Development of Two-Phase Dense Fluid Expander for Advanced Cryogenic Air Separation and Low-Grade Heat Recovery

> Air Products and Chemicals, Inc. Ravi Pantula 7201 Hamilton Blvd Allentown, PA 18195 pantulsr@airproducts.com

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## **Presentation Outline**

- Project Objectives
- Background
- Prototypes machines
- Test results
- Next phase of testing.



## **Project Objectives**

3

• The first objective is to better understand the limitations associated with two-phase dense fluid expansion from aerodynamic, thermodynamic, and mechanical perspectives

 The second objective is to apply this knowledge to construct <u>two</u> prototype devices to further explore the basic properties of twophase dense fluid expansion



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- Cryogenic air separation is the state of the art technology used to supply the vast amounts of oxygen required for coal gasification
- Power needed to drive the main air compressor (MAC) in a typical air separation unit (ASU) represents approximately 70-90% of ongoing operating cost for the entire ASU
- Usage of a dense fluid expander (DFE) within an ASU allows for more efficient plant operation, and therefore less power is required to produce an equivalent amount of oxygen product
- Typically 1HP refrigeration power created by the DFE equates to 5-6HP of electrical power savings





- Developing a successful two-phase dense fluid expander for cryogenic air separation will open doors for additional DFE applications and overall ASU 1.2 bar plant efficiency improvement instant Temperature Lines onstant Entropy Lines
  - Run traditional DFE applications two phase leading to more efficient plant 1. operation. Kurren PEtrope back-pressured to kege discharge flow single phase.
  - 2. Savings equal to ~0.3% of MAC - electrical power = 30/1P\*
  - Replacement of letdown values with DEE's (3-6 very typical ASU) 7450HR\*
  - Savings equal to -1% of MAC electrical bow 3. Waste mean requiring two phase Dfgd svapor
    - Savings equal to ~5% of MAC electrical power

Enthalpy (Heat Content) plits between O2 and N2, depending on the cycle

6

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HPCOL 5.5 bar

Lia

Enthalpy (Heat Content) Crude LOX

Vapor



- State of the art cryogenic dense fluid expanders used in air separation are typically limited to single-phase flow (liquid in, liquid out)
- A single-phase DFE design with only liquid in the discharge typically experiences very little volume change upon expansion
- A two-phase DFE may experience volume increases of up to 10 times upon expansion
- The large volume difference between vapor and liquid poses challenges to designing equipment as it relates to machine efficiency, durability, erosion, stable operation, and other performance criteria



Two different types of expander prototypes identified.

- 1. Centrifugal machine with two phase operation.
  - Two part testing
  - Part 1 : Identification of two phase operation and issues in the plant.
  - Part 2 : Modifications for improvement of plant performance in two phase operation
- 2. Axial Impulse type machine for higher vapor phases.



# Centrifugal DFE

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## Part 1 - Testing

 Lube Oil Supply (TI-1022) & Lube Oil Drain (TI-1011): Replace existing elements (unused and both in thermowells) with a 4-wire RTD.

Lube Oil Flow Meter (FE-1021)

 Replace existing variable area meter with a new turbine-type meter. New meter to be plumbed external to existing panel and connected via hoses in order to achieve the required straight upstream and downstream lengths.









## Part 1 - Testing



## Part 1- Testing



## Part 2 - Testing

• New prototype device based on the data from part -1 testing was designed.

• In process of manufacturing and assembling the machine.

• Part-2 testing Mid June 2019.



## Axial Impulse DFE

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## Axial Impulse DFE

Axial Impulse design is attractive from various aspects

- High tolerance to 2 phase mixtures both at inlet and discharge
- Slower rotor speeds improved reliability, lower cost (manufactured and installed)
- Simple and inexpensive to manufacture relative to radial inflow designs
- Low cost installation (no lubrication system, limited monitoring/controls)
- Ability to use off the shelf induction motor as basis for the unit for our application





## AIT – Mechanical testing



- Motor/generator wired to a 480V variable frequency drive (VFD)
- Plugged inlet nozzles
- Seal gas supply connected to an instrument air system and a flow meter
- Seal gas vent connected to a flow meter
- Discharge connection covered with a blind flange (for personnel protection)
- Accelerometer with portable vibration monitor attached to motor housing









## AIT – Mechanical testing



- The machine was operated at various speeds from 10 to 100% (3,520 rpm) for approximately one hour while observing the housing vibration.
- After the test, the discharge housing was removed, and a visual inspection of the turbine impeller was performed. It was concluded that the turbine passed all mechanical test acceptance criteria and is ready for the next step: two-phase cryogenic nitrogen testing.





## AIT – Performance test plan

- Planned performance testing.
- Identified location for testing.
  Lancaster, PA.
- Finished P&ID and test plan.

\*\*\*\*\*\*\*\*\*\*

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### AIT – Performance test plan



## AIT – Next steps

• Complete testing week of 4/22/19 at Lancaster, PA facility.

 Finalize and create reports of the test data by June 2<sup>nd</sup> week and conclude AIT prototype program.



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