

the Energy to Lead

Energy Efficient GO-PEEK Hybrid Membrane Process for Post-combustion CO₂ Capture

DOE Contract No. DE-FE0026383

Shiguang Li, Travis Pyrzynski, James S. Zhou, Howard Meyer,
Gas Technology Institute (GTI)

Miao Yu, *University of South Carolina (USC)*

Yong Ding, Ben Bikson, *PoroGen Corporation (PoroGen)*

Presentation for Kickoff meeting

December 7, 2015

Outline

- > Introduction to team members
- > Project overview
- > Technology fundamentals/background
- > Plans for each budget period

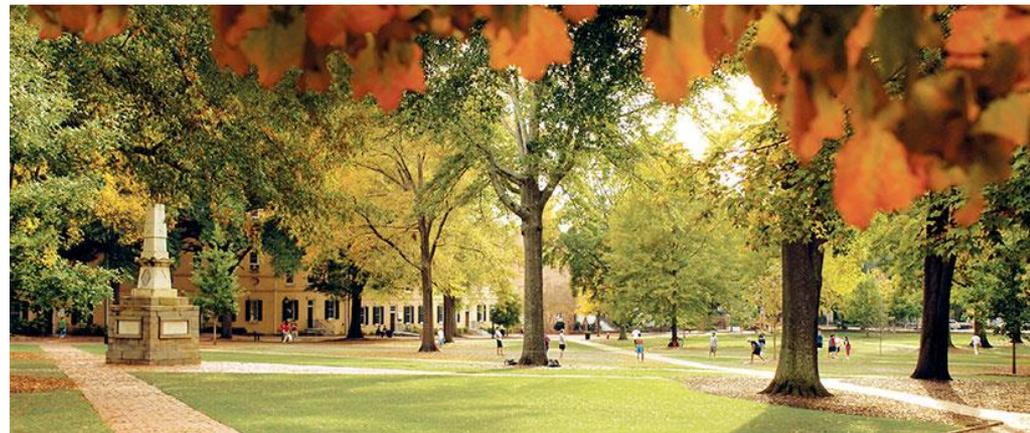
Introduction to GTI and USC



UNIVERSITY OF
SOUTH CAROLINA

- > **Not-for-profit** research company, providing energy and natural gas solutions to the industry since 1941
- > **Facilities**: 18 acre campus near Chicago, 28 specialized labs

- > **Co-educational research university** located in Columbia, South Carolina
- > **Prof. Yu Group**: expertise in thin films, coatings, membranes, absorption and transport mechanisms



Introduction to PoroGen and Trimeric



TRIMERIC CORPORATION

- > **Materials technology** company commercially manufacturing products from high performance plastic polyether ether ketone (PEEK)
- > Products ranging from membrane filters to heat transfer devices
- > Chemical process engineering, R&D, and other technical services
- > Extensive experience on CO₂ processing facilities
- > Several staff members have led carbon capture technoeconomic evaluation projects for the DOE

Project overview

- > **Performance period**: Oct. 1, 2015 – Sep. 30, 2018
- > **Funding**: \$1,999,995 from DOE; \$500,000 cost share
- > **Objectives**:
 - Develop a hybrid membrane process combining a conventional gas membrane unit and a hollow fiber membrane contactor (HFMC) unit to capture $\geq 90\%$ of the CO_2 from flue gases with 95% CO_2 purity at a cost of electricity 30% less than the baseline CO_2 capture approach
- > **Project participants**:

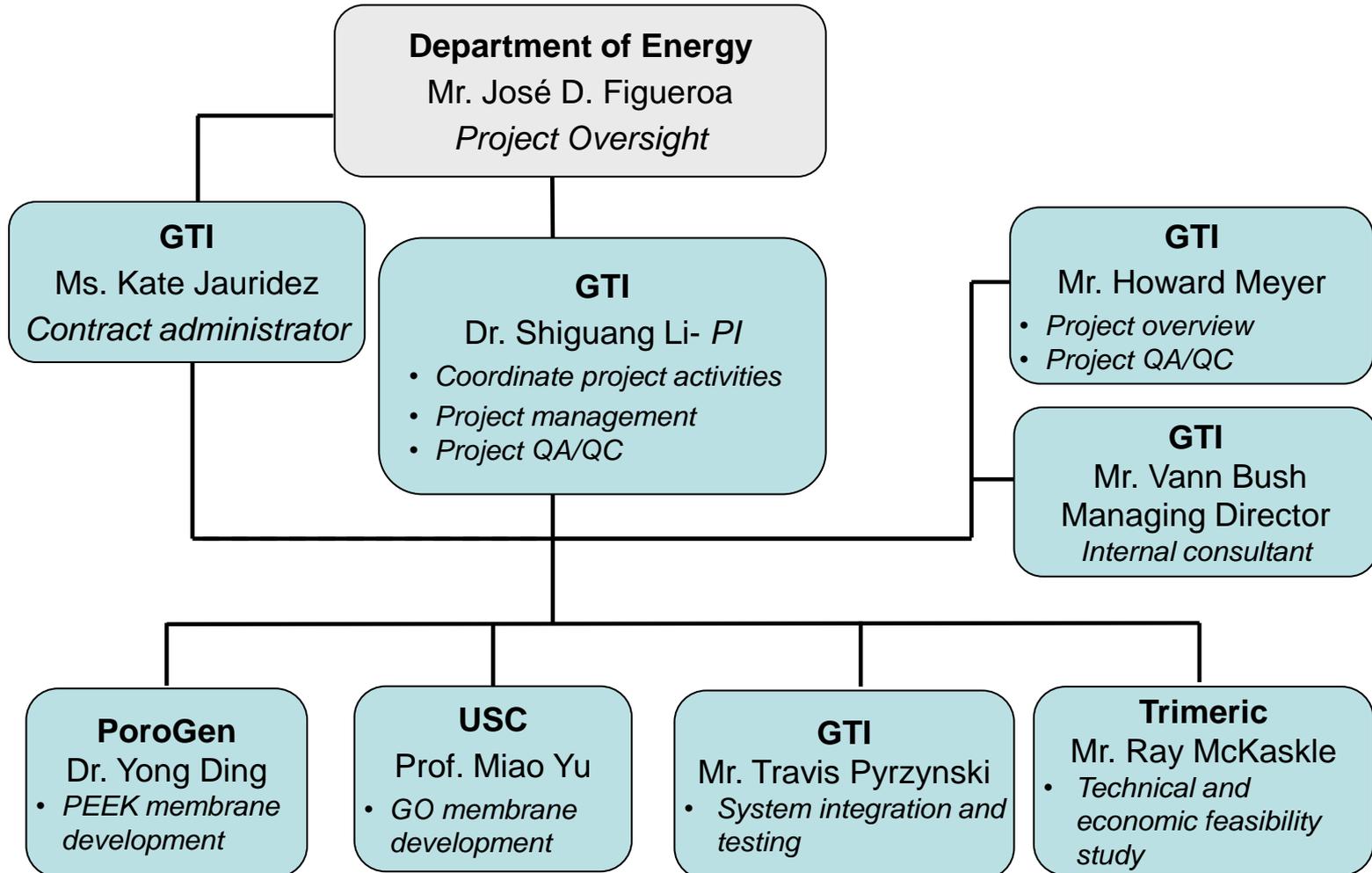


TRIMERIC CORPORATION

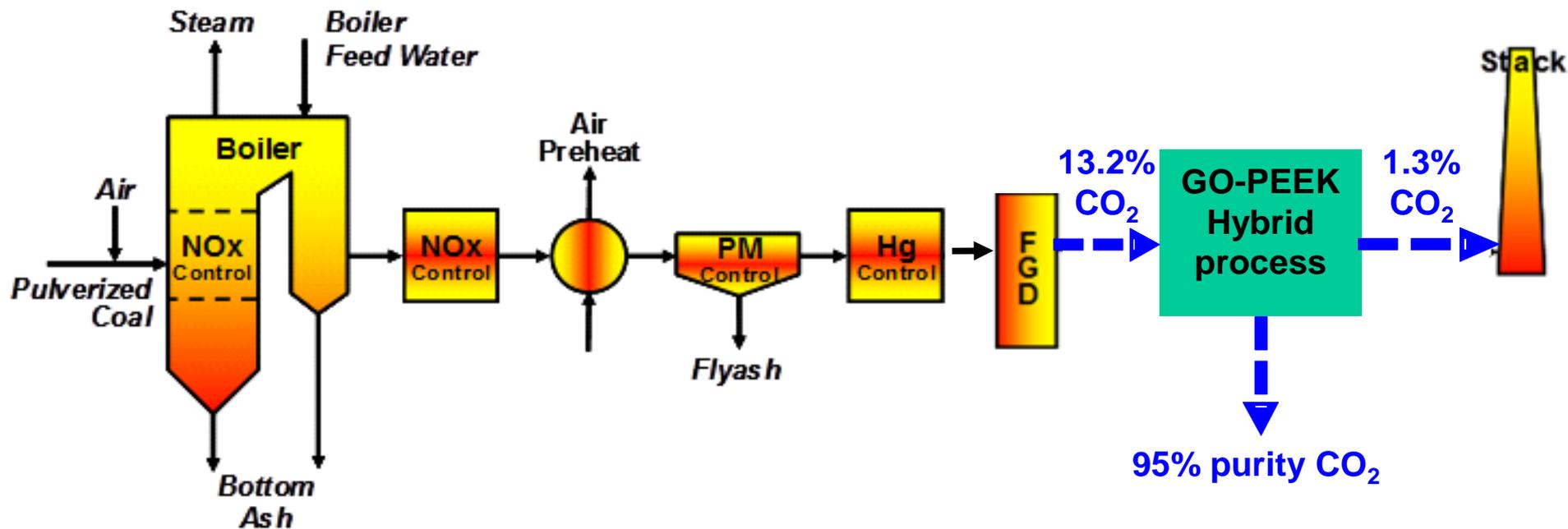
Team member roles

Member	Specific Project Roles
	<ul style="list-style-type: none"> > Project management and planning > Quality control and performance testing for graphene oxide (GO) and PEEK membranes > Construct an integrated GO-PEEK testing system > CO₂ capture testing of the integrated GO-PEEK process
	<ul style="list-style-type: none"> > GO membrane development: CO₂ permeance $\geq 1,000$ GPU; CO₂/N₂ selectivity ≥ 90
 	<ul style="list-style-type: none"> > PEEK membrane development: intrinsic CO₂ permeance $> 3,000$ GPU
	<ul style="list-style-type: none"> > High-level technical and economic feasibility study

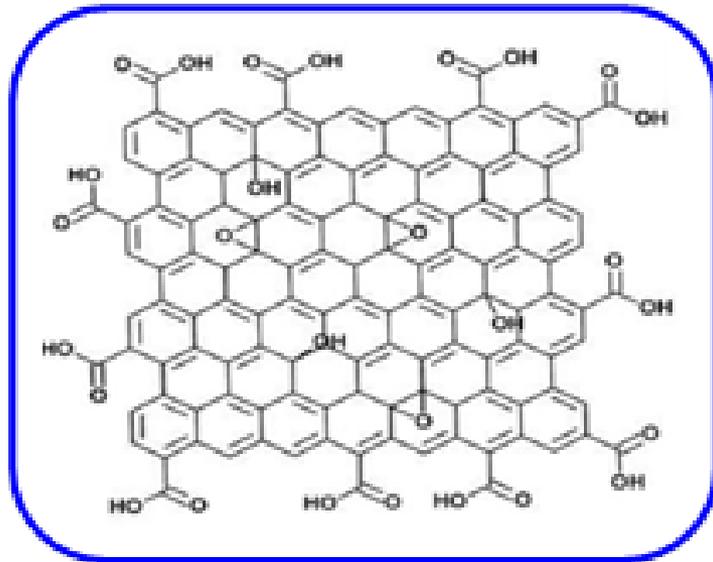
The project organization and structure



Integration with coal-fired power plants: installed downstream of FGD



GO conventional gas membrane process



GO: single-atomic layered, oxidized graphene

GO membrane technology based on our pioneering work published in *Science* (2013, 342 (6154) 95)

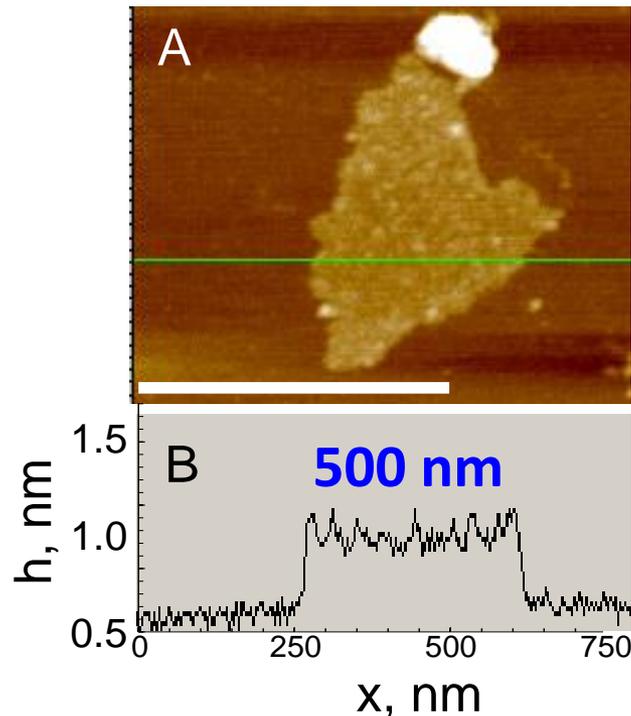


Ultrathin, Molecular-Sieving Graphene Oxide Membranes for Selective Hydrogen Separation

Hang Li *et al.*

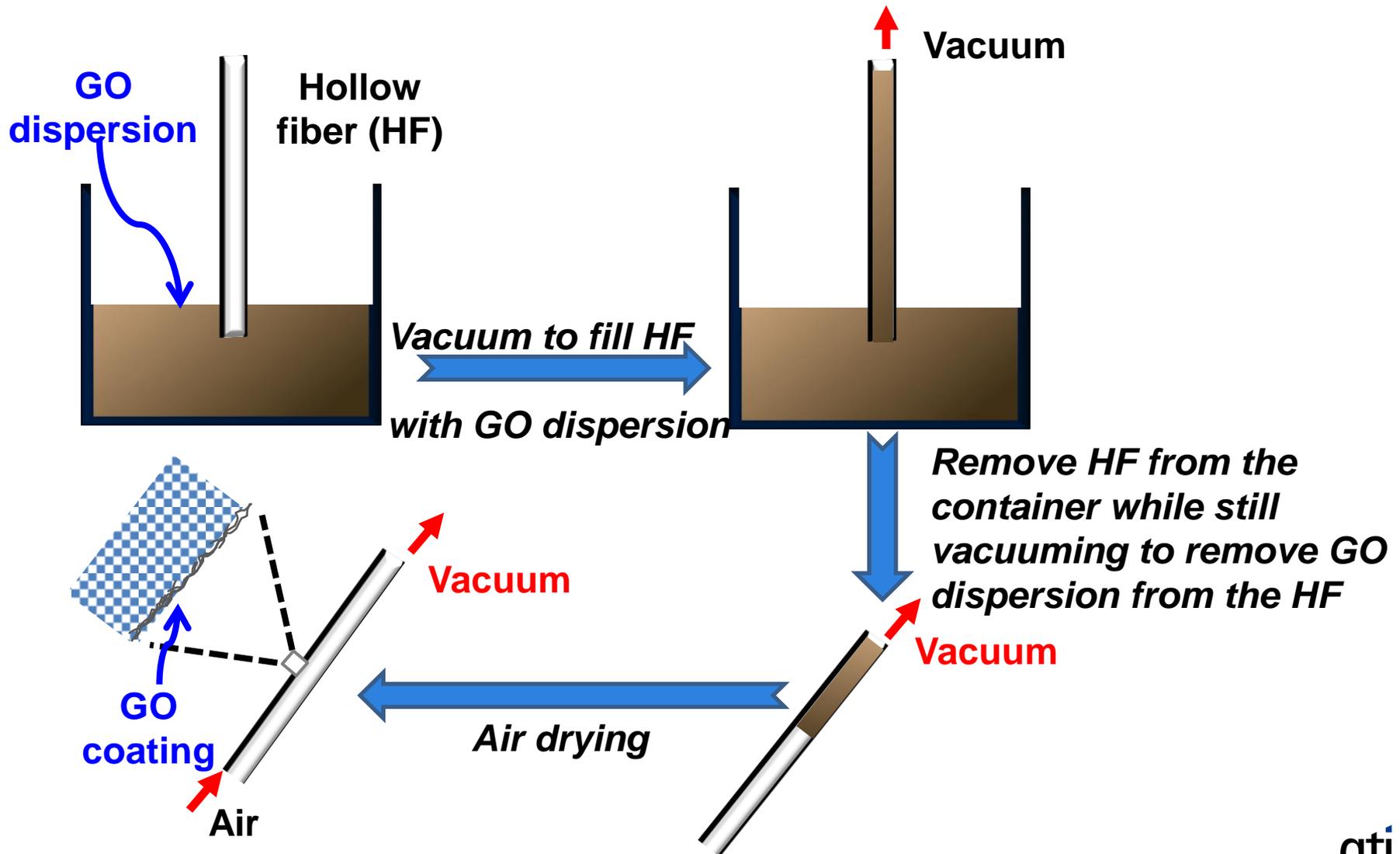
Science **342**, 95 (2013);

DOI: 10.1126/science.1236686

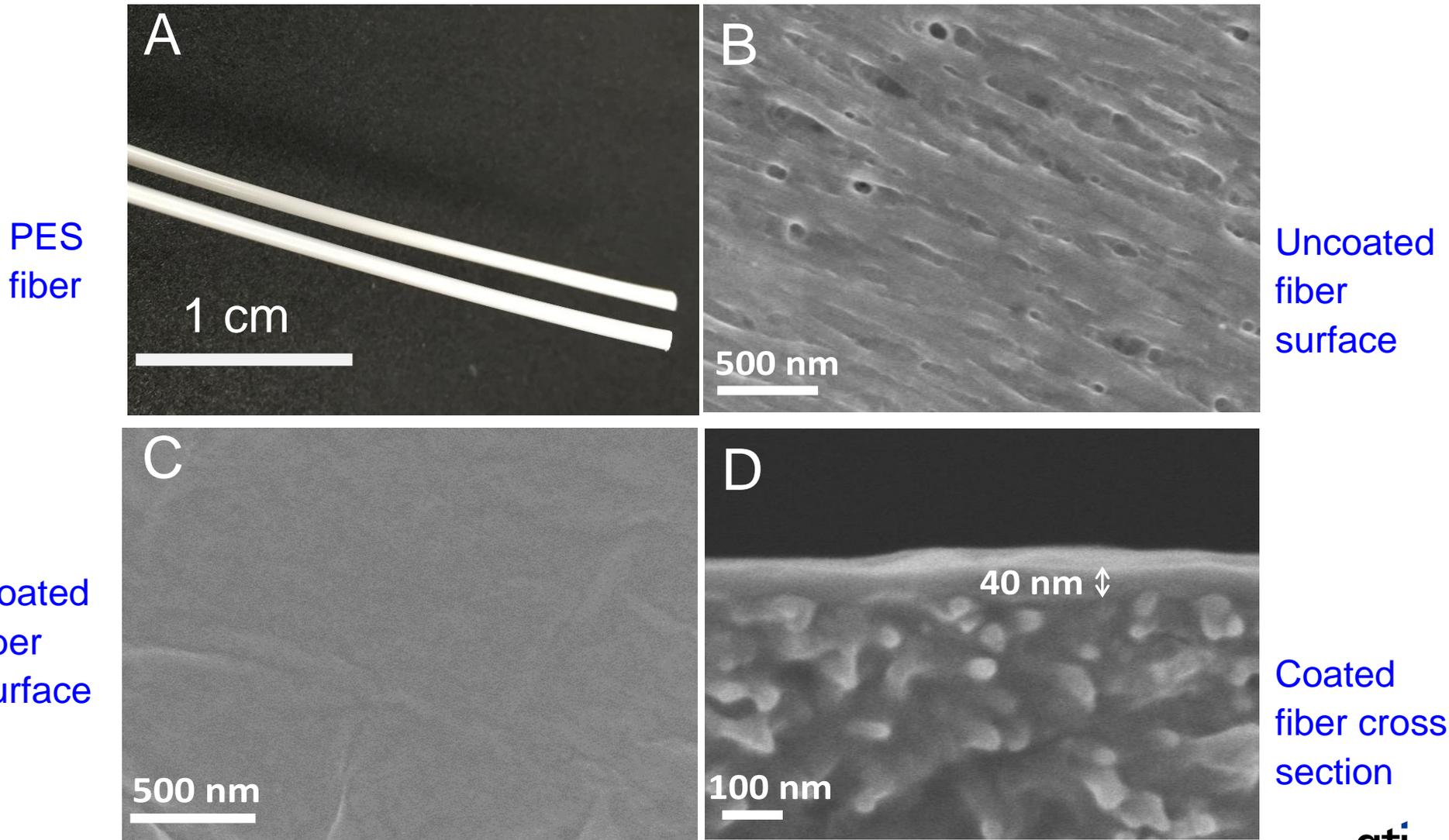


Single-layered GO flake
prepared as thin as 0.7 nm

Procedure developed for coating GO on hollow fiber support towards CO₂/N₂ separation



GO membrane supported on polyethersulfone (PES) hollow fiber as thin as 40 nm

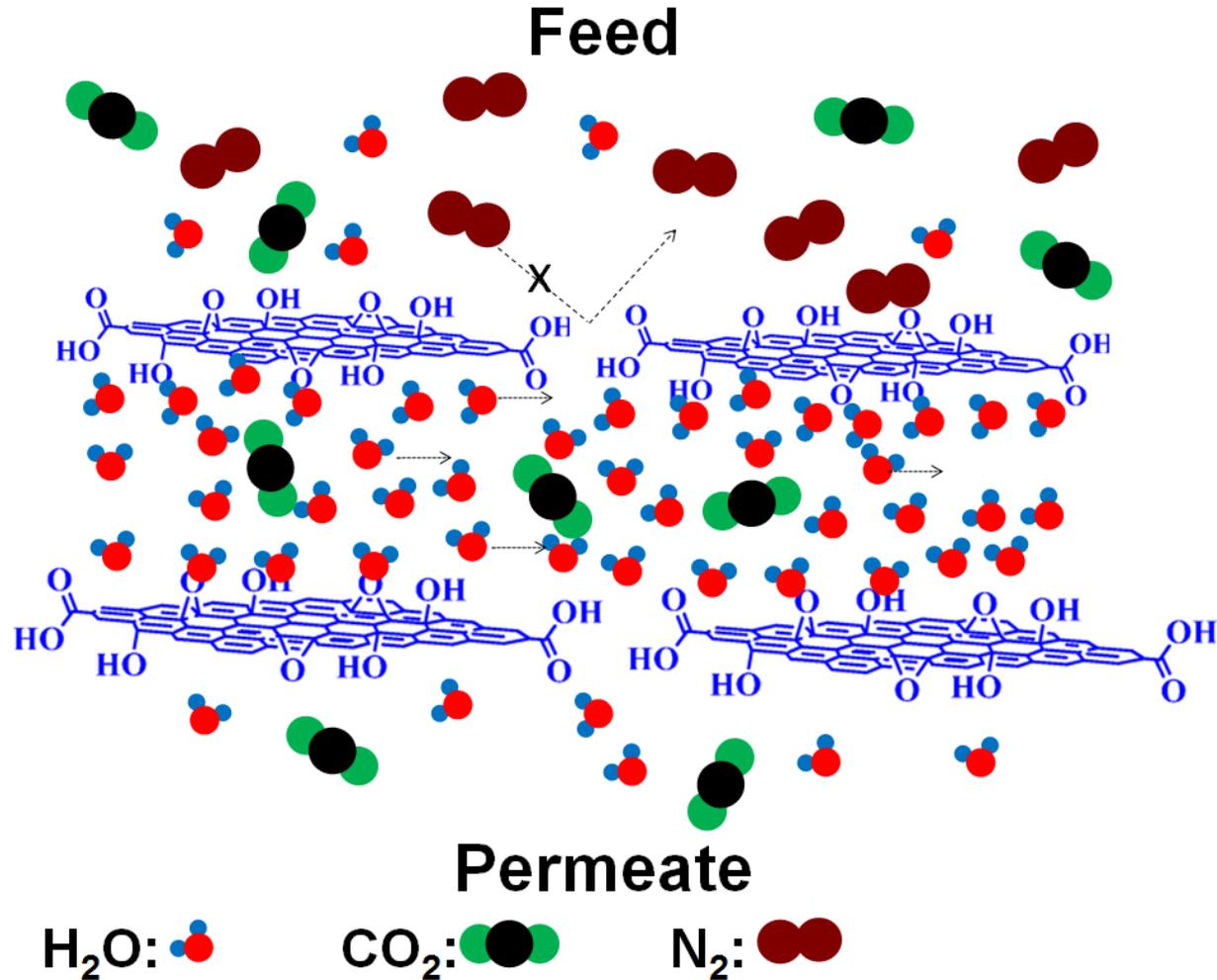


CO₂ permeance of 100 GPU and $\alpha_{\text{CO}_2/\text{N}_2}$ of 49 obtained at 40°C for a humidified CO₂/N₂ mixture

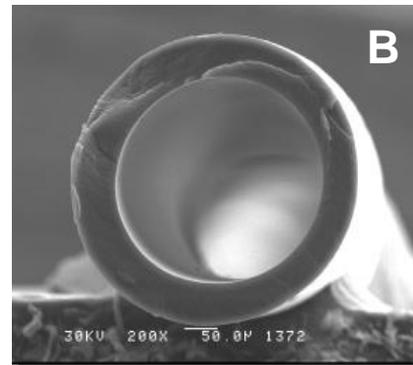
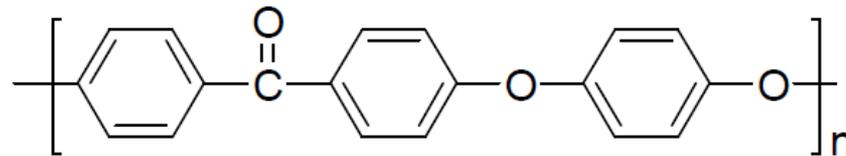
Membrane	Permeance, GPU		Ideal selectivity
	CO ₂	N ₂	
PES support	240	280	0.86
Dry GO on PES	20	15	1.3
Wet GO on PES*	97	2	49

* Pure gas with 75% saturated water

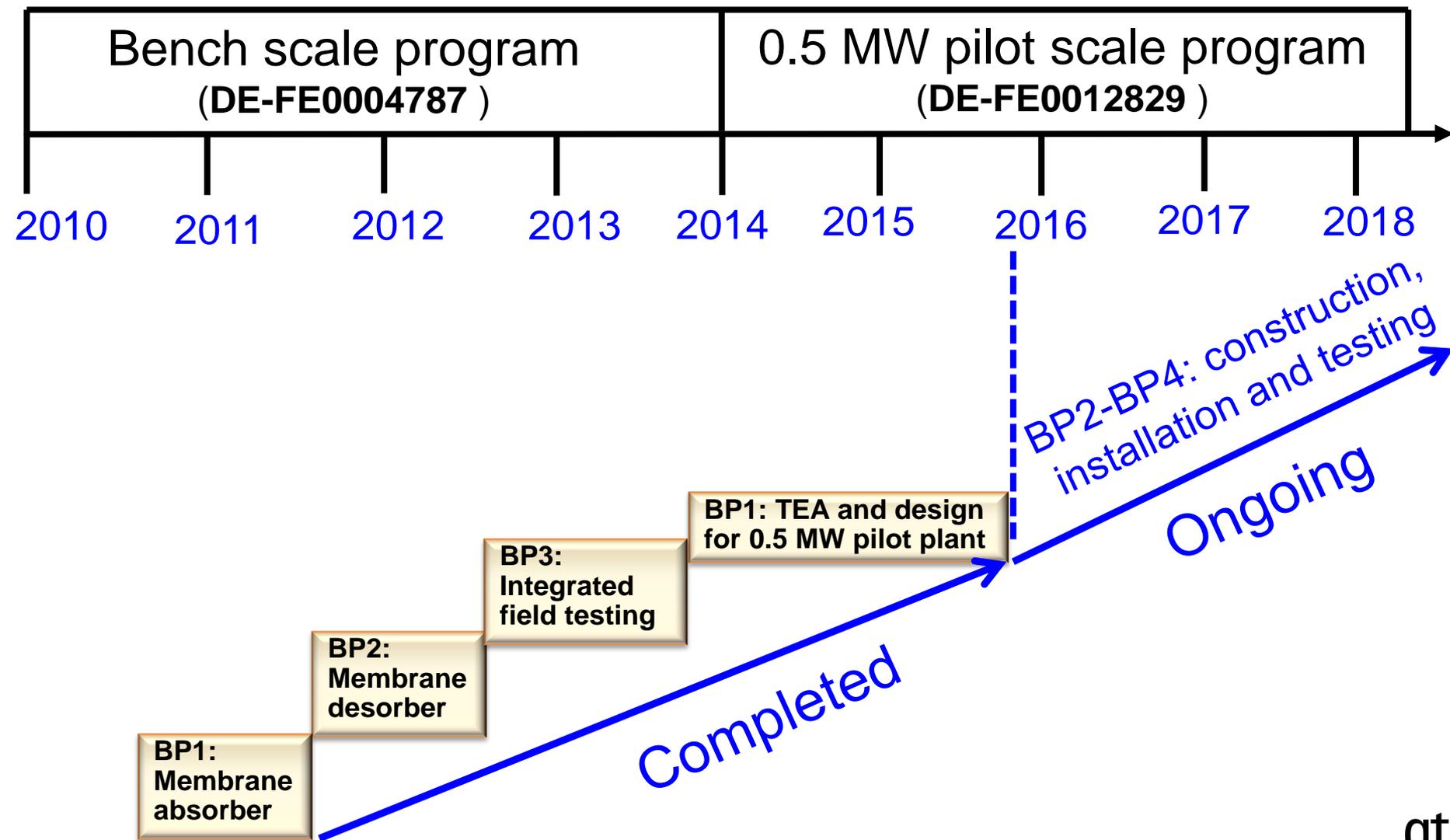
Transport mechanism: hybrid surface/solution diffusion



PEEK HFMC process

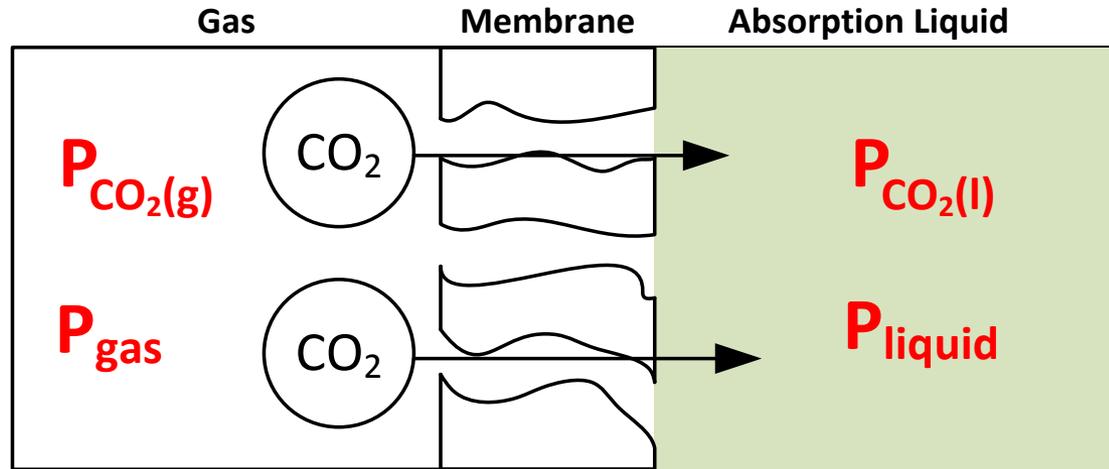


Background: GTI, PoroGen have been developing singular PEEK HFMC technology since 2010



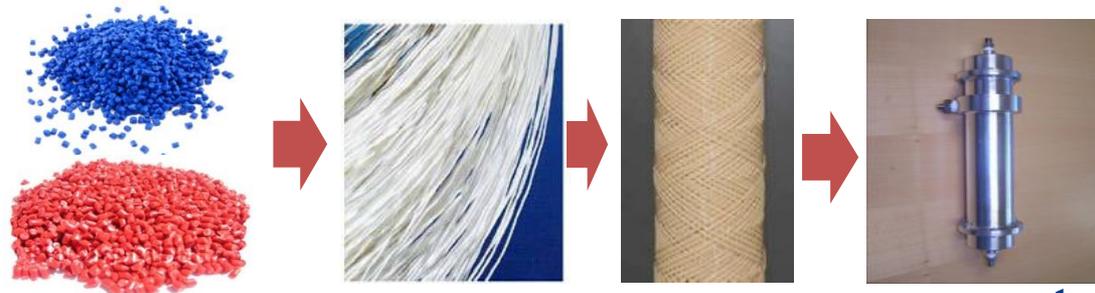
What is a membrane contactor?

- > High surface area membrane device that facilitates mass transfer

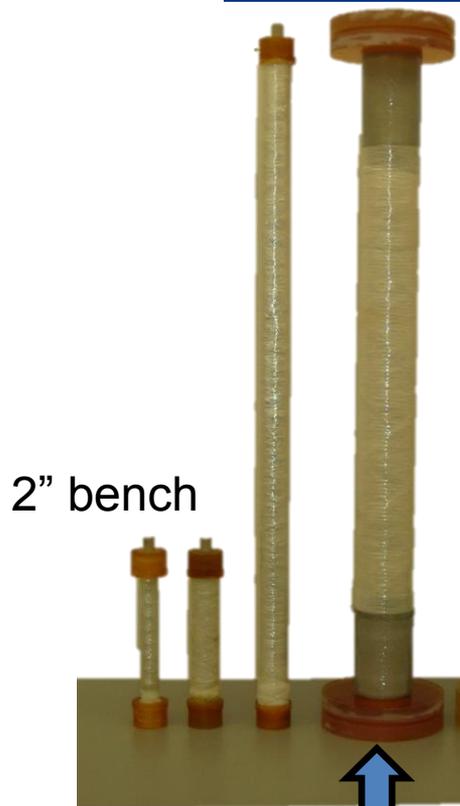


- > **Separation mechanism:** CO₂ permeates through membrane and reacts with the solvent; N₂ does not react and has low solubility in solvent
- > Why **PEEK HFMC**?

Polymer	Max service temperature (°C)
Teflon™	250
PVDF	150
Polysulfone	160
PEEK	271



Membrane module scaled to 4-inch diameter, successful field testing completed at Midwest



- > 4" diameter
- > 60" long
- > 2,000 GPU CO₂ permeance



- High mass transfer coefficient achieved with aMDEA solvent

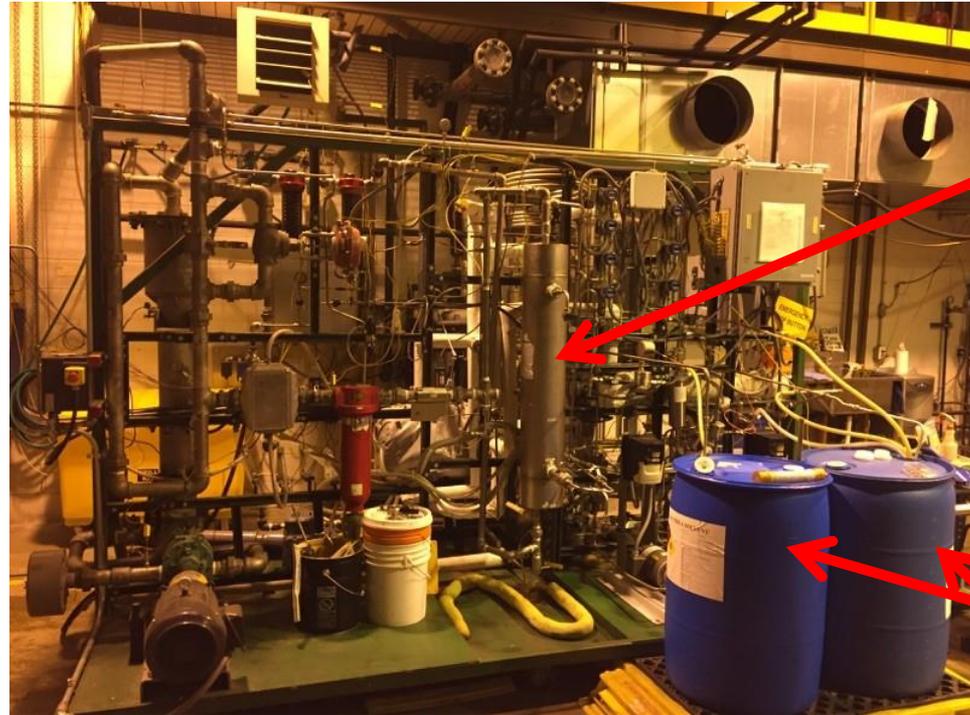
CO ₂ removal rate	Mass transfer coefficient,
93.2%	1.2 (sec) ⁻¹

Conventional contactors: 0.0004-0.075 (sec)⁻¹

Recently module further scaled to 8-inch, and showed contactor mass transfer coefficient of 2.0 (sec)^{-1}



- > 8" diameter
- > 60" long
- > 2,600 GPU CO_2 permeance



8-inch module

aMDEA solvent

CO_2 removal rate	Mass transfer coefficient
90.3%	2.0 (sec)^{-1}

Preliminary TEA for GO-PEEK Hybrid Membrane Process

Preliminary TEA: COE of GO-PEEK process can be 31.4 % lower than that of DOE Case 12

> To achieve DOE's cost target (COE 30% < Case 12) requires

- Lower capital and operating costs: the projected capital costs for GO-PEEK are 14% lower than Case 12
 - Higher net plant efficiency: 31.6% for GO-PEEK vs. 28.4% for Case 12
- 45%/45% capture case preliminary TEA results

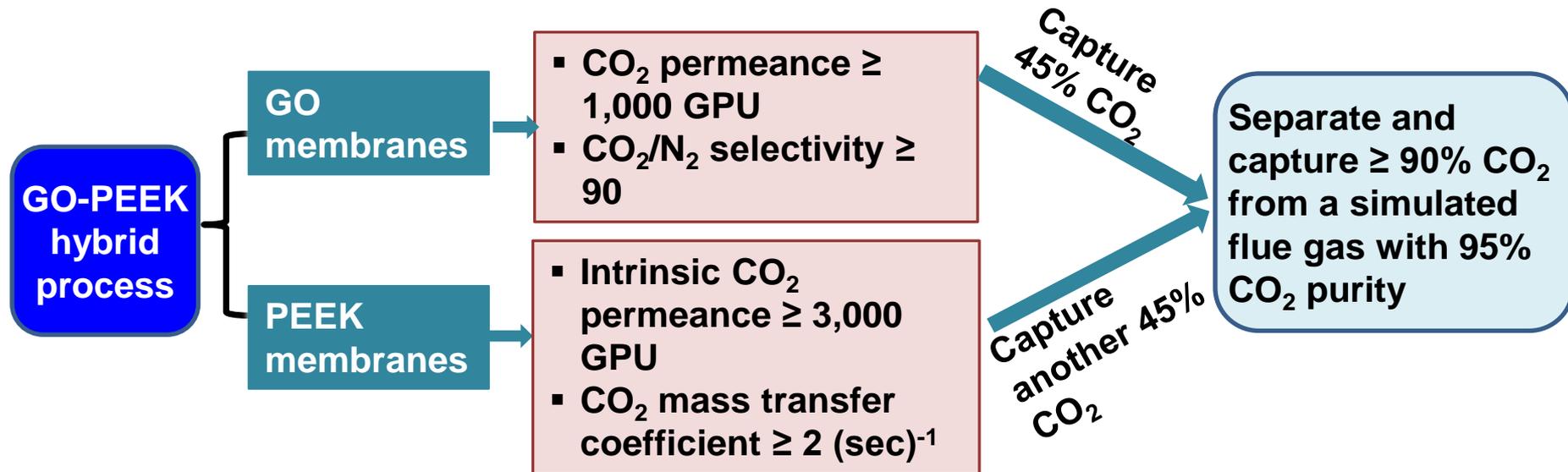
550 MW net power plant	mills/kWh (2012\$)
Total capital costs	48.58
Total fixed operating costs	6.57
Total variable operating costs	8.56
Fuel	33.81
CO ₂ TS&M	9.99
Total LCOE for GO-PEEK process	107.51
Total COE for GO-PEEK process	84.81
Total COE for Case 12	123.61
% of COE less than DOE Case 12	31.4%

Plans for Each Budget Period (BP)

Two BPs, each 18 months

Technical goals and success criteria

> Technical goals:

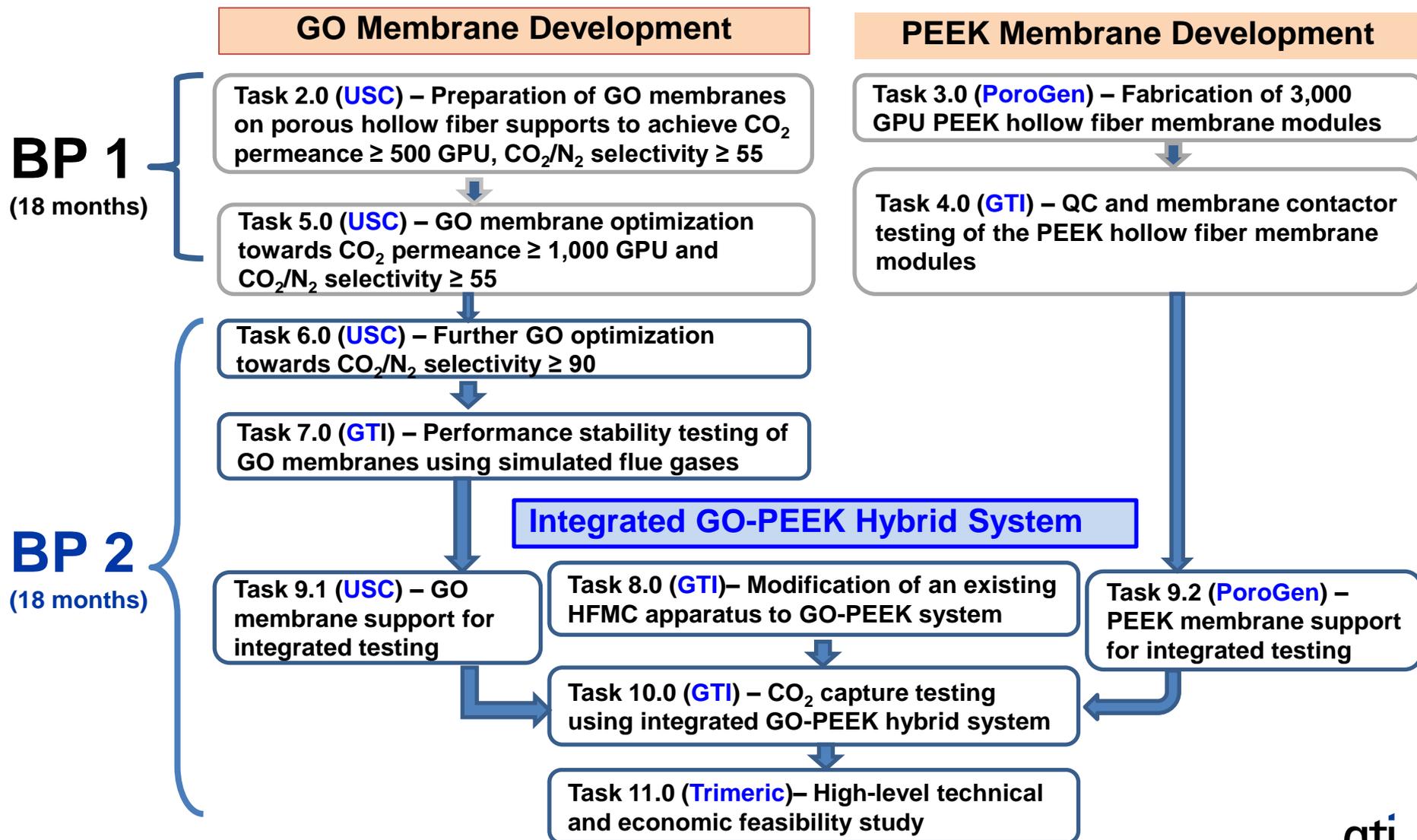


> Success criteria

- Integrated GO-PEEK process testing complete, 90% CO₂ removal rate and 95% CO₂ purity achieved
- Technical and economic feasibility study report issued. DOE cost goal (COE 30% less than baseline CO₂ capture approach) validated
- Final technical report submitted to DOE

Overview/roadmap

Task 1: Project management and planning (*throughout the project*)

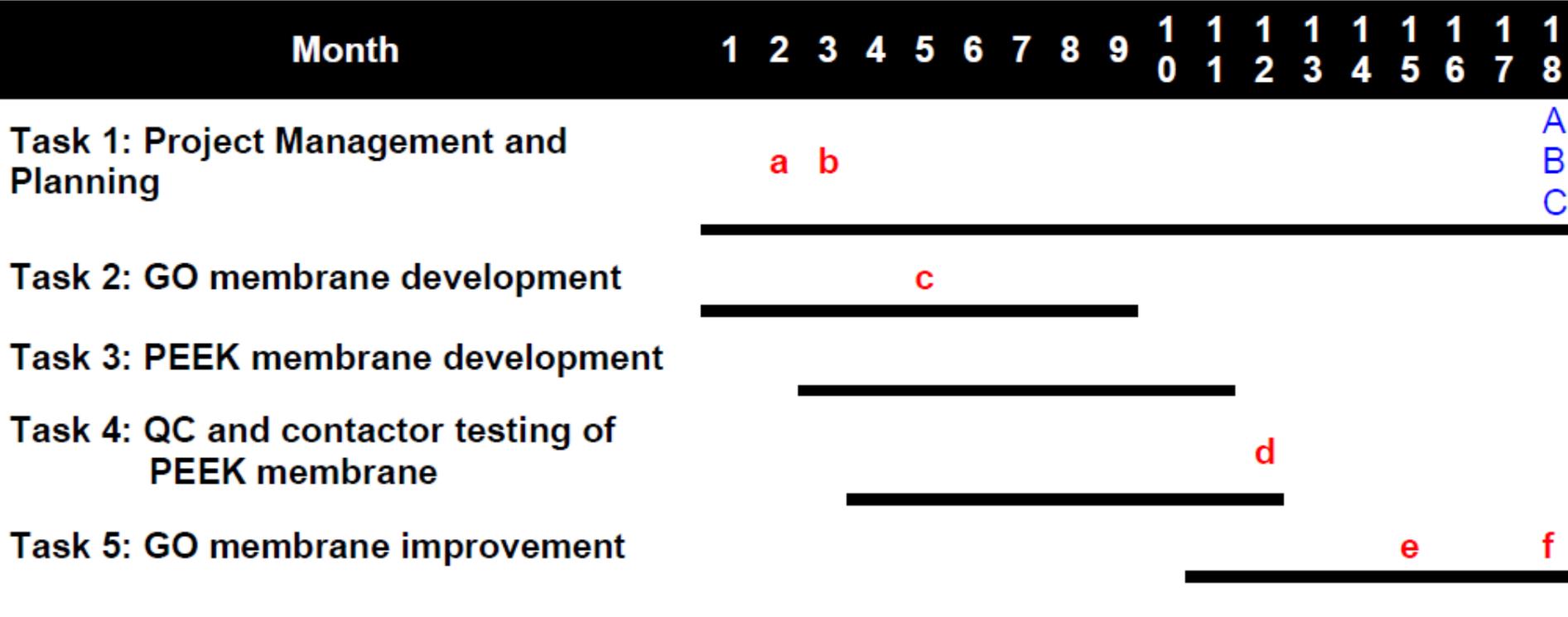


BP1 overview

- > **Performance period:** Oct. 1, 2015 – March 31, 2017
- > **Funding:** \$814,748 from DOE; \$255,624 cost share (24%)
- > **Objectives:**
 - **GO membrane unit:** CO₂/N₂ selectivity ≥55 and CO₂ permeance ≥1,000 GPU
 - **PEEK HFMC unit:** membrane intrinsic CO₂ permeance ≥3,000 GPU; Selectivity will be achieved through the use of aMDEA solvent
- > **Project participants:**



BP1 timeline, tasks, milestones and decision points



Milestones		Decision Points
a	PMP updated	A: Successful completion of all work proposed in BP1 B: Achievement of BP1 milestones C: Submission and approval of the Continuation Application
b	Kickoff Meeting complete	
c	GO membranes with thickness <30 nm prepared	
d	PEEK CO ₂ permeances of 3,000 GPU achieved	
e	GO membranes with thickness <15 nm prepared	
f	GO membranes exhibit CO ₂ /N ₂ selectivity ≥55 and CO ₂ permeance ≥1,000 GPU	

Status/progress of BP1 tasks as of Dec. 7, 2015

- > **Task 1**: Project management and planning
 - Agreement with USC signed
 - Agreement with PoroGen (acquired by Air Liquide) is under review
 - Weekly teleconferencing meetings with USC and PoroGen
- > **Task 2**: Preparation of GO membranes (USC)
 - Fabrication of GO membrane commenced
- > **Task 3**: Development of PEEK membrane (PoroGen)
 - A 2-inch module with new fibers shipped to GTI for testing
- > **Task 4**: QC and membrane contactor testing (GTI)
 - The new received 2-inch module is under testing
- > **Task 5**: GO membrane improvement (USC)
 - Won't start until July 1, 2016

BP2 overview

- > **Performance period**: April 1, 2017 – Sep. 30, 2018
- > **Funding**: \$1,185,247 from DOE; \$244,376 cost share (17%)
- > **Objectives**:
 - **GO membrane unit**: GO membrane further improved to achieve CO_2/N_2 selectivity ≥ 90 and CO_2 permeance $\geq 1,000$ GPU
 - **Integrated GO-PEEK membrane process laboratory-scale testing** to achieve 90% CO_2 removal rate, 95% CO_2 purity
- > **Project participants**:



TRIMERIC CORPORATION

Trimeric: responsible for high-level technical and economic feasibility study (TEFS)

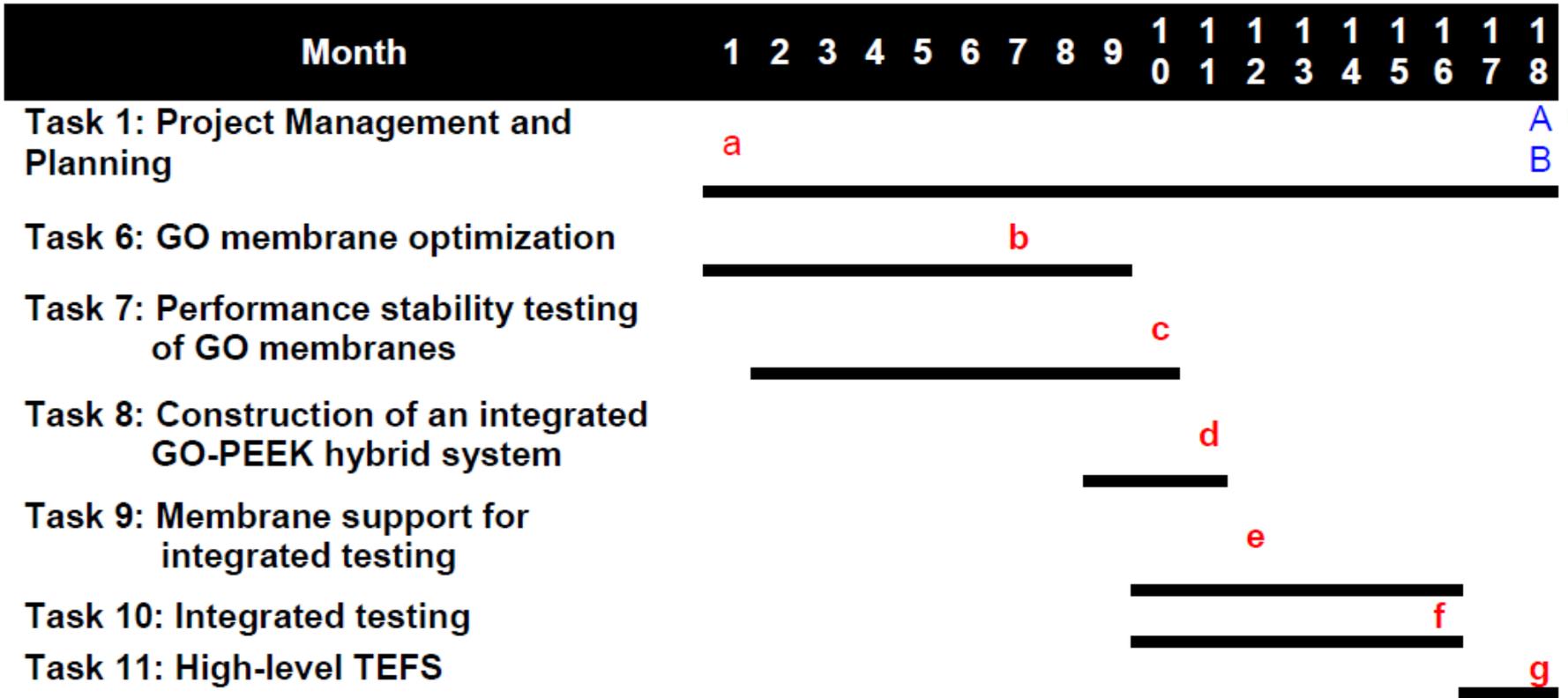
Base:

- Coal-fired 550 MW_e net power plant
- Information from the Pilot Project TEA
- Lab-testing data

Topic Report

- Basic process design
- Sensitivity study
- Estimated equipment, operating, and maintenance costs

BP2 timeline, tasks, milestones and completion of the project



Milestones		Completion of the project
a	BP1 Technical Report submitted	A: Achievement of technical and cost goals B: Submission of Final Technical Report
b	GO membranes shipped to GTI for testing	
c	GO membranes showed CO ₂ /N ₂ selectivity ≥90 and CO ₂ permeance ≥1,000 GPU	
d	Integrated GO-PEEK hybrid system ready for testing	
e	Both GO and PEEK shipped to GTI for integrated testing	
f	Integrated testing complete	
g	Issue high-level TEFS Report	

Summary

- > We are developing a novel CO₂ capture process combining a conventional gas membrane unit and a hollow fiber membrane contactor unit
- > Preliminary estimate suggests the projected cost can be 31% lower than DOE benchmark technology for a 45%/45% capture case
- > SOPO and PMP updated
- > BP1 research activities commenced

Acknowledgements

> Financial support



UNIVERSITY OF
SOUTH CAROLINA



> DOE NETL José Figueroa