



University Turbine Systems Research Project Review Meeting 5 November, 2019 Improving NOx Entitlement with Axial Staging Contract DE-FE0031227

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- Introduction
- Objectives
- Experimental Facility
- Fuel Only Jet Preliminary Results
- Premixed Jet Preliminary Results
- PIV and TDLAS Measurements
- Modeling
- Year 3 Work









INTRODUCTION







Introduction



Axial Stage Combustion System



H.Karim et al. GE power, TurboExpo 2017

- Lean premixed combustion for the headend
- Axially staged fuel injection with short residence time
- Higher firing temperature

Minimize NOx with increasing turbine inlet temperature











- Gas Turbine OEM's are under pressure to increase efficiency without increasing emissions.
- Increasing turbine inlet temperature is one method to increase efficiency, but NO_x increases rapidly.
- NO_x is a function of peak flame temperature and residence time.
- By injecting some of the fuel late in the combustor (axial staging) it burns with a shorter residence time, minimizing the NO_x penalty.
- OEM's have tested full size axial staging designs at engine conditions, but are unable to obtain detailed measurements of the reacting jet-in-crossflow.

Axial Stage Combustion System Applications

- Power Generation
- Potential for Aircraft Engines







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S. Martin et al., Siemens Energy, Orlando, FL

U.S. Patent 8,387,398, 2013

- Apparatus and method for controlling the secondary injection of fuel.
- Adds multiple fuel nozzles in the transition.
- Can be used to improve temperature pattern factor entering the turbine.











H. Karim et al., GE power, Greenville, SC

ASME Turbo Expo, 2017

- Lean-lean two stage combustion system
- Development testing in FA and HA class gas turbine
- Validation testing for 7HA.01 engine
- Premixers in a can (PM) vs Axial Fuel Staging (AFS)













OBJECTIVES

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Develop a high pressure axial stage combustion test facility and explore novel configurations to implement axial staging with direct involvement of original equipment manufacturers (OEMs).

- Conduct experiments using a high pressure combustion facility.
- Tune rig headend to give similar NOx curve as current engines.
- Axial stage testing with Fuel/Air and Fuel/Diluent axial mixtures with various levels of premixing.
- Obtain detailed measurements of the burning jet to understand the design space and model validation.
- Axial Stage Modeling : Develop reacting jet-in-crossflow correlation and validate existing CFD capabilities.









EXPERIMENTAL FACILITY

























- Three optical access windows for imaging diagnostics
- Interchangeable top plate for different jet geometries
- Wall flush jet injector
- ▶ <u>4 mm</u> and 12.7 mm jet injectors
- Pressure 5 atm.
- > Air flow rate 0.5 kg/s











Fuel Only Jet Preliminary Results









Optical Diagnostics

□ High-Speed CH* Chemiluminescence

- 10,000 frames per second
- FOV = 4.9 x 3.5 in
- 430 nm filter (used for methane jet)

Axial Stage Conditions

- □ Methane non-premixed jet
 - J = 10-115
 - $\Phi_{\text{inlet}} = 0.48-0.72$
 - T_{inlet}: 1260-1650°C
- Hydrogen non-premixed jet
 - J = 10-115
 - $\Phi_{\text{inlet}} = 0.58-0.72$
 - T_{inlet}: 1350-1650°C











Flame Stabilization – Hydrogen Non-premixed Jet



Crossflow Equivalence Ratio

J is momentum flux ratio

- Lower temperature inlet conditions burn further upstream and wider
- Leeward and windward flames
- □ Leaner crossflow provides more oxygen









Flame Stabilization – Hydrogen Non-premixed Jet

□ Momentum flux ratio

- Crossflow $\Phi = 0.58$
- All flames lifted
- Lower momentum flux ignites the same and burns slower
- Higher momentum flux leads to better oxygen entrainment













Flame Stabilization – Methane Non-premixed Jet



Crossflow Equivalence Ratio

- J = 115 (top) J = 10 (bottom)
- Leaner flame burns further upstream
- Leeward shear layer flames
- □ Leaner crossflow provides better oxygen entrainment









Flame Stabilization – Methane Non-premixed Jet

□ Momentum flux ratio

- Crossflow $\Phi = 0.58$
- Wall jet does not burn in leeward side but on windward side
- Wall jet not stable experiences blow-off
- Higher momentum flux entrains enough oxygen on both sides to remain lit













Jet Centerlines

Leanest Crossflow - Methane

 Leaner crossflow burned in shear layer on leeward side of jet











Jet Centerlines

Richest Crossflow – Methane

- Richest crossflow flame burned downstream of viewing section
- Jet trajectory matches non-reacting correlation











Leaner crossflow entrains more oxygen

- Higher velocity gradients (large J) entrain oxygen better and burn further upstream
- Two flames observed: stabilized jet with flame kernels constantly forming and flame propagation

RJIC penetrates further due burning in the wake relative to non-reacting









Premixed Jet Preliminary Results







Experimental Approach: Target Conditions









Results: Flame Shape Constant Crossflow



$\Box \text{ Crossflow Temperature: 1352}^{\circ} \text{ C} \qquad \text{Jet } \mathbf{\phi} = 4$















Rich jet approaches non-premixed jet behavior.











Crossflow Temperature: 1352° C

Jet $\phi = 4$



Jet $\phi = 8$







Results: Centerline Trajectory Comparison





□ Lefebvre jet trajectory correlations: $\frac{y}{d_j} = 0.82J^{0.5} \left(\frac{x}{d_j}\right)^{0.33}$ Where $J = \frac{\rho_j U_j^2}{\rho_m U_m^2}$ —Non-Reacting, Jet $\varphi=4$ —Non-Reacting, Jet $\varphi=8$ ---- Reacting, Jet $\varphi=4$ ---- Reacting, Jet $\varphi=8$ ---- Lefebvre ---- Lefebvre





CFD of Premixed CH4 Flames, 4mm Jet

















- □ An increase of crossflow temperature reduces ignition time and flame liftoff.
- □ Autoignition process occurs on the leeward side of flame followed by flame propagation.
- Reacting jet in crossflow at higher pressure over penetrate compared to non-reacting jet.









PIV AND TDLAS MEASUREMENTS









Diagnostic Setup



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- Began PIV setup
 - Achieved proper seed density
 - Set delta T between laser beams
 - Finalize optical lens setup
- Start Formaldehyde PLIF setup
 - Timing
 - Optical lens setup







Inlet Velocity Profile





- $\succ \text{ Crossflow } \varphi = 0.575$
- Velocity profile at inlet of test section





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Thermocouple	Baseline	Total Mass	Total Main Air	Total Fuel	Total Air	Global Phi	Local Phi							
1316	1400	0.548	0.406	0.0176	0.531	0.575	0.750							
														1
Pressure (PSIG)	Split %	Axial Air	Main Air	Seeder Air	Bypass Air	Axial Air ROU	Main Air ROU	Bypass Air ROU	Seeder ROU	Axial PSIG	Seeder PSIG	Bypass PSI	J	Y(in)
60	20%	0.065	0.341	0.025	0.100	0.22	0.5625	0.24	0.089	151	350	154	15	2.1
60	22%	0.065	0.341	0.028	0.098	0.22	0.5625	0.24	0.1	151	320	163	15	2.1
60	25%	0.065	0.341	0.031	0.094	0.22	0.5625	0.24	0.1	151	367	156	15	2.1
60	27%	0.065	0.341	0.034	0.091	0.22	0.5625	0.24	0.1	151	398	151	15	2.1











Beer-Lambert Law for Species Detection $\alpha = -\ln\left(\frac{I}{I_0}\right) = \sum_{i} \sum_{j} S_{ij}(T) X_j P L \phi_{ij} \left(\nu - \nu_{0}_{ij}\right)$ **Raw Sensor Data** Test Cell **HITRAN/HITEMP/PNNL** Databases, UCF Lab I_0 PCB/CTAP -or- TDLAS ϕ_i, P, T, X_i Hardware Constraint/Constant **Processed Sensor Data** $I = Transmitted Intensity\left(\frac{W}{cm^2 srHz}\right)$ ϕ_{ii} = Lineshape Function (cm) $I_0 = Incident Intensity\left(\frac{W}{cm^2 srHz}\right)$ v = Optical Frequency (Hz) $S_{ij} = Linestrength\left(\frac{cm^{-2}}{atm}\right)$ $v_{0_{ii}}$ = Line Center Optical Frequency (Hz) T = Static Temperature (K)



i = *Quantum Transition*

j = Atomic/Molecular Species



 $X_i = Mole Fraction$

L = Path Length (cm)

P = Static Pressure (atm)







- Initial measurements (top image) utilized a fixedwavelength, direct absorption approach to measure water & temperature.
- Two wavelength multiplexed, pitched through combustor, then demultiplex in the catch box using diffraction gratings.
- Entire system required continuous purge with dry N₂ and cooling, so the equipment did not overheat (outside measurements).
- New approach (bottom image) will utilize wavelength-modulation-spectroscopy (WMS).
- This approach simplifies demultiplexing, eliminates the number of optical surfaces (for water to condense on), and requires only one detector. The system is smaller, simpler, and less sensitive to noise.
- Thermal electric coolers (TECs) will be employed to regulate equipment temperatures.













MODELING









CFD with Star CCM+

A STORE OF CALL OF UNIT

- Symmetric jet-in-crossflow axial stage geometry
- Structured, locally refined mesh with (1–50) E6 cells
- Computational Cost: 1000-5000 datacenter hours

• Reactive Domain:

A) Detailed Chemistry

- **B)** Flamelet Approach
 - Non-premixed: Steady Laminar Flamelet
 - Partially Premixed: FGM with Turbulent Flame Closure
 - Premixed: FGM with Coherent Flame Model



CFD of Non-Premixed CH4 Flames, 4mm Axial Jet







Axial Stage: NO_x Emission CFD prediction and comparison with literature data

Preferred: Detailed Chemistry Model Poor: Flamelet + Thermal NO_x Model







Unheated 4mm jet, control parameters to *accelerate* local flame ignition:

Windward branch	Lee-side branch
$\dot{m}_{CH4}^{crossflow}\downarrow$	$T^{crossflow}$ \uparrow
$w_{O2}^{crossflow}$	$w_{O2}^{crossflow}$ \uparrow



Combustion instabilities visible in the windward flame branch





CFD of Partially Premixed CH4 Flames, 4mm Jet



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W_{CH^*} @ z=0 [CFD] and CH* Chemi [Exp.]



Jet Penetration



Divided flame









- □ Perform flow field analysis using particle image velocimetry (PIV)
- □ Study flame structure through PLIF
- □ Vary levels of partially premix in axial jet
- \square Explore pressure effect on NO_x
- Obtain NO and CO emissions with Tunable diode laser absorption spectroscopy (TDLAS)











Questions





