

Evaluation of Steam Cycle Upgrades to Improve the Competitiveness of US Coal Power Plants

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Project Description and Objectives

- Examine the feasibility of retrofitting advanced materials to improve heat rate, while minimizing plant modifications
- Reduce coal consumption of existing utility fleet by increasing steam cycle efficiency
- Increase steam temperatures to Advanced Ultra-supercritical (AUSC), or USC conditions – while maintaining original pressure
- Employ advanced nickel-based high-temperature materials
 - Result of DOE-funded materials R&D
- Estimate improved capacity factor, and economic benefit from higher plant efficiency

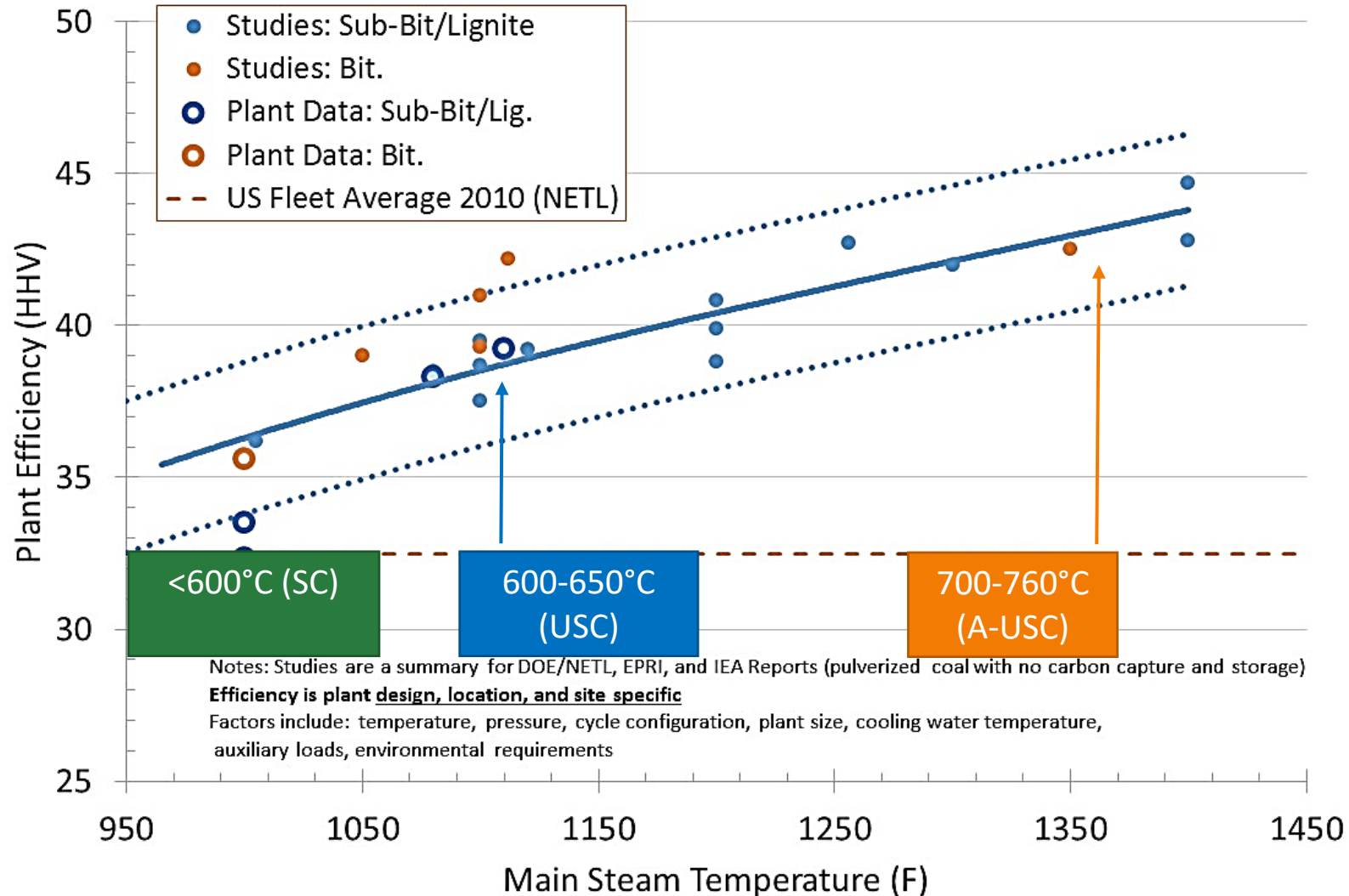
Strategic Alignment with DOE Fossil Energy Objectives

Power Plant Efficiency Improvements – Develop cost-effective, reliable technologies to improve the efficiency of new and existing coal-fired power plants.

- This project aims to evaluate options for existing plants to upgrade steam temperature for higher cycle efficiency
 - Average efficiency of US coal-fired fleet = 33% HHV
 - Efficiency increases to over 41% HHV at 1,350°F steam temperature
 - Base cases defined to represent 80% of existing coal-fired fleet

Motivation for AUSC Coal-Fired Power Plants

Plant Efficiency (HHV) as a Function of Steam Temperature



Project Status

- Worked with utility partner (Southern Company) to validate representative subcritical and supercritical base case models
- Developed thermodynamic performance models for the upgrade cases
- Evaluated technical feasibility (boiler & turbine) for upgrade cases
 - Nine original upgrade cases completed
 - Added three new cases
- Estimating capital costs associated with feasible upgrade options
- Preparing the unit dispatch model – impact on asset profitability

AUSC Retrofit Study – Work Scope



- Model technical feasibility of required modifications
- Generate capital cost estimates
 - GE – boiler and steam turbine
 - AECOM – balance-of-plant
- Estimate the value of the heat rate improvements by detailed modeling of the unit dispatch in several regional U.S. power markets (EPRI's US-REGEN model)
 - Compare revenue of upgraded units vs. non-upgraded units
- Prepare technical report

Improve heat rate while minimizing power plant modifications

Project Structure - Tasks

- 1 Project management and planning
- 2 Evaluation of technical feasibility
 - 2.1 Thermodynamic performance models of base case at full load
 - 2.2 Impact of upgrades to base cases at full load
 - 2.3 Part load performance for flexible operation scenarios
 - 2.4 Dynamic modeling of system for fluid circulation
- 3 Unit dispatch modeling (EPRI's US-REGEN model) to 2050
- 4 Capital cost estimation to AACE Class III (+/-30%)
- 5 Overall economic evaluation

Two-year project ends in January 2020

Background – Challenges for AUSC Technology

- Greenfield A-USC steam plants may not be cost effective
 - Conventional USC (1100°F or 593°C) power plants use lower cost materials
- Retrofits to higher temperature may be more cost effective option
 - Significant reuse of existing equipment – decreased capital cost
 - Increase only steam temperature – not steam pressure
 - Limit the scope of equipment replacement
 - Superheater and reheater panels
 - Steam turbine
 - Piping between the superheater/reheater and steam turbine

Technical Approach - Summary

- Maximize the applicability of the study results to existing fleet
 - 300+ units with ~2,400 psia (16.6 MPa) main steam (subcritical)
 - 100+ unit with ~3,500 psia (24.1 MPa) main steam (supercritical)
- Insure that results reflect actual situations in US fleet
 - Data from existing operating units supplied by Southern Company
- Evaluate a variety of temperature upgrade options
- Employ an experienced technical team that has worked together on prior DOE-funded AUSC project (ComTest)
 - EPRI, GE, AECOM, HES

Technical Approach – Original Upgrade Cases Planned

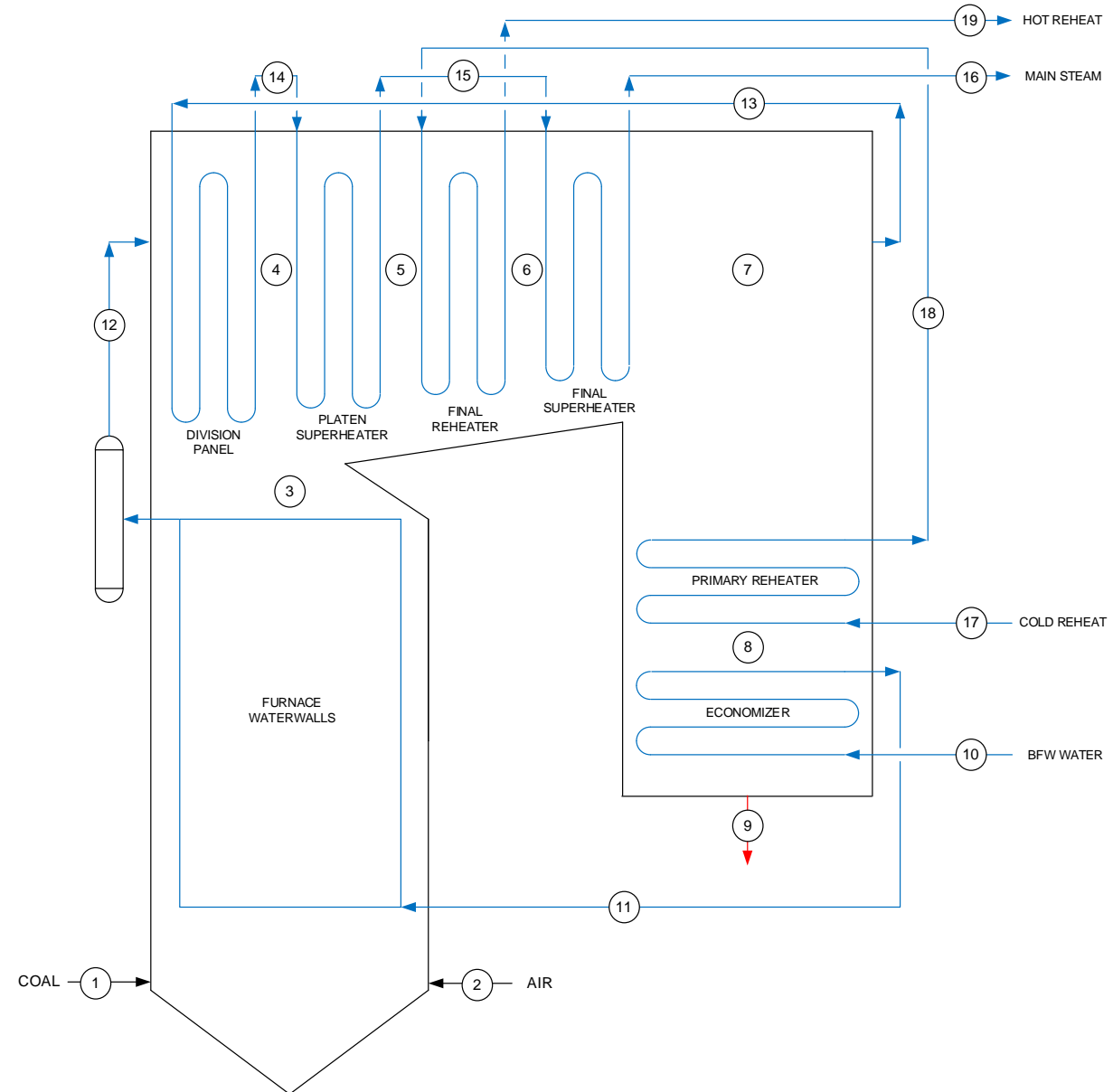
Case Name	Main Steam Pressure	Main Steam Temperature	Reheat Steam Temperature
Subcritical Base Case	2400 psi (16.6 MPa)	1000°F (538°C)	1000°F (538°C)
Subcritical USC Option	2400 psi (16.6 MPa)	1100°F (593°C)	1100°F (593°C)
Subcritical A-USC Option 1	2400 psi (16.6 MPa)	1200°F (649°C)	1200°F (649°C)
Subcritical A-USC Option 2	2400 psi (16.6 MPa)	1000°F (538°C)	1350°F (732°C)
Subcritical A-USC Option 3	2400 psi (16.6 MPa)	1350°F (732°C)	1350°F (732°C)
Supercritical Base Case	3500 psi (24.1 MPa)	1000°F (538°C)	1000°F (538°C)
Supercritical USC Option	3500 psi (24.1 MPa)	1100°F (593°C)	1100°F (593°C)
Supercritical A-USC Option 1	3500 psi (24.1 MPa)	1200°F (649°C)	1200°F (649°C)
Supercritical A-USC Option 2	3500 psi (24.1 MPa)	1000°F (538°C)	1350°F (732°C)
Supercritical A-USC Option 3	3500 psi (24.1 MPa)	1350°F (732°C)	1350°F (732°C)
Supercritical A-USC Molten Salt	3500 psi (24.1 MPa)	1350°F (732°C)	1350°F (732°C)

Base Case Model Development

- Base cases were intended to be realistic, based on information from existing power plants
- These are not intended to be identical representations of existing units
- Allowed a more direct comparison, and matching parameters
 - Fuel (PRB coal)
 - Output (750 MW)
 - Steam turbine efficiency (identical)
 - Feedwater heater configuration (identical)
 - Site location and ambient conditions (Kenosha, Wisconsin)

Supercritical PC Boiler Base Case Preliminary Sizing

Furnace			Roof, Walls, Screen Tubes		
Duty	2,650	MMBTU/hr	Duty	252	MMBTU/hr
Total Surface Area	75,648	ft ²	Total Surface Area	35790	ft ²
Furnace Width	98	ft	Materials		
Furnace Depth	49	ft	CS	916	tons
Wall Height Below Nose	170	ft			
Hopper Height	25	ft	Final Superheater		
Height Wall Above Nose	21	ft	Duty	464	MMBTU/hr
Overall Boiler Height	216	ft	Total Surface Area	37810	ft ²
Materials			Number Panels	138	
CS	1131	tons	Panel Width	7.7	ft
			Panel Length	18	ft
Division Panels			Materials		
Duty	346	MMBTU/hr	T91	191	tons
Total Surface Area	9962	ft ²			
Number Panels	8		Primary Reheater		
Panel Width	29	ft	Duty	632	MMBTU/hr
Panel Length	16	ft	Total Surface Area	54466	ft ²
Materials			Number Panels	186	
T91	53	tons	Panel Width	8.2	ft
			Panel Length	18	ft
Platen Superheater			Materials		
Duty	475	MMBTU/hr	CS	68	tons
Total Surface Area	14693	ft ²			
Number Panels	113		Economizer		
Panel Width	3.2	ft	Duty	626	MMBTU/hr
Panel Length	20	ft	Total Surface Area	92407.9408	ft ²
Materials			Number Panels	253	
T91	64	tons	Panel Width	10.2	ft
			Panel Length	17.5	ft
Finishing Reheater			Materials		
Duty	509	MMBTU/hr	CS	410	tons
Total Surface Area	21085	ft ²			
Number Panels	113				
Panel Width	4.9	ft			
Panel Length	18	ft			
Materials					
T91	23	tons			



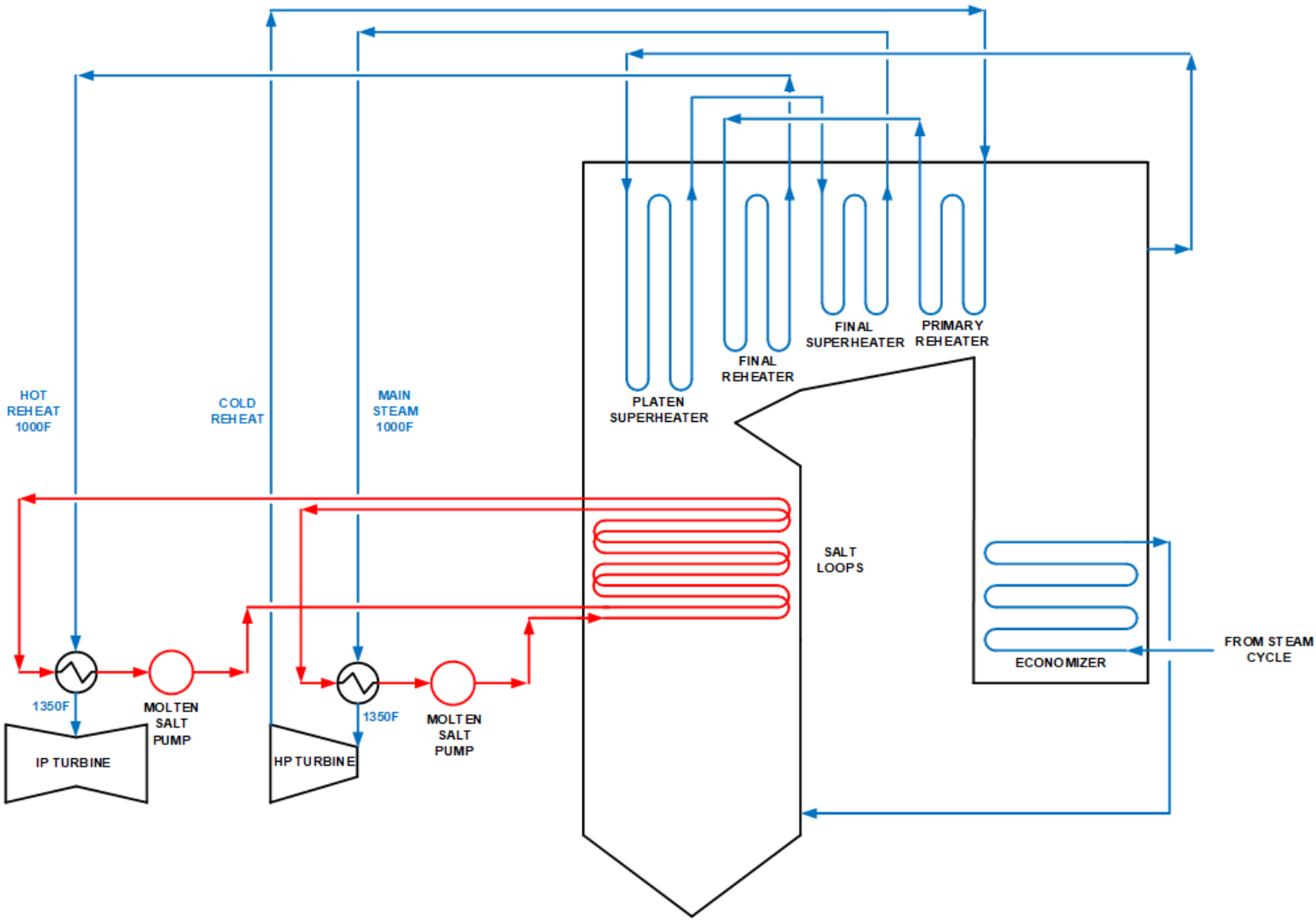
Model Details for Steam Cases

- Nine original upgrade options evaluated using
 - EPRI's PC-Cost for preliminary boiler sizing, and
 - AspenPlus™ for heat and material balance for boiler and steam cycle
- Net power output set to match applicable base case
 - Avoid upgrades to the switchyard and transmission lines
- Technical feasibility of boiler and steam turbine sections evaluated

Model Details for Molten Salt Case

- Evaluate molten salt option – goal to reduce costs associated with nickel alloy steam transfer piping from boiler to steam turbine
- Existing main and reheat steam piping will be used to carry 1000°F (538°C) steam from the superheat and reheat headers down to the level of the steam turbine.
- Separate low pressure molten salt system installed in the furnace
 - Extract heat at high temperature (up to 1400°F or 760°C)
 - Deliver the molten salt to a heat exchanger at the steam turbine level where the 1000°F (760°C) superheat and reheat steam flows will be heated to 1350°F (732°C) before entering the steam turbine.

Molten Salt Case Configuration



Full Load and Part Load Evaluation for Each Case

- Evaluate the thermodynamic performance
- Calculate the amount of heat transfer surface required
- Determine impact upon piping and steam turbine
- Model the performance at 75% load and 50% load

Conclusions from Evaluation of Original Upgrade Cases

- Steam cases at 1,100°F / 1,100°F (SH/RH) are feasible for both subcritical and supercritical configurations
- The 1,350°F steam temperature cases are not feasible
 - Insufficient space in existing boiler for needed heat exchanger surface
- Some 1,200°F steam temperature may be feasible – at least under some conditions

Technical Feasibility Results – Original Upgrade Cases

Case Name	Main Steam Pressure	Main Steam Temp.	Reheat Steam Temp.
Subcritical Base Case	2400 psi (16.6 MPa)	1000°F (538°C)	1000°F (538°C)
Subcritical USC Option	2400 psi (16.6 MPa)	1100°F (593°C)	1100°F (593°C)
Subcritical A-USC Option 1	2400 psi (16.6 MPa)	1200°F (649°C)	1200°F (649°C)
Subcritical A-USC Option 2	2400 psi (16.6 MPa)	1000°F (538°C)	1350°F (732°C)
Subcritical A-USC Option 3	2400 psi (16.6 MPa)	1350°F (732°C)	1350°F (732°C)
Supercritical Base Case	3500 psi (24.1 MPa)	1000°F (538°C)	1000°F (538°C)
Supercritical USC Option	3500 psi (24.1 MPa)	1100°F (593°C)	1100°F (593°C)
Supercritical A-USC Option 1	3500 psi (24.1 MPa)	1200°F (649°C)	1200°F (649°C)
Supercritical A-USC Option 2	3500 psi (24.1 MPa)	1000°F (538°C)	1350°F (732°C)
Supercritical A-USC Option 3	3500 psi (24.1 MPa)	1350°F (732°C)	1350°F (732°C)
Supercritical A-USC Molten Salt	3500 psi (24.1 MPa)	1350°F (732°C)	1350°F (732°C)

Path Forward on Technical Feasibility Evaluations

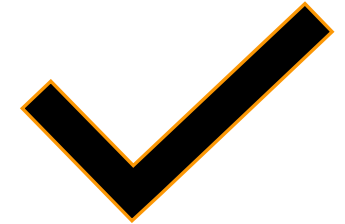
- Expand upgrade options to include three new cases
 - Steam case at 1,000°F / 1,200°F (SH/RH) for subcritical
 - Steam case at 1,000°F / 1,200°F (SH/RH) for supercritical
 - Molten salt case at 1,200°F / 1,200°F (SH/RH)

Summary of Current Cases – Three Additional Cases

Case Name	Main Steam Pressure	Main Steam Temp.	Reheat Steam Temp.
Subcritical Base Case	2400 psi (16.6 MPa)	1000°F (538°C)	1000°F (538°C)
Subcritical USC Option	2400 psi (16.6 MPa)	1100°F (593°C)	1100°F (593°C)
Subcritical A-USC Option 1	2400 psi (16.6 MPa)	1200°F (649°C)	1200°F (649°C)
Subcritical A-USC Option 2	2400 psi (16.6 MPa)	1000°F (538°C)	1350°F (732°C)
Subcritical A-USC Option 2A	2400 psi (16.6 MPa)	1000°F (538°C)	1200°F (732°C)
Subcritical A-USC Option 3	2400 psi (16.6 MPa)	1350°F (732°C)	1350°F (732°C)
Supercritical Base Case	3500 psi (24.1 MPa)	1000°F (538°C)	1000°F (538°C)
Supercritical USC Option	3500 psi (24.1 MPa)	1100°F (593°C)	1100°F (593°C)
Supercritical A-USC Option 1	3500 psi (24.1 MPa)	1200°F (649°C)	1200°F (649°C)
Supercritical A-USC Option 2	3500 psi (24.1 MPa)	1000°F (538°C)	1350°F (732°C)
Supercritical A-USC Option 2A	3500 psi (24.1 MPa)	1000°F (538°C)	1200°F (732°C)
Supercritical A-USC Option 3	3500 psi (24.1 MPa)	1350°F (732°C)	1350°F (732°C)
Supercritical A-USC Molten Salt	3500 psi (24.1 MPa)	1350°F (732°C)	1350°F (732°C)
Supercritical A-USC Molten Salt A	3500 psi (24.1 MPa)	1200°F (732°C)	1200°F (732°C)

A-USC Retrofit Study – Current Status / Work Completed

- Completed thermodynamic performance models – two base cases
- Upgrade cases have been modeled
 - Full-load and part-load evaluations for original steam cases
 - Original molten salt upgrade option configuration
 - Evaluated technical feasibility of original upgrade options
- Calculated sizing of heat exchanger banks
- Certain high-temperature options for the supercritical case have been determined to be technically non-feasible
- Added three additional upgrade options – being evaluated



Design and performance work done; costs underway

Market Benefits/Assessment

- The average efficiency of the US coal-fired fleet is approximately 33% (HHV)
- Capacity factor of existing coal-fired power plants is limited by efficiency
- Steam temperature increases to AUSC conditions, have the potential to increase efficiency to over 41% (HHV)
- This AUSC upgrade path is applicable to 80% of existing fleet
 - Technically feasible options could be widely deployed
 - Present project intends to quantify potential economic benefits of increased efficiency (temperature increase to AUSC conditions)

Technology-to-Market Path

- Plant upgrades to USC or AUSC steam temperatures are compatible with DOE's goals to achieve power plant efficiency improvements
- Candidate demonstration plants for initial upgrades have been identified
- Primary technology challenges relate to the fabrication of full-scale AUSC components and supply chain development
 - Phase II of DOE-funded ComTest project (DE-FE0025064) addresses these
 - ComTest is scheduled to be completed in September 2021

Conclusions

- Upgrades to existing coal-fired plants have the potential to increase the steam temperature, and cycle efficiency
- Maintaining original pressure can minimize plant modifications
- Some technically feasible upgrade options have been identified
- Capital costs are being calculated for the feasible options
- Higher efficiency is expected to lead to increased capacity factor
- Unit dispatch models will help to evaluate the potential long-term return on investment for the plant upgrade

A-USC Retrofit Study Support Acknowledgement

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