



FuelCell Energy

**Project Kickoff Meeting
Transformational SOFC Technology
(DE-FE0027584)**

**Presented To:
National Energy Technology Laboratory (NETL)**

**November 16, 2016
Webconference**

Public Version

Ultra-Clean, Efficient, Reliable Power

Attending Organizations: National Energy Technology Laboratory (NETL/DOE), FuelCell Energy, Inc. (FCE), Northwestern University (NU)

12:15 pm - 12:30 pm	Introductions and brief procurement discussions	NETL
12:30 pm – 12:40 pm	Project Overview	H. Ghezal-Ayagh
12:40 pm – 1:05 pm	Cell Technology and Manufacturing	Scott Barnett / Eric Tang
1:05 pm - 1:25 pm	Stack Design and Fabrication	Scott Corey / Keith Davis
1:25 pm - 1:30 pm	Q&A and Follow up Discussion	All

* Times are in EDT (Eastern Daylight Saving Time)

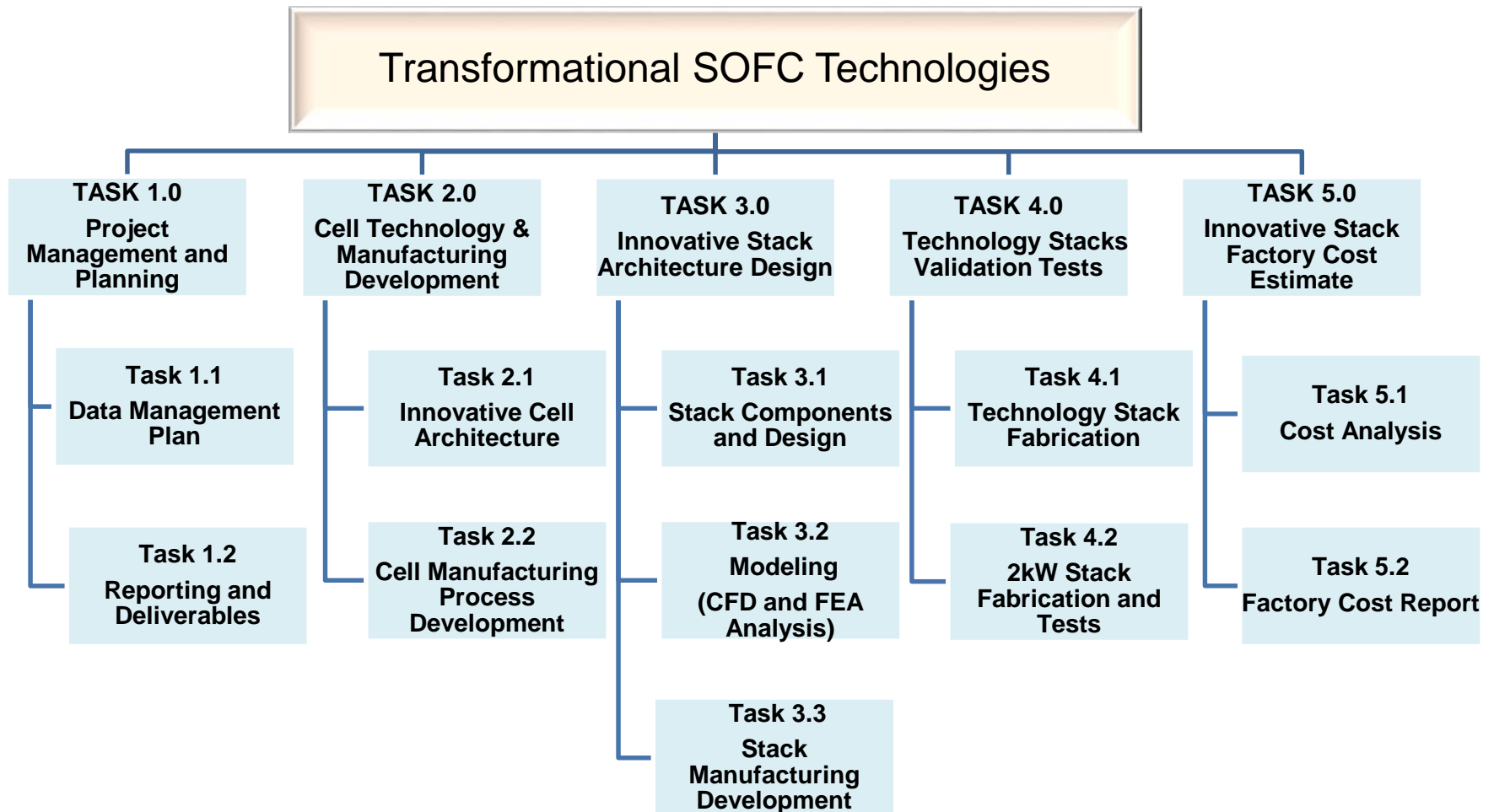
Project Overview

The overall project goal is to advance the SOFC technology at the cell and stack levels by focusing on the following objectives:

- Enhancements in reliability, robustness and endurance
- Reduction in overall system cost
- Reduction in operating and maintenance cost

The approach in meeting the objectives are targeted on:

- Increased redox stability of the existing cell technology
- Developing a new novel single-stage sintered cell technology
- Develop an integrated stack architecture incorporating balance-of-plant functionality and enabling reduction in materials usage
- Simplify plant maintenance and repair



The work breakdown structure is designed to ensure success in achieving the program objectives with minimal risk.

FuelCell Energy Danbury

Project Coordination

Integrated Stack
Design

BOP Components
Design and Integration

Validation Tests

Factory Cost
Estimate

FuelCell Energy Calgary

TSCIII Optimization for
Redox Tolerance

Cell Manufacturing
Process Modification

Stack Repeat
Components Design

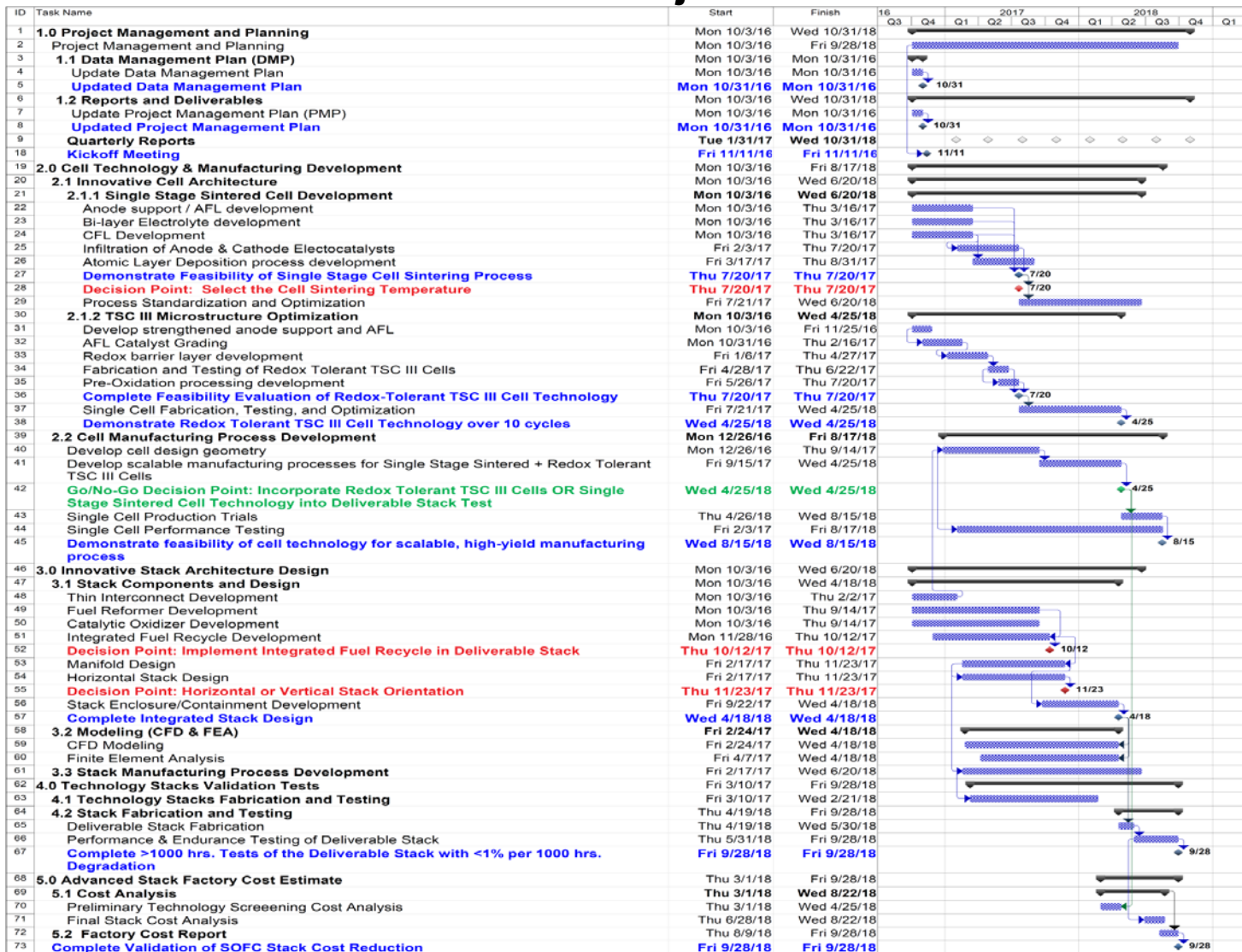
Technology Cell &
Stack Tests

Northwestern University

Single-Stage Sintered
Cell

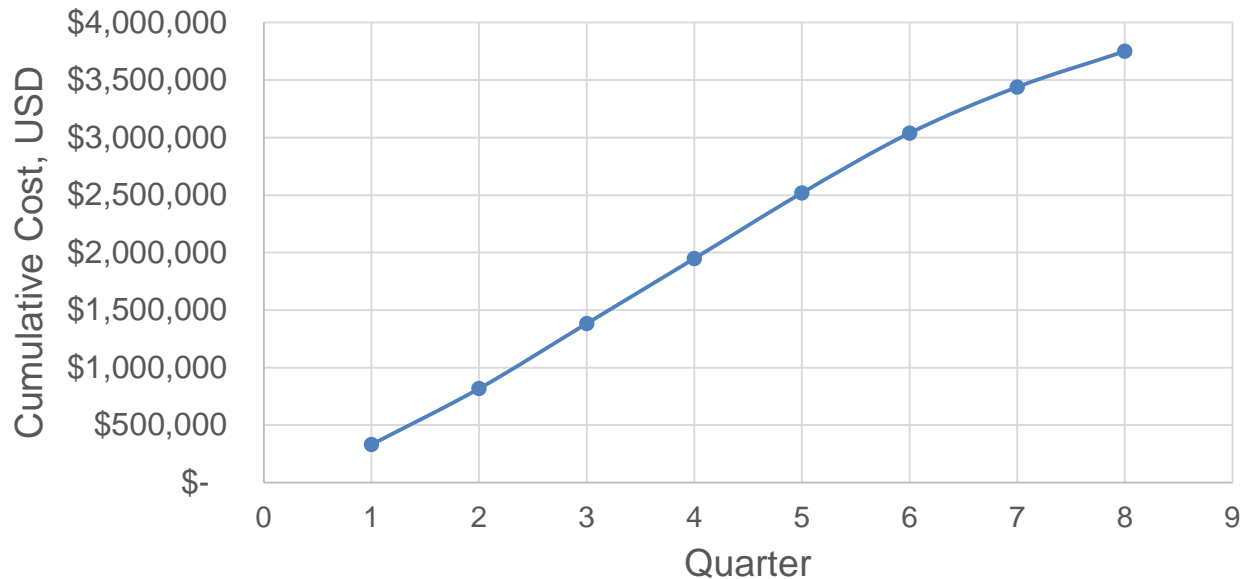
Bi-layered Electrolyte

Two-Year Project Schedule



	Project Period 10/01/16-09/30/18		Total
	Government Share	Cost Share	
Total	\$3,000,000	\$750,000	\$3,750,000
Percentage	80.0%	20.0%	

Spending Plan



Risk Categories:

- Technology
- Resources
- Management

Degree of Risk Calculation Chart

PROBABILITY	HIGH	Moderate	High	High
	MOD	Moderate	Moderate	High
	LOW	Low	Moderate	Moderate
		LOW	MODERATE	HIGH
		IMPACT		

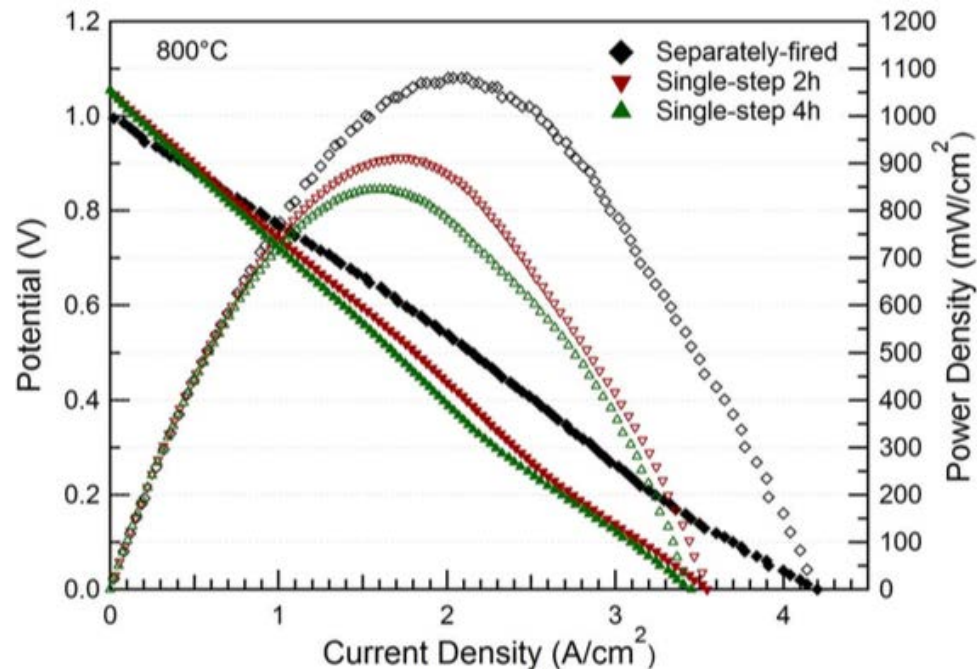
Id.	Task /Subtask No.	Milestone Description	Planned Completion	Actual Completion	Verification Method
1	1.1	Updated Data Management Plan (DMP)	10/31/16	10/31/16	DMP File
2	1.2	Updated Project Management Plan (PMP)	10/31/16	10/31/16	PMP File
3	1.2	Project Kickoff Meeting	11/11/16	11/16/16	Presentation File
4	2.1.1	Demonstrate Feasibility of Single Stage Cell Sintering Process	7/20/17		Quarterly Report
5	2.1.2	Complete Feasibility Evaluation of Redox-Tolerant TSC III Cell Technology	7/20/17		Quarterly Report
6	2.1.2	Demonstrate Redox Tolerant TSC III Cell Technology over 10 Testing cycles	4/25/18		Quarterly Report
7	2.2	Demonstrate Feasibility of Cell Technology for Scalable, High-Yield Manufacturing Process	8/14/18		Quarterly Report
8	3.1	Complete Integrated Stack Design	4/18/18		Quarterly Report
9	4.2	Complete >1000 hrs. Tests of the Deliverable Stack with <1% per 1000 hrs. Degradation	9/28/18		Quarterly Report
10	5.2	Complete Validation of SOFC Stack Cost Reduction	9/28/18		Factory Cost Report

Decision Point	Date	Success Criteria
Select Cell Sintering Temperature	7/20/17	The lowest single stage cell sintering temperature (<1350 °C) will be selected which provides adequate electrolyte densification and also prevents interdiffusion amongst layers. The decision will be based on the results of cell testing.
Implement Integrated Fuel Recycle in Deliverable Stack	10/12/17	CFD modeling, and/or bench-testing, shows the feasibility of integrated anode recycle concepts to provide sufficient levels of steam to achieve a steam-to-carbon ratio >1.6 at the anode inlet.
Implement Horizontal or Vertical Stack Orientation in Deliverable Stack Test	11/23/17	Based on the results of CFD and FEA modeling, horizontal stack architecture will be selected if it shows promise to enable larger stacks without introducing significantly-greater technical risks.

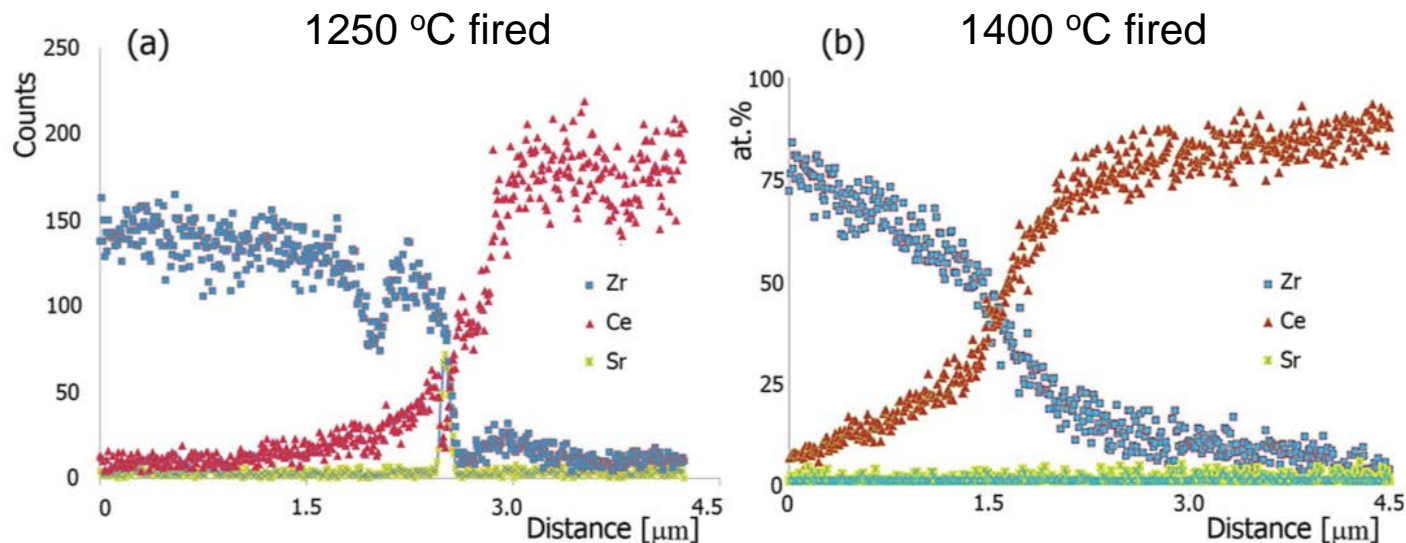
Work Scope Task 2

- Objective
 - To develop cell materials that are tolerant to reduction and oxidation cycling (Redox cycling) which can be expected in real-world system operation
- Approach
 - Building on VPS' strong anode-supported cell development experience since 1997
 - Leveraging cell and stack advancements from previous SECA projects
 - Implementing multi-prong approaches in developing innovative redox tolerant anode-supported cell through reducing anode strain upon Ni re-oxidation
- Work Plan
 - Promising results from several approaches will be incorporated in a redox tolerant TSCIII cell technology
 - The final cell design will undergo a testing regime with 10 thermal cycles and 10 Redox cycles in single-cell (10 cm x 10 cm) test platform
 - Single-cell tests will be deemed successful by targeting equivalent or lower performance loss on redox cycling than that is found with thermal cycling.

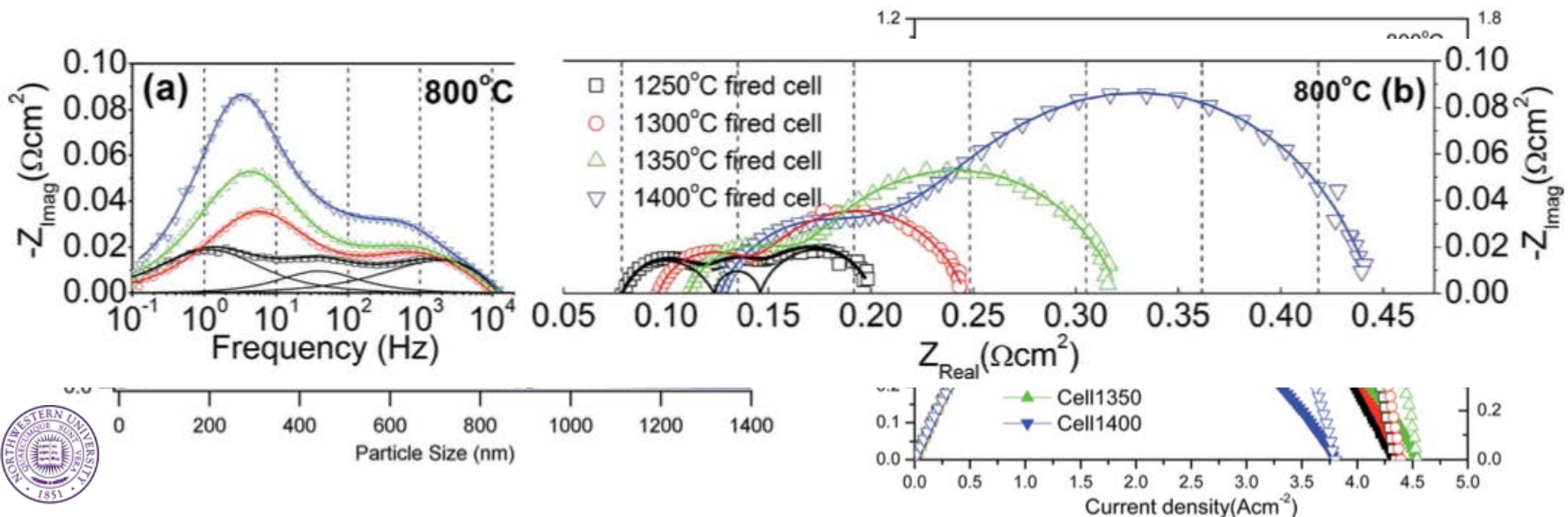
- Single-step firing: process simplification
- Reduced temperature firing
 - Essential to minimize cathode sintering, electrolyte interactions
 - Single-step (1250 °C) fired cells (Ni-YSZ / YSZ / LSM-YSZ) show similar performance as conventional cells



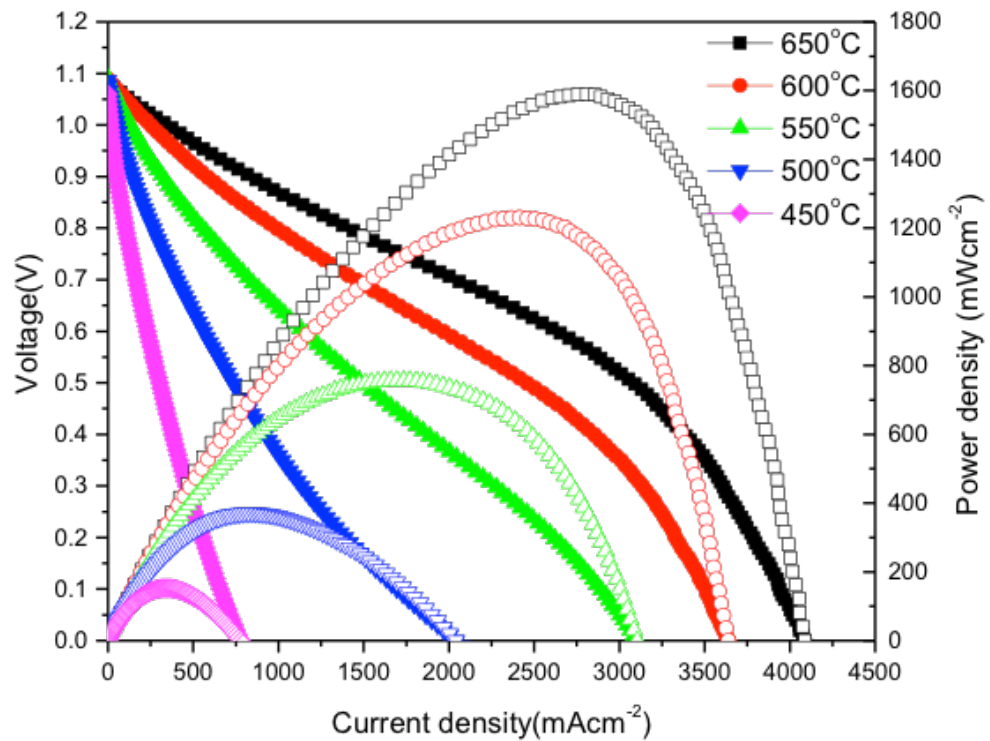
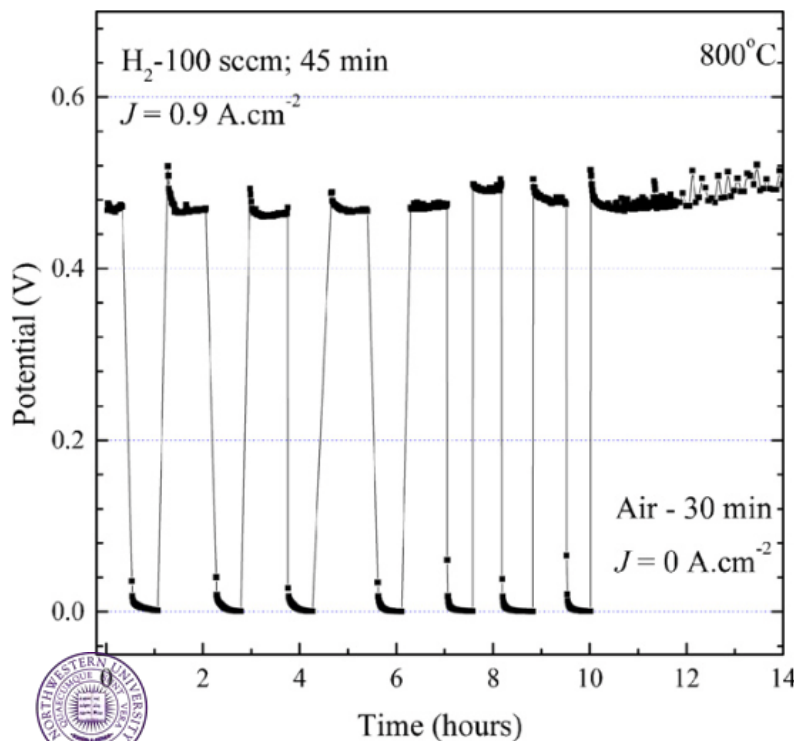
- Single-step firing: process simplification
- Reduced temperature firing
 - Essential to minimize cathode sintering, electrolyte interactions
 - Essential to minimize YSZ/GDC interdiffusion
 - Reduced interdiffusion eliminates large ohmic resistance



- Single-step firing: process simplification
- Reduced temperature firing
 - Essential to minimize cathode sintering, electrolyte interactions
 - Essential to minimize YSZ/GDC interdiffusion
 - Finer-scale anode microstructure - improved performance
- Data from Ni-YSZ / YSZ / GDC / LSCF cells



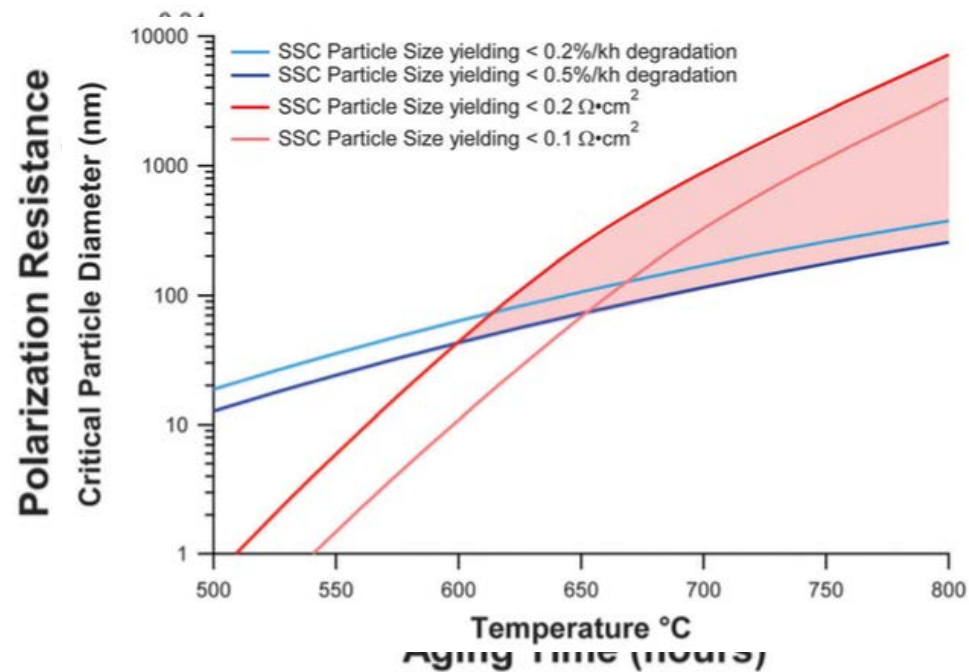
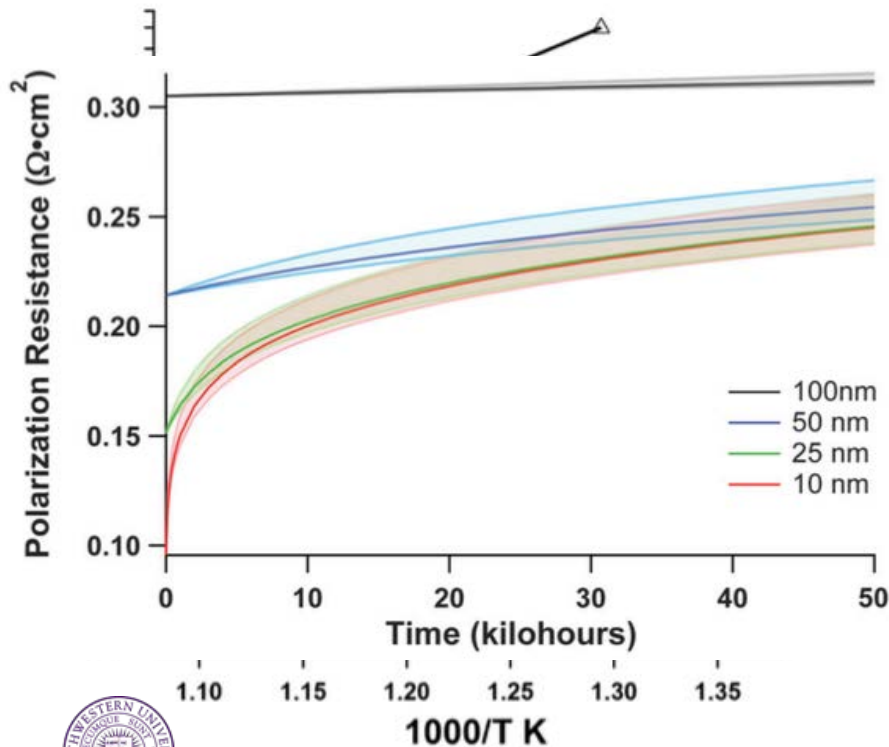
- Redox cycle stability: (left) stable operation after several redox cycles of a cell with (Sr,La)TiO₃ support, Ni-YSZ AFL, YSZ electrolyte, and LSM-YSZ cathode
- Good low-temperature performance of cell after infiltration of nano-scale Ni particles into anode



Pillai et al., *J Power Sources* 185 (2008) 1086-1093

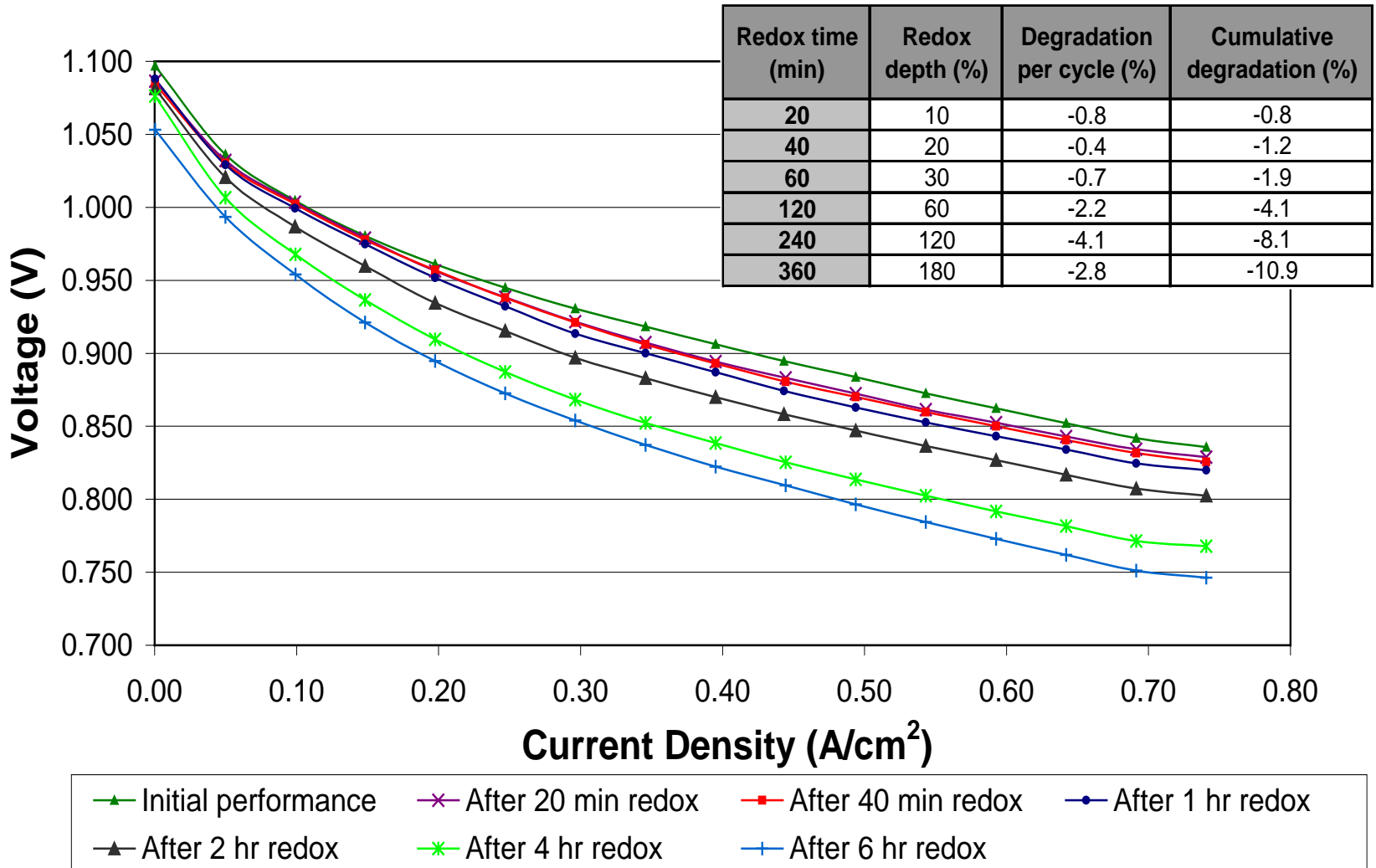
Gao, Barnett, et al., submitted

- Selection of best infiltrate/scaffold combinations
- Performance and long-term stability validation
 - Accelerated testing and modeling

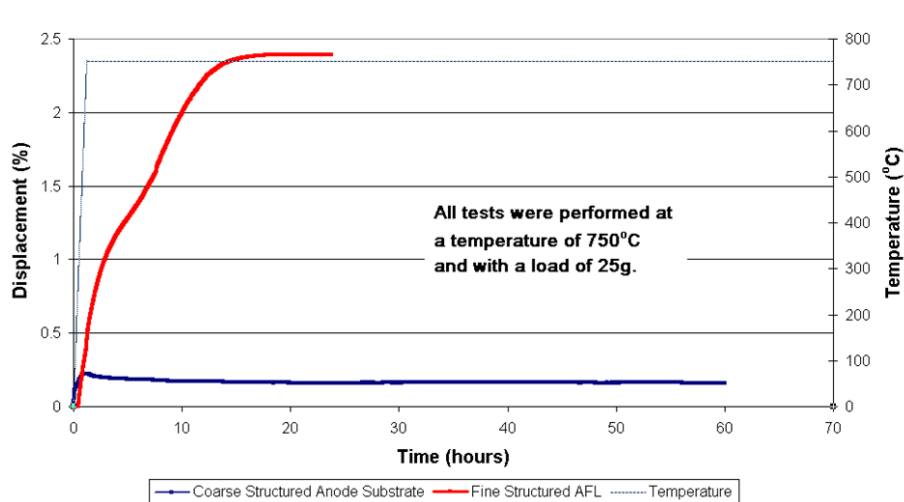
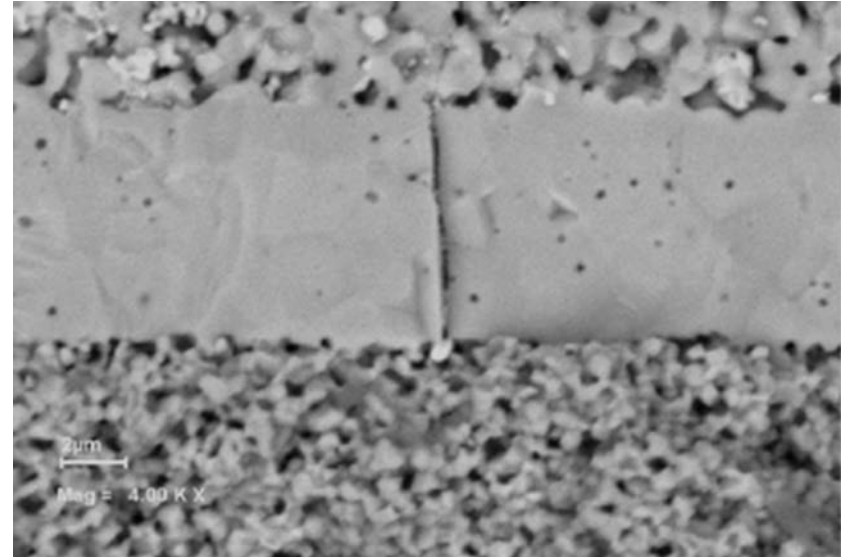


Railsback, J. G., Gao, Z. & Barnett, S. A. *Solid State Ionics* 274 (2015) 134-139

Call et al., *PCCP* 18, 13216-13222 (2016)



- Nickel in the anode expands 69% by volume upon oxidation to nickel (II) oxide
- Sarantaridis *et al* showed numerically that mechanical failures occur by different mechanisms and result in different allowable anode expansions before failure for different SOFC cell architectures
- Anode-supported cells fail by tensile cracking of the electrolyte and may tolerate very limited anode expansion using 7-8 um electrolyte
- Redox tests of baseline cells showed electrolyte cracking in SEM posttest analysis



- Ni-YSZ anode support and anode functional layer has porosity of 15-25% as prepared and 35-45% reduced
- Thermomechanical analysis of pressed bars with AFL microstructure showed that upon re-oxidation:
 - Anode substrate does not change measurably in bulk dimensions due to the nickel content, porosity and microstructure
 - Anode functional layer (AFL) expanded by more than 2%

- Objective
 - Major cell material improvements, breakthroughs and cost reduction achievements from Task 2.1 will be validated and incorporated into the improved production cells through extensive cell manufacturing process development
- Approach
 - Explore cell fabrication boundary for cell size and thickness for various stack design approaches.
 - Computational thermo-mechanical modeling will be further developed and expanded for the analysis of various cell designs to improve compliance and reliability during manufacturing and normal operating conditions.
 - Cell geometry, including aspect ratio, will be cost-benefit-analyzed and defined.
 - Various cell component design parameters will be evaluated to identify the optimum cell configuration for system operation.
- Work Plan
 - A new baseline cell technology will be established based on inputs from Task 2.1
 - After meeting cell performance and endurance criteria, a sufficient number of cells will be produced for assembly for the technology stacks and the 2-5-kW validation stack

Work Scope Tasks 3, 4, and 5

- **Goals**

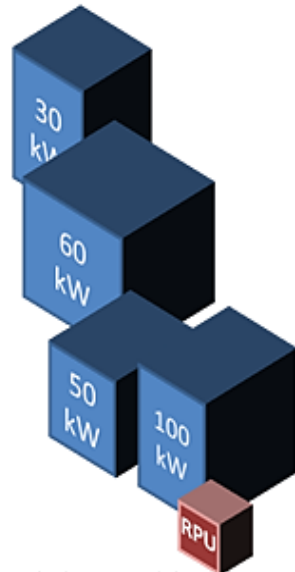
- Develop a transformational hot-swappable stack that enables low-cost, densely packaged SOFC systems.
- Demonstrate performance of stack with integrated system elements at 2-to-5 kW power level for ≥ 1000 hours of operation.
- Develop factory and integration cost estimates that undercut DOE's cost goals for SOFC plants.

- **General approach**

- Investigate incorporating system level elements (heat exchangers, oxidizer, anode gas recycle) into the Innovative stack assembly.
- Focus component designs amenable to high volume, low cost fabrication.
- Reduce installation and maintenance costs significantly
- Aim for **reducing \$/kWdc, not just increasing W/cm²**
 - $>2x$ reduction in \$/kWdc is a plausible target

Each integration of BOP into the Modular Power Block (MPB) resulted in a number of benefits

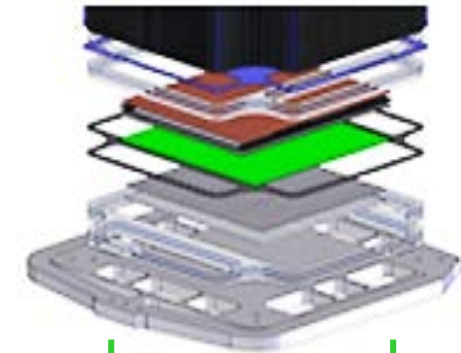
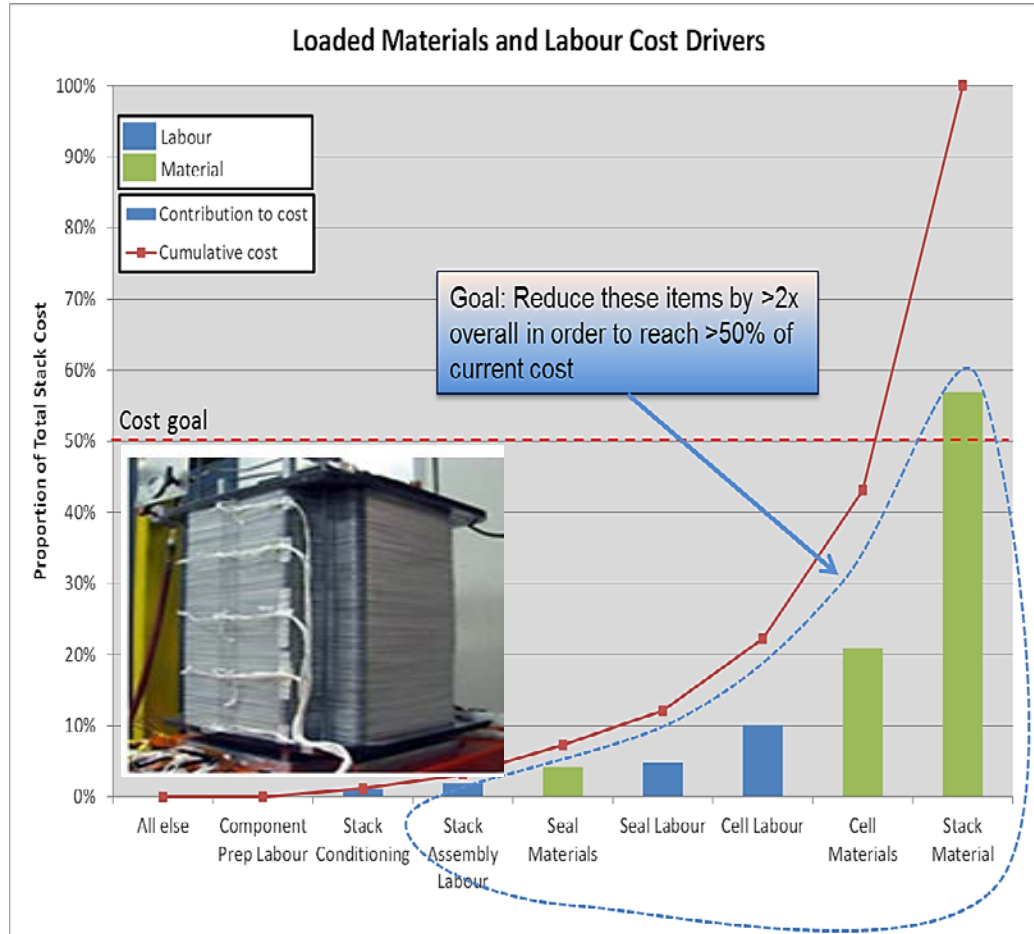
- Improved cell thermal performance
- Reduced chrome poisoning
- Increased power density and decreased parasitic losses
- Reduction in plant footprint, material costs, and capital costs



MODULE (kW)	STATUS	Level of Integration	WIDTH (in)	DEPTH (in)	HEIGHT (in)	Volume (ft ³)	Vol % vs. 60kW	Pwr Dens % kW/ft ³
30	Built	No Integration. Single Stack or Tower	64.0	64.0	96.4	228	58%	.132
60	Built	Quad Base, Fuel Radiator HX, Elec. Series Towers	90.5	86.0	87.6	394	100%	.152
50	In Test	60 Plus: Cat. Ox/HX & Reformer	59.5	76.5	69.7	184	47%	.272
100	In Mfg	50 Plus: Anode Recup., Desiccant Regen HX, Ceramic Start-up Heaters	61.5	69.9	91.5	228	58%	.438
100 (RPU)	Proposed	Stack-Level Integration of all Hot System Processes	36	25	36	19	<5%	5.25

SOFC system power density, kW/ft³ > 5

- Design activities will build upon cost reduction development activities from DE-FE0026093

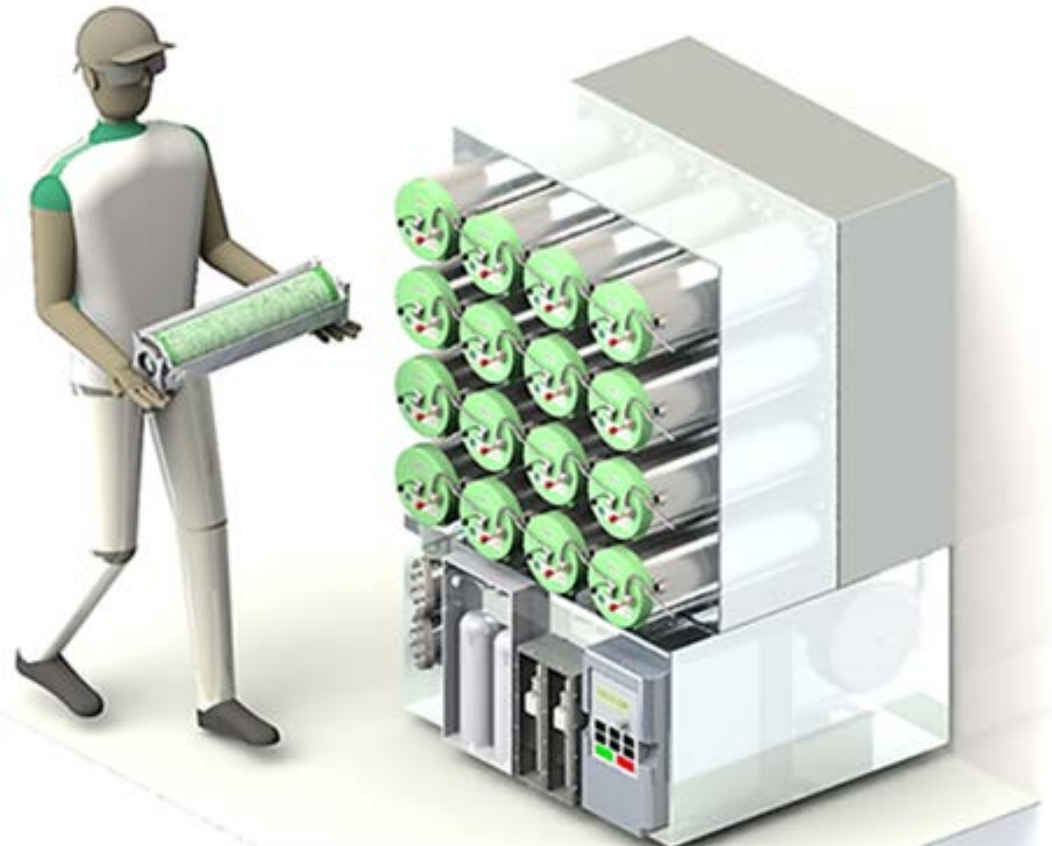


stack material reductions

70% reduction of required seal material



- Serviceable by a single technician, minimal tooling
- No heavy equipment required during maintenance
- Hot-swappability minimizes number of shutdowns during plant lifecycle
- Reduction in equivalent forced outage rates (EFOR)
- Lower \$/kW, Higher kW/ft³



Objective

- Validate the advanced cell architectures and stack design features developed under Tasks 2.0 and 3.0.

Test Plan

- Fabricate and test (@ NOC) a 2-5 kW stack (RPU)
- Test duration for ≥ 1000 hours to demonstrate the performance and stability improvements of the integrated stack system
- Lead-up activities include testing of reduced cell-count (250 W to 500 W) to prove-out the cell / stack design features and manufacturing processes developed
 - Validate CFD models to iteratively arrive at the optimum stack design
- Test stand modifications will be made, as necessary, to accommodate the new stack architecture interfaces

- A factory cost model will be developed for RPU
 - Will include capital costs, depreciation and maintenance costs
 - Will include labour estimates and allowance for labour efficiency and yield
 - Will include representative overhead costs
- Quotes will be secured for components at target volumes
 - Start at 250 kW/yr volumes to avoid costs that are only feasible at higher volumes
 - Extend cost exercise up to 250 MW/year to show potential and identify roadblocks to large volumes
- Estimates of installation and maintenance costs will also be developed