



Exposure Limits of Higher Hydrocarbons for SOFC SECA 2010 Workshop NETL Fuel Cell Group July 29, 2010

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Overview

- NETL FC Group Background
- Discussion of Coal Syngas Exposure Results
 - Individual contaminants testing protocol
 - Mercury
 - Naphthalene, Benzene
 - PEG/DME
- Conclusions
- FY11 planned research



NETL Fuel Cells Group

• Federal activity

- 5 federal research projects
 - Anode contaminates and liquid metal anode
 - Cathode infiltration
 - Hybrid gas turbine / FC operation and controls
 - GC-ICP/MS
- 4 federal researchers and 5 post-doctoral research associates

• University activity

- 5 university research projects (CMU and WVU)
 - Cathode crystallographic evolution
 - Cathode infiltration and microstructural modeling (2 projects)
 - Fundamentals of oxygen reduction reaction (ORR)
 - Hybrid controls

Contract labor support

- Research management and support activities

Contaminants - Problem Outline

- Analyze the interaction of trace materials in direct syngas with the solid oxide fuel cell (SOFC) anode
- Thermodynamic analysis
 - Elements present
 - As, Cd, Hg, Pb, Sb, Se
 - Elements interacting
 - As, Sb
 - Stable secondary phases
- Laboratory results
 - As, P, S, Se



Trace Material Concentration

A. Martinez, K. Gerdes, R. Gemmen, and J. Poston, Journal of Power Sources, 195, (2010) p5206–12.

• Additionally interested in higher hydrocarbons and process materials (benzene, naphthalene, ethylene, Selexol)

Contaminants - Background

- Trace material can attack the anode by any (or all) of three primary degradation mechanism classes
- <u>Class I</u> Physical blocking of fuel feed pores
 - Carbon whiskers (graphite), incombustible materials (Si)
- <u>Class II</u> Surface adsorption
 - Deactivation of catalytic sites (S, Se)

J. Hansen, "Correlating Sulfur Poisoning of SOFC Nickel Anodes by a Temkin Isotherm" Electrochem. Solid-State Lett., Volume 11, Issue 10, pp. B178-B180 (2008)

- <u>Class III</u> Chemical reaction
 - Class IIIA Formation of secondary metal phases (P, As, Sb)
 - Class IIIB Formation of metal solutions (C)



HHC Contaminants - Background

- Standard cell is purchased commercially
 - Ni/YSZ anode; YSZ electrolyte; LSM cathode
- Cell is exposed to precisely controlled mass of trace material
 - Benzene @ 15 and 150 ppm
 - Naphthalene @ 100 and 500 ppm
 - PEG/DME @ 1 and 3.5 ppm
 - Mercury @ 1 and 10 ppm
 * Exposure significantly exceeds gasifier effluent concentration
- Electrochemical reaction monitored
 - Temporal voltage, EIS
- Post-operational microscopy
 - SEM/EBSD, XPS, TEM



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M.F. Singleton and P. Nash

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Test Parameters

- Cathode Air @ 1000 mL/min
- Anode:
 - Hydrogen:
 - Carbon monoxide:
 - H₂O:
 - Carbon dioxide:
 - Nitrogen:

- 87.3 mL/min (29.1%)
- 85.8 mL/min (28.6%)
- 81.8 mL/min (27.3%)
- 36.0 mL/min (12.0%)
- 9.6 mL/min (3.2%)

- Temperature 800 C
- Operating condition 250 mA/cm²

Mercury Overpotential



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Mercury Data (1 ppm data/equation shown)

SEM - Mercury



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Mercury Exposure (1 ppm)

Naphthalene overpotential



Naphthalene Data (500 ppm data/equation shown)

Naphthalene impedance



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Naphthalene Impedance - 500 ppm

SEM – Naphthalene



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Naphthalene SEM Image - 500 ppm

XPS - Naphthalene

• Naphthalene exposed samples showed minimal carbon



TEM imaging – Naphthalene

- Titan 80-300 (aberration corrected HR-STEM)
 - Accelerating V=300 kV
 - Resolution = 0.07 nm
- The beam size is substantially smaller than the particle (<1 nm)



• Five elements within inclusion: Ni, Al, Si, C, and O



TEM/EDS – Naphthalene

- JEOL 2100F Cs-Corrected STEM (U Michigan, a system which is comparable to Titan system)
- C distributes evenly in the Ni grain.
 - Result is consistent with Titan data.
- C observed everywhere through the 500 ppm sample.
 - Sample is cleaned using ion-mill but C remains.
 - New sample prepared and similar result acheived.
- <u>Preliminary</u> confirmation that C is major solid solution specie.

Image





Benzene overpotential



Benzene Data (150 ppm data/equation shown)

Benzene impedance



Benzene Impedance - 15 ppm

PEG/DME Overpotential



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Discussion – Analysis Method

- Empirical degradation model assumptions
 - Initial degradation is well modeled by exponential decay
 - Long term (2000 + hours) cell degradation is linear



Exposure limit - Naphthalene

- First order with respect to concentration in range of 100-500 ppm
- Exposure limit depends on
 - Assumed baseline cell degradation rate (1%, 0.5%, 0.25% / 1000 hours)
 - Acceptable final operating voltage



1.0% / 1000 h

0.50% / 1000 h

0.25% / 1000 h



Exposure limit - Benzene

- Zero order with respect to concentration in range of 15-150 ppm
 - Degradation rate too similar b/n two concentrations to extrapolate limit



Conclusions

• Naphthalene

- SOFC exposed to naphthalene at 150 and 500 ppm demonstrated obvious performance degradation
 - Rates greater than those for benzene.
- After 40,000 h, the SOFC will produce usable potential of :
 - 0.7 V at 110 ppm @ base cell degr rate of 0.25% per 1000 h.
 - 0.6 V at 1200 ppm @ base cell degr rate of 0.25% per 1000 h.
 - **0.6 V at 360 ppm** @ base cell degr rate of 0.50% per 1000 h



Conclusions

• Mercury

- SOFC exposed to mercury at 1 and 10 ppm shows no performance degradation
- Results agree with thermodynamic analyses and literature
- Mercury cleanup is not required for fuel cell

• Benzene

- SOFC exposed to benzene at 15 and 150 ppm showed noticeable performance degradation.
- Cleanup to less than 150 ppm is recommended



Continued HHC Exposure testing

- Complete tests on PGE/DME (3.5 ppm repeat)
- Initiate Ethylene tests at 100-1000 ppm
 - Predict exposure limitations
- Carefully monitor grain growth
 - Record sufficient microstructure observations to ensure statistical relevance
- Spot check literature results for H₂Se and AsH₄



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