



# Advanced Thermally Robust Membranes for High Salinity Extracted Brine Treatment via Direct Waste Heat Integration

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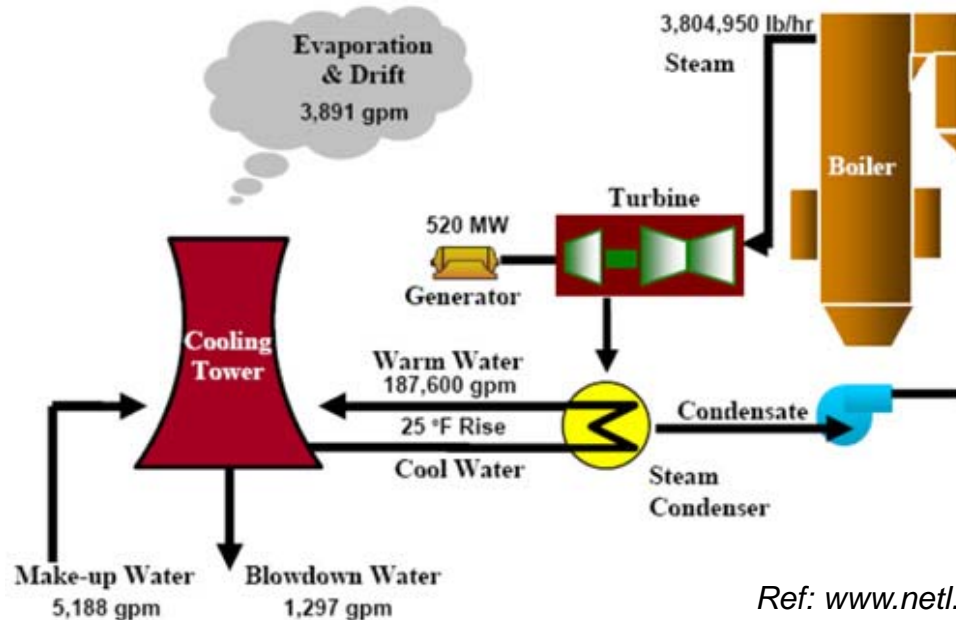


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- **Energy production from fossil fuels relies heavily on clean water**
  - Clean water for boiler steam, FGD unit & cooling – Water usage is dominated by cooling needs.



- An estimated ½ gallon of water is consumed per kWh of electric power produced
- Water needs will increase significantly due to carbon capture (CC)
  - 30% increase in water consumption due to CC in pulverized coal power plant



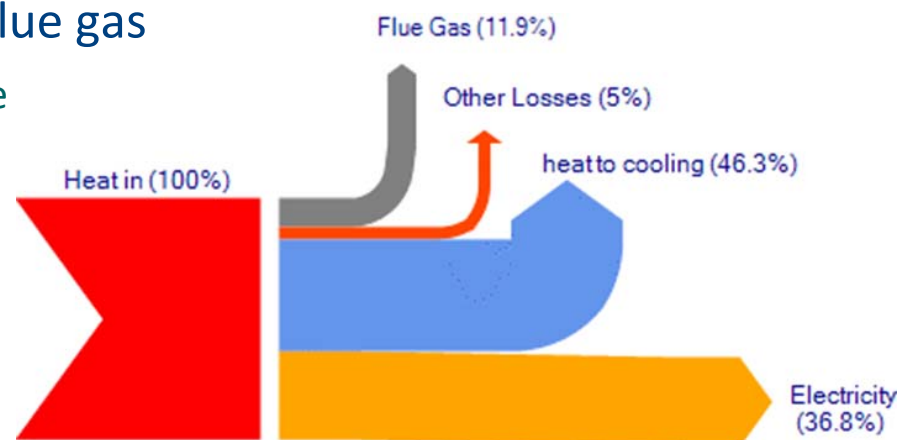
## Water Management

# Growing water and energy needs, and fresh water scarcity mandate water conservation, treatment & re-use

### ↳ Lost water recovery

#### ➤ Evaporation from cooling towers and flue gas

- ❑ Difficult to capture: Low partial/total pressure
- ❑ 6 to 13 % water vapor depending on the coal feedstock and FGD
- ❑ Potential to supply 10 to 33% of boiler make-up water
- ❑ Water vapor recovery will improve efficiency by latent and sensible heat recovery



#### ➤ FGD & cooling tower blowdown water treatment & re-use

### ↳ Alternate water resources: Extracted brines and RO reject stream

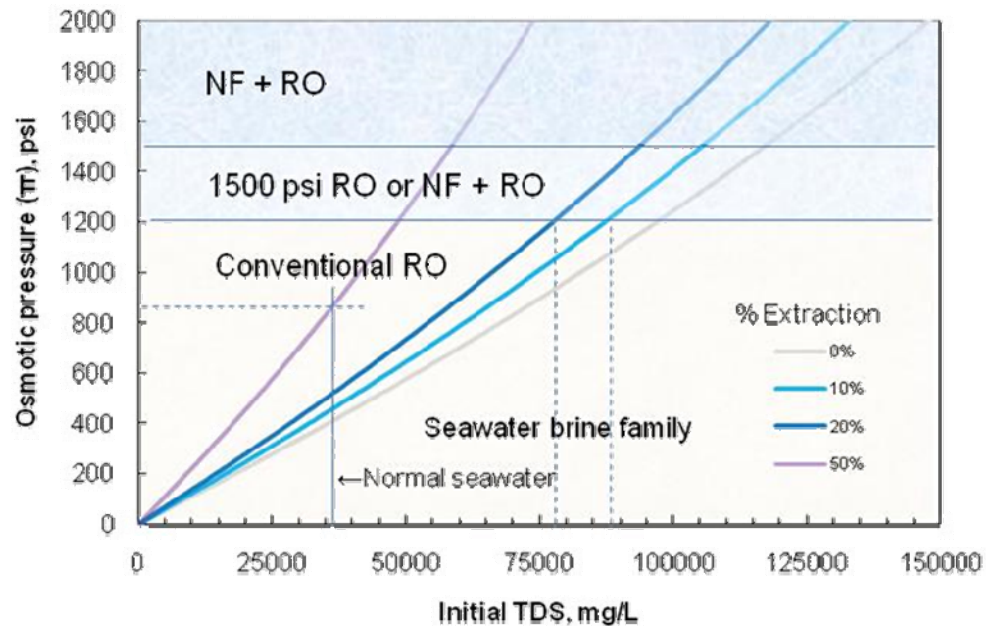
- Require extensive processing to produce power plant quality water
  - ❑ High salinity brine; salinity ranging from > 40,000 mg/L to >300,000 mg/L



# High Salinity Brine Treatment

## Reverse osmosis – Most energy efficient for desalination

- Widely used for seawater (TDS < 40,000) desalination on large industrial scale
- Inherently limited to low salinity brine



### TDS Limitations

- Limited opportunities to treat high salinity brine having TDS > 50,000 mg/L

### Temperature Limitations

- The low operating temperatures of current RO membranes (typ. < 50 °C) limits energy efficient integration into high temperature high salinity streams (70 to > 150 °C) and power plant waste streams (120 to 140 °C).

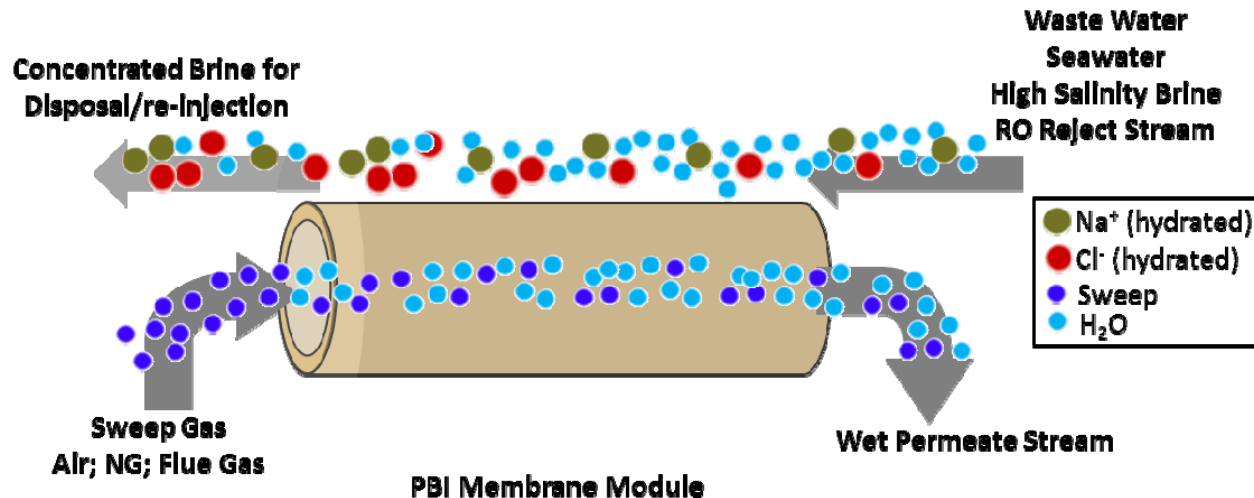
## Other Industrial technologies: Evaporative crystallization (EC) and mechanical vapor compression (MVC)

- High Cost, High Parasitic Load, Energy Inefficient

# Advanced Water Treatment Method

↪ **Membrane distillation/pervaporation is attractive technology for brine separations.**

- Supplement clean water needs for power plants operation
- Improve power generation opportunities/efficiencies (e.g. Brayton cycle)
- Reduce brine disposal costs.



**Hot Sweep Membrane Brine Separations (HGSMBS)**

➤ HGSMBSM can be thought of as MD in extreme operating environments



# Technology Challenges & Opportunities

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↻ **Advances in membrane materials and systems capable of withstanding thermo-chemically challenging operating conditions of the HGSMBS process are required.**

- High hydrolytic and thermo-oxidative stability (process scheme dependent)
- Stability in high TDS environments
- Fouling resistance
- Resistance to other extracted water components/contaminants
- Appropriate water/water-vapor transport properties

↻ **Current commercial membrane limitations for HGSMBS**

- Low thermo-chemical stability especially in presence of steam, superheated water, and oxidizing environments
  - Industry standard membrane materials cellulose acetate, polyamide, polyimide have low hydrolytic stability
- Fouling and degradation in high salinity feed streams

# Thermo-chemically Robust Membrane Material Development & Demonstration

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# Background: PBI Based Materials/Membranes

➤ Polybenzimidazole-based materials/membranes exhibit exceptional thermo-chemical stability

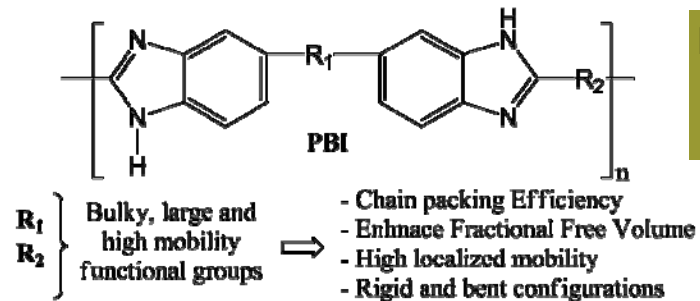
- $T_g > 400\text{ }^\circ\text{C}$ , presented board temperature operating regime
- Tolerance to “bad actors” such as steam and  $\text{H}_2\text{S}$

➤ Known syngas separation performance indicates potential for excellent salt rejection performance for PBI materials

Species	$\text{H}_2\text{O}$	$\text{H}_2$	$\text{CO}_2$	$\text{N}_2$	Hydrated $\text{Na}^+$	Hydrated $\text{Cl}^-$
Kinetic Diameter (Å)	2.65	2.89	3.30	3.64	7.2	6.6
$\alpha (\text{H}_2\text{O}/\text{X})$	-	3	69	300	$\gg 300^*$	$\gg 300^*$

\* estimated

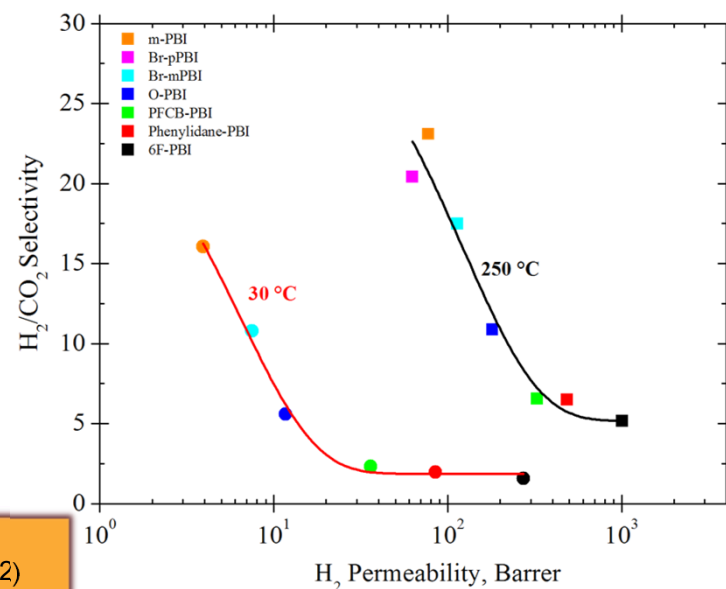
➤ Demonstrated ability to tailor transport properties via materials design and processing protocols



Material Design to Tailor Structure-Property Relationships



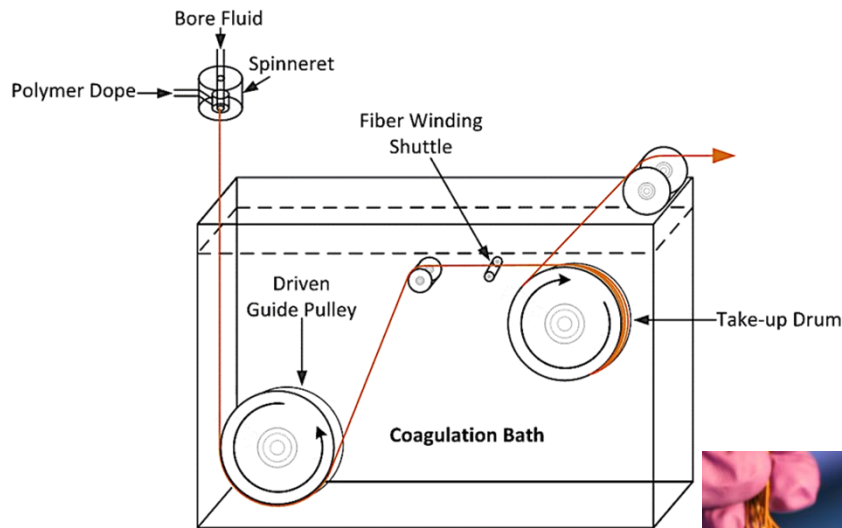
Li, *J Membrane Sci* 461(2014)  
Berchtold, *J Membrane Sci* 415 (2012)  
Pesiri, *J Membrane Sci* 415 (2003)





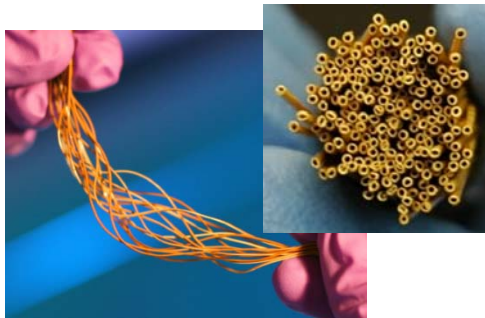
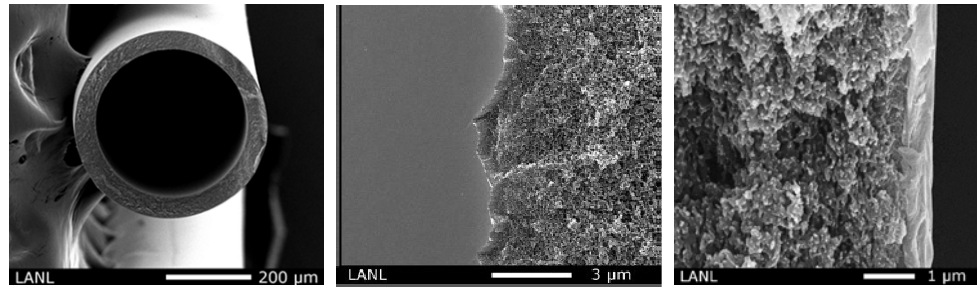
# Background: PBI Membrane Deployment

- Next generation thermo-chemically robust high performance PBI hollow fiber membrane platform developed & demonstrated for gas separation applications



*Liquid-liquid de-mixing based phase inversion hollow fiber spinning process*

High Performance Mechanically Robust Composite Structures Developed for Operation in High T&P Conditions



First generation multi-fiber modules under development

- Rapid translation to high TRL platform enabled by prior work (follow-on effort)

Patent Application: 20160375410

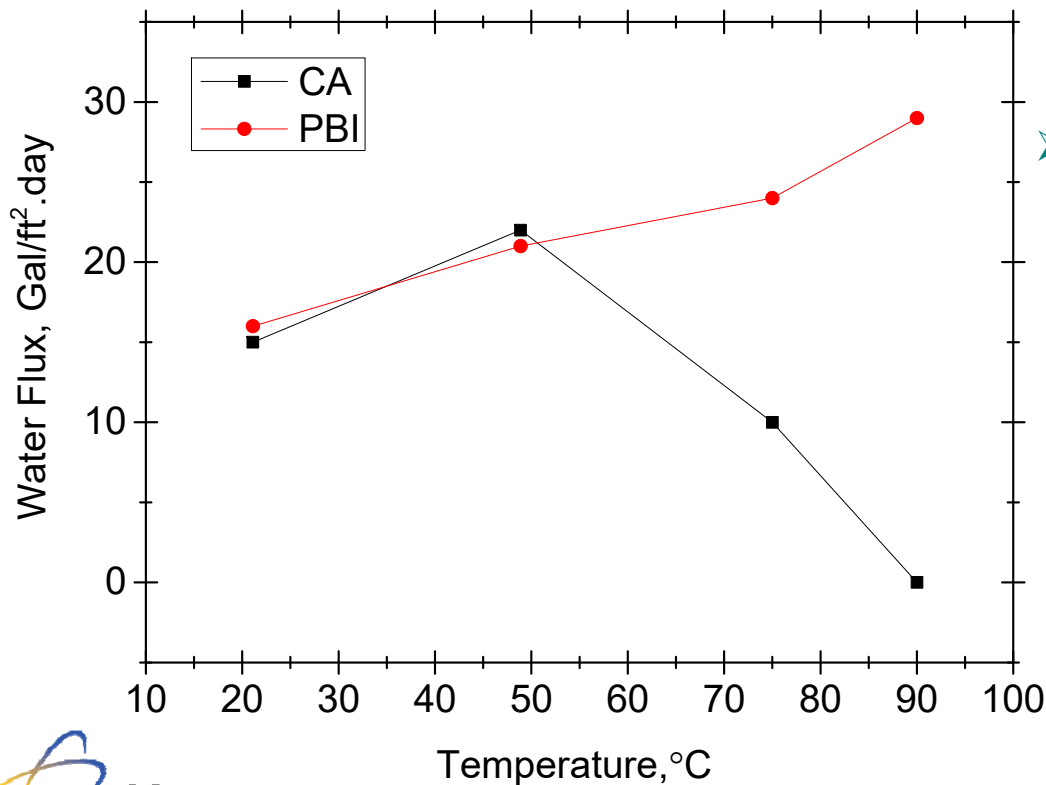


# Salt Rejection Characterization

↻ **PBI (Hollow fiber membranes) has been explored as a:**

- Reverse osmosis membrane for low concentration ( $\leq 0.5\%$ ) brine separation at temperatures up to  $90^{\circ}\text{C}$

## PBI as a “High Temperature” RO Membrane



➤ PBI membranes showed significant improvement in water flux compared to that of CA at elevated temperatures

- Salt rejection  $\geq 95\%$
- Cellulose acetate completely degraded at elevated temperatures



## Project Overview

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### ↳ Objectives

- Realize high performance PBI-based membranes for high salinity brine separation
  - Optimize materials selection to tailor water vapor transport and maximize salt rejection at process relevant conditions
  - Characterize membrane thermo-chemical stability characteristics at process relevant conditions with a specific focus on oxidative stability and stability in high salinity brine environments
  - Characterize membrane flux and salt rejection characteristics at process relevant conditions

# Thermo-Chemical Stability

## Goals

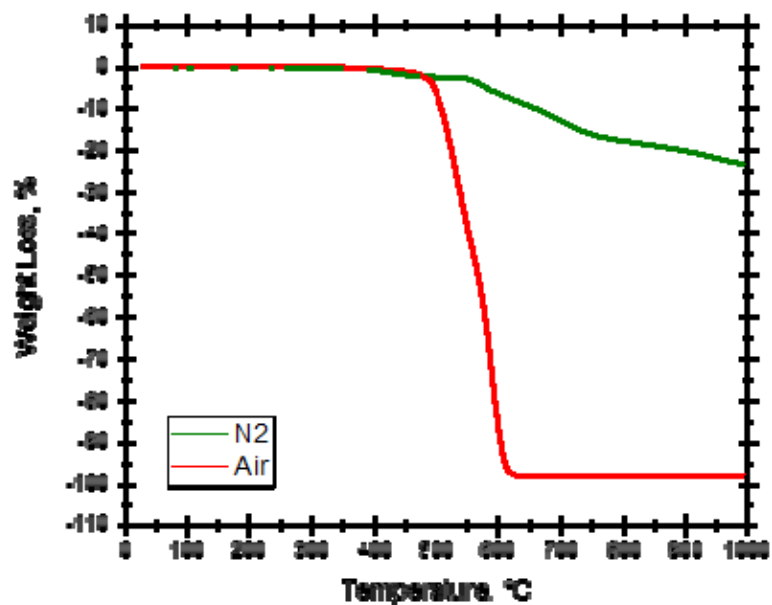
Characterize membrane thermo-chemical stability characteristics at process relevant conditions

- in oxidative environments and
- in high salinity brine environments

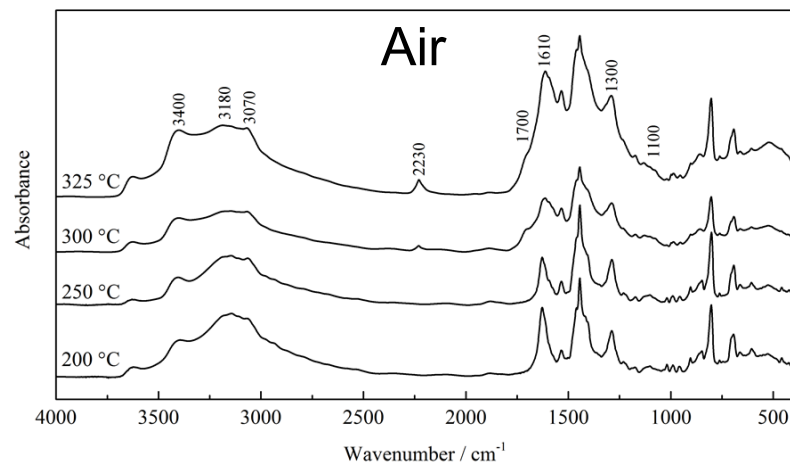
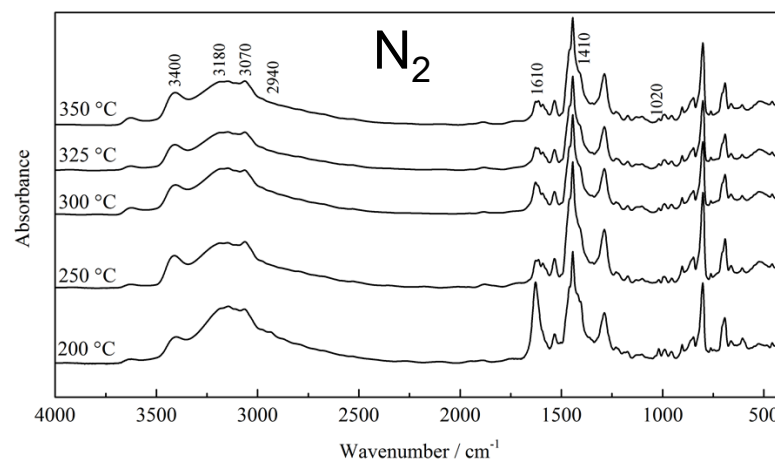
## ↪ PBI materials have exceptional thermal stability in inert and oxidizing environments

➤ Spectroscopic evaluation conducted to understand the thermo-chemical stability of PBI

- TGA: Exceptional thermal stability up to 400 °C in N<sub>2</sub> & Air



- FTIR: No degradation evident in N<sub>2</sub> and air in films exposed for 24 hours at temperatures up to 350 and 250 °C, respectively





# Influence of Salt Solution Exposure

- ↪ **Pure water transport of PBI membranes measured after high salinity exposure at elevated temperatures**
- ↪ **Performance studies conducted at 120 °C in pervaporation mode**
  - Membrane samples exposed to high salinity solutions at reflux conditions (90 to 96 °C) for 24 hours followed by pure water flux evaluation
    - Decrease in water flux after salt solution exposure (thermal annealing & slow water sorption saturation not factored in these experiments)
    - Water flux levels measured for exposed membranes attractive for industrial applications

Membrane	Measured Dense Film Water Flux, $\text{kg m}^2 \text{hr}^{-1}$	Estimated for Industry Relevant 200 nm Selective Layer, $\text{kg m}^2 \text{hr}^{-1}$
Pristine	0.67	185
Exposed to 100,000 mg/L salt solution	0.48	132
Exposed to 200,000 mg/L salt solution	0.36	99

- Membrane evaluation in higher exposure temperatures & subsequent longer term stable flux measurement on-going.

# Water/Water-Vapor Transport Characterization

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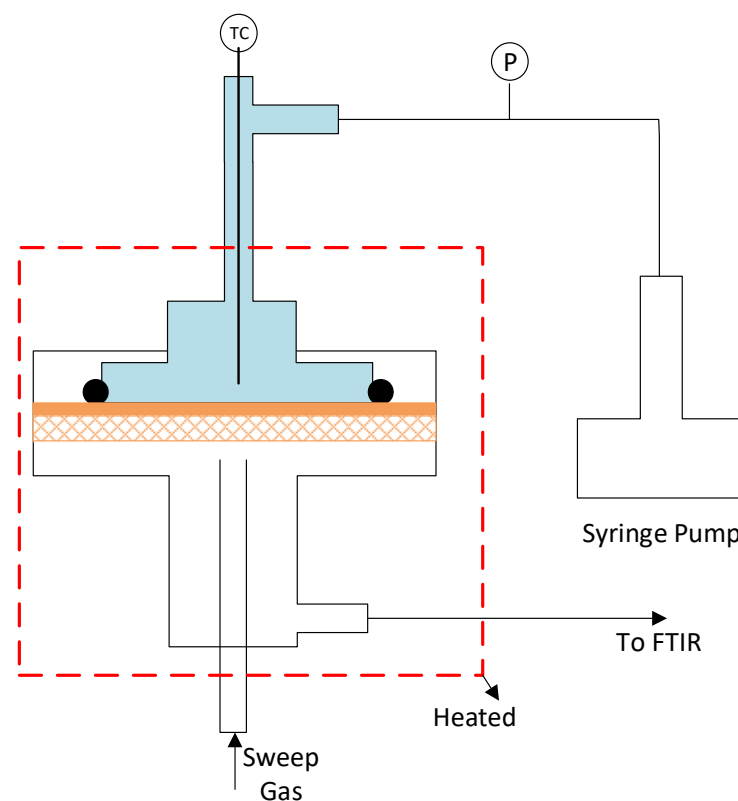
## Goals

Optimize materials selection to tailor water vapor transport and to performance benchmark membrane water flux

# Transport in Permeate Sweep Mode

## ↪ Ideal water vapor transport characteristics of PBI measured using $N_2$ sweep stream

- Custom laboratory set-up using FTIR multi-gas detector for composition analysis

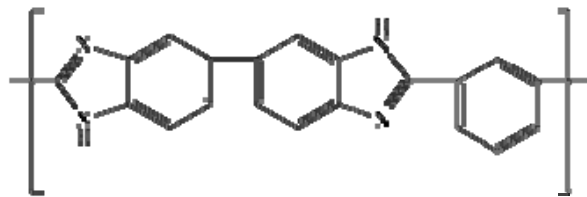




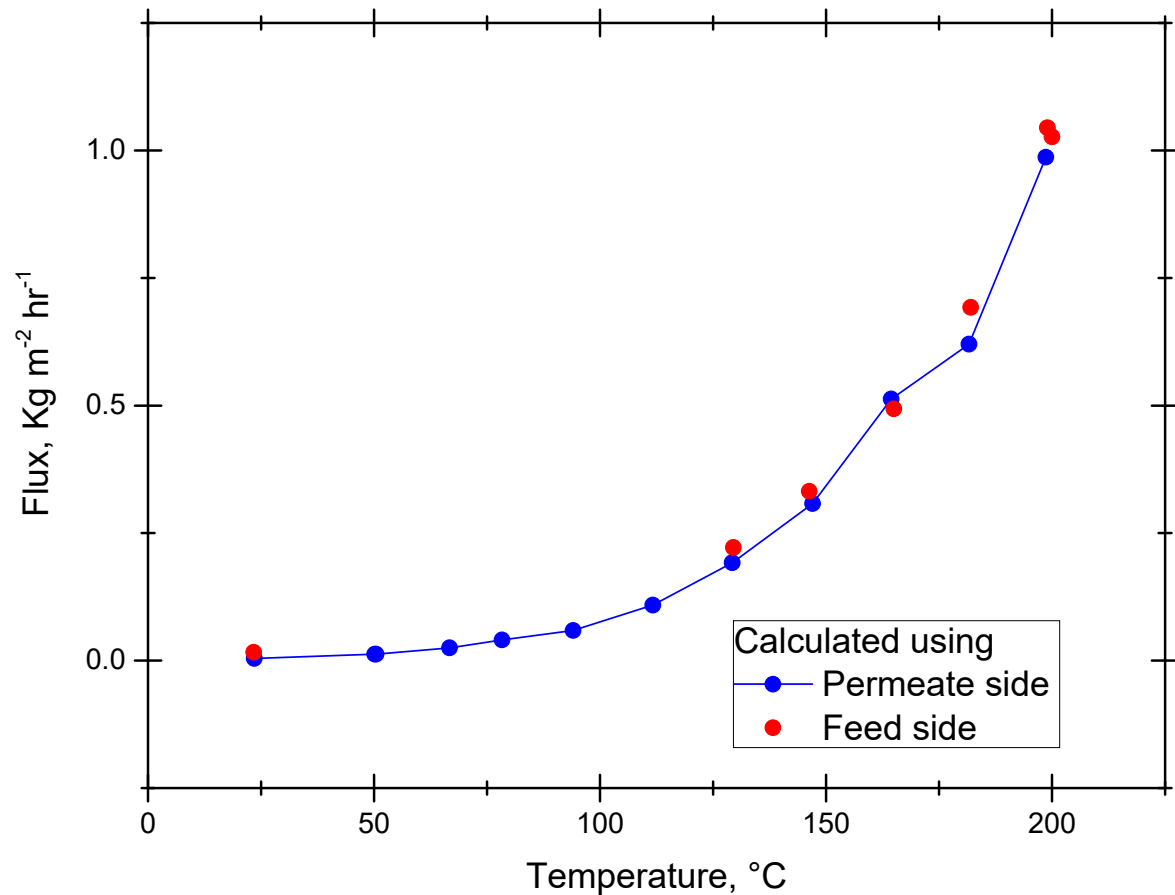
# High Water Permeation Rate

↪ **H-bonding characteristics and presence of N-H group results in high water vapor transport characteristics**

➤ Exponential increase in water vapor permeation rate at temperatures > 100 °C



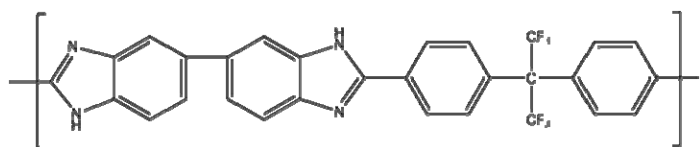
- 55 μm film
- Feed pressure = 250 psi
- Consistent flux calculated using feed side water volume decrease rate or water fraction measured in permeate stream



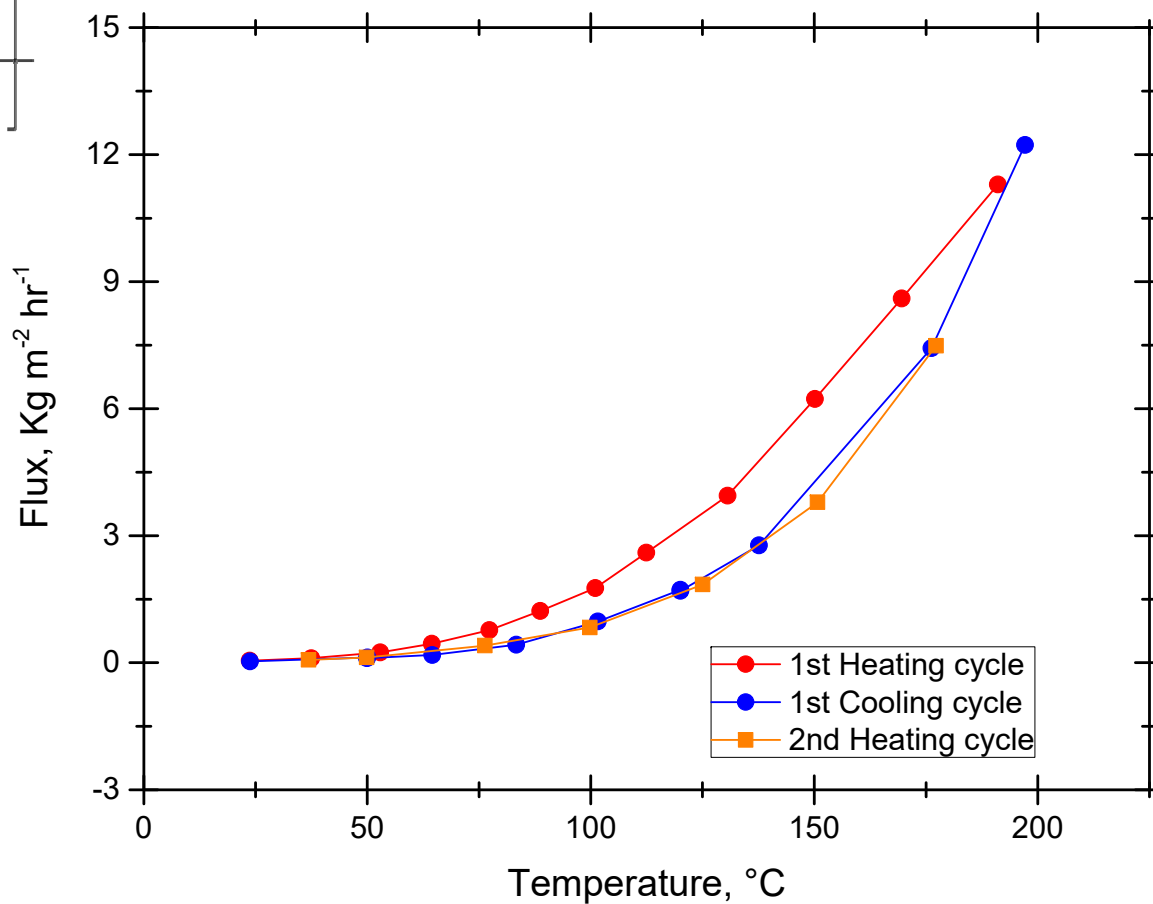
# 6F-PBI Membrane

## Water vapor transport of 6F-PBI similar to m-PBI

- Similar trend in water flux as a function of temperature as observed for m-PBI

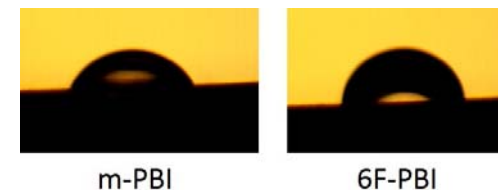
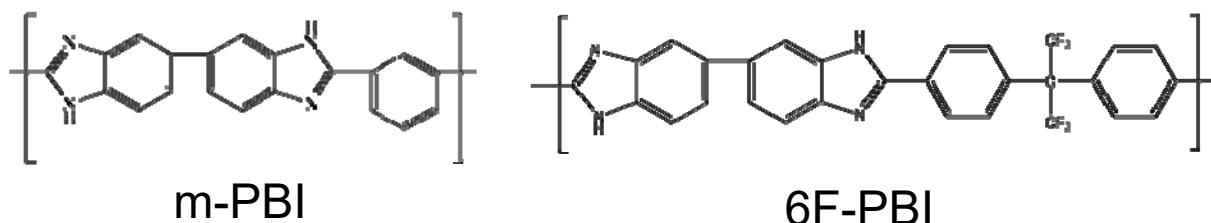


- 7  $\mu\text{m}$  film
- Feed pressure = 250 psi
- Water flux decreased after membrane exposure to 200  $^{\circ}\text{C}$ . Polymer structure re-arrangement or loss of residual solvent

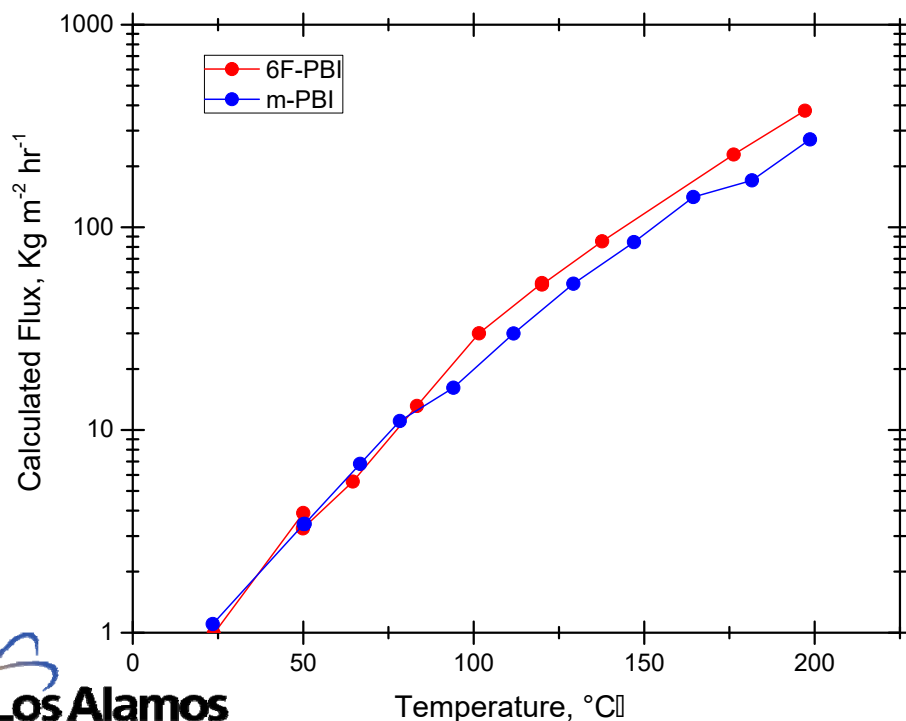


## Two PBI material chemistries evaluated

- 6F-PBI has approximately one order of magnitude higher H<sub>2</sub> permeability as compared to m-PBI



6F-PBI is more hydrophobic than m-PBI



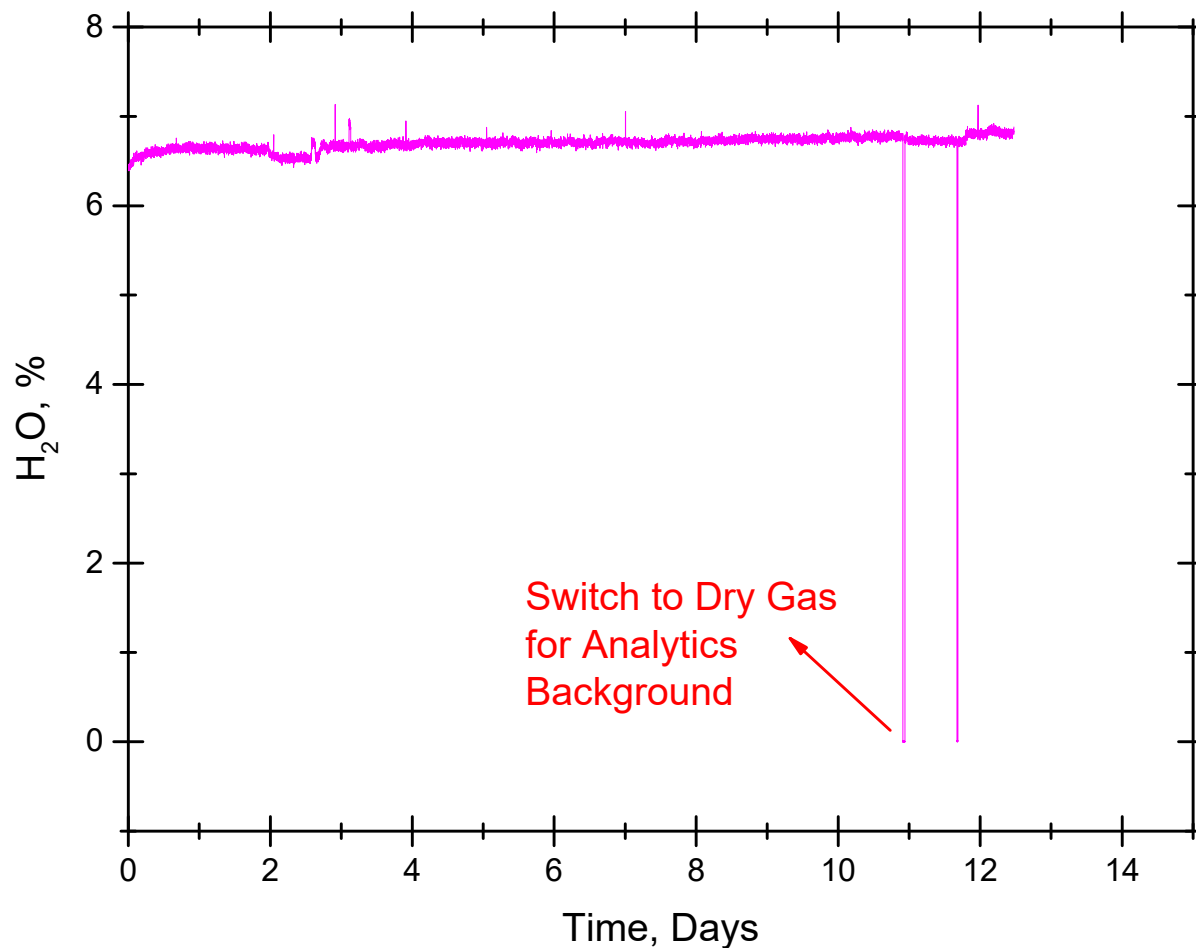
- Calculated flux derived assuming an industrially relevant, 200 nm thick membrane selective layer
- 6F- and m-PBIs exhibit similar fluxes at temperatures < 100 °C  
6F-PBI has a 30% higher water flux than m-PBI at 200 °C



# Exceptional Hydrolytic Stability Demonstrated

## ↻ PBI membrane demonstrated exceptional hydrolytic stability

- Stable water vapor fraction in permeate stream measured for pure water feed at 178 °C at 250 psi for 6F-PBI membrane



# Other Potential Applications Development

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## Goal

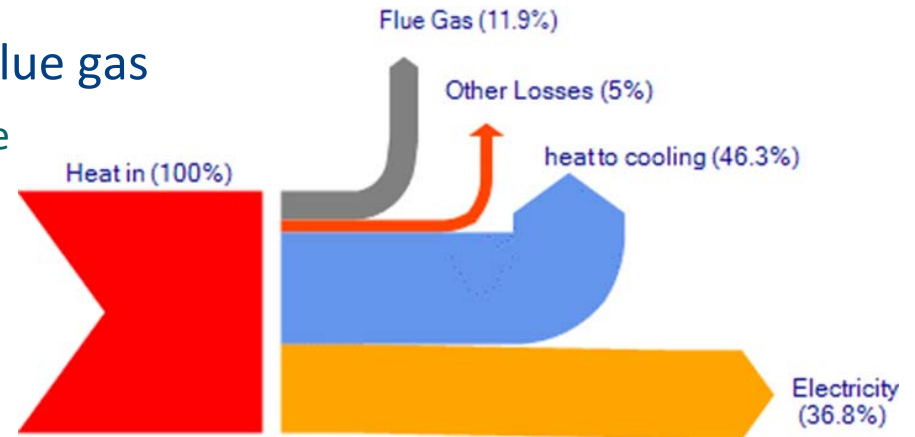
Develop process intensification strategies to deploy PBI membranes for solving water treatment challenges in power plants



# Flue Gas Dehydration

## ↻ Lost water recovery

- Evaporation from cooling towers and flue gas
  - Difficult to capture: Low partial/total pressure
  - 6 to 13 % water vapor depending on the coal feedstock and FGD
  - Potential to supply 10 to 33% of boiler make-up water
  - Water vapor recovery will improve efficiency by latent and sensible heat recovery



## ↻ No industry standard process to capture water from flue gas

- Condensing heat exchangers, membranes and liquid desiccant based dehumidification techniques proposed for flue gas dehydration
- Chemically challenging stream due to the presence of SO<sub>x</sub> & NO<sub>x</sub>
  - Acid formation during condensation mandates the use of expensive alloys to minimize corrosion

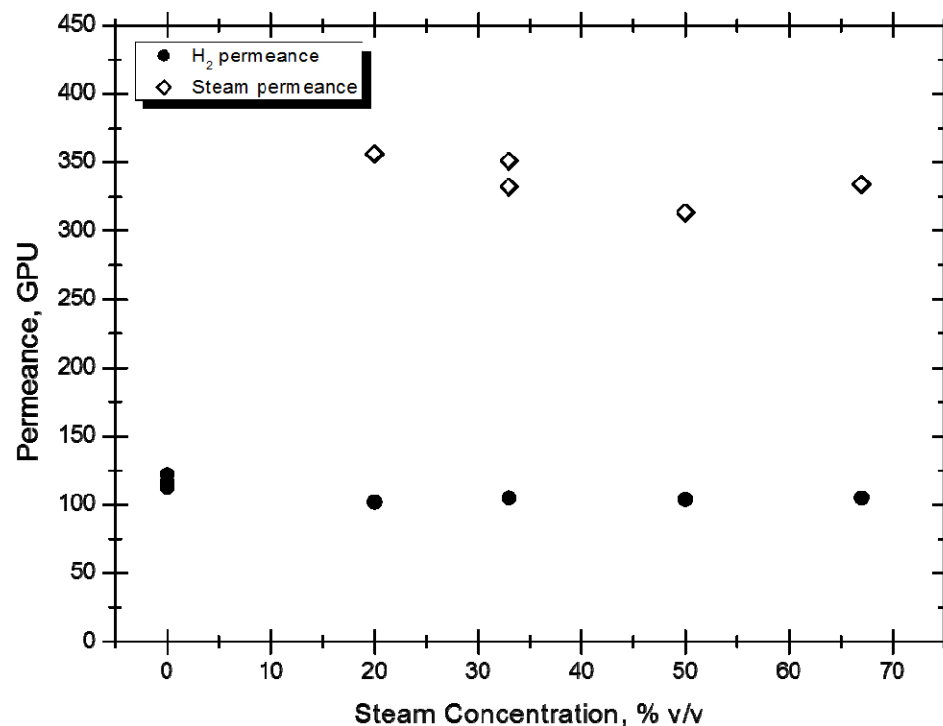


# Membrane for Flue Gas Dehydration

- Sulfonated PEEK (Sijbesma, 2008) evaluated in pervaporation mode
  - Water quality was not high enough for boiler make-up; significant transport of  $\text{SO}_2$  and  $\text{NO}_2$
- Inorganic transport membrane condensers (Wang, 2012) enabled 40% water vapor capture & 5% increase in efficiency.
  - Presence of minor amount of sulfate and carbon in permeate water reported.

## ↪ PBI membrane potential for flue gas dehydration

- Low  $\text{N}_2$  permeability (0.01 barrer)
- Previously evaluated for steam/ $\text{H}_2$  feed mixtures at 250 °C
  - $\text{H}_2\text{O}/\text{H}_2$  selectivity = 3
  - $\text{H}_2\text{O}/\text{N}_2$  (est.)  $\approx$  300
- Higher selectivity expected at lower flue gas relevant temperatures (60 to 180 °C)
- Thermo-chemically robust to withstand  $\text{SO}_x$  &  $\text{NO}_x$
- High surface area platform

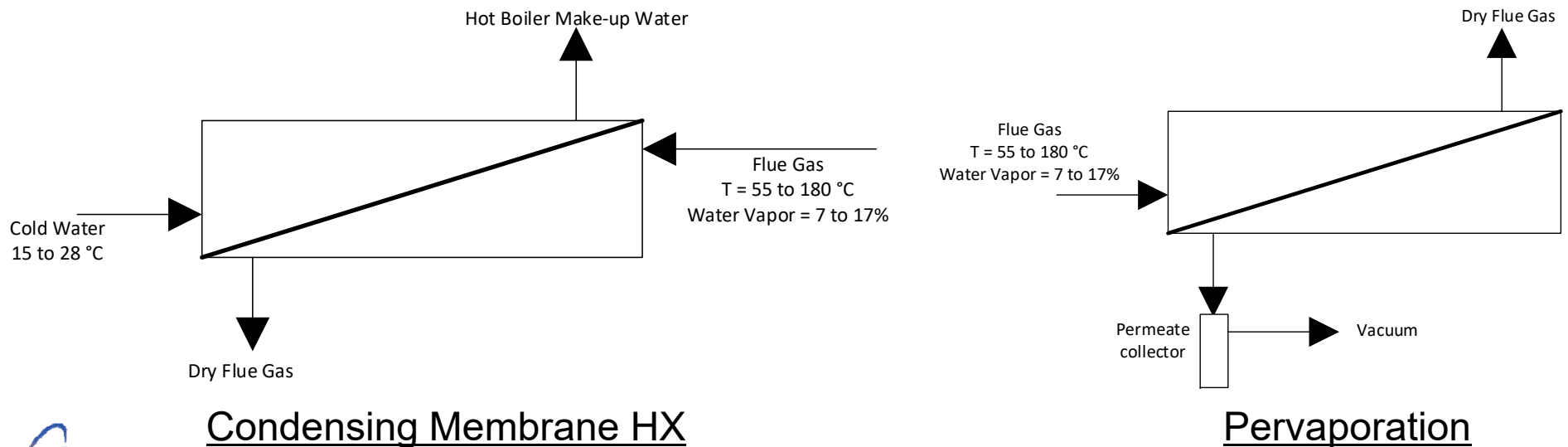




# PBI Membranes for Flue Gas Dehydration

**Leveraging high water vapor perm-selectivity & exceptional thermo-chemical tolerance of PBI membranes for water and heat recovery from flue gas?**

- ↪ Heat/water recovery from flue gas
- ↪ Additional flue gas cooling to near ambient temperatures may improve efficiency of carbon capture technology







## Conclusions & Future Work

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- ↪ **Thermo-chemically robust polybenzimidazole-based membranes having high water/water-vapor transport characteristics are attractive for brine treatment**
- ↪ **Water transport rate of PBI membrane increase exponential at elevated temperature exceeding 100 °C provide opportunities for power plant waste heat utilization**
- ↪ **Demonstrated tolerance of PBI to oxidizing and hydrolytic conditions at elevated temperatures**
- ↪ **Potential to achieve industrially relevant water flux even after exposure to high salinity conditions**
- ↪ **Future work: Demonstrate tolerance to high salinity brines and measure salt rejection characteristics at higher temperatures.**



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