



# **Thermal Management in a Coal-Based SOFC Hybrid Through Numerical Simulation**

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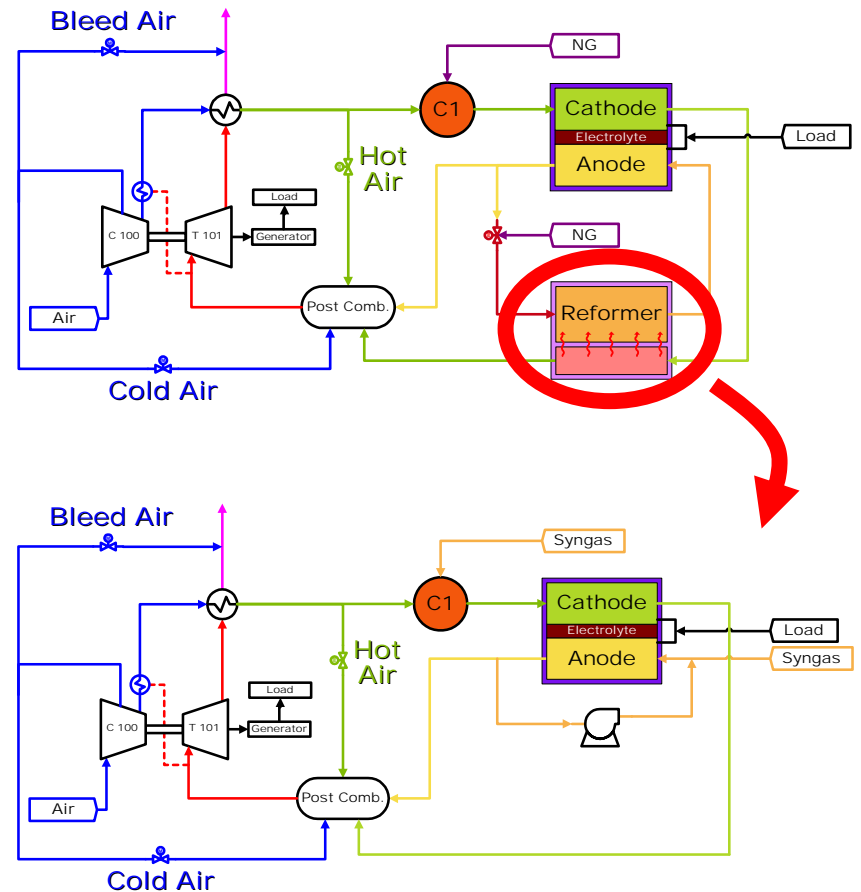
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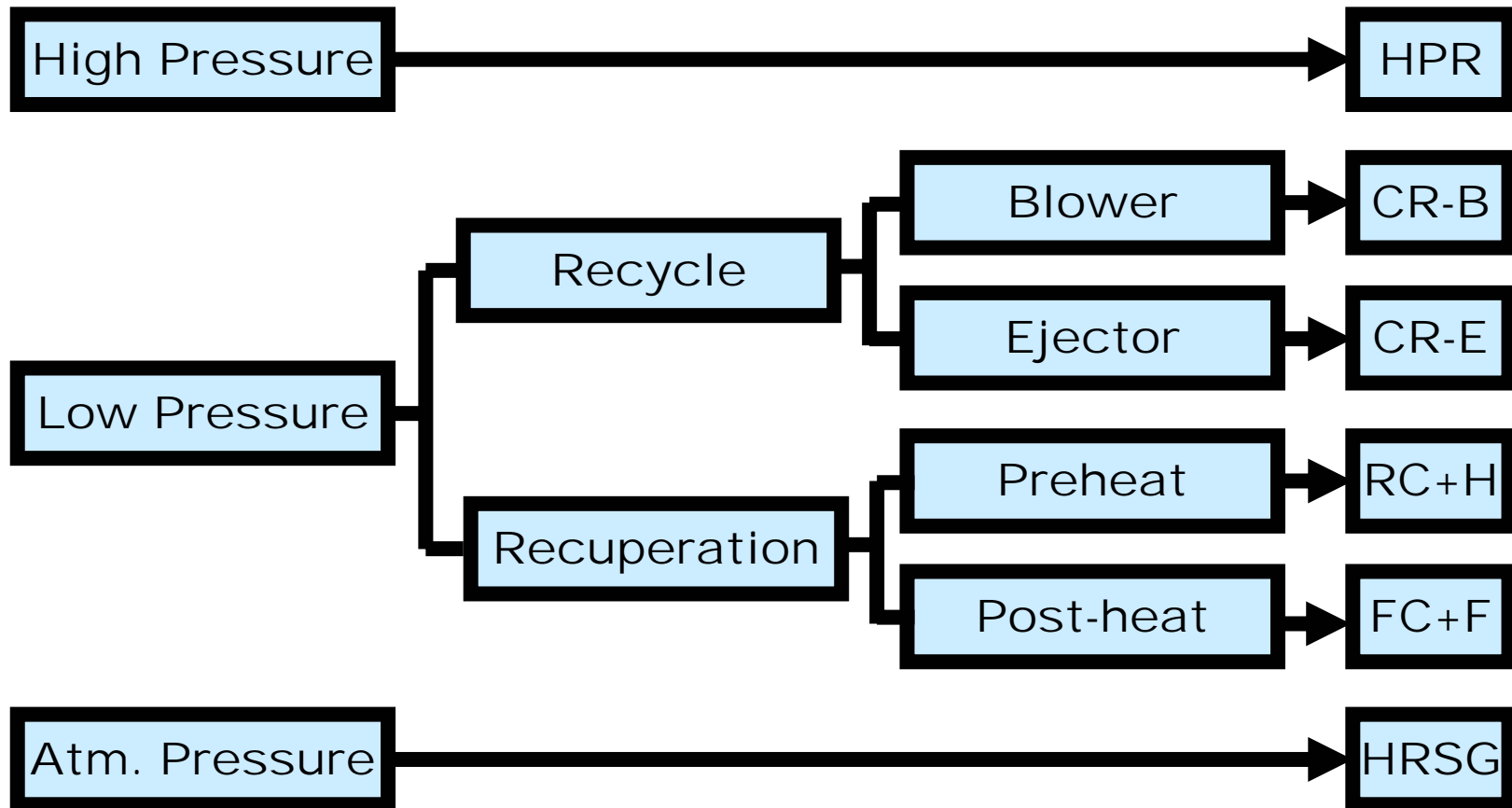
# Objective

Provide a relative comparison of methods commonly considered for thermal management in coal-based fuel cell turbine systems

- Previous work based on NG
- Higher air mass flows required
- Fix fuel cell load in each case
- Fuel varied to get target fuel cell power
- Turbine load based on available heat
- Compressor airflow to target  $\Delta T=150^{\circ}\text{C}$
- Efficiency based on HHV syngas
- Power density evaluated for each case
- Lumped fuel cell model for ASPEN
- 1D fuel cell model for performance



# Configurations Studied



# Fuel Cell Parameters

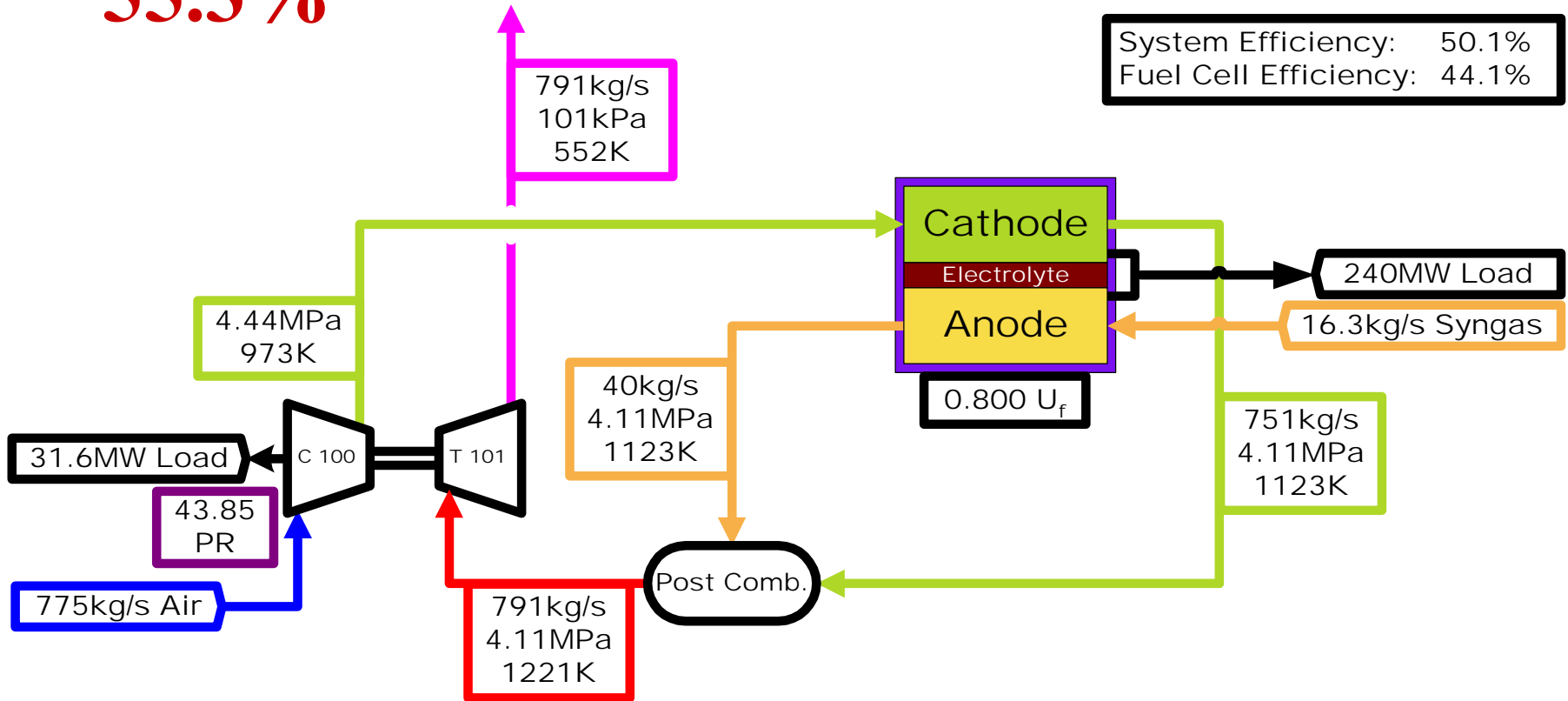
<b>Parameter</b>	<b>Value</b>
Initial Cell Voltage at 101.325kPa	0.7V
Initial Current Density at 101.325kPa	500mA/cm <sup>2</sup>
Stack Power	240MW
Stack Fuel Utilization	80%
Cell Temperature	1123K
Fuel Cell Inlet Temperature	973K
Fuel Cell $\Delta T$	150K

# Turbine Parameters

<b>Parameter</b>	<b>Value</b>
Compressor Isentropic Efficiency	80%
Turbine Isentropic Efficiency	90%
Gas Turbine Mechanical Efficiency	98%
Generator Efficiency	97%
Inverter Efficiency	98%
Fuel Cell Pressure Drop	2.5%
Combustor and Manifolds Pressure Drop	5.0%
Recuperator Pressure Drop	2.5%
Recuperator Effectiveness	89%

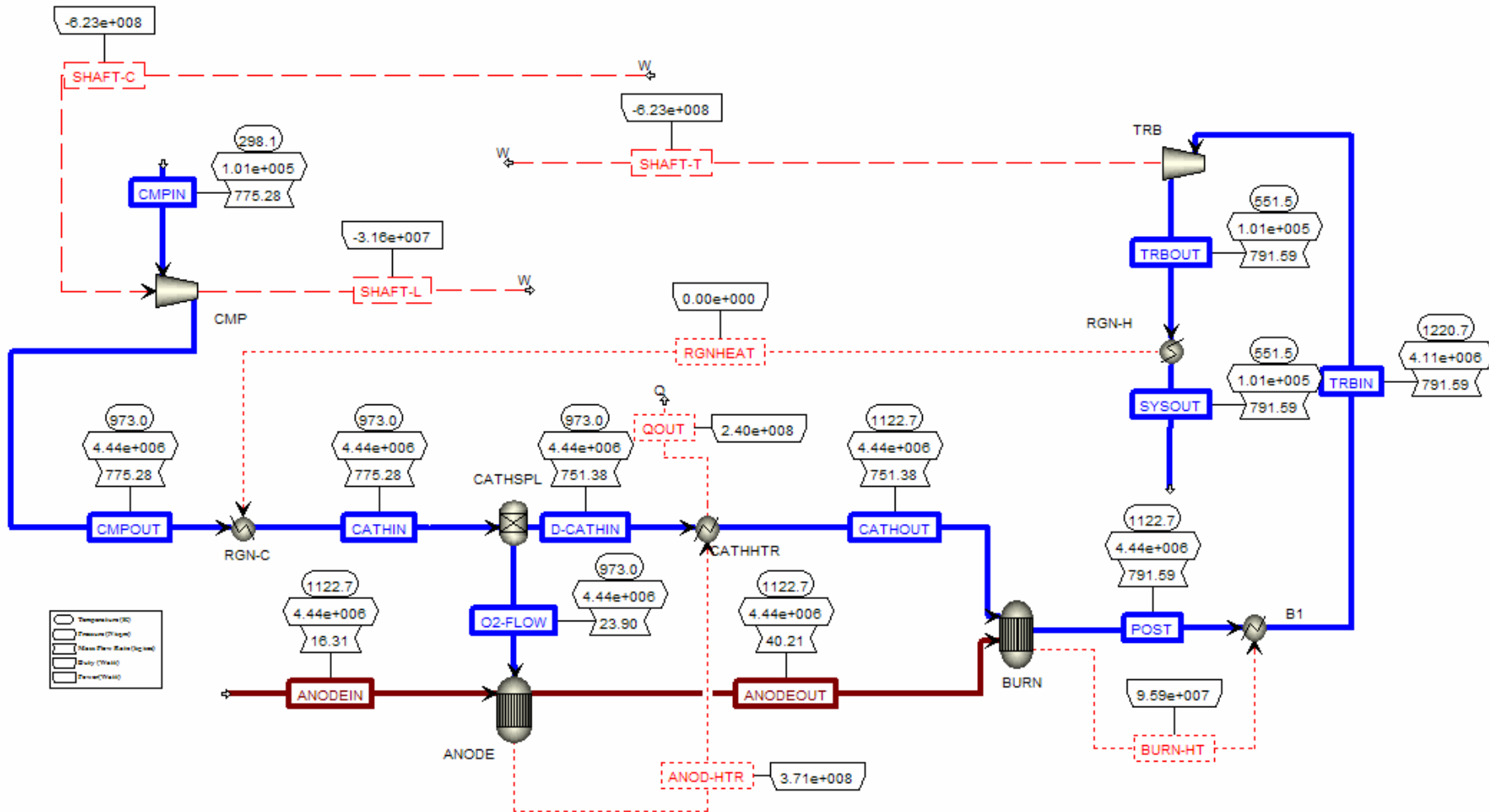
# Heat of Compression Configuration

**HPR**  
**55.3%**



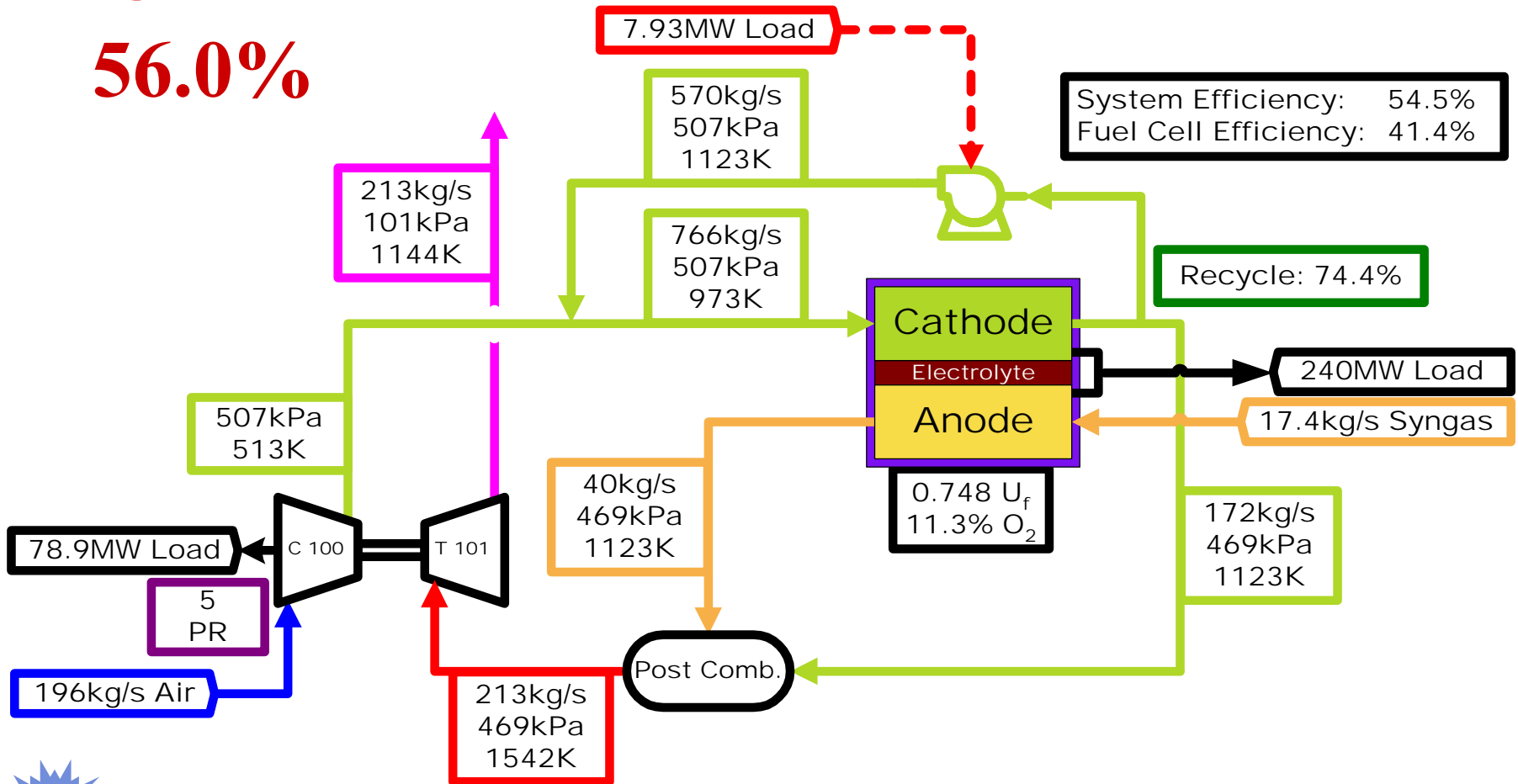
# Heat of Compression Configuration

- PR = 43.85 used to get target cathode  $T_{in}$  of 700°C (973K)
- Fuel flow used to get a FC power of 240MW
- Compressor Flow used to get 150°C  $\Delta T$  across FC
- 44.1% FC Eff. (HHV)
- 50.0% System Eff (HHV)
- $\Delta P = 7.5\%$



# Cathode Recycle Configuration with Blower

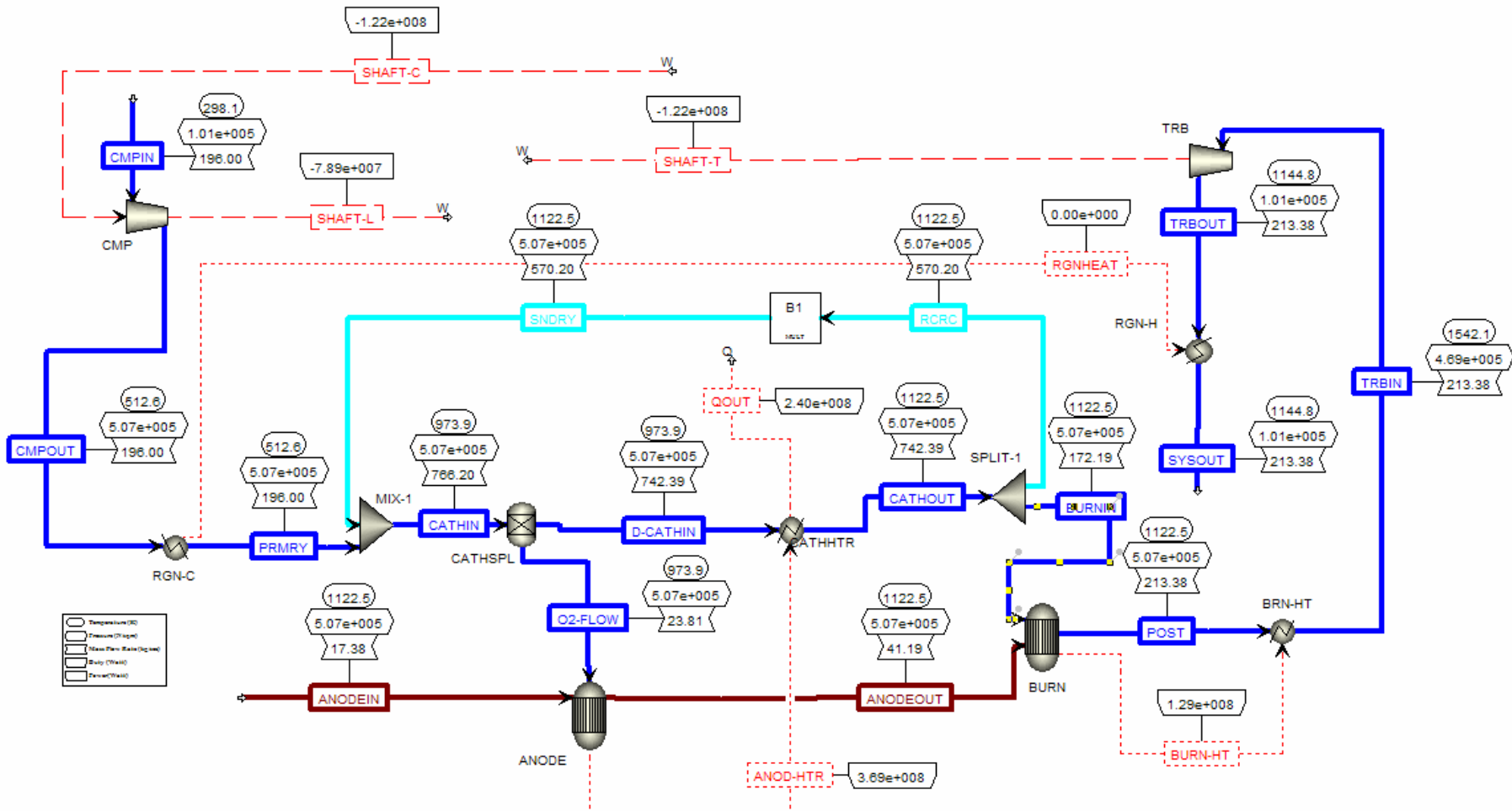
**CR-B**  
**56.0%**





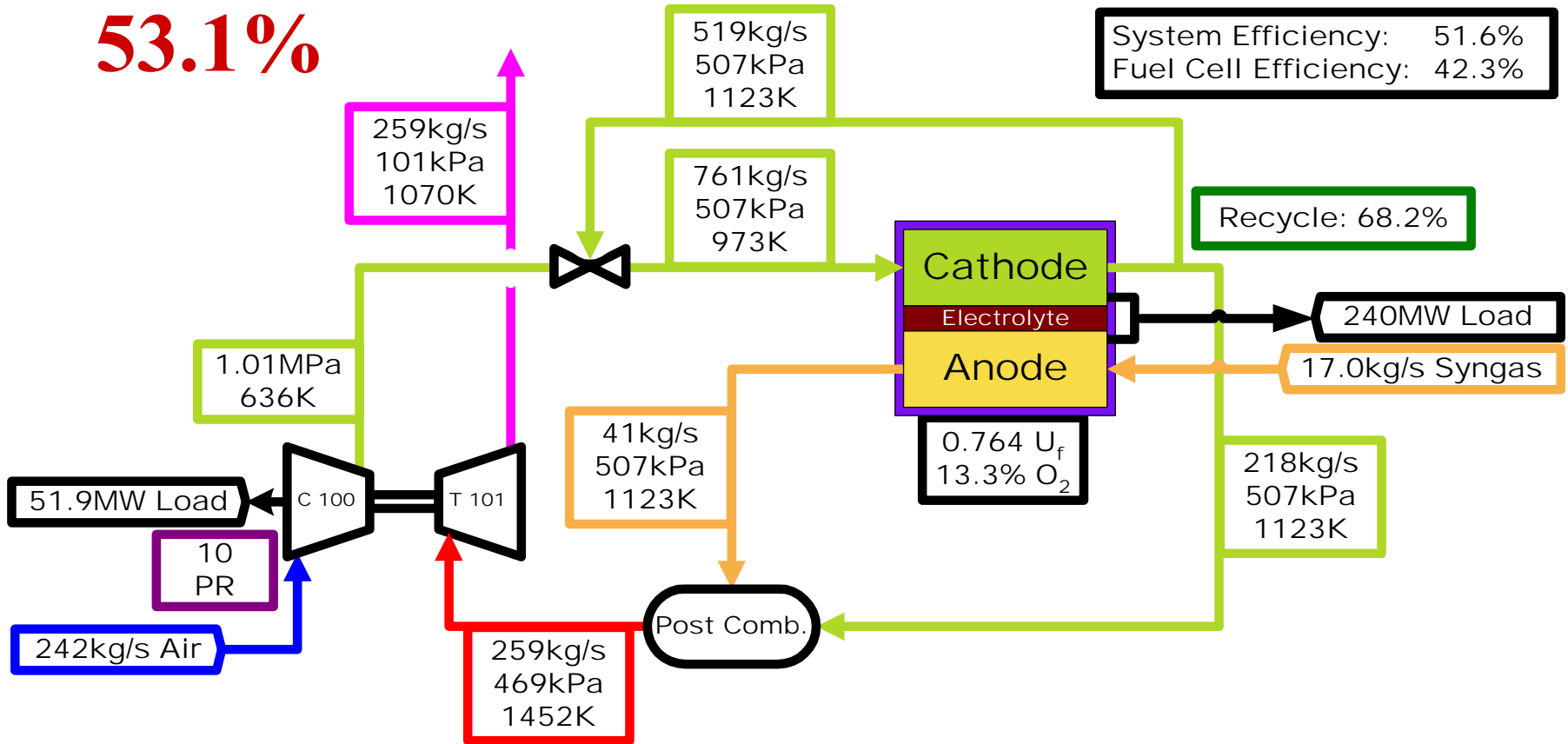
# Cathode Recycle Configuration with Blower

- Recycle ratio of 74.4% to get cathode  $T_{in}$  of 700°C (973K)
- Fuel flow used to get a FC power of 240MW
- Compressor Flow used to get 150°C  $\Delta T$  across FC
- 41.4% FC Eff.
- 54.5% System Eff.
- $\Delta P = 7.5\%$



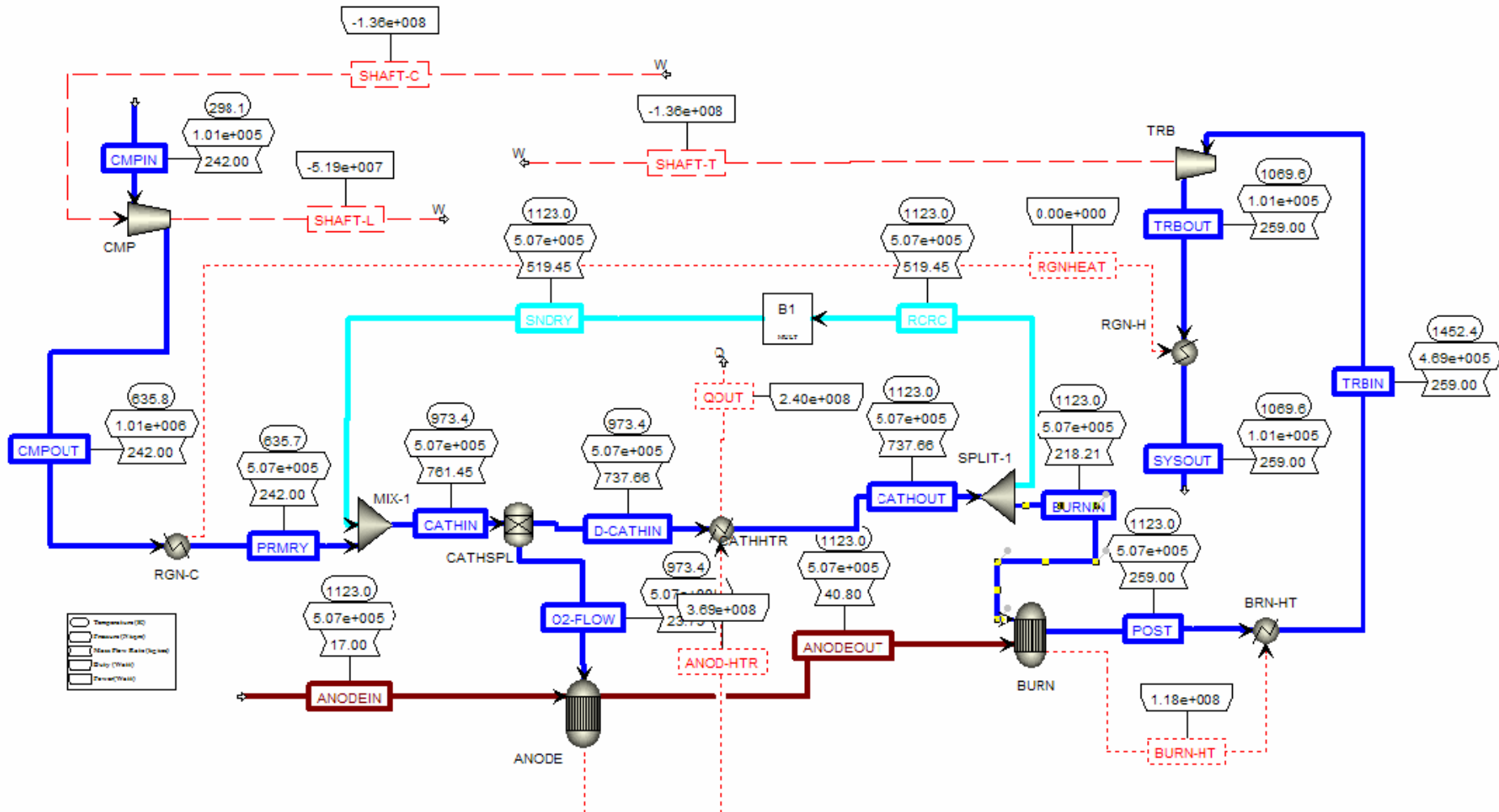
# Cathode Recycle Configuration with Ejector

**CR-E**  
**53.1%**



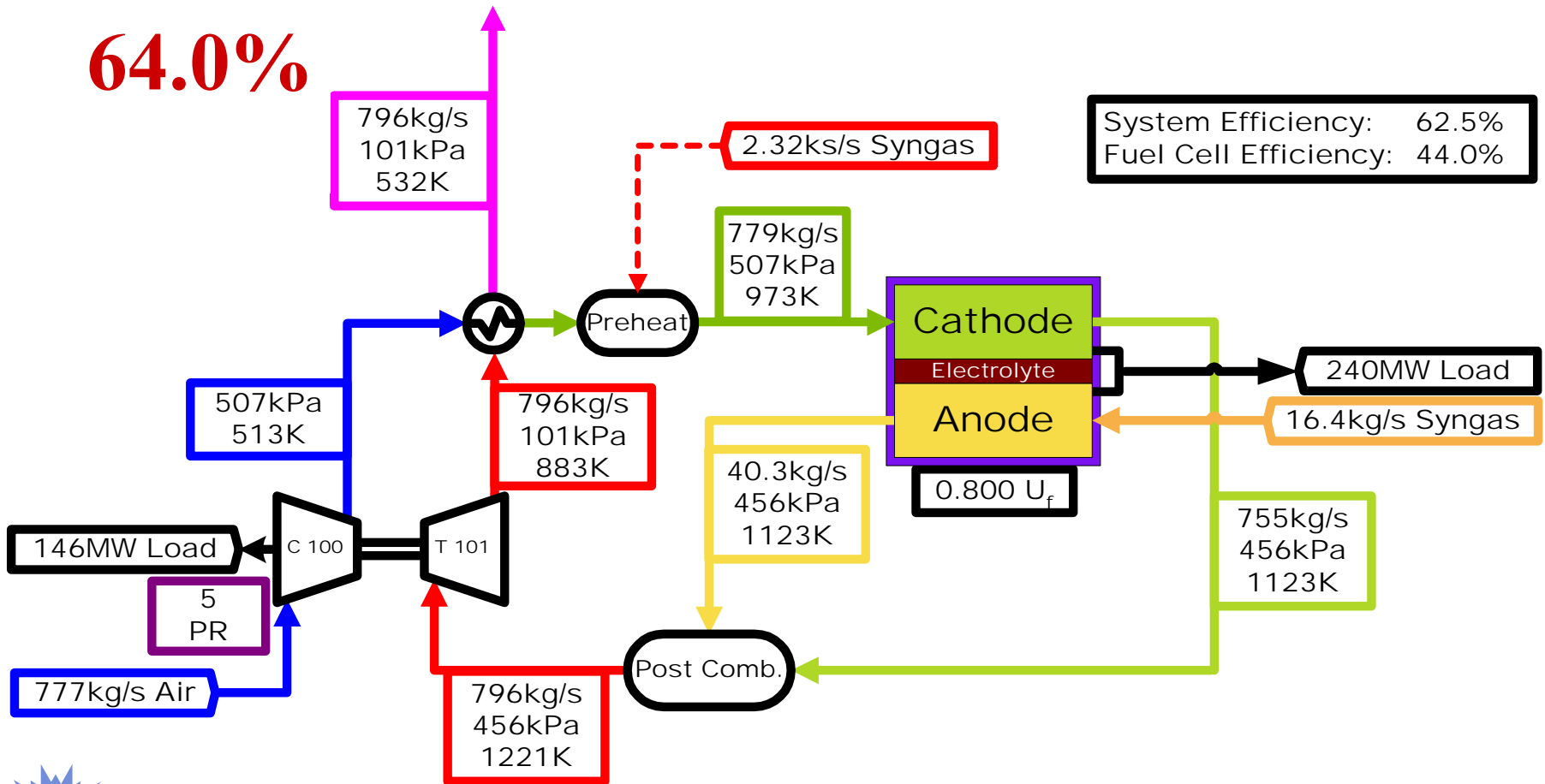
# Cathode Recycle Configuration with Ejector

- Recycle ratio of 70.3% to get cathode  $T_{in}$  of  $700^{\circ}\text{C}$  (973K)
- Fuel flow used to get a FC power of 240MW
- Compressor Flow used to get  $150^{\circ}\text{C}$   $\Delta T$  across FC
- 51.6% FC Eff.
- 42.3% System Eff.
- $\Delta P = 53.8\%$



# Recuperated Configuration with Pre-Heat

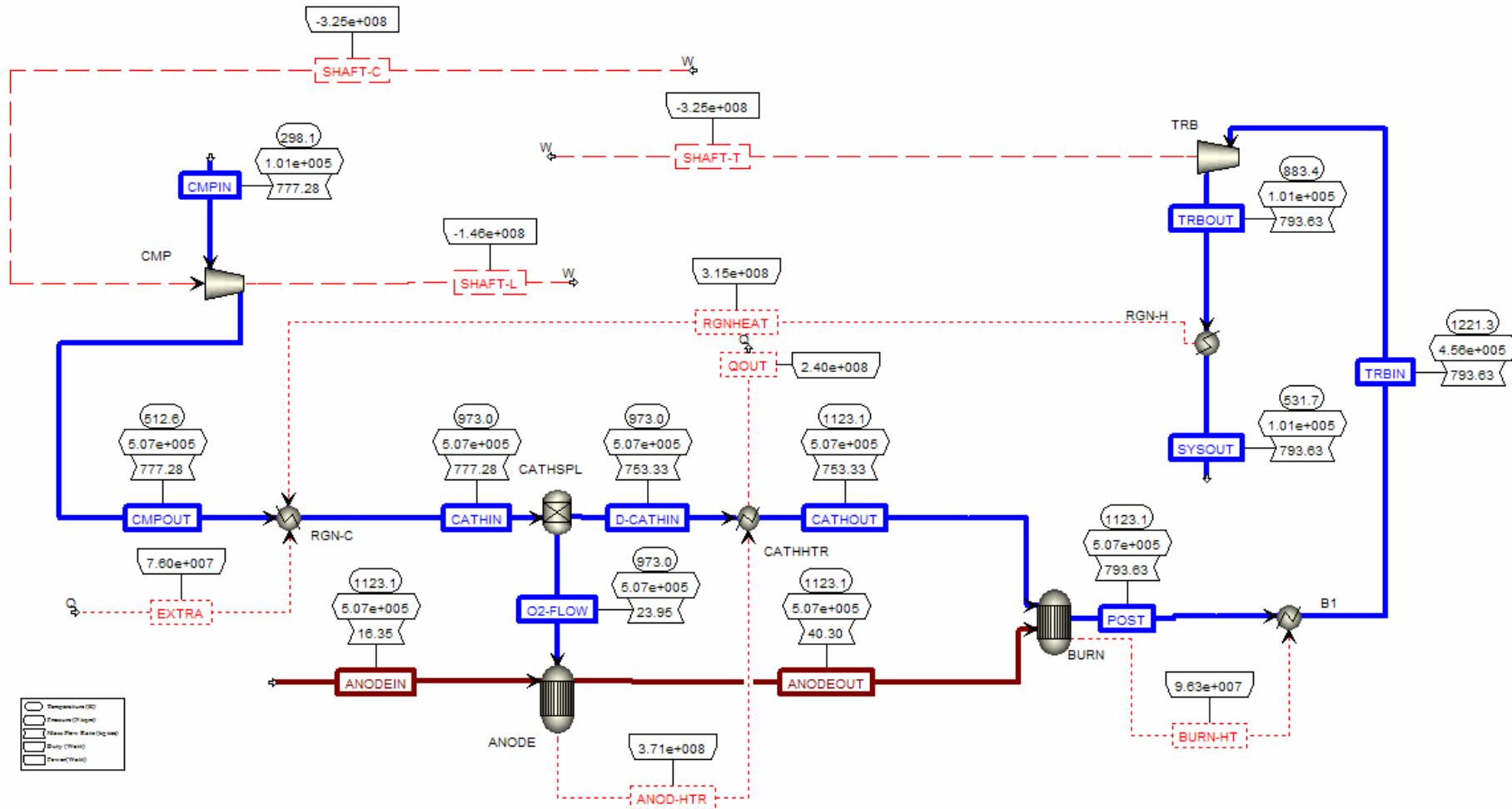
**RC+H**  
**64.0%**



# Recuperated Configuration with Pre-Heat

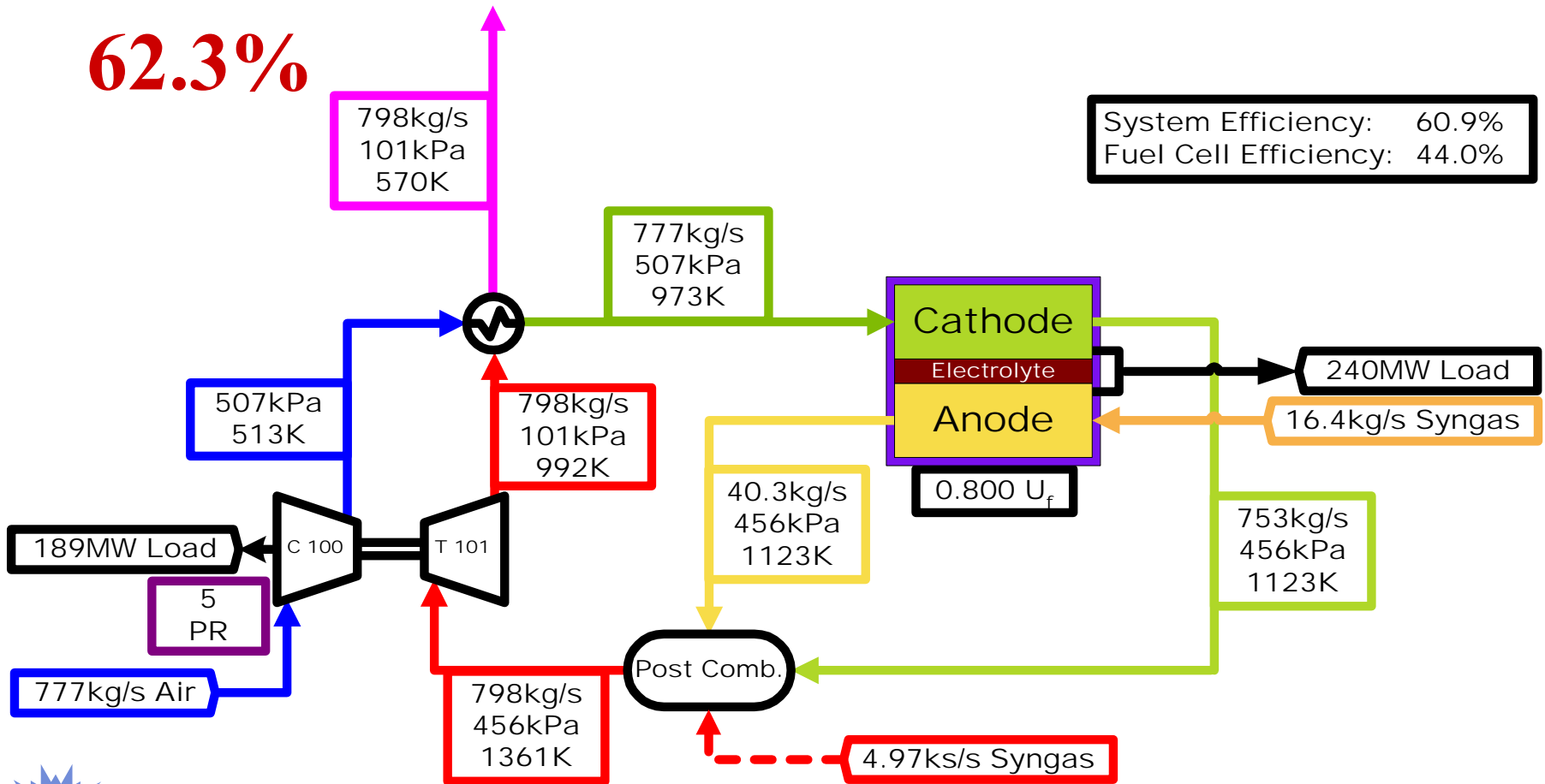
- Pre-heat used to get target cathode  $T_{in}$  of  $700^{\circ}\text{C}$  (973K)
- Fuel flow used to get a FC power of 240MW
- Compressor Flow used to get  $150^{\circ}\text{C}$   $\Delta T$  across FC

- 44.0% FC Eff. (HHV)
- 62.5% System Eff. (HHV)
- $\Delta P = 10\%$



# Recuperated Configuration with Post-Heat

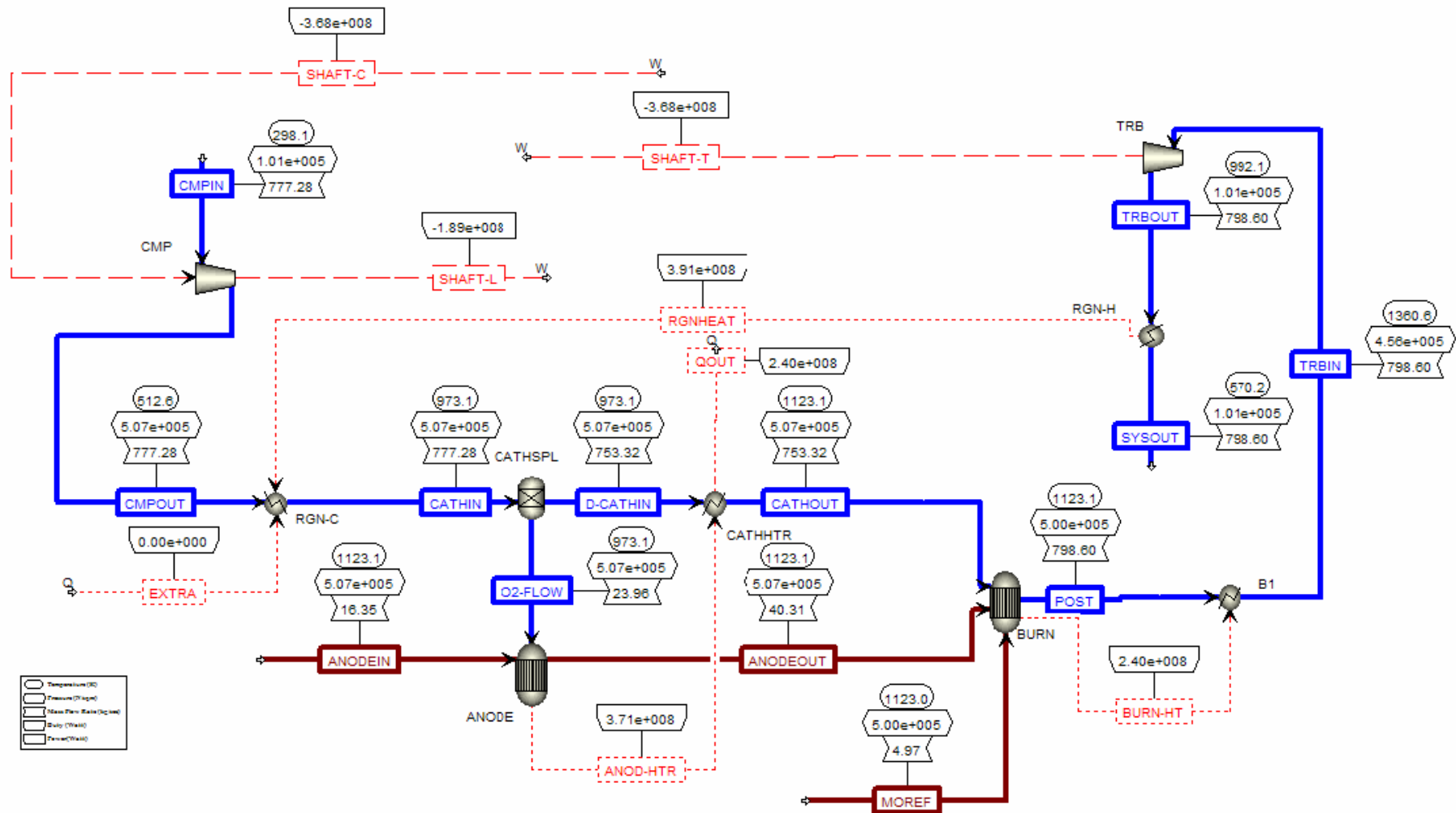
**RC+F**  
**62.3%**



# Recuperated Configuration

- Extra fuel used to get turbine exhaust T to target cathode Tin of 700°C (973K)
- Fuel flow used to get a FC power of 240MW
- Compressor Flow used to get 150°C ΔT across FC

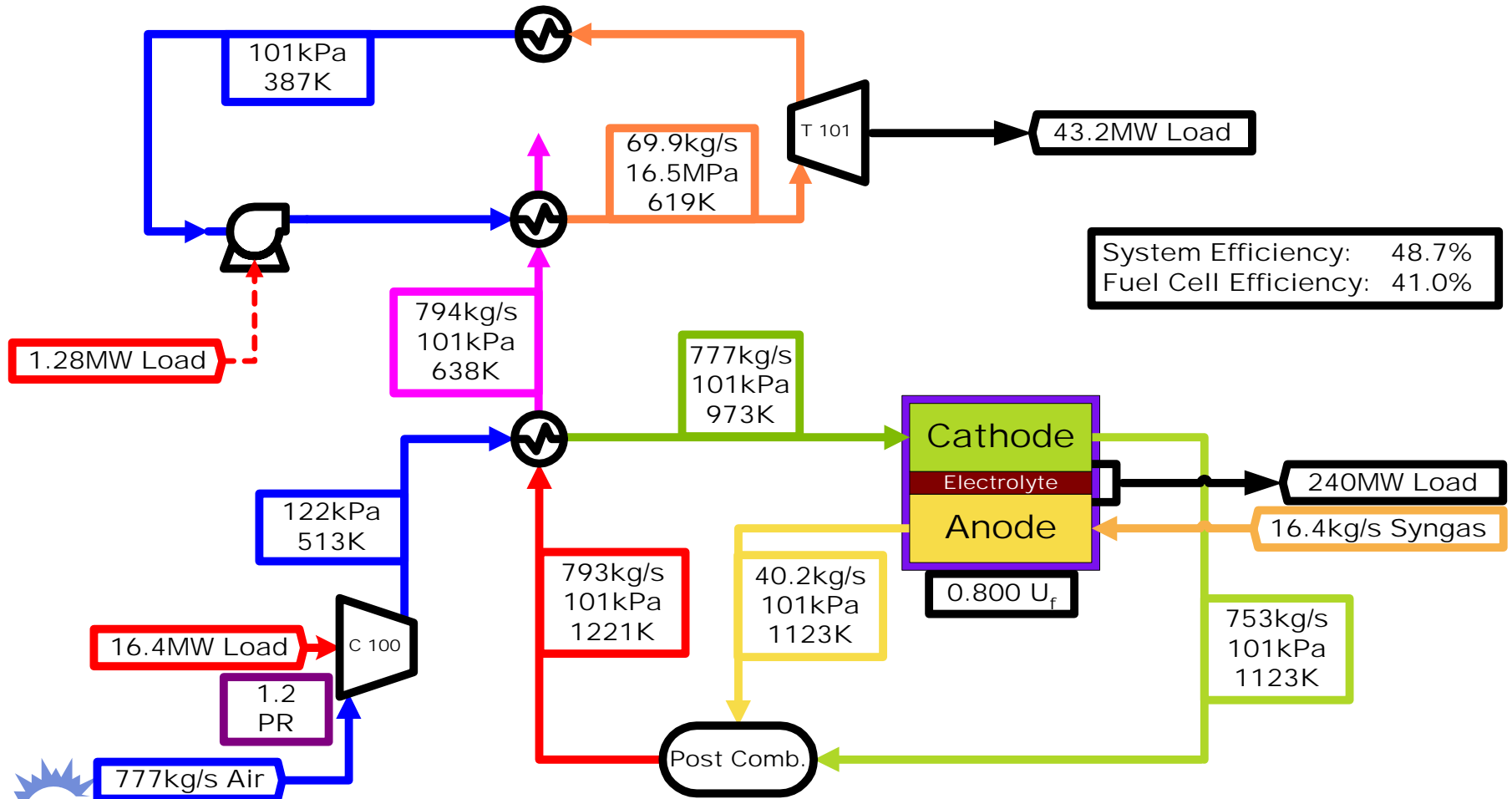
- 44.0% FC Eff. (HHV)
- 60.9% System Eff. (HHV)
- ΔP = 10%



# Atmospheric Fuel Cell with Steam Bottom

## HRSG

### 48.7%





# Summary of Results

Parameter	HPR	CR-B	CR-E	RC+H	RC+F	HRSG
Highest System Efficiency	55.3%	56.0%	53.1%	64.0%	62.3%	48.7%
Highest Fuel Cell Efficiency	47.2%	43.4%	44.3%	46.1%	46.1%	41.0%
Total Syngas (kg/s)	16.3	17.4	17.0	18.7	21.3	16.4
Pressure Ratio	43.85	5	10	5	5	1.2
Comp. Mass Flow (kg/s)	775	196	242	777	777	777
Turbine Power (MW)	32	79	52	148	189	43.2
Turbine Inlet Temp. (K)	1220	1542	1452	1220	1360	619
System Exhaust Temp. (K)	552	1144	1070	532	570	387
Total Pressure Drop	7.5%	7.5%	53.8%	10%	10%	20%
Cathode Mass Flow (kg/s)	775	766	761	777	777	777
Recycle Ratio	N/A	74.4%	68.2%	N/A	N/A	N/A



# Conclusions

## Heat of Compression

- Mechanically simple
- Higher power density
- Lower fuel cell material cost
- Fuel cell integration issues
- Lower efficiency

## Recuperation

- Highly efficient
- Complex

## Steam Bottom

- Mechanically simple
- Available Technology
- Integration with Other Steam
- Lowest efficiency

## Cathode Recycle

- No recuperator
- Reasonable performance at lower pressure
- Higher grade heat from exhaust
- Reduced control options for air flow management
- Methods of recycle require further study

# Acknowledgements

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- Dave is the Hyper project facility operator assigned to the project by Parsons Power, Inc.

