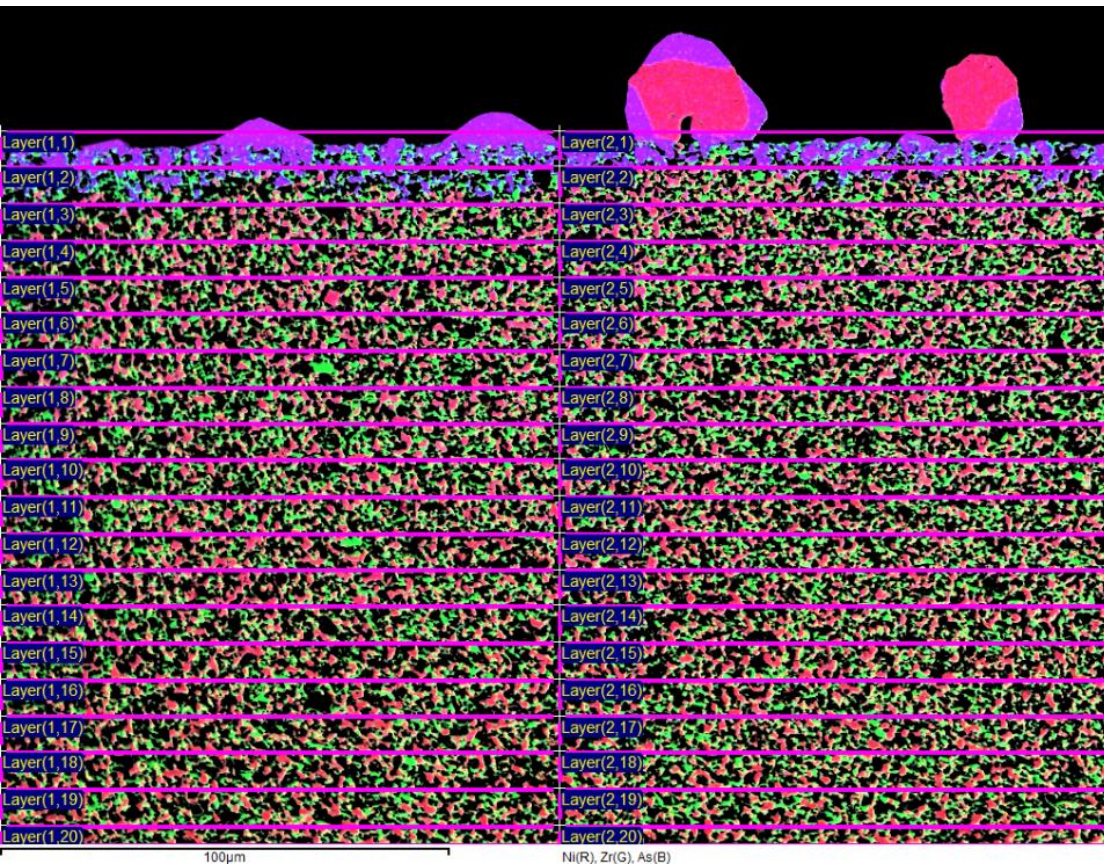
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Yellow orange is Ni_5As_2 , orange-red is Ni with varying levels of As, blue purple is YSZ

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1000 h, 0.05 ppm AsH₃ in simulated coal gas, 800°C



As is detectable down to ~150 µm below the surface.

Spectrum	Ni	As	Y	Zr	O
Layer 1	40.005	13.03	0.81	13.27	32.88
Layer 2	32.78	4.685	1.195	18.31	43.025
Layer 3	35.29	2.135	1.135	18.42	43.02
Layer 4	34.43	1.95	1.205	18.67	43.74
Layer 5	35.025	1.985	1.175	18.56	43.25
Layer 6	33.715	1.745	1.225	18.955	44.365
Layer 7	33.99	1.77	1.215	19	44.025
Layer 8	34.535	1.665	1.22	18.775	43.81
Layer 9	33.43	1.52	1.255	19.105	44.695
Layer 10	34.84	1.465	1.23	18.6	43.87
Layer 11	35.21	1.375	1.195	18.71	43.51
Layer 12	36.025	1.285	1.22	18.555	42.91
Layer 13	36.335	1.185	1.23	18.42	42.825
Layer 14	34.52	0.975	1.23	18.815	44.45
Layer 15	37.225	0.95	1.21	18.55	42.07
Layer 16	36.025	0.785	1.245	18.785	43.15
Layer 17	37.435	0.71	1.195	18.66	41.995
Layer 18	36.47	0.595	1.24	18.765	42.93
Layer 19	35.36	0.485	1.315	19.1	43.73
Layer 20	39.72	0.475	1.22	17.955	40.635

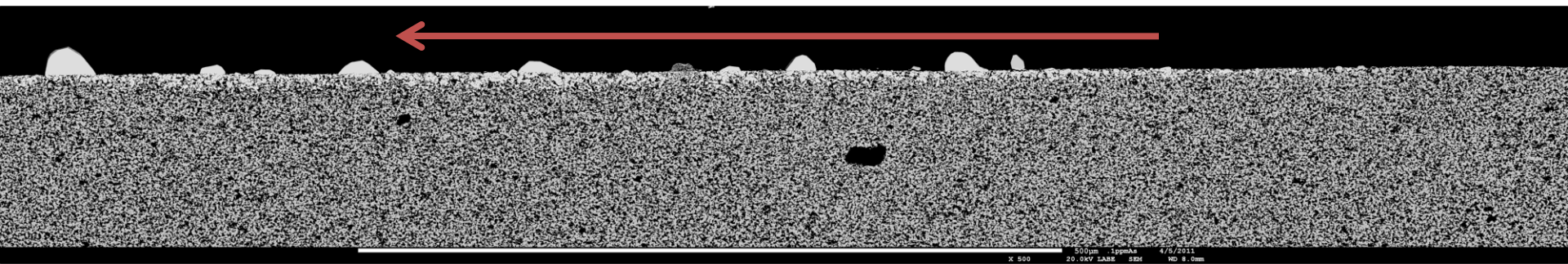
Average values of both depth profiles.
All results in atomic%



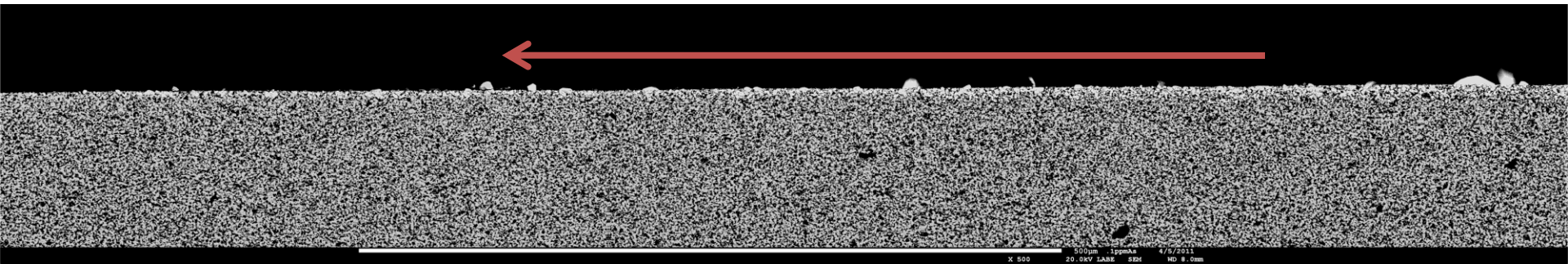
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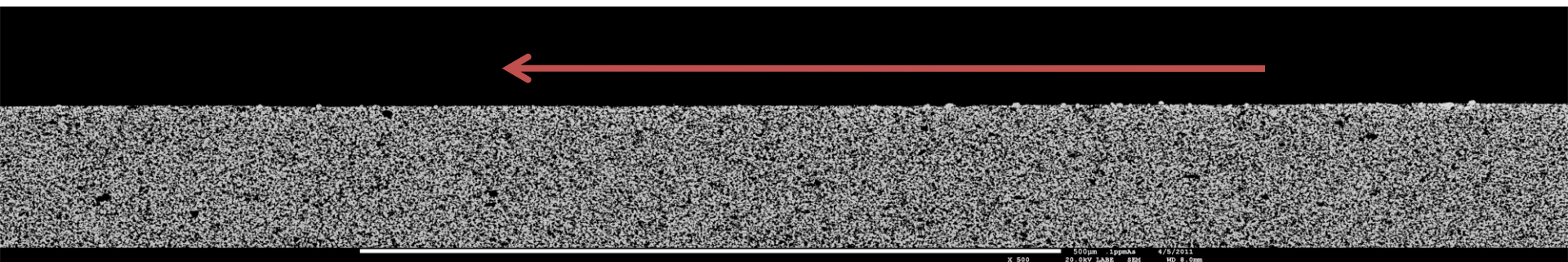
500 h, 0.1 ppm AsH₃ in simulated coal gas, 800°C



▶ Region 1 (inlet)

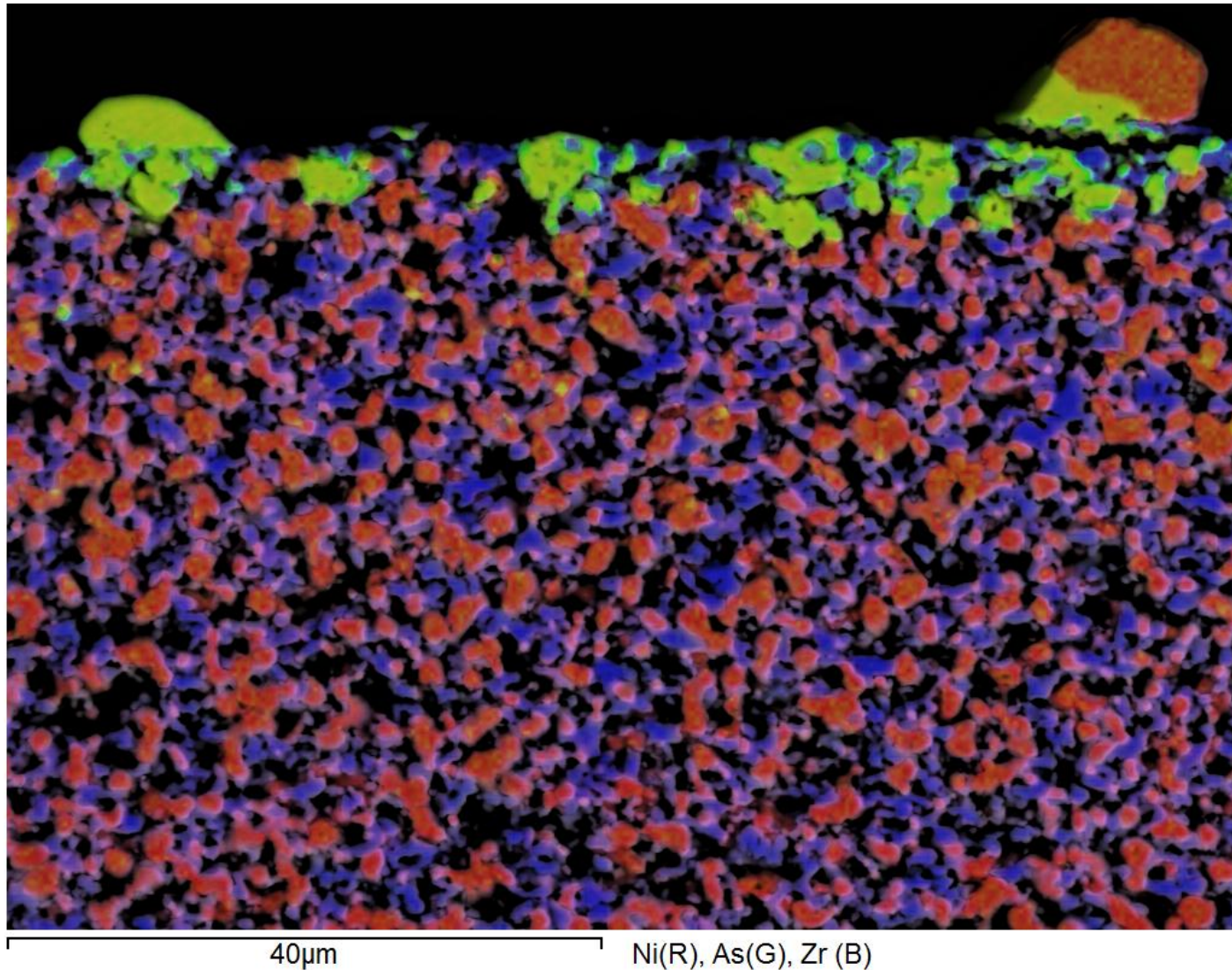


▶ Region 2



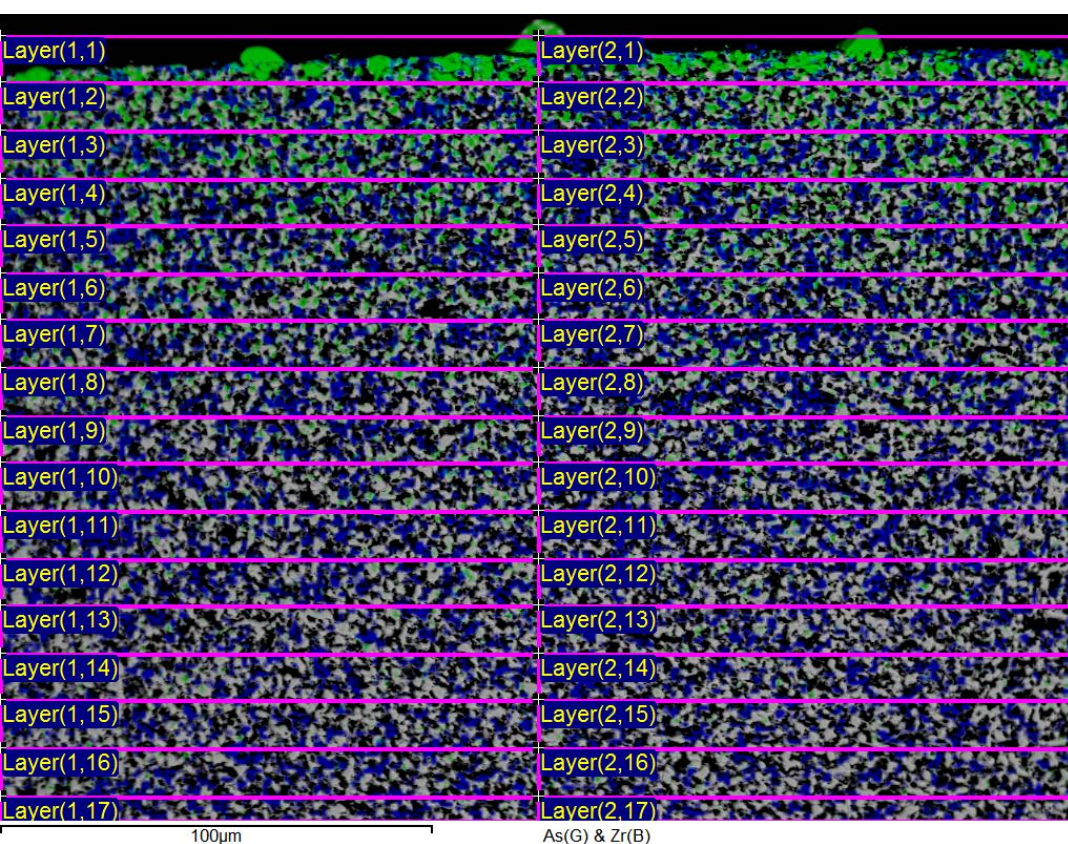
▶ Region 3

500 h, 0.1 ppm AsH_3 in simulated coal gas, 800°C



Green is Ni_5As_2 , Orange is Ni with levels of As below that of Ni_5As_2 , purple is YSZ.

500 h, 0.1 ppm AsH₃ in simulated coal gas, 800°C

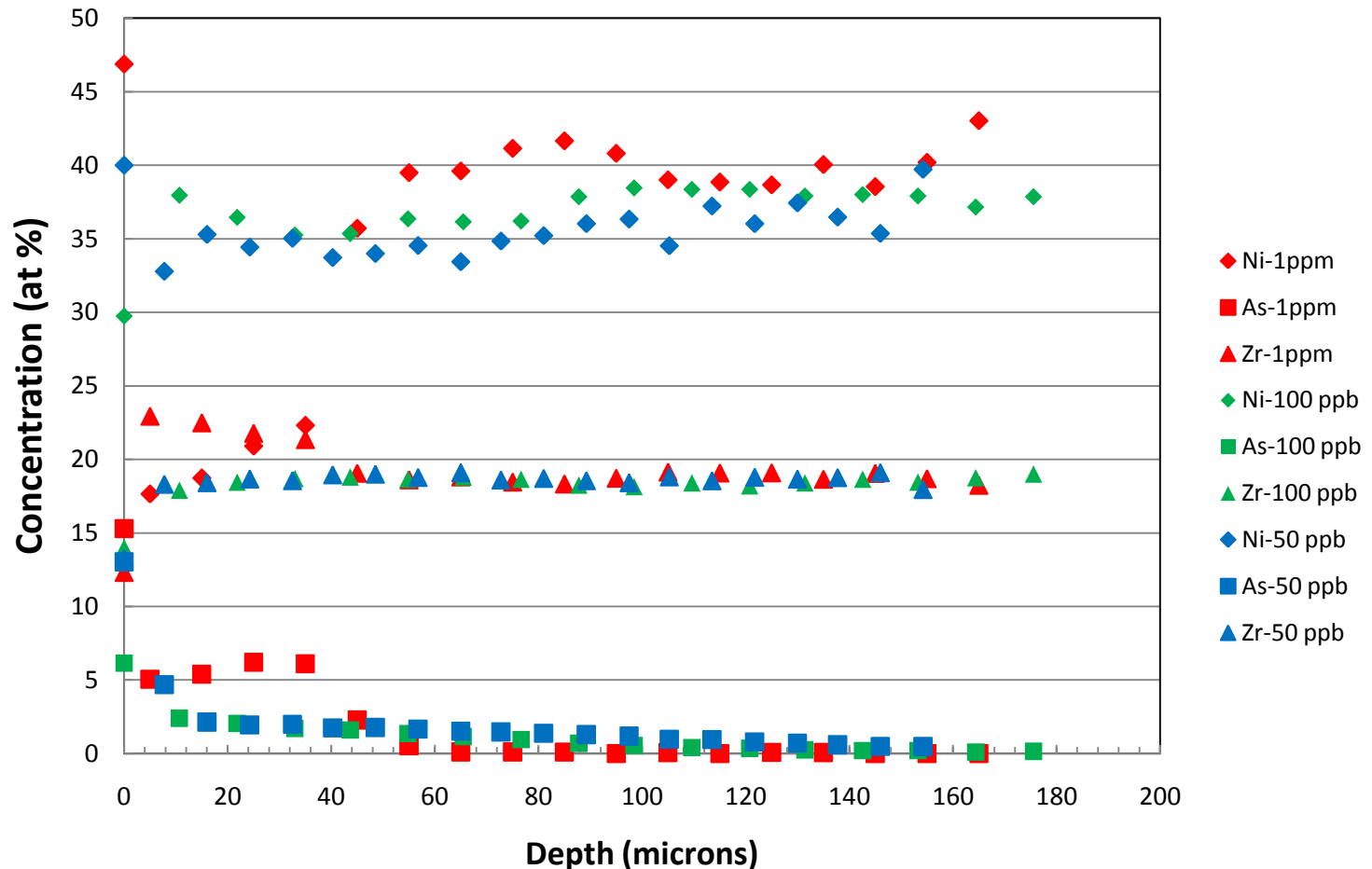


Spectrum	Ni	As	Y	Zr	O
Layer 1	29.75	6.15	0.95	14	49.1
Layer 2	37.95	2.4	1.3	17.9	40.45
Layer 3	36.45	2.05	1.4	18.45	41.7
Layer 4	35.25	1.7	1.4	18.7	42.9
Layer 5	35.35	1.6	1.45	18.8	42.9
Layer 6	36.35	1.35	1.35	18.65	42.25
Layer 7	36.15	1.15	1.4	18.8	42.55
Layer 8	36.2	0.95	1.35	18.65	42.8
Layer 9	37.85	0.7	1.35	18.25	41.7
Layer 10	38.45	0.55	1.35	18.15	41.5
Layer 11	38.35	0.4	1.35	18.4	41.5
Layer 12	38.35	0.35	1.35	18.2	41.75
Layer 13	37.9	0.25	1.4	18.4	42
Layer 14	38	0.2	1.45	18.65	41.75
Layer 15	37.9	0.2	1.45	18.45	42
Layer 16	37.15	0.1	1.45	18.75	42.45
Layer 17	37.85	0.15	1.4	19	41.7

Average values of both depth profiles.
All results in atomic%

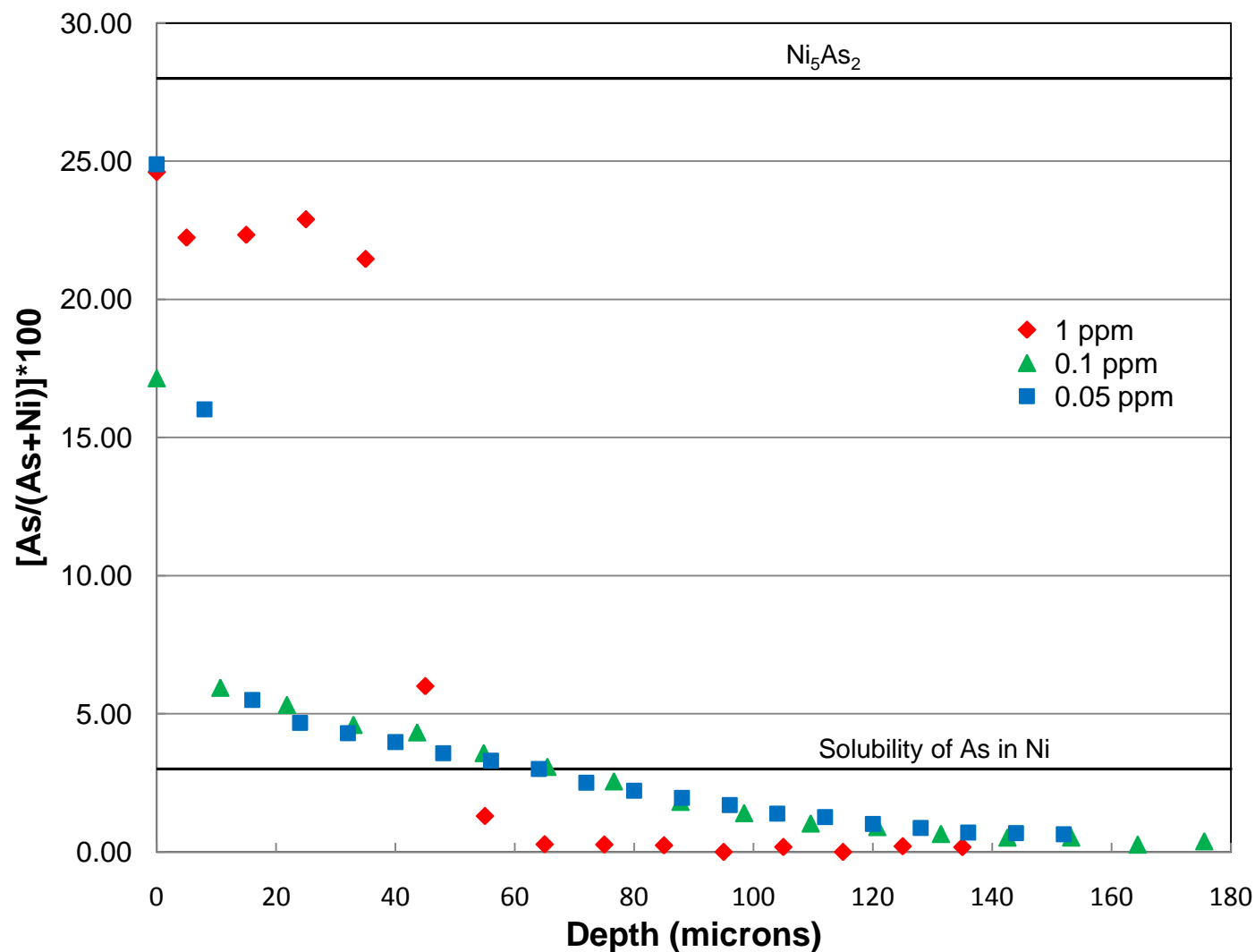
As is detectable down to ~140 µm
below the surface.

Concentration profiles from EDS analyses: Absolute concentration (at%)



- Extensive arsenide formation zone at 1 ppm; negligible As doping of Ni below arsenide zone; Ni depletion in reaction zone resulted from extensive formation of arsenide above surface of anode
- Narrower arsenide formation zone at 50 or 100 ppb, but extensive region of As-doped Ni below the arsenide zone

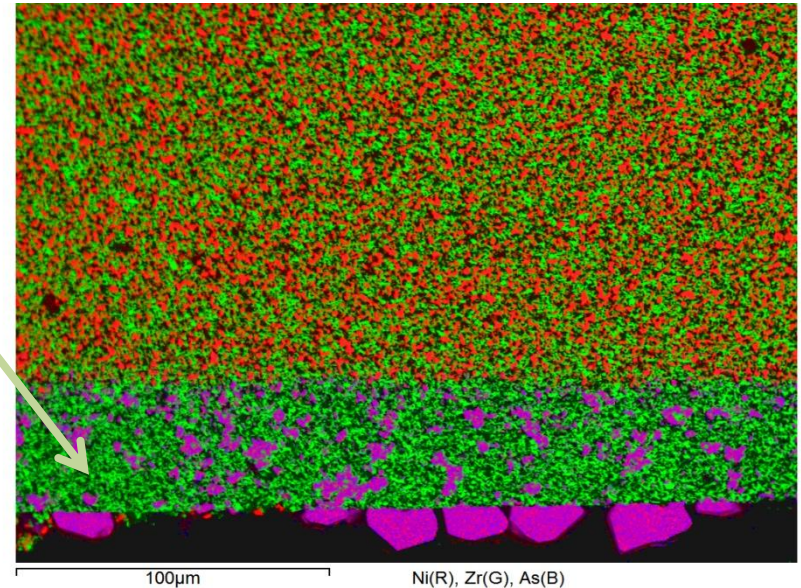
Depth Profile: As / (Ni + As)



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Length of primary reaction zone as f(concentration/time)



Test #	Concentration	Time (h)	Approx. Length of "Arsenide zone"
1	1.00 ppm	50	5 mm
2	0.50 ppm	100	TBD
3	0.10 ppm (100 ppb)	500	2 mm
4	0.05 ppm (50 ppb)	1000	2 mm
5	0.01 ppm (10 ppb)	5000	TBD

Summary

- ▶ Strong interactions occur between Ni-based anodes and P and/or As contaminants in fuel
- ▶ These interactions result in formation of secondary phases
 - Nickel phosphide solid phases: e.g., Ni_3P , Ni_5P_2
 - Nickel arsenide solid phases: e.g., Ni_5As_2 , $\text{Ni}_{11}\text{As}_8$
- ▶ Arsenide formation (Ni_5As_2) was confirmed with As concentrations as low as 50 ppb (in simulated coal gas)
 - Consistent with thermodynamic calculations, which indicate arsenide formation at much lower concentrations (< 1 ppb at 800°C)
 - Arsenide formation zone occurred in anode surface region near fuel inlet
 - Sharp boundaries were observed between arsenide formation zone and “unreacted” anode below that region
 - However, for $[\text{As}] = 50$ or 100 ppb, substantial As doping of Ni was observed underneath the arsenide formation region
- ▶ Implications for SOFC stacks:
 - Interaction zone between anode and arsenic will be concentrated near the fuel gas inlet of the cells, but will, of course, lengthen over time
 - For coal gas fuels cleaned to ppb levels, secondary phase formation is expected, but the low rate of contaminant delivery may significantly reduce degradation rates, and also simplify upstream mitigation

Future Work

- ▶ Complete analysis of results of equivalent dosage tests (As, P, As+P between 10 ppb and 1 ppm) at 700 and 800°
 - Correlate dosing level and time with extent and nature of interactions between anode and contaminant(s)
- ▶ Perform variable time reaction tests at a constant contaminant level to evaluate development of reaction zone geometry and composition



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- NETL: Shailesh Vora, Briggs White, Rin Burke, Travis Shultz, and Joe Stoffa
- PNNL: Clyde Chamberlin and Alan Schemer-Kohn



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