

# Liquid Tin Anode Fuel Cell Direct Coal Conversion

T. Tao, J. Bentley, M. Koslowske, M. Slaney, L. Bateman, J. Brodie, C. MacKean,

CellTech Power LLC, Westborough MA

Project Manager: Joe Stoffa, NETL

## ABSTRACT

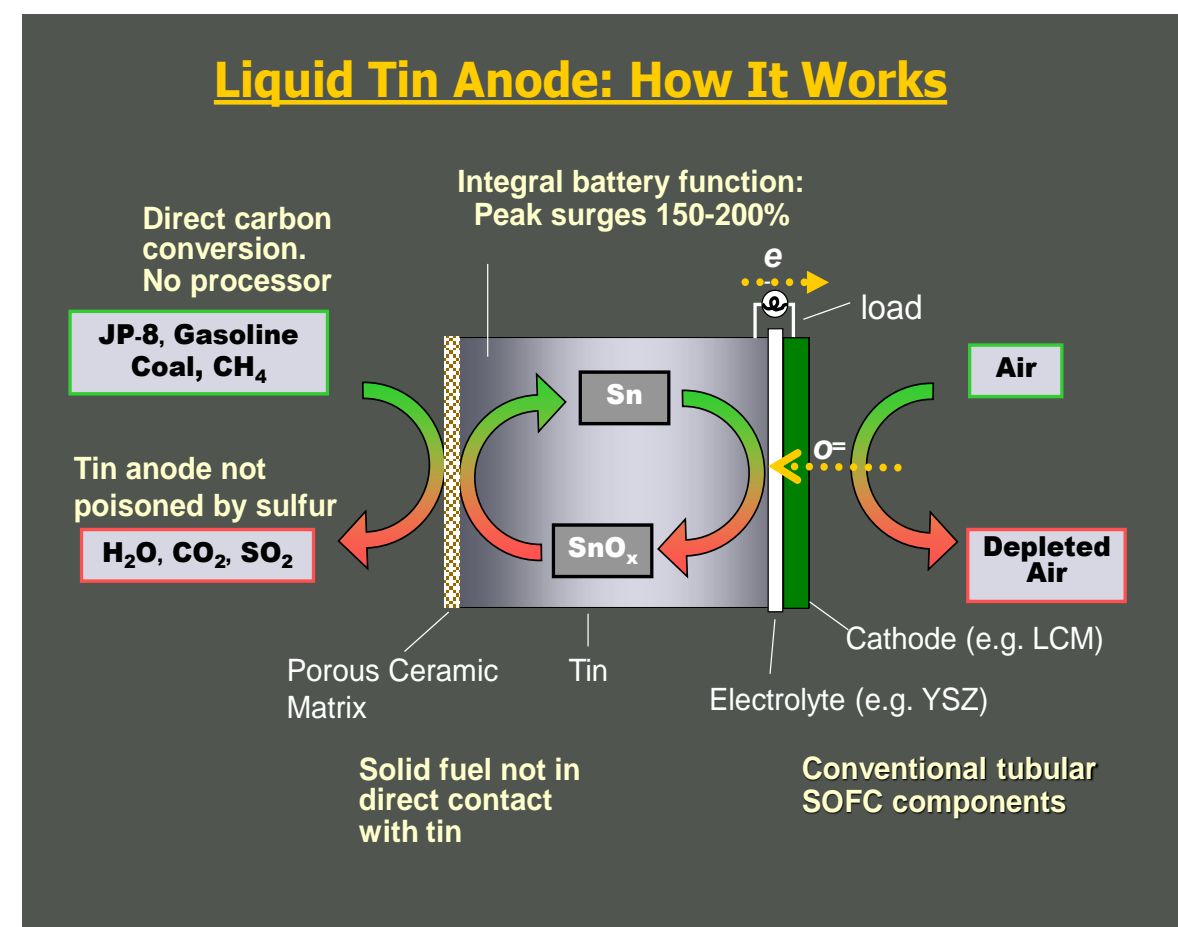
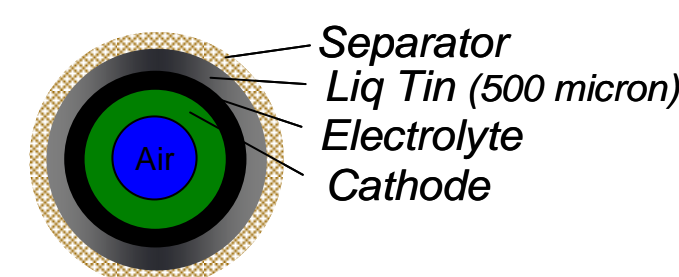
The Liquid Tin Anode Solid Oxide Fuel Cell (LTA-SOFC) is a direct conversion fuel cell and does not require fuel processing, reforming or water.<sup>1,2,3,4</sup> Power is generated directly from any solid, liquid or gaseous carbonaceous fuel. Sulfur and carbon species are fuel not a poison to the LTA-SOFC. CellTech's LTA-SOFC is the only known fuel cell capable of direct operation on heavy hydrocarbons such as military logistics fuel. Its versatility and fuel flexibility allow applications ranging from compact sub-kilowatt portable/mobile power units to stationary MW-scale power plants. This poster will discuss technology development activities which address major opportunities in direct coal conversion:

### References:

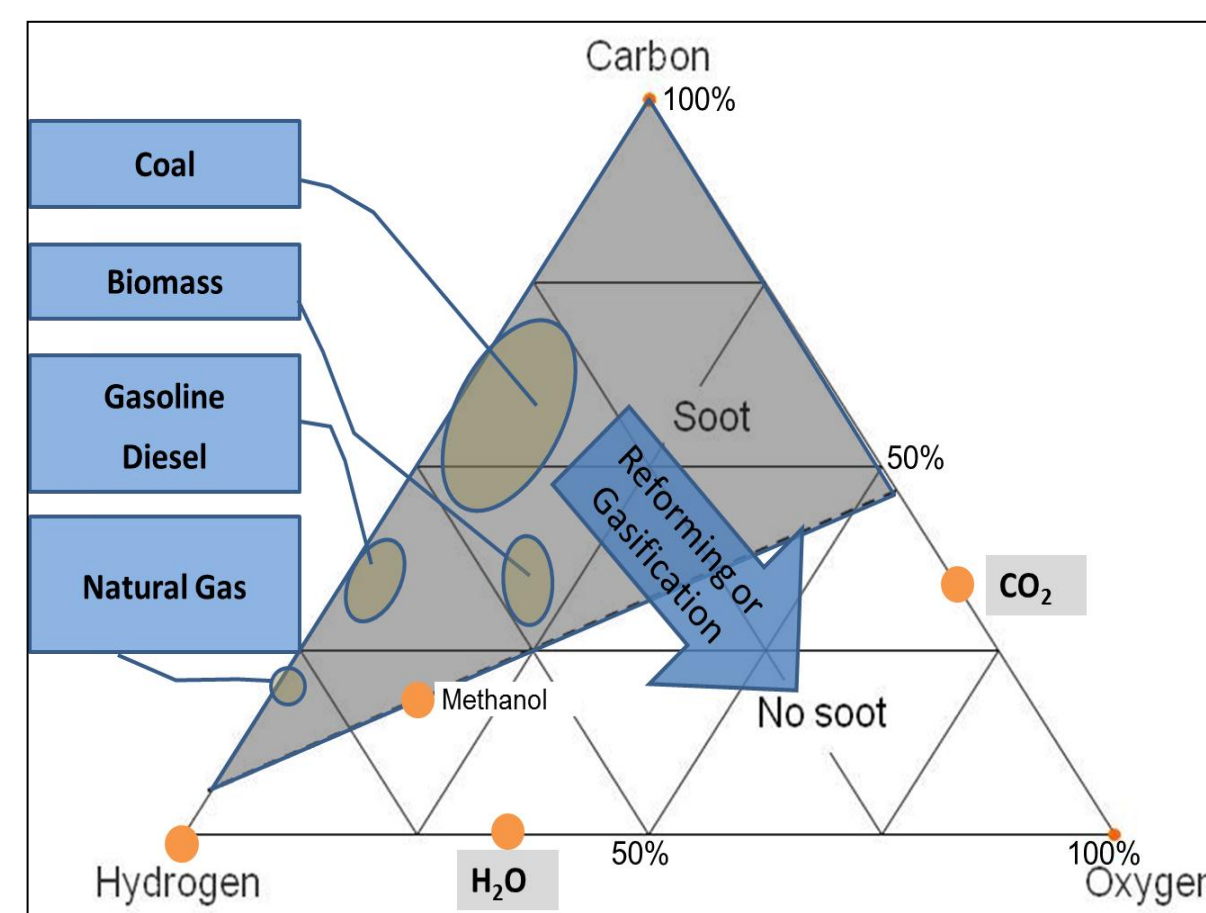
1. Advancement in Liquid Tin Anode - Solid Oxide Fuel Cell Technology Thomas Tao, et al, ECS Trans. 12 (1), 681 (2008).
2. Anode Polarization in Liquid Tin Anode Solid Oxide Fuel Cell Thomas Tao, et al, ECS Trans. 7 (1), 1389 (2007).
3. Liquid Tin Anode Solid Oxide Fuel Cell for Direct Carbonaceous Fuel Conversion Thomas Tao, et al, ECS Trans. 5 (1), 463 (2007).
4. Performance of the Gen 3.1 Liquid Tin Anode SOFC On Direct JP-8 Fuel, M. T. Koslowske et al., Advances in Solid Oxide Fuel Cells IV, Ceramic Engineering and Science Proceedings, Volume 29, Issue 5, 2008, pg. 39.
5. Program on Technology Innovation: Systems Assessment of Direct Carbon Fuel Cells Technology, EPRI report 1016170, April 2008.

## CELL OPERATION

- Tubular cell geometry with internal cathode →
- Anode is liquid tin contained by porous ceramic which allows fuel transport to tin surface
- Sn to SnO<sub>x</sub> redox transport facilitates operation



Direct Fuel Conversion of simple and complex fuels, such as biomass, JP-8 and coal is possible in both the soot forming and non-sooting regimes.



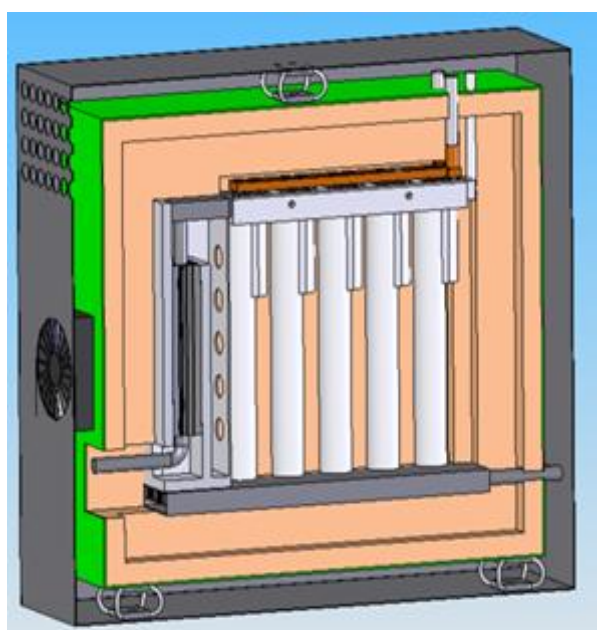
## CELL, STACK and SYSTEM DEVELOPMENT:

Parallel efforts for logistic fuel and biomass funded by DOD and NSF allow Liquid Tin Anode SOFC technologies mature.

5-Cell panel

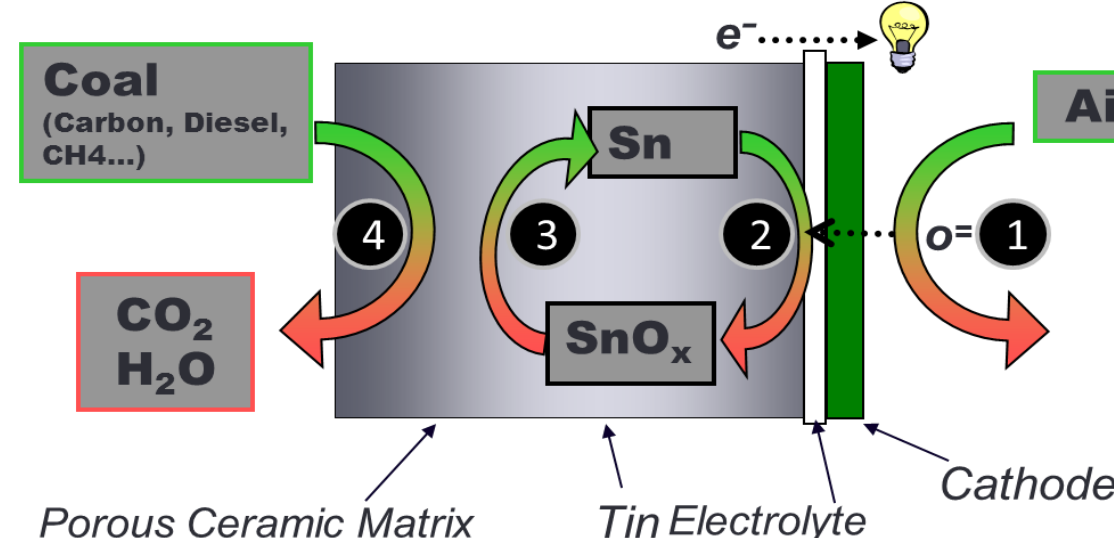
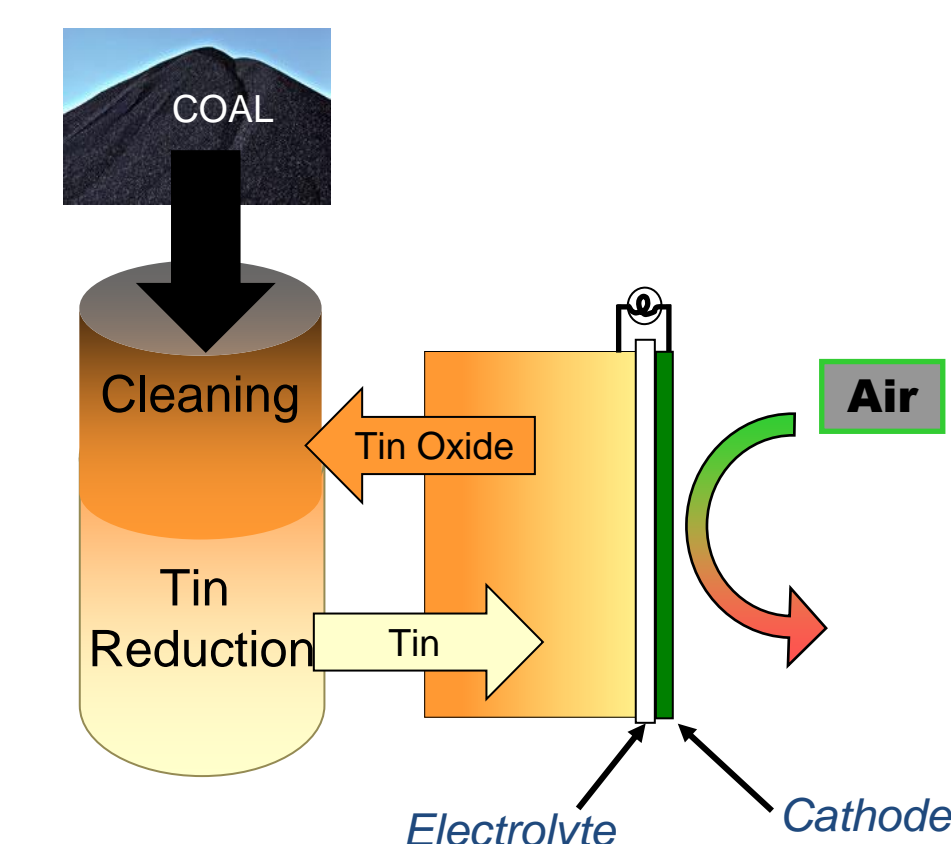


60 Watt JP-8 Battery Charger



## Electrochemical Looping

Based on Coal-Tin Reactor  
DE-NT0004111, DE-ER85006

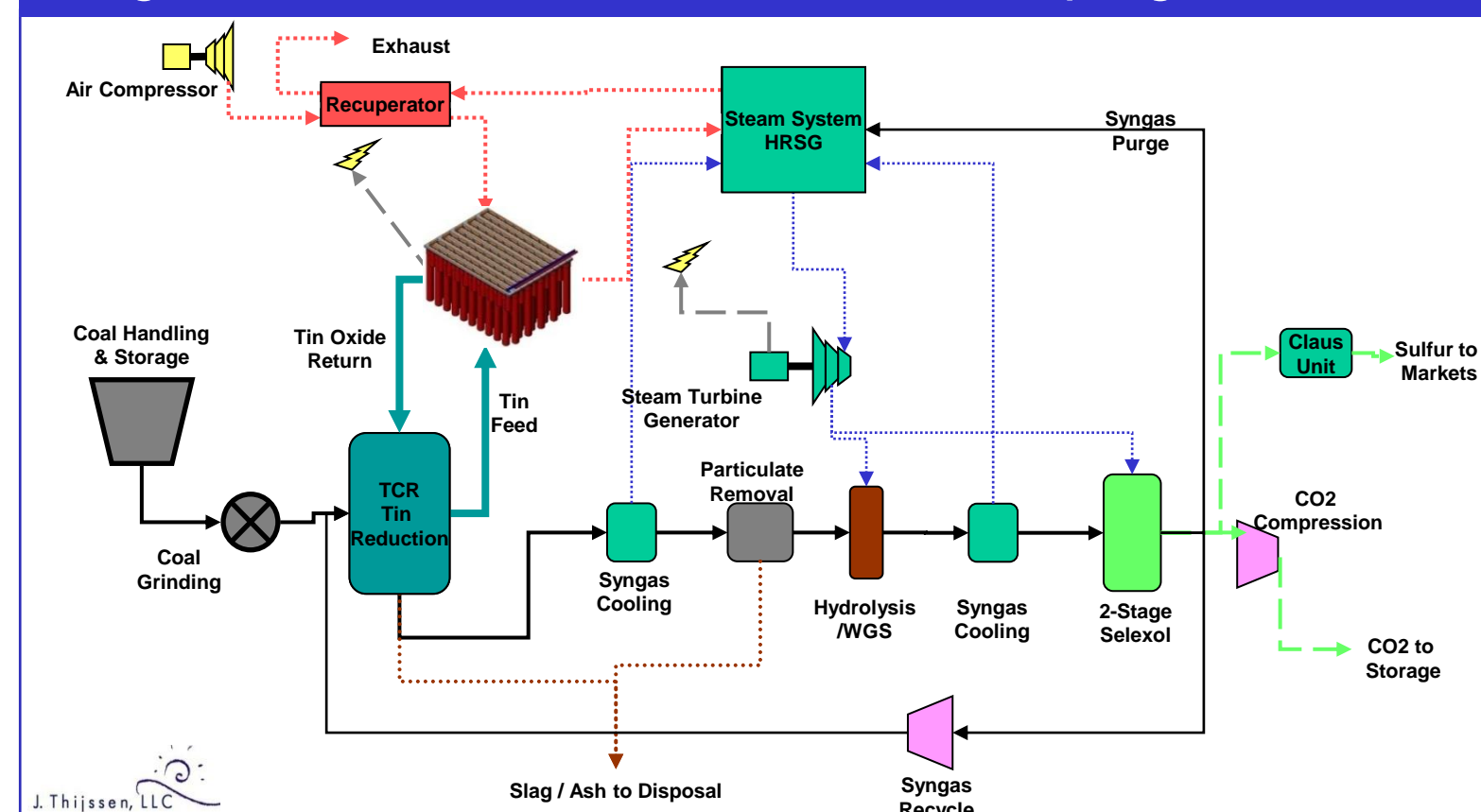


- 1 Oxygen ions extracted from air by cathode and cross the electrolyte
- 2 Ions react with tin, releasing electrons and forming tin oxide
- 3 Tin oxide is independently reduced back to tin by reaction with fuel
- 4 Fuel directly contacts tin

## Most thoroughly analyzed concept to-date

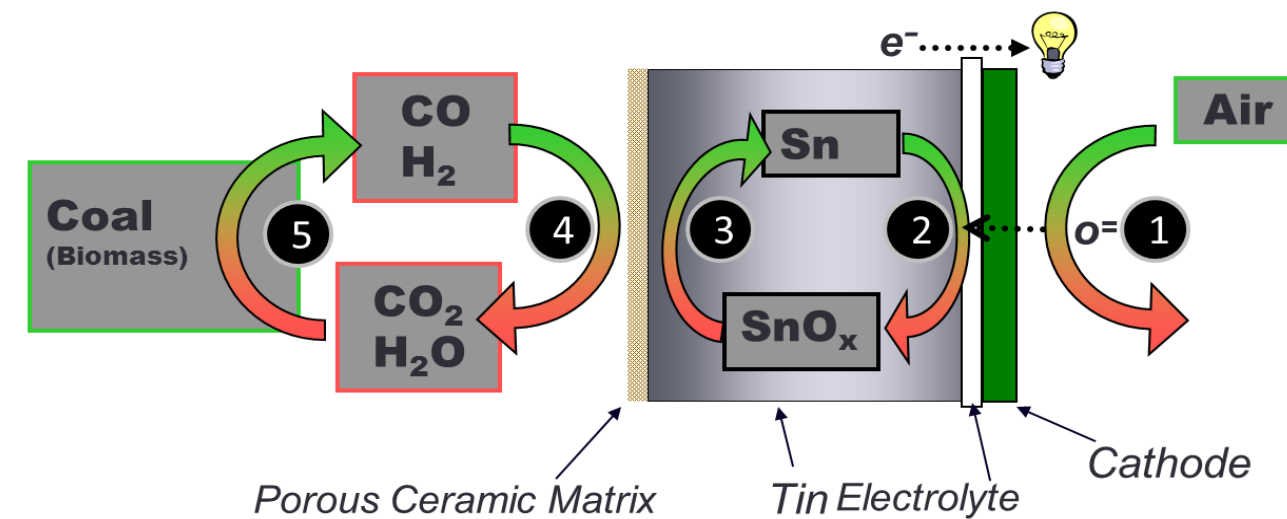
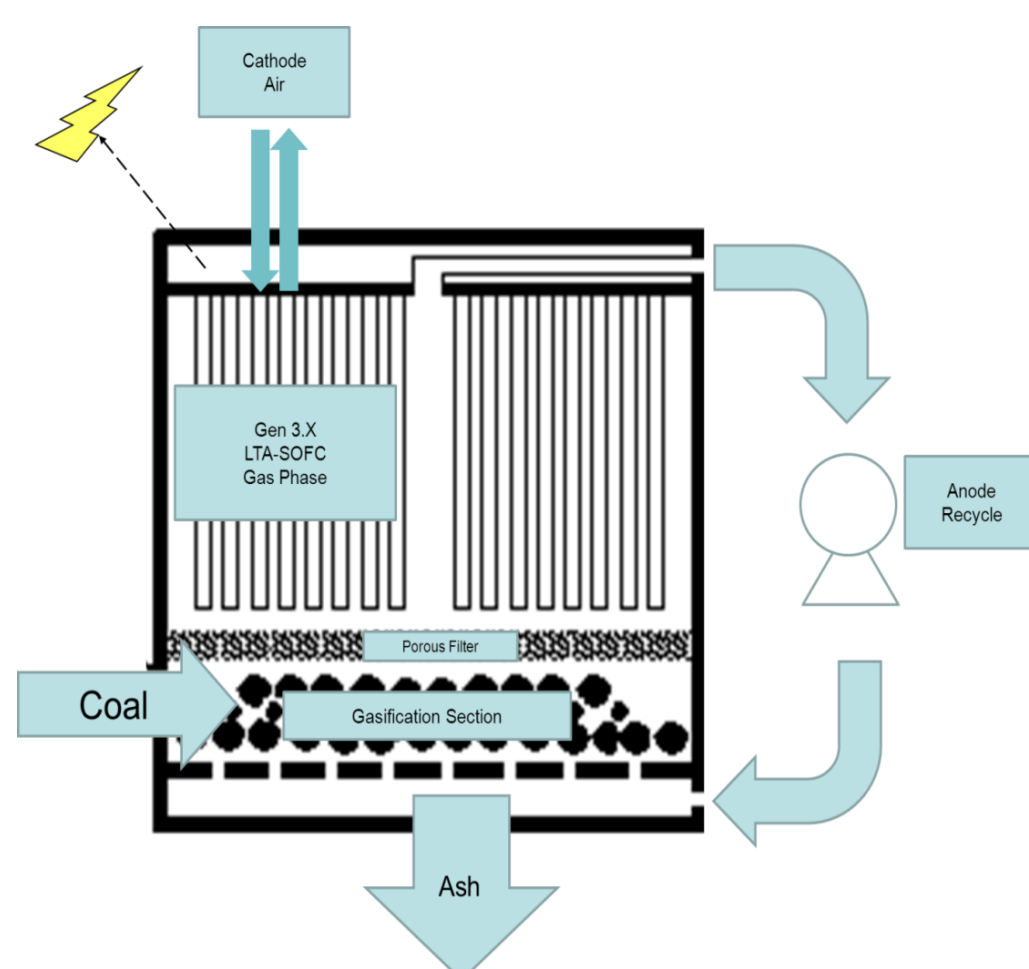
- 63% System efficiency with CO<sub>2</sub> capture and compression
- System CAPEX: \$1400 – 2400/kW (similar to IGCF)
- Near 100% CO<sub>2</sub> capture
- Tin provides separation of ash/impurities
- Requires development of Tin Coal Reactor similar to liquid metal gasifiers
- High tin recirculation rate required to meet O<sub>2</sub> transport requirements.
- Tin anode requires electric current break

## High Level PFD of Electro Chem Looping with CCS



## Insitu Gasifier

Based on Portable Power Cell  
DE-ER95350S10

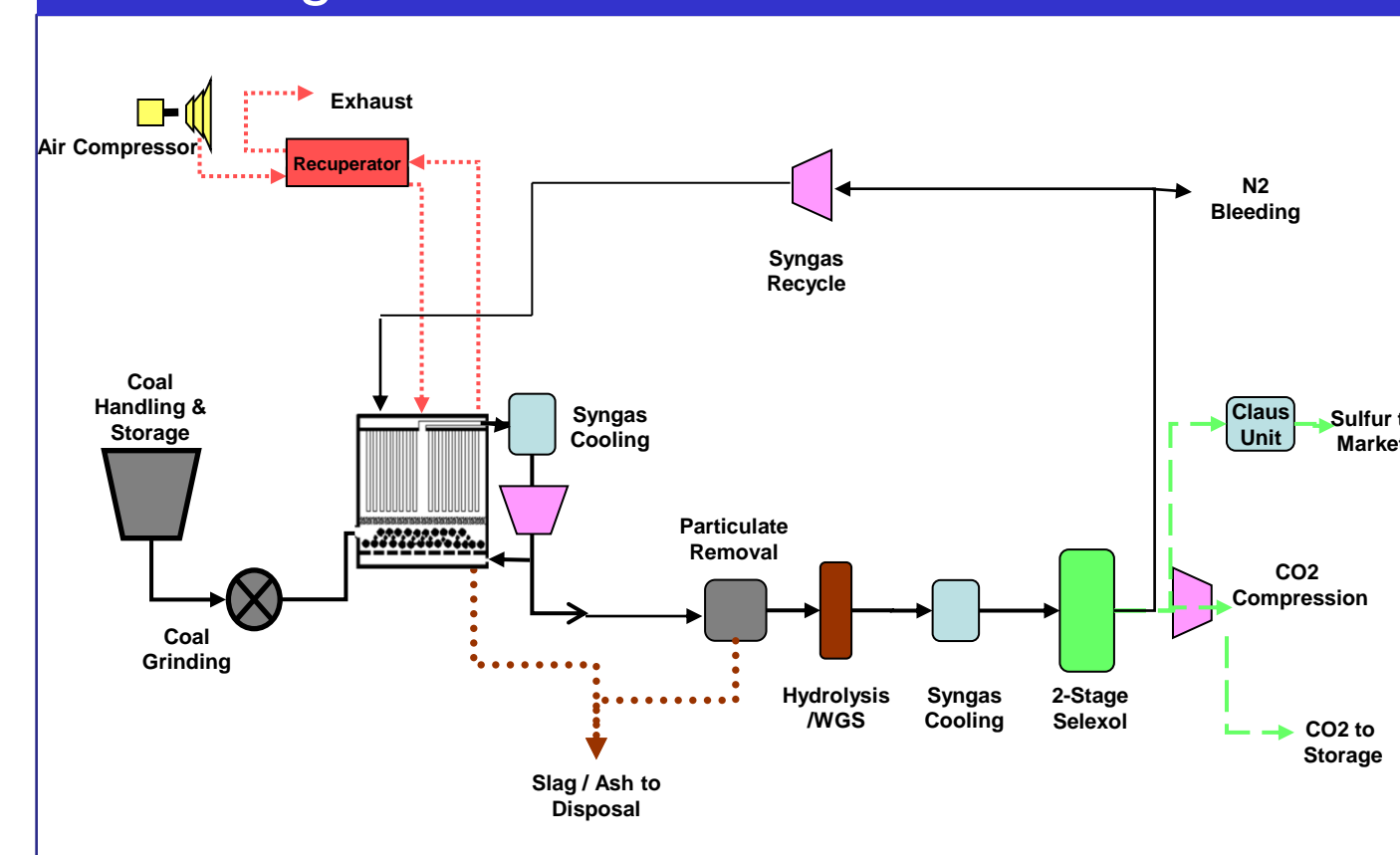


- 1 Oxygen ions extracted from air by cathode and cross the electrolyte
- 2 Ions react with tin, releasing electrons and forming tin oxide
- 3 Tin oxide is independently reduced back to tin by reaction with fuel
- 4 Tin-fuel interaction can occur inside tin or across a porous ceramic membrane
- 5 Coal or other solid fuel is gasified insitu by the cell reaction products

## Uses cells with porous separator, like existing CellTech Gen 3 design

- No direct contact between tin anode and solid fuel.
- Gasification is driven by CO<sub>2</sub> and H<sub>2</sub>O produced by cells (no Oxy plant required).
- Isolated anodes allow cell voltage build up.
- Ash, tar and carbon clogging of separator could be an issue.
- Volatile metal oxides in coal impact on cells unknown.
- Could test concept with Gen 3.1 cells and lab gasifier.
- Cathode air flow may increase to remove cell heat load.

## High Level of PFD of Insitu Gasifier



## Direct Coal Summary

### OPPORTUNITY:

- Previously reported studies have projected that LTA-SOFC can achieve 63% efficiency in a large direct coal power plant with carbon capture<sup>5</sup>.

### KEY RISKS:

- Cell component degradation during operation on very high (ca. 4%) sulfur levels.
- Impact of coal ash creation and residual contaminants on long term material stability.

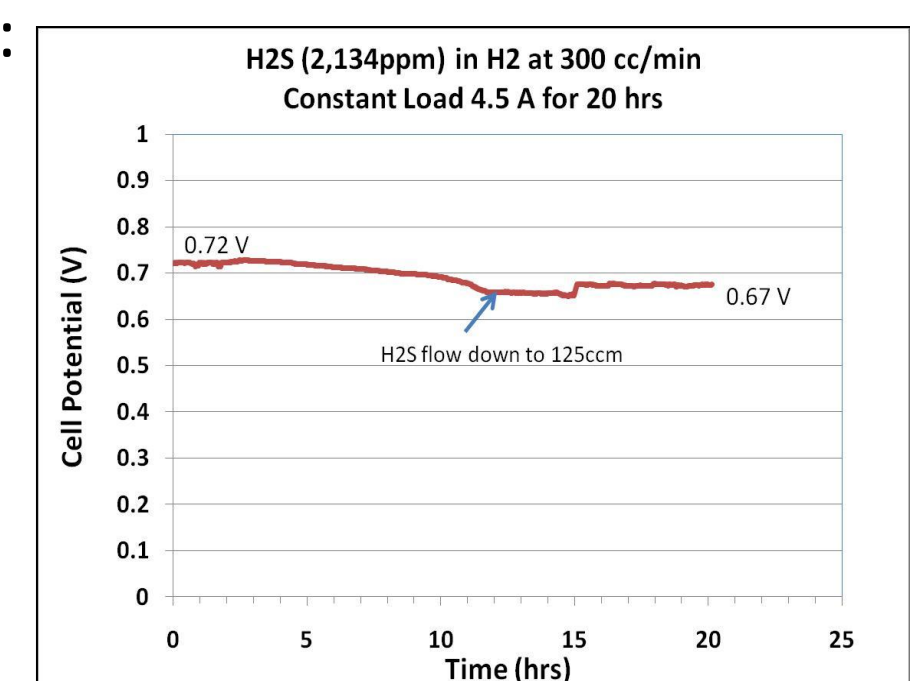
### PROGRAM OBJECTIVES:

The focus of the coal effort is to identify cell durability liabilities in coal contaminant environments through long-term testing of single cell test articles. Cell testing will be conducted using both a tin bath reactor and internal gasification methods.

### Internal Gasification Test:

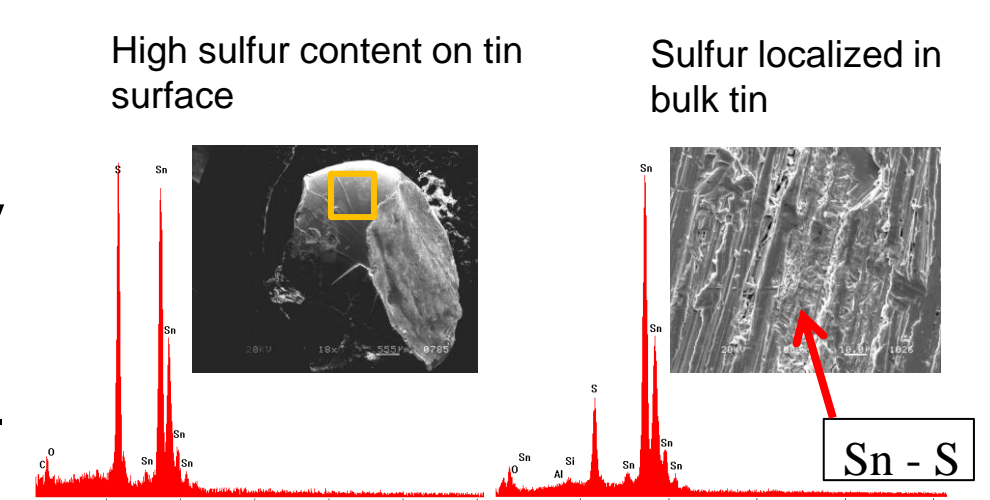
Determine the effect of high sulfur content on LTA-SOFC operation.

- Simulate a high sulfur coal environment, Illinois #6 coal (DECS-24) - 4.8 wt% sulfur, using H<sub>2</sub>S (2,134ppm, 3.5wt%) in H<sub>2</sub>.
- **Goal: 20 hr operation**



### Results:

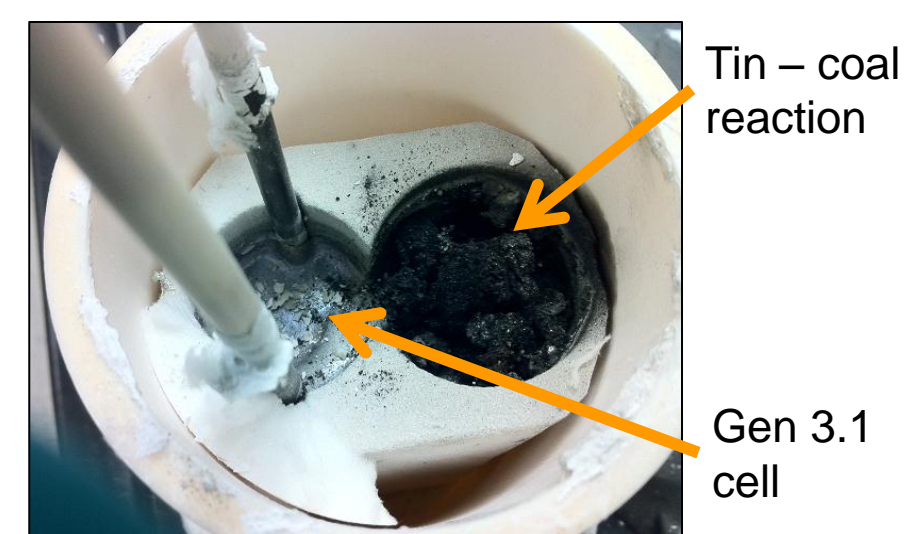
- Completed 20 hour test
- Total Sulfur = 1.1 gram
- Fuel delivery inconsistency contributed to decrease in performance.
- Cell Stable for last 5 hours.
- Sulfur remains on / in tin



### Tin Bath Reactor Test:

Determine the effect of ash on direct tin coal interaction.

- Illinois #6 coal (DECS-24) with 4.8 wt% sulfur was fed onto tin surface for 24 hours.



### Results:

**Average Power** 0.97 Watts  
**Runtime at load** 1412.00 Minutes  
**Total Coal Input (Illinois #6)** 20.36 grams  
**Average Flow Rate** 18.36 mg/min  
**LHV Illinois #6** 28453.96 J/g

