Front-End Engineering Design Study for Retrofit Post-Combustion Carbon Capture on a Natural Gas Combined Cycle Power Plant Award Number: DE-FE0031842 NETL Federal Project Manager: Carl Laird

Abhoyjit S. Bhown, Ph.D. Program Manager, Advanced Generation and CCS

February 23, 2022

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Acknowledgment

Acknowledgment

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Agenda

- Project Overview Electric Power Research Institute
 - Structure
 - Timeline
 - Team
 - Deliverables
- Project Background and Scope California Resources Corporation
 - Project background and commercial drivers
 - Elk Hills Power Plant Site
- FEED Study Fluor Corporation
 - Econamine FG+SM Background and Experience
 - Process Description and Application to Project Site
- Confidential Session
 - Fluor and CRC only
 - CRC only
- Conclusion Electric Power Research Institute

Project Overview

- Title: Front-End Engineering Design Study for Retrofit Post-Combustion Carbon Capture on a Natural Gas Combined Cycle Power Plant
- Project Period: October 1, 2019 February 28, 2022 (29 months, ~10 quarters)
- Funding: \$8,644,807 = \$6,915,845 (Federal) + \$1,728,962 (Cost-Share)
- Spent through Dec 31, 2021: \$8,520,345 (80% Federal, 20% cost-share)
- Federal Project Manager: Carl Laird
- EPRI: Abhoyjit Bhown (PI), Adam Berger, Des Dillon
- CRC: Kenneth Haney, Christopher Kolar
- Fluor: Satish Reddy, Timothy Simonson, John Gilmartin
- Overall Goal: Conduct FEED study for capturing 4,000 t CO₂/day at CRC's 550 MWe NGCC Elk Hills Power Plant using Fluor Econamine FG+SM aqueous amine technology. The captured CO₂ will be used by CRC for enhanced oil recovery or storage in fields adjacent to the power plant.

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Project Structure

Task 1 – Project Management and Planning

Task 2 – Feed Scope

 Objective is to develop design basis document (FEED Scope) to be used by Fluor under Task 3

Task 3 – Feed Study

Objective is to develop FEED document as defined in SOPO-1

Feed Package = Feed Scope (Task 2) + FEED Study (Task 3)

Project Timeline

| | | _ | Oct 1, | 2019 | - Feb 2 | 28, 202 | 22 (~10 |) Quar | ters) | | |
|---|------------|------------|--------|------|------------|---------|---------|--------|-------|------------|------------|
| | Q1 | Q2 | Q3 | Q4 | Q1 | Q2 | Q3 | Q4 | Q1 | Q2 | Q3 |
| Task 1.0 - Project Management and Planning | | | | | | | | | | | |
| Milestones | | | | | | | | | | | |
| Finalize Project Management Plan | \diamond | | | | | | | | | | |
| Feed Package Submitted | | | | | | | | | | \diamond | |
| Final Report Submitted (90 days post close) | | | | | | | | | | | \diamond |
| Task 2.0 – FEED Scope | | | | | | | | | | | |
| Milestones | | | | | | | | | | | |
| Project Design Basis Package | | \diamond | | | | | | | | | |
| Task 3.0 – FEED Study | | | | | | | | | | | |
| Subtask 3.1 – Design and Engineering of Primary Plant Systems | | | | | | | | | | | |
| Subtask 3.2 – Constructability, Cost, and Supporting Systems | | | | | | | | | | | |
| Milestones | | | | | | | | | | | |
| Design of Primary Plant Systems | | | | | \diamond | | | | | | |
| Engineering FEED Package | | | | | | | | | | \diamond | |
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Deliverables

| Deliverable Title | Due Date |
|--|--|
| Project Management Plan | Due 30 days after award with updates resulting from negotiations. Revisions to the PMP shall be submitted as requested by the NETL FPM (Complete) |
| FEED Package (SOPO-1) | Due to the NETL FPM by end date of project |
| Final Report - A non-proprietary publicly disclosable overview of the sections of the FEED Study | Due 90 days after the completion of the project per the Federal Assistance Reporting Checklist and instructions |





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CRC's Elk Hills Oil & Gas Complex is Primed For CCS



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A "Real" Solution: CalCapture Implements California's Carbon Goals at Elk Hills

- ✓ Significant immediate emissions reductions
- ✓ Clean, safe, affordable energy and reliable base-load power generation for California
- Prolific economic impact on local, state and national economies
- NGCC power plant capture technology deployment

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Source: California Air Resources Board

1.5 Million Tonnes of CO₂ Stored per Year



1 Pending adoption of a CCS protocol into CA Cap & Trade

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Carbon Credits are a Strong Economic Enabler



CalCapture: Strategic Plan

| | | 20 | 20 | | | 20 | 21 | | | 20 | 22 | |
|---------------------------|----|----|----|----|----|----|----|----|----|----|----|----|
| | Q1 | Q2 | Q3 | Q4 | Q1 | Q2 | Q3 | Q4 | Q1 | Q2 | Q3 | Q4 |
| Regulatory and Permitting | | | | | | | | | | | | |
| - CEQA/EIR/CUP's | | | | | 7 | 7 | | | | | | |
| - UIC Expansions | | | | | 7 | | | | | | | |
| - LCFS | | | | | Z | 7 | | | | | | |
| - 45Q | | | | | 7 | 7 | | | | | | |

Additional Upside

- Cap & Trade Escalation
- Clean Power Contract

CalCapture with EOR Cuts Oil Production Emissions to Far Below all California Imports

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CA Average

M_{exico}

CRC Average

V

Data from CARB 2019 Calculation of Production/Transport Crude Carbon Intensity * Elk Hills Crude produced with CO_2 EOR and CCS (Utilization ~.34 tonnes CO_2 per bbl oil)

South America

Nigeria

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CalCapture Economic Impacts will be Significant

| Study by IMPLAN Group, LLC. Data reflects | Annual | Millions of \$ | |
|--|--------|-----------------|-------|
| US impacts per project design estimates 6/2020 | Jobs | Economic Output | Taxes |
| Capture Plant (3 yr. construction) | 3,890 | 1,624 | 222 |
| Capture Plant (20 yr. operation) | 217 | 1,454 | 197 |
| EOR (CAPEX/OPEX) 20 years | 857 | 3,249 | 421 |

\$6.3B Total Economic Output \$840 million Taxes

ΙΜΡΙΛΝ



CalCapture FEED: 1/2020 – 2/2022

US Department of Energy

- CRC Awarded Funding for Carbon Capture FEED
 - \$7mm federal award
- Partners
 - FLUOR Amine Absorption Technology/Construction
 - Electric Power Research Institute (EPRI) Lead Applicant and Project Manager



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CO₂ Sourcing Alternatives Reviewed 2018 - Present

EHPP Capture

- Absorption Amines
- o Fluor Econamine FG+
- \circ Shell Cansolv
- Mitsubishi Heavy Industries
- \circ Compact Carbon
- $\circ \ \text{Linde}$
- \circ Next Decade
- Absorption Other
- \circ General Electric Chilled Ammonia

Adsorption

- $\circ \mathsf{ARI}$
- Svante (Inventys)

Membranes

Membrane Technical Research

Fuel Cells

 $_{\odot}$ Fuel Cell Energy



Alternative CO₂ Sources

- Refinery Renewable Diesel
- H₂/CO₂ ATR from NATGAS
- Oxy Combustion
- Bio Fuels (3 Technologies)
- Ammonia Plants
- Ethanol Plants
- Gas Processing

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Fluor Technology Selection

Amine Absorption

- ➢ Highest TRL
- ➢ Ready to scale

Fluor's Econamine FG+SM

- > 30+ commercial Econamine FG operating plants
- \geq 15 years of operating experience on a gas turbine
- Solvent maintenance system provides for low air emissions and waste generation
- Low solvent make-up



© Fluor, Used with Permission Demonstration Plant, Germany **FLUOR**



Elk Hills Power Plant

- Commissioned 2003
- Dual GE 7FA combustion turbine generators (CTG's).
- Two supplementary-fired heat recovery steam generators (HRSG's)
- GE D11 Steam Turbine Generator (STG)
- Selective Catalytic Reduction (SCR) systems for the control of NO_x , CO & VOC.
- Natural gas fuels CTG's/Duct Burners.



Image from CRC

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Fluor Capture Plant FEED Study



FEED

- ✓ Class III Estimate(+/-15%)
- ✓ Validated ~8% Savings
- ✓ Black & Veatch OE Review

Optimization

- Steam integration
- "Fit for Purpose" PLA
- Contracting Strategy

Next Steps

- Alternatives Benchmarking
- FOA 2660 Application
- Open/Closed Book EPC



Value Engineering: Steam Integration with Power Plant

Modify existing steam turbine to allow capture plant to draw 100% of regeneration steam requirement

- Eliminates natural gas fired boiler packages
 - More CO₂ captured from power plant
 - Higher CO₂ emissions avoided
- Frees up capacity in existing cooling tower
 - Eliminates some Wet Surface Air Coolers
- CAPEX and OPEX Savings
 - Adds ~450k lb./hr steam
 - Parasitic load addition 30-35MW
 - Turbine modifications cost TBD
- GE Engagement

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- Phase 1 Feasibility complete
- Progressing to Phase II Design



CRC Energy Transition Positioning



STABLE CONVENTIONAL ASSETS PROVIDE STRONG FINANCIAL FOUNDATION

- Low decline, conventional assets with integrated infrastructure
- Disciplined capital allocation with strong financial foundation
- Robust Free Cash Flow generation
- Potential enhanced oil recovery through CalCapture in the future

PROVIDING LOW CARBON INTENSITY ENERGY TO CALIFORNIA

- Delivering lowest carbon intensity hydrocarbon production of the top 100 US producers¹
- Incorporating and developing renewable solar opportunities | 45 MW BTM^{2,3} solar in active development | Up to 1,000 MW FTM³ solar in early-stage development

ADVANCING LOW CARBON FUTURE THROUGH CARBON TERRAVAULT

- Anticipate establishing one or more CCS projects that inject CO₂ into depleted underground reservoirs
- Dedicated business group and leadership structure
- Identified up to 1 BMT of potential permanent CO₂ storage capacity³
- Targeted Early-Stage Development Goals: 1st Injection by 2025⁴ | 200 MMT permitted by 2025 | 5 MMTPA injection by 2027³



(1) According to Clean Air Task Force, June 2021. (2) 45 MW of BTM solar represents opportunities with SunPower in CRC owned land. (3) Source: Internal estimates. (4) First injection date dependent on permitting, capture facility type and the structure, financing and ownership of the project which have not yet been negotiated.

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Front-End Engineering Design Study for Retrofit Post-Combustion Carbon Capture on a Natural Gas Combined Cycle Power Plant

Summary of Key Findings



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Background

- FEED study objective determine technical and economic feasibility to retrofit post-combustion carbon capture on 550 MW commercially operating NGCC power plant at Elk Hills
- Carbon capture unit based on Fluor's proprietary Econamine FG PlusSM (EFG+) technology
- Designed to recover 4,000 MTPD CO₂ from flue gas streams produced by two existing CTGs along with flue gas produced from new boiler package

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Block Flow Sketch for Post Combustion Carbon Capture at Elk Hills



Block Flow Sketch for Post Combustion Carbon Capture at Elk Hills



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ZERO 2023

Flue Gas Design Basis

| | CTG1 | CTG2 | New Boiler | Total |
|------------------------------------|-----------|-----------|------------|-------------|
| Total Available Flue Gas (MMSCFD) | 990 (Max) | 990 (Max) | 166 | 2,146 (Max) |
| Total Flue Gas Draw (MMSCFD) | 630 - 941 | 630 - 941 | 157 | 1,728 |
| Percent Flue Gas Draw (%) | 63% - 95% | 63% - 95% | 95% | - |
| Temperature (°F) / Pressure (psig) | 210/0.0 | 210/0.0 | 298 / 0.0 | 218 / 0.0 |
| N ₂ / Ar (vol%) | 73.75 | 73.75 | 69.78 | 73.39 |
| O ₂ (vol%) | 11.59 | 11.59 | 2.50 | 10.76 |
| H ₂ O (vol%) | 10.31 | 10.31 | 17.46 | 10.96 |
| CO ₂ (vol%) | 4.35 | 4.35 | 10.25 | 4.89 |
| CO (ppmv dry) | < 0.1 | < 0.1 | < 61 | < 5.7 |
| NO _x (ppmv (dry) | < 1.9 | < 1.9 | < 2.5 | < 1.8 |
| NH ₃ (ppmv dry) | < 5.9 | < 5.9 | < 6.1 | < 5.9 |

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Site Specific Design Requirements

- ▶ EFG+ unit designed to capture 90% of CO₂ from flue gas to unit
- On-stream factor of 95% with 40% turndown
- Solvent make-up storage capacity of 30 days
- Water minimization is required
 - Priority to significantly reduce water requirement associated with Pre-FEED design
 revised cooling strategy to reduce water make-up
- Modularization highly investigated to reduce site construction hours
 - Nearest viable port is Port of Stockton (225 miles from project site)
 - Module envelope limited to 120 ft (L) x 20 ft (W) x 18 ft (H) at 250,000 lb
 - Conclusion was that modularization was not beneficial due to transport window limitations





Project Site Location

- Capture plant to be placed on site located just to the south of EHPP
- Project site was a location of a different process unit which has been demolished
 - Owner will bathtub site to remove subsurface interferences

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- Seismic Zone 3
- Design dry / wet bulb temperatures: 92°F / 66°F



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Water Minimization

- Initial design was a 100% water-cooled plant
 - Quench water from DCC used to supplement cooling water make-up
 - RO Unit provided to treat and recover 65% of cooling tower blowdown
 - Water consumption was still too high to meet CRC requirements
- Consideration given to 100% air-cooled plant
 - Design ruled out due to hot ambient conditions
 - Required significantly large number of air cooler bays leading to higher CAPEX
 - Hot Summer conditions would result in inefficient plant operation leading to higher OPEX
- Final design based on hybrid air and water-cooled solution

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Hybrid Air and Water-Cooled Approach



<u>Air Coolers</u> Services that do not need to be below ambient conditions + Approach

Courtesy Alfa Laval <u>Wet Surface Air Coolers</u> Large Duty Process Water Services <u>Cooling Tower</u> For streams impractical to use other methods





Courtesy SPX Cooling

Breakdown of Cooling

PRE-FEED DESIGN

FEED DESIGN



Raw Water Make-up Reduced by 63%



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Steam Supply and Water Recovery

- Dedicated Boiler Packages provided to meeting all CCU steam demands
 - Water tube boiler burns a nominal 550 MMBtu/hr of mixed fuel gas blend provided by CRC
 - Make-up water to Boiler Packages provided from an RO Unit, included within CCU scope
 - RO Unit treats blowdown from Cooling Tower and WSACs to recover 65% of the water
 - No material change to EHPP performance with inclusion of dedicated Boiler
 Packages versus use of steam extraction





Steam and Water System Block Flow Diagram



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ZERO 2023

Other CCU Utility Requirements

- Instrument and plant air
 - CCU equipped with dedicated instrument and plant air package
- Raw water, potable water, nitrogen and fuel gas
 - Provided by CRC at the CCU battery limits
- Electrical power (~35 MW)
 - Provided through the existing CRC Elk Hills transmission system
 - New 115 kV line brought from existing CRC substation to new CCU substation where it is stepped down to 13.8 kV / 4160 V / 480 V







Simplified EFG+ Process Flow Sketch

- Combined flue gases routed to DCC (C-101) for cooling
- ▶ 90% of CO₂ in flue gas chemically absorbed in the Absorber (C-201)
- CO₂ loaded solvent is routed to Stripper (C-301) where CO₂ is desorbed
- ▶ Low pressure CO₂ product from C-301 overhead routed to compression and dehydration



TREATED GAS

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Overall H&MB

| | | Combined Flue Gas Feed | DCC Excess Water to CT Basins | Treated Flue Gas to Atm. | Treated RO Water to Abs. | Compressed CO2 Product |
|---|---------------------------------------|---------------------------|----------------------------------|-----------------------------|-----------------------------|---------------------------|
| | Temperature | 218 °F | 123 °F | 95 °F | 105 °F | 130 °F |
| | Pressure | 13.8 psia | 60 psia | 14.0 psia | 14.2 psia | 2,314 psia |
| | <u>Composition</u> | | | | | |
| | H ₂ O | 11.0 mol% | 100 mol% | 5.9 mol% | 100 mol% | 526 ppmv |
| | CO ₂ | 4.9 mol% | 40 ppmw | 0.5 mol% | 0.0 mol% | 99.9 mol% |
| | N ₂ / Ar | 73.4 mol% | 10 ppmw | 81.6 mol% | 0.0 mol% | 184 ppmv |
| | 0 ₂ | 10.8 mol% | 3 ppmw | 12.0 mol% | 0.0 mol% | 13 ppmv |
| | СО | 4.7 ppmv | 0.0 mol% | 5.2 ppmv | 0.0 mol% | 0.0 ppmv |
| | NO _x (as NO ₂) | 1.8 ppmv | 0.0 mol% | 1.9 ppmv | 0.0 mol% | 0.0 ppmv |
| | SO ₂ | 0.6 ppmv | 0.0 mol% | 0.0 ppmv | 0.0 mol% | 0.0 ppmv |
| | Total Flow Rate | 1,200,101 SCFM | 401 gpm | 1,079,627 SCFM | 10 gpm | 8,355 lbmol/hr |
| | Total Mass Flow Rate | 5,359,820 lb/hr | 198,450 lb/hr | 4,799,460 lb/hr | 4,970 lb/hr | 367,510 lb/hr |
| F | LUOR | | T UDIC | | | NET ZERO 2023 |

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Rendering of CCU Facility



End of FEED Cost Cutting Measures

- Towards end of FEED, Fluor and CRC teams brainstormed and evaluated several potential cost cutting measures
- Those with positive outcome have been incorporated into final FEED design
- One item is still under evaluation
 - Reconsider extracting steam from EHPP and eliminate boiler packages
 - Reduces power plant output by an estimated 35 MW
 - Frees up significant portion of EHPP cooling load
 - Apply freed up cooling load to CCU and eliminate up to 5 of the 8 WSACs
 - Fluor has roughly estimated a potential savings of up to \$35-\$45 MM







Final Capital Cost Estimate

| Plant Area | Total Installed Cost |
|--------------------------------|----------------------|
| CO ₂ Capture Island | \$387 MM USD |
| CO ₂ Compression | \$61 MM USD |
| Utility Systems | \$267 MM USD |
| Balance of Plant | <u>\$33 MM USD</u> |
| TOTAL | \$748 MM USD |

- ▶ Estimate accuracy → ±15%
- Lump Sum EPC with performance guarantees and liquidated damages
 - **FLUOR**_®

- ► Forward escalation included from 2020 to project completion →\$39 MM
- Project execution based on Union labor
- Sales Tax included at \$8.5 MM
- Pre-commissioning, commissioning, Startup and Performance Testing included
- Contingency included at \$57 MM
- Licensor fee excluded
- Mass excavation of site excluded





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Elk Hills CO2 Recovery Project Econamine FG PlusSM

EPCC Summary Schedule

| EED Complete Francescom Francesco |
|--|
| EED Complete Post FEED RFOs, RFPs, update Priorig C-RC: Obtaming Project Franciscog Michael Sproton EEX Auground for FNTP Intel Completion EEX Auground for FNTP Intel Completion MR42 |
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| |
| Site Prep & Grading |
| 1st Pile (Start of Construction) |
| |
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| Substation Energized Energize Substation |
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| Pre-Commissioning / Commissioning |
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| Start-up & Performance Testing Start-up & Test |
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| Schedule Contingency |
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| Month -> 13 -12 -11 -10 -9 -8 -7 -6 -5 -4 -3 -2 -1 0 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 22 23 24 25 26 27 28 29 30 31 32 33 34 35 36 37 38 39 40 41 42 43 44 45 46 47 48 49 |
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Elk Hills CO2 Recovery Project Econamine FG PlusSM

EP Summary Schedule



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Elk Hills CO2 Recovery Project Econamine FG PlusSM

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CC Summary Schedule





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Agenda

- Project Overview Electric Power Research Institute
 - Structure
 - Timeline
 - Team
 - Deliverables
- Project Background and Scope California Resources Corporation
 - Project background and commercial drivers
 - Elk Hills Power Plant Site
- FEED Study Fluor Corporation
 - Econamine FG+SM Background and Experience
 - Process Description and Application to Project Site
- Confidential Session
 - Fluor and CRC only
 - CRC only
- Conclusion Electric Power Research Institute

Non-Confidential

EPRI

Project Highlights

- 4,000 t CO₂/day captured: 3,325 t/day from CTGs + 765 t/day from auxiliary boiler
 - 90% CO₂ captured from flue gas entering EFG+ process
 - 74% capture of total CO₂
- CO₂ to be used for enhanced oil recovery or saline storage adjacent to power plant
- Economic drivers exist for commercial deployment
- This FEED study could lead to world's first full-scale, commercial deployment of carbon capture on NGCC power plant, and can be readily duplicated at other NGCCs across the world

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