



NOVEL FLOW SHEET FOR LOW ENERGY CO₂ CAPTURE ENABLED BY BIOCATALYST DELIVERY SYSTEM

Kick off Meeting

Project: DE-FE0012862

DOE-NETL; Pittsburgh, PA.

November 22, 2013

OUTLINE

- Project Overview
- Observations
- Approach and Analysis
- Objectives
- Preliminary Data
- Tasks & Milestones
- Project Structure/Organization
- Schedule
- Budget Summary
- Decision points/ Success Criteria

PROJECT OVERVIEW

Participants, Duration, Funding



■ Project awardee and subcontract TEA:



WorleyParsons

resources & energy

■ Enzyme Supply:



■ Fabrication and Instrumentation:



■ Duration: 36 months (Oct 2013 to Sept 2016)

■ Funding:

DOE Funding:	\$ 2,999,560
Akermin Cost share:	\$ 2,066,889 (40.8%)
Total Project:	\$ 5,066,449

PROJECT TEAM

 **FUNDING AGENCY**
Andrew Jones
 NETL Project Manager

 **Dr. Alex Zaks**
 Program Manager

 **Mr. John Reardon**
 PI/Project Manager

- Task 1**
Project Management and Reporting
- Task 2.2**
Modify Lab-reactors to support BDS testing
- Task 3**
Optimize Novel Flow Sheet
- Task 5**
Engineering of Bench Unit Mods
- Task 6**
Procure and Fabricate Bench Unit Mods
- Task 7**
Restart and Operate Bench Unit at NCCC
- Task 8.2**
EH&S Risk Assessment

Project Division of Labor by Task
 AOI 1B1 Novel Flow Sheet for Low Energy CO₂ Capture Enabled by Biocatalyst Delivery System

 **Dr. Tracy Bucholz**
 Co-PI, Polymer Systems

 **Dr. Matthew Hulvey**
 Analytical Chemistry

 **Mr. Sean Black**
 VP-Business Development

 **Mr. Vladimir Vaysman**
 Worley Parsons

- Task 2.1**
Identify critical process parameters
- Task 2.3**
Optimize BDS production using lab-CLR
- Task 2.4**
Optimize BDS in lab-CLR, varied column internals

- Task 4**
Preliminary TEA
- Task 8.1**
Final TEA

THE PROBLEM: REDUCE COST OF CAPTURE

DOE Goal: 90% capture, less than 35% increase in COE (20.6 \$/MWh ICOE)

Key issues/opportunities:

■ Incremental Power Plant Capital

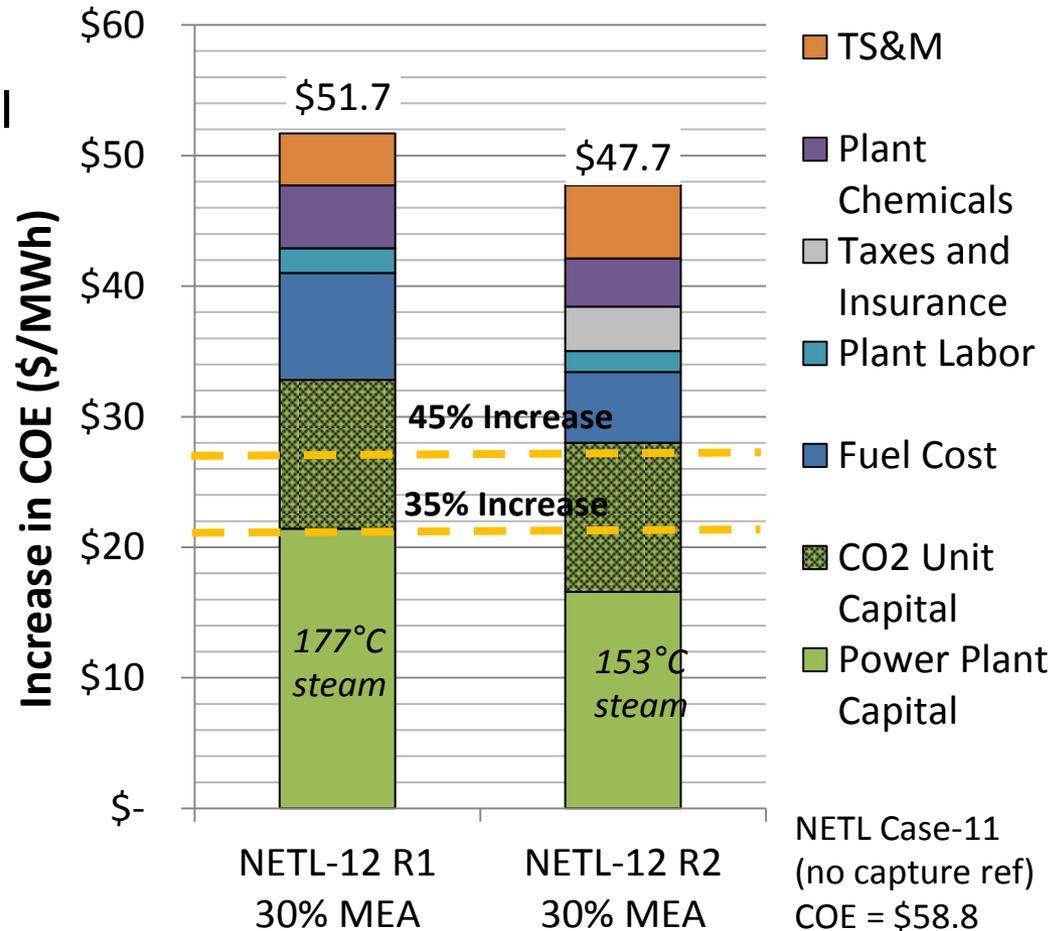
- Equivalent Work of Steam (re-boiler duty and temp.)
- Parasitic Power (compression, fans, pumps)

■ CO₂ Capture Unit Capital

- Absorber
- Stripper
- OH Wash
- DCC (flue gas cooler)
- Cross-Exchanger

■ Increased Fuel & Chemicals

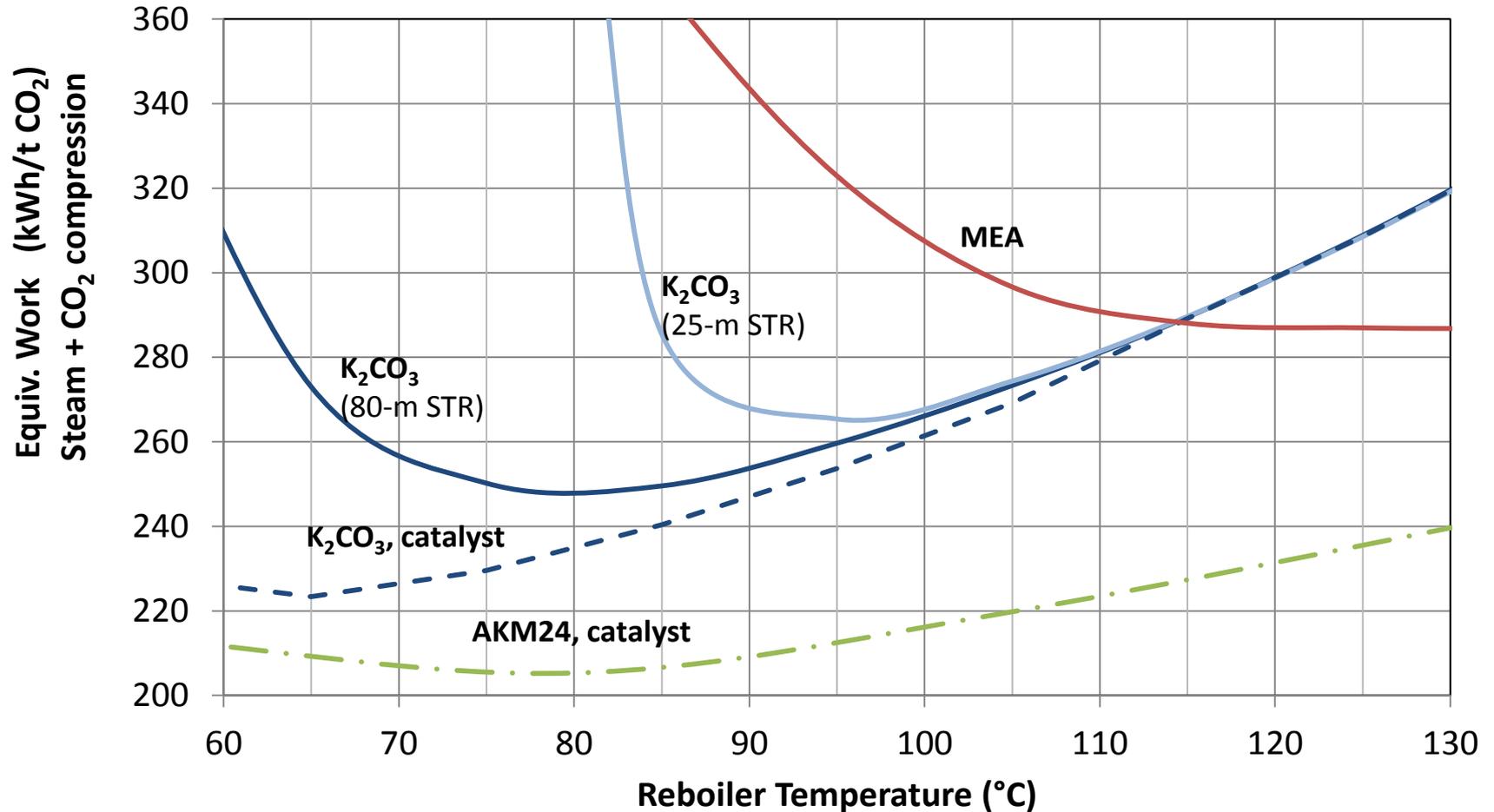
- Parasitic Power driven



Improving energy efficiency is key, impacts many areas;
reducing extraction steam temperature improves efficiency/cost;

EQUIVALENT WORK OF STEAM + COMPRESSION

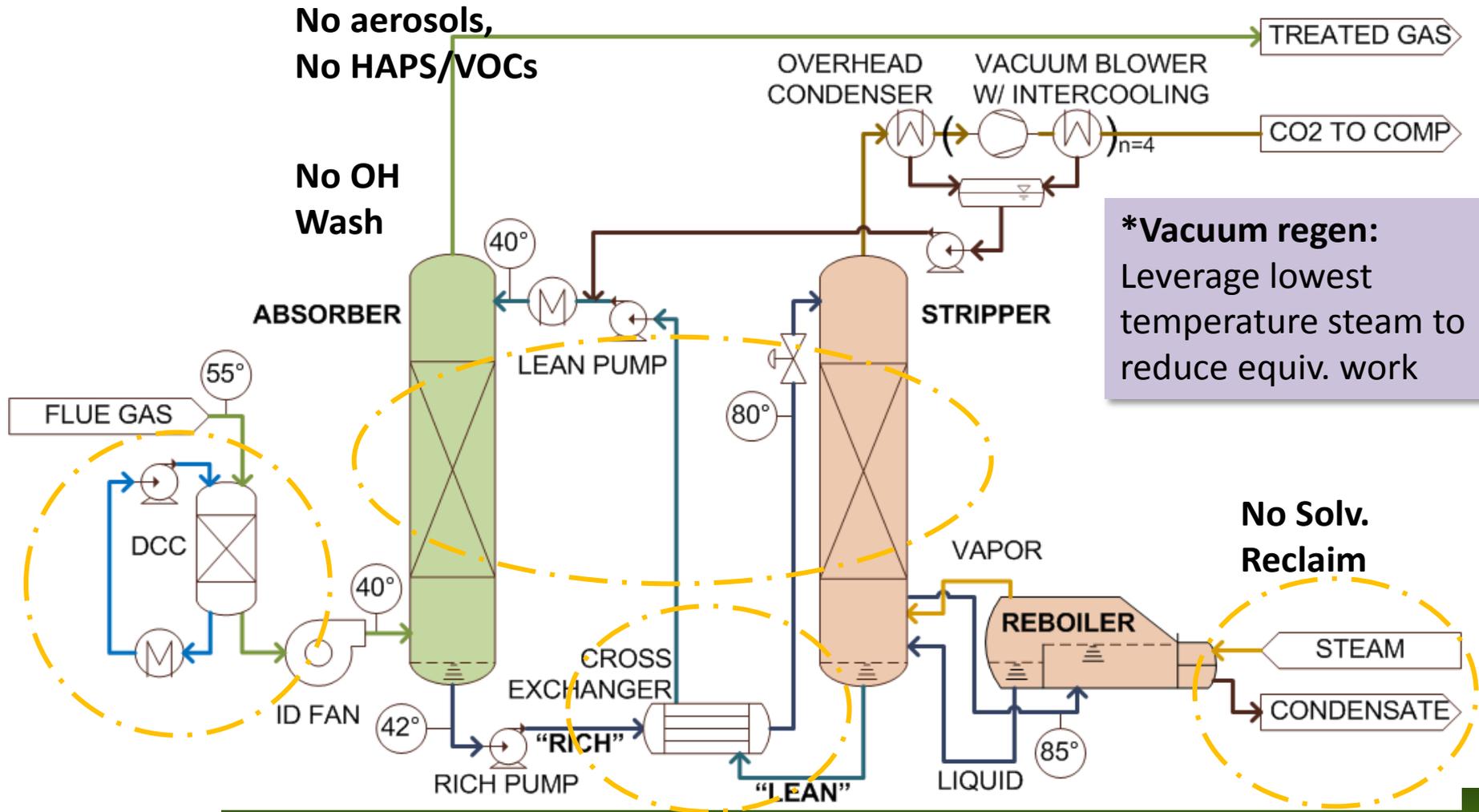
30% MEA (~83 kJ/mol), 20% K_2CO_3 (~28 kJ/mol) and AKM24 compared



Minimum equivalent work benefits from solvent and catalyst

APPROACH: BIOCATALYST ENABLED SOLVENTS

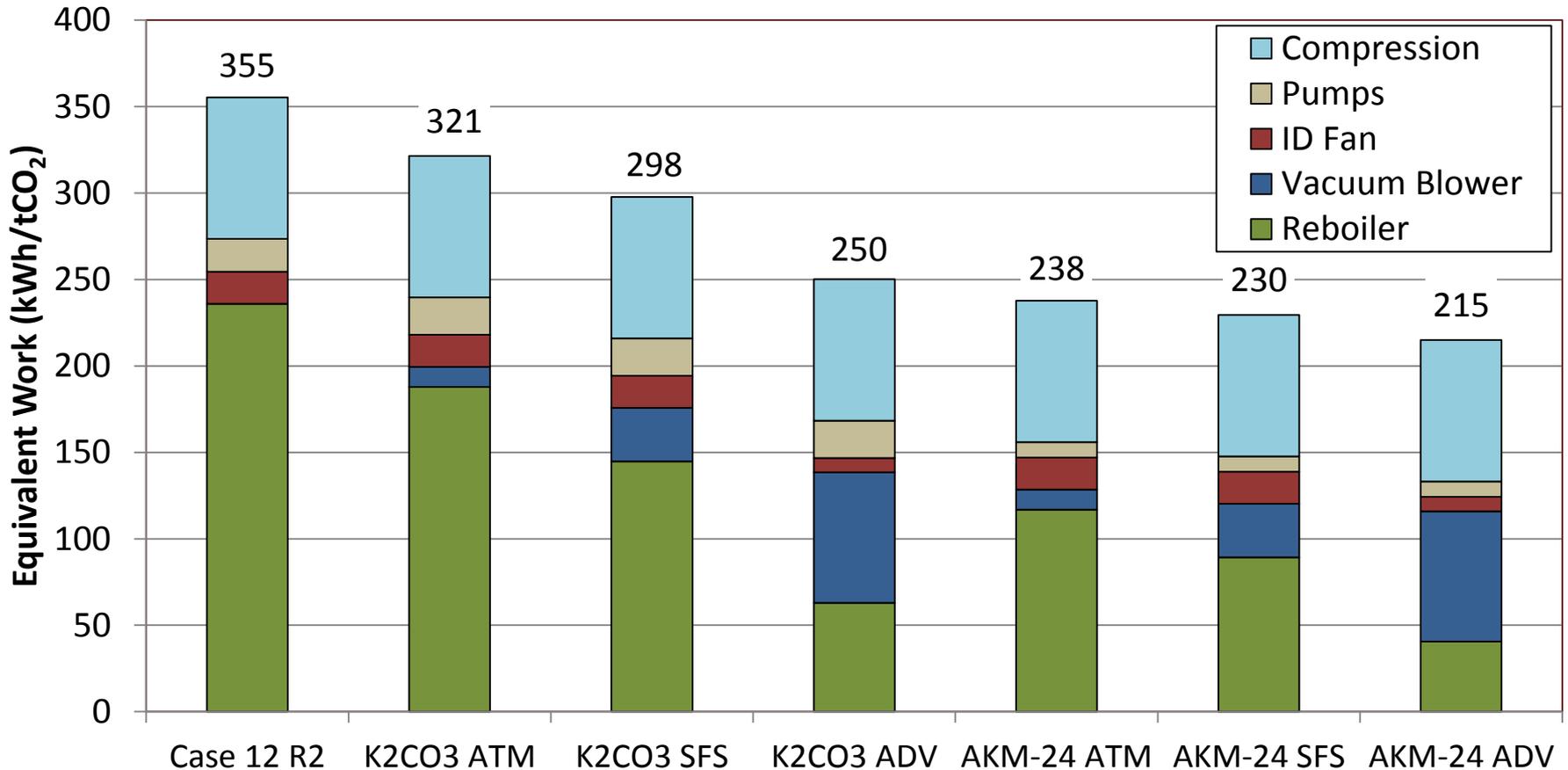
Biocatalyst enabled AKM₂₄ solvent; improvement is proposed in circled areas



Low energy, low volatility solvent AKM₂₄ enabled by biocatalyst system

LOWER EQUIVALENT WORK

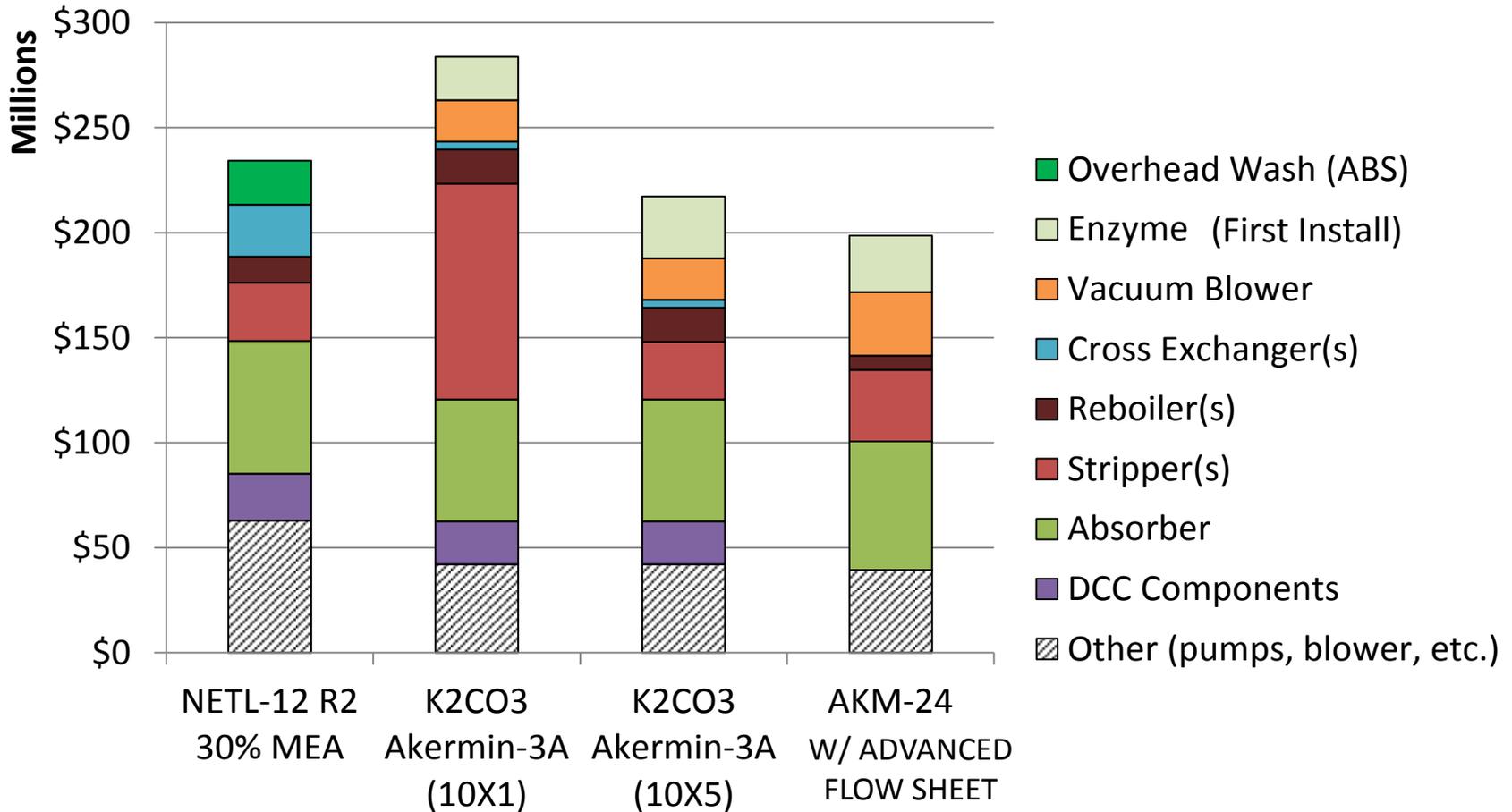
Net parasitic power depends on steam temperature (efficiency) and reboiler heat duty



AKM-24 with advanced flow sheet ~ 37% reduction in equivalent work and potentially ~30% reduction in capital relative to Case 12 (30% MEA)

PRELIMINARY CAPITAL COST ESTIMATES

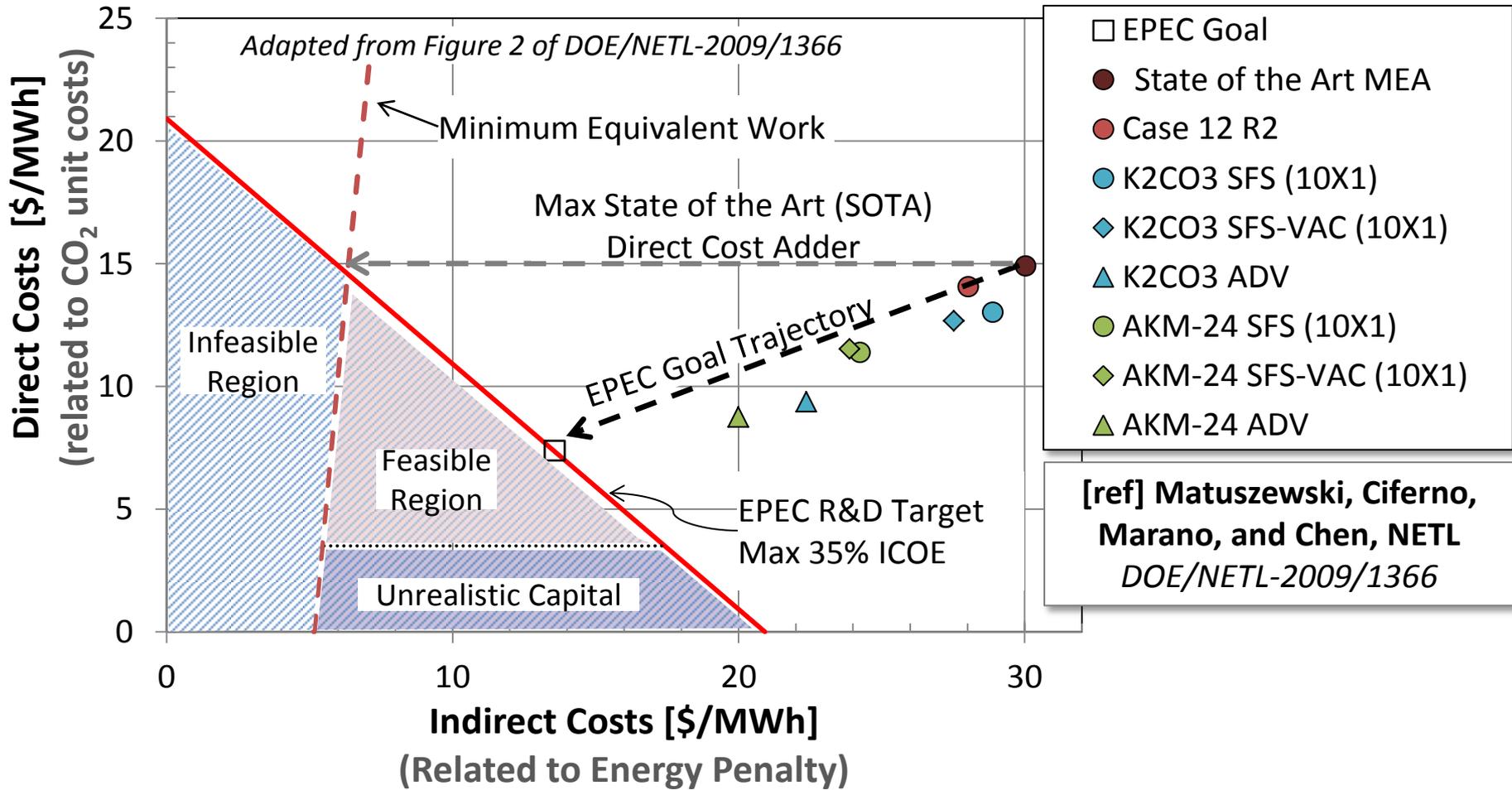
Data from previous project used for advanced flow sheet cost estimation
 For 3A Case: ("Absorber Reduction Factor" X "Stripper Reduction Factor")



Biocatalyst enhancement benefits absorber and stripper costs

PROGRESS TOWARDS DOE GOAL

Two Paths: Reduction of Direct (CO₂ Unit) Costs and Indirect (Energy Penalty) Costs



Combination of AKM-24 with isothermal flow-sheet enabled by catalyst starts to approach DOE EPEC cost goal for CO₂ capture

PROJECT OBJECTIVES

- Reduce cost of capture by >30%
- Achieve parasitic power: 200 to 220-kWh/t CO₂
 - lowest grade steam for solution regeneration
- Reduce capital costs >20%
 - Catalyst deployed throughout system, reduce and eliminate equipment
- Demonstrate *on-stream* catalyst replacement
- Deploy non-volatile, environmentally benign solvent with significantly higher CO₂ absorption capacity than 20% K₂CO₃
- Complete six-month demonstration at the National Carbon Capture Center (NCCC) using coal combustion flue gas
- Complete techno-economic and engineering merit study w/WP
- Demonstrate progress toward DOE long-term goals

90% CO₂ capture is assumed for all DOE goals

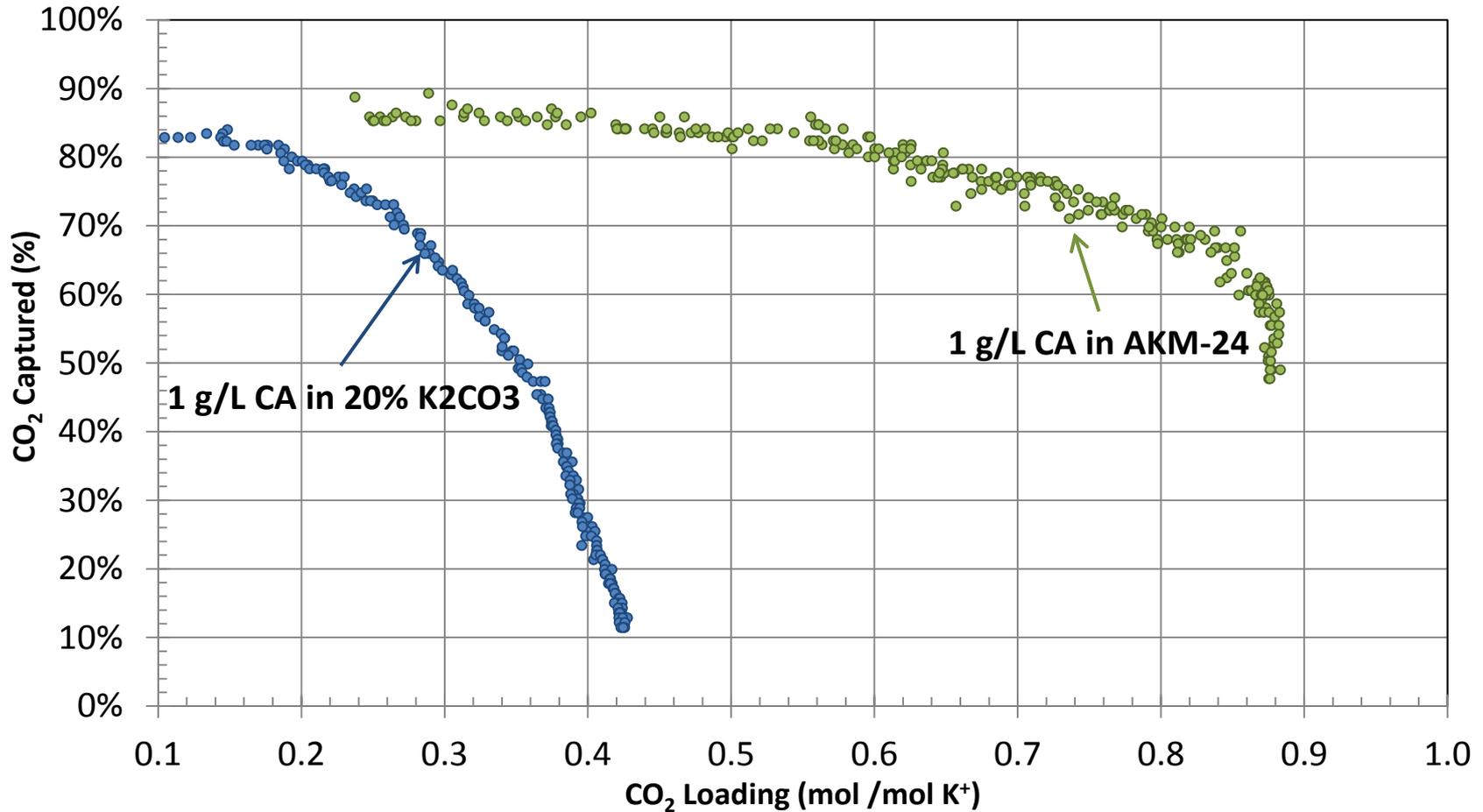
SECOND GENERATION SOLVENT: AKM 24

AKM-24, high performing solvent:

- ✓ Non-volatile
- ✓ Thermally stable
- ✓ Highly water-soluble
- ✓ Low molecular weight
- ✓ High CO₂ loading
- ✓ Low regeneration energy
- ✓ Low EH&S risks

CA PERFORMANCE IN 20% K_2CO_3 & AKM-24

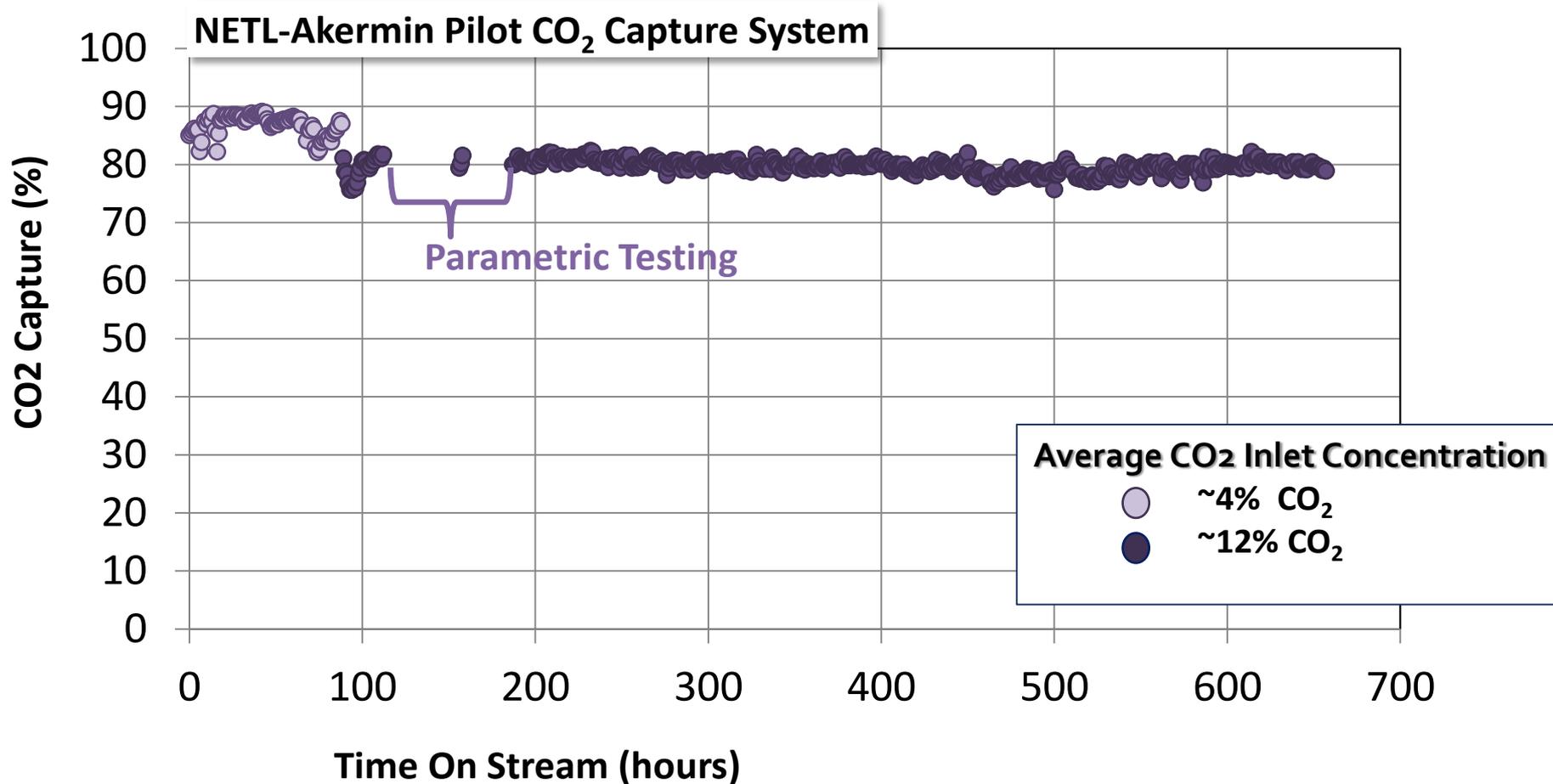
SPR – 400 SCCM gas flow w/ 15% CO_2 , 25 mL/min solvent, 25 °C, 1 psig, 65 g packing



Rate enhancement is extended over a greater range of CO₂ loading for AKM-24 compared to K₂CO₃

AKM-24 PILOT PLANT DATA W/ BIOCATALYST (10/31/13)

Time on-stream, data at design flow ($31.5 \text{ Nm}^3/\text{hr}$, 275 LPH), $X_{C,Lean} \sim 0.28$



~650 hours on stream demonstrates stability, performance in AKM24

SCOPE OF WORK

- Optimize production of the novel Biocatalyst Delivery System.
- Demonstrate consistent long-term performance in lab-prototype closed loop reactors.
- Optimize the isothermal process flow sheet to achieve lowest equivalent work.
- Provide independent techno-economic analysis and EH&S evaluation with third party firms.
- Demonstrate the energy performance and sustained activity over-time using commercially-generated flue gas at a scale of 500 to 1000 standard liters per minute of flue gas feed.

RESOURCE LOADED SCHEDULE—PERIOD (1)

SOPO BREAKOUT SCHEDULE		BP-1						Cost by Task
WBS	DESCRIPTION OF TASK OR SUBTASK	Oct-13	Jan-14	Apr-14	Jul-14	Oct-14	Jan-15	
1.0	Project Management & Planning	a	b					\$ 334,189
2.0	Optimize production of immobilized biocatalyst					j		\$ 1,748,955
2.1	Identification of critical BDS process parameters		c					
2.2	Modify lab-scale CLR to support BDS testing		d					
2.3	Optimize BDS production using lab CLR feedback		e			g	h	
2.4	Optimize BDS in CLR with varied column internals							
3.0	Optimize Flow Sheet, Minimize Eq. Work, Cost							\$ 142,359
3.1	Thermodynamic, kinetic, precip data into Aspen							
3.2	Optimize novel flow sheet with AKM24			f				
4.0	Preliminary Techno-Economic Analysis							\$ 260,623
4.1	Consulting engineering to support TEA							
4.2	Preliminary TEA					i		
5.0	Engineering of Bench Unit Modifications							\$ 312,407
5.1	Engineering and costing of bench unit mod							k
5.2	Bench Unit PHA							l
							BP1 Total	\$ 2,798,533

RESOURCE LOADED SCHEDULE—PERIOD (2)

SOPO BREAKOUT SCHEDULE		BP-2						Cost by Task
WBS	DESCRIPTION OF TASK OR SUBTASK	Apr-15	Jul-15	Oct-15	Jan-16	Apr-16	Jul-16	
1.0	Project Management & Planning							\$ 374,133
6.0	Procurement and Fabrication of Bench Unit Mods							\$ 1,069,251
6.1	Procure bench unit modifications	m						
6.2	Modify Bench Unit			n				
7.0	Comission and Operate Bench Unit at Test Site							\$ 552,151
7.1	Commission and establish baseline				o			
7.2	Parametric and endurance testing with biocat				p		q,r	
7.3	Bench unit decomissioning							
8.0	Final Technology Assessment							\$ 272,381
8.1	Final TEA						s	
8.2	EH&S risk assessment						t	
							BP2	\$ 2,267,916
							Total	\$ 5,066,449

BUDGET SUMMARY: AWARD #DE-FE0012862

Final negotiated budget

NETL AWARD DE-FE0012862					
	Budget Period 1 10/1/2013 - 3/31/2015		Budget Period 2 4/1/2015 - 9/30/2015		TOTAL
	Gov't Share	Cost Share	Gov't Share	Cost Share	
Akermin	\$ 1,516,664	\$ 1,141,801	\$ 1,230,592	\$ 925,088	\$ 4,814,145
Worley Parsons	140,067		112,237		252,304
Total	\$ 1,656,731	\$ 1,141,801	\$ 1,342,829	\$ 925,088	\$ 5,066,449
Cost Share	59.2%	40.8%	59.2%	40.8%	

Akermin is providing >40% cost share

DECISION POINTS/SUCCESS CRITERIA

Budget Period 1

- Successful completion of all BP-1 proposed work
- Preliminary modeling shows < 220 kWh/tCO₂
- Demonstrate 500 hrs @ $> 90\%$ retention of activity w/ one catalyst makeup cycle
- Deploy a non-volatile, environmentally benign solution that doubles CO₂ absorption capacity relative to 20% K₂CO₃
- Submit preliminary Techno Economic Analysis
- Submit fixed cost proposal for bench unit modifications
- Submit and have approved a continuation application for BP-2

DECISION POINTS/SUCCESS CRITERIA

Budget Period 2

- Successful completion of all BP-2 proposed work
- Modified bench unit demonstrates > 2000 hrs on stream
- Final TEA demonstrates > 30% reduction in cost of capture relative to NETL-12
- Final TEA demonstrates potential to achieve DOE target of 90% capture with <\$40/t CO₂
- Submit final Techno Economic Analysis
- Submit EH&S risk assessment
- Submit final report

AKERMIN INC.

Company profile

- **St. Louis-based biotechnology company**
- Developing lower cost, environmentally friendly solutions for CO₂ capture for variety of applications
- Integrating proprietary biocatalyst delivery with various solvent systems



- **DOE/NETL:** *This material is based upon work supported by the Department of Energy National Energy Technology Laboratory under Award Number DE-FE0004228.*
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