

Investigation of Autoignition and Combustion Stability of High Pressure Supercritical Carbon Dioxide Oxy-combustion

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Performance period: Oct. 2015 – Sept. 2018

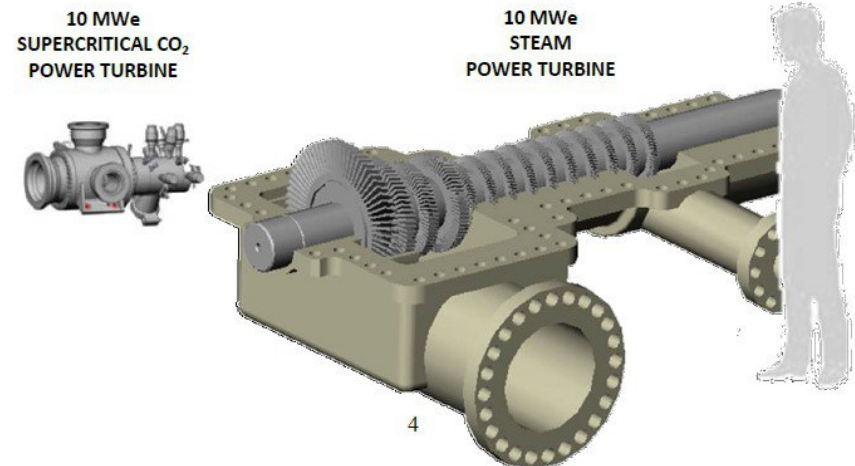
UTSR Project: DE-FE0025174 PM: Seth Lawson

2016 UTSR Project Review Meeting

Background of Directly Fired Supercritical CO₂ cycle



- High plant conversion efficiencies (~52% LHV) with ~100% carbon capture
- Lower electricity cost (by ~15%)
- Supercritical CO₂ (sCO₂) is a single-phase working fluid
 - No thermal fatigue or corrosion as in 2-phase flow (e.g., steam)
- Compact Systems possible
- Many challenges on combustion to address to develop system
 - Kinetics
 - Dynamics



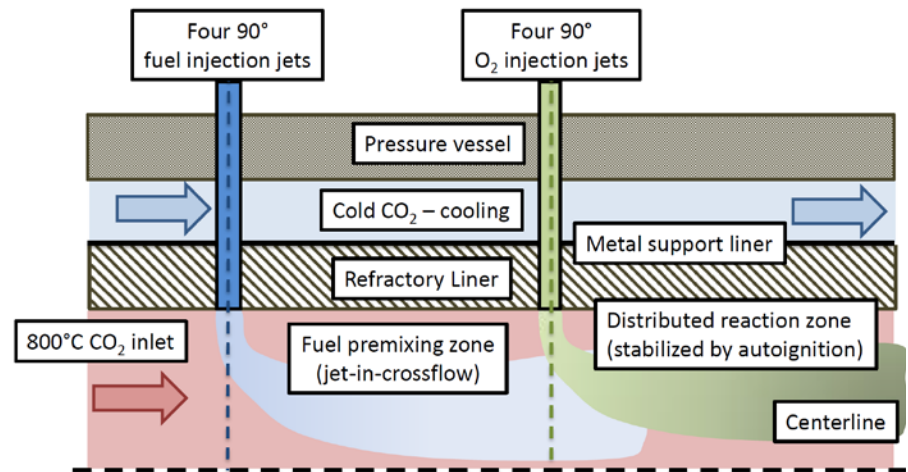
Echogen's 10 MWe sCO₂ power turbine compared to a 10 MWe steam turbine.

Overview of the Scientific Problem

- What fundamental combustion properties/knowledge we need in order to design combustor for sCO₂ oxy-combustion?
- High temperature (~1100 K) and high pressure (~200-300 atm) inlet condition, severe thermal environment for fuel injector and flame holder
 - Mechanical strength (pressure)
 - Thermal strength (cold fuel, hot process)
 - Difficulty to meet 30,000 hours of operation
 - Nickel super alloys are limited to creep rupture strengths of 41 atm, less than 1,280 K

Autoignition delays and flame dynamics of jet in crossflow

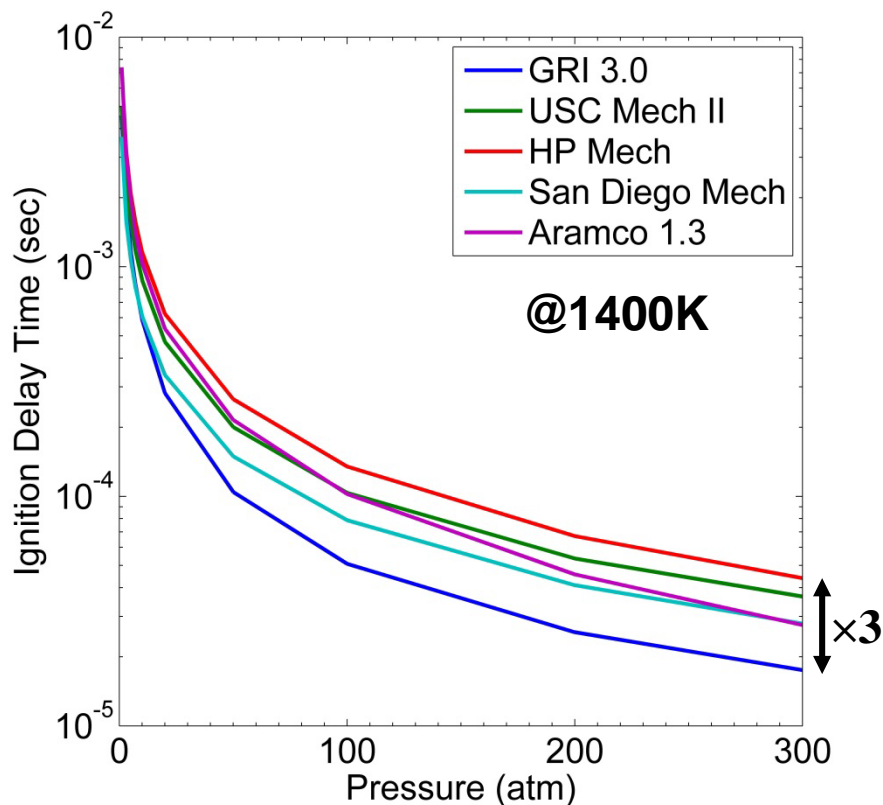
Concept of autoignition stabilized combustor*



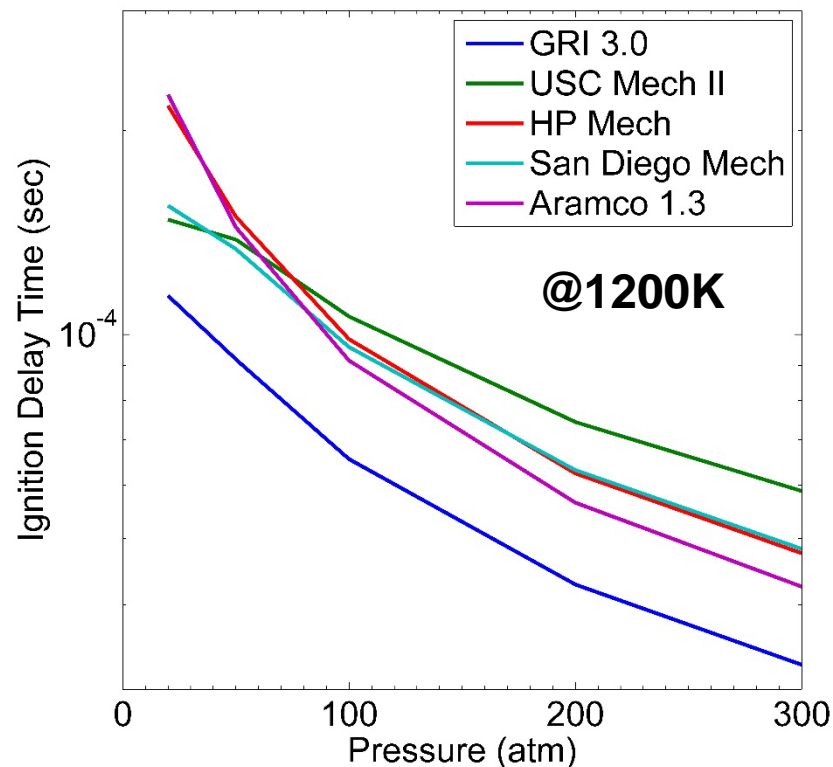


Kinetic Challenges for sCO₂-fuel-O₂ Mixtures

Deviation increases with pressure: knowledge gap
Kinetic models must be validated at regime of interest



CH₄/O₂/CO₂ (9.5%:19%:71.48%)



H₂/CO/O₂/CO₂ (14.8%:14.8%:14.8%:55.6%)

More intriguing results later !!

Overview of the Scientific Questions and Proposed Work

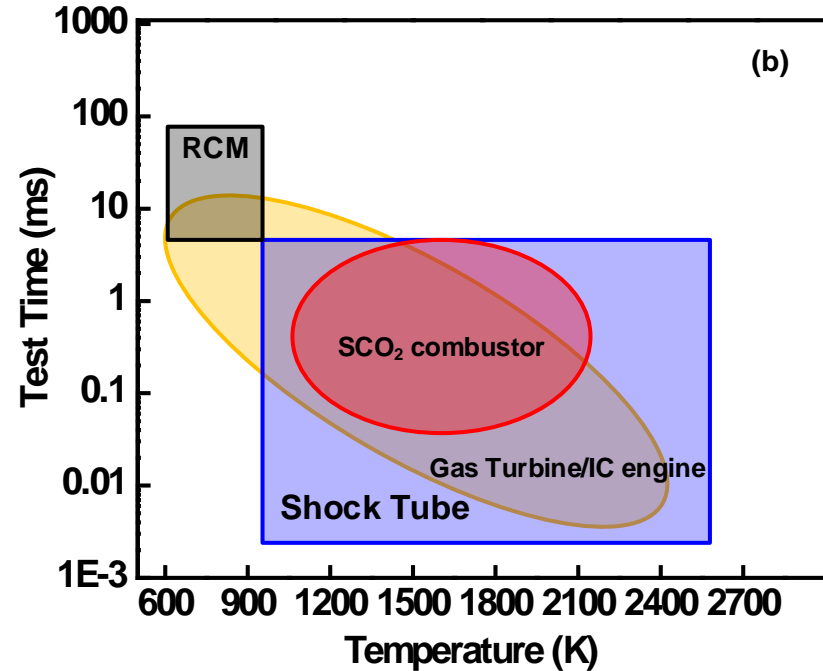
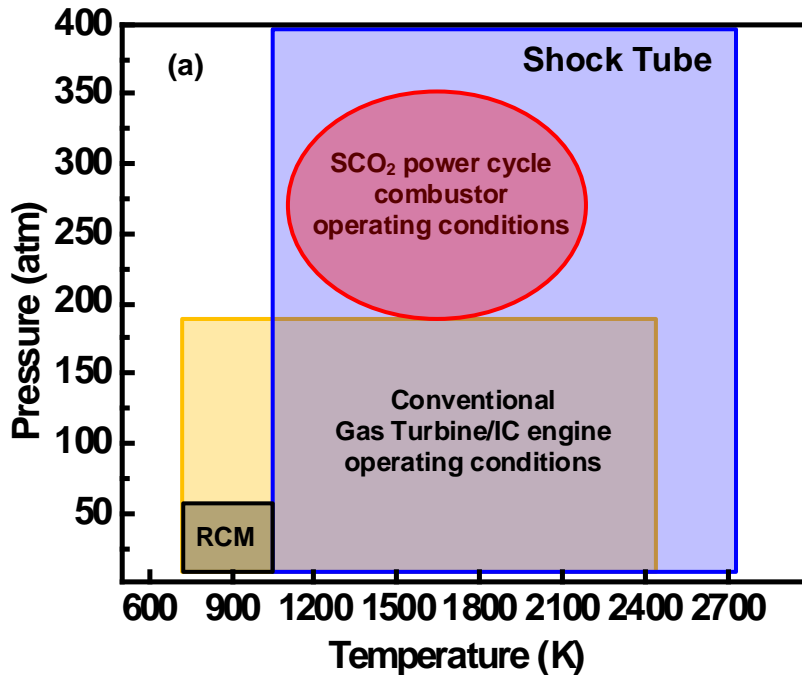


- What is the fundamental combustion properties?
 - Experimental investigation of chemical kinetic mechanisms for $s\text{CO}_2$ Oxy-combustion (Task 1&2: Ranjan & Sun)
- How can we use the kinetic model to design combustors?
 - Development of a compact and optimized chemical kinetic mechanism for $s\text{CO}_2$ Oxy-combustion (Task 3: Sun)
- What is the combustor dynamics at this new condition?
 - theoretical and numerical investigation of combustion instability for $s\text{CO}_2$ Oxy-combustion (Task 4&5: Lieuwen, Menon & Sun)



Task 1: Development of a High Pressure Shock Tube for Combustion Studies

- How to study autoignition delays at sCO₂ Oxy-combustion condition?
 - Why Shock-Tube?



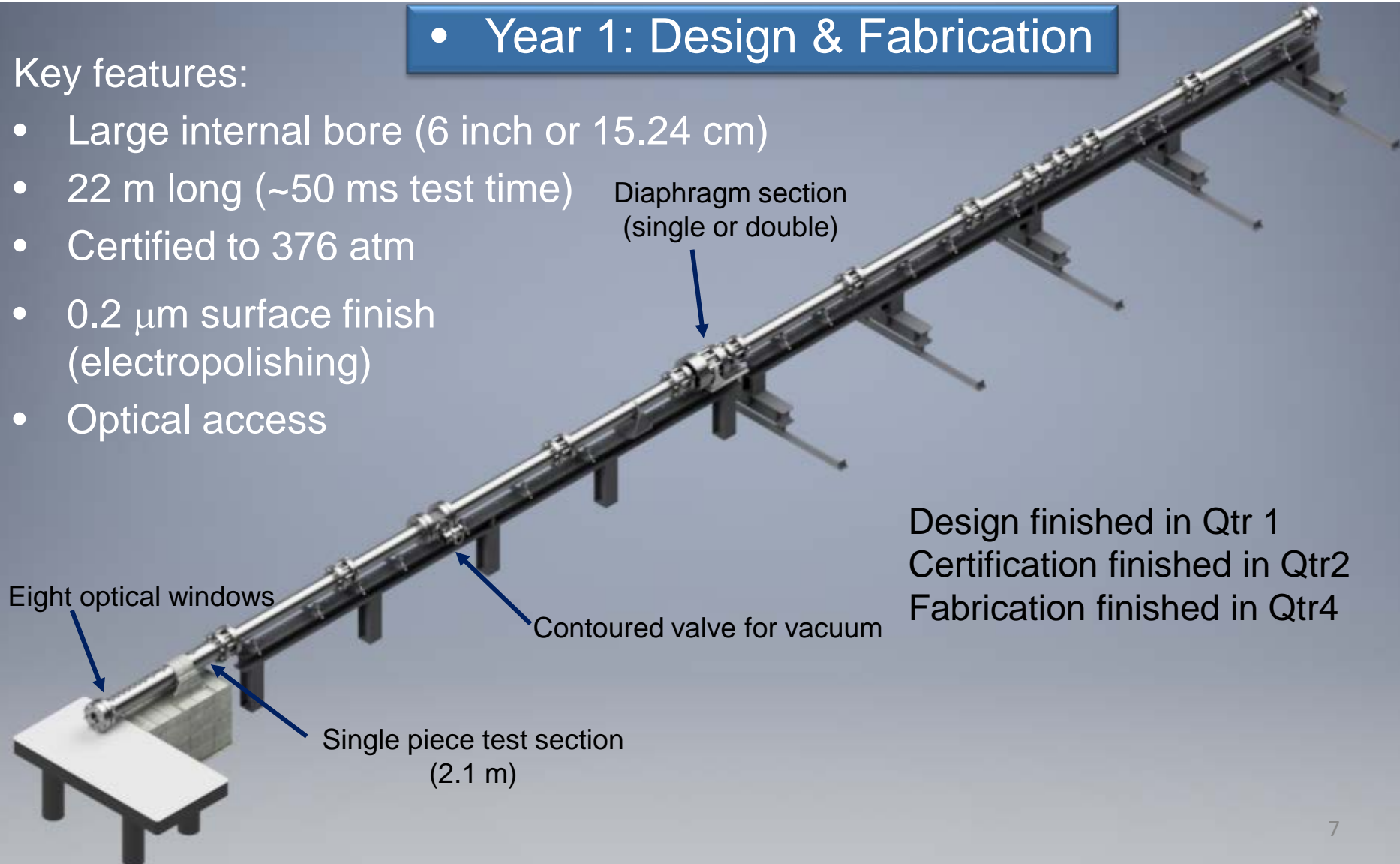


Task 1: Development of a High Pressure Shock Tube for Combustion Studies

• Year 1: Design & Fabrication

Key features:

- Large internal bore (6 inch or 15.24 cm)
- 22 m long (~50 ms test time)
- Certified to 376 atm
- 0.2 μm surface finish (electropolishing)
- Optical access



Design finished in Qtr 1
Certification finished in Qtr2
Fabrication finished in Qtr4

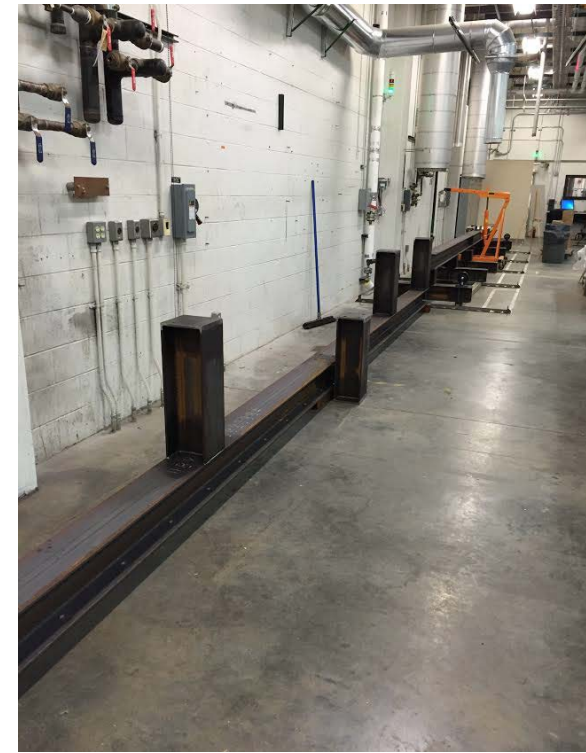
Task 1: Development of a High Pressure Shock Tube for Combustion Studies



March 2016



April 2016



May 2016
Supporting frame installation

Task 1: Development of a High Pressure Shock Tube for Combustion Studies



Machining of test section



Dead mass metal casing delivering to GT

April 2016

Task 1: Development of a High Pressure Shock Tube for Combustion Studies



Paintings supporting frame



Filling dead mass casing with reinforced concrete



May & June 2016



Task 1: Development of a High Pressure Shock Tube for Combustion Studies

- Tube assembled for certification
- Hydraulic Tested at 376 atm
- Sent out for electropolishing



May & June 2016



Task 1: Development of a High Pressure Shock Tube for Combustion Studies

- Anchoring supporting frame and dead mass
- Installing supporting wheels
- Waiting for the arrival of shock tube



July & Aug. 2016

Arrived!

- After tons of paper work and coordination



Sept. 2016

Here It Is!

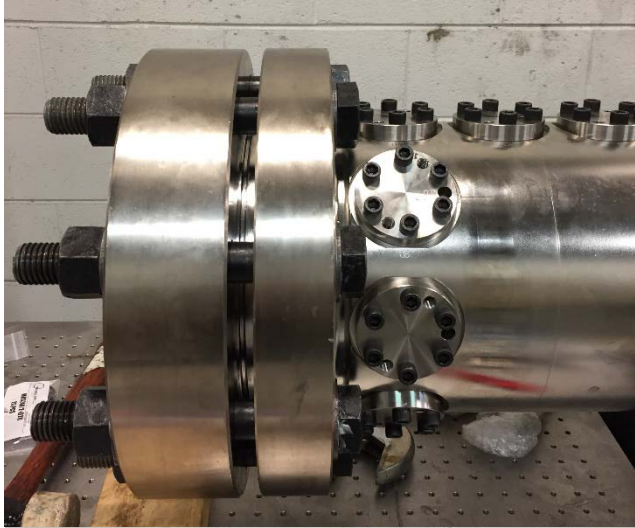
Driven side view



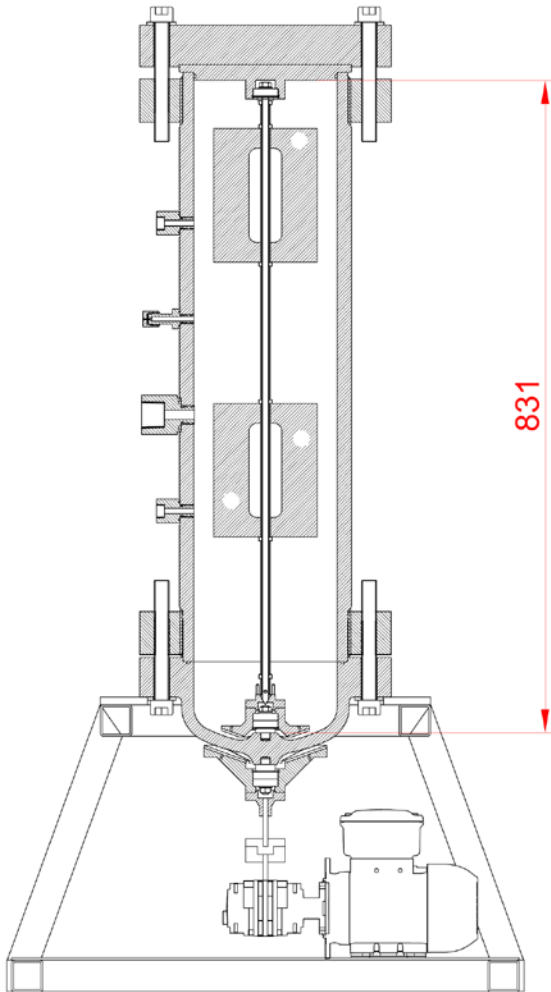
Driver side view



Test Section



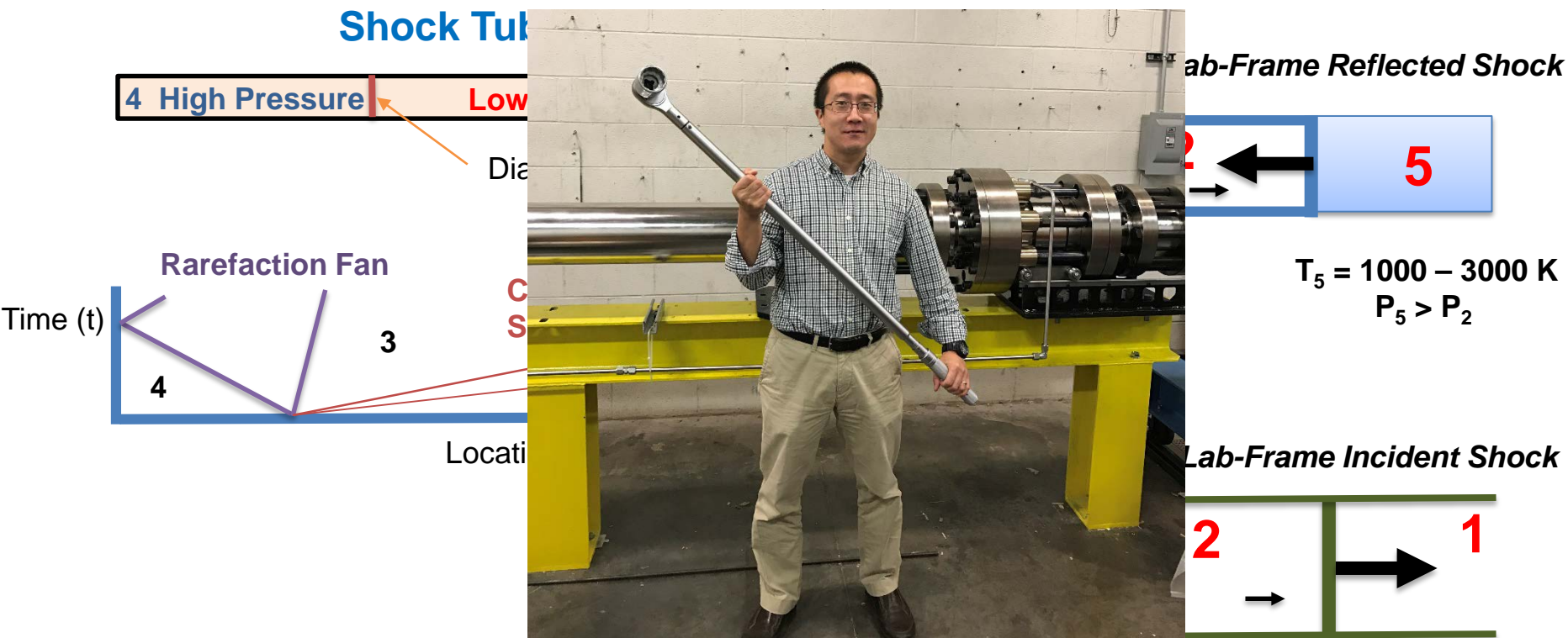
Mixture Preparation Tank



- Magnetic stir to promote mixing
- High accuracy Baratrons (**0.05%** accuracy) to measure partial pressure for mixture preparation

Task 1: Development of a High Pressure Shock Tube for Combustion Studies

Basics regarding the shock-tube:



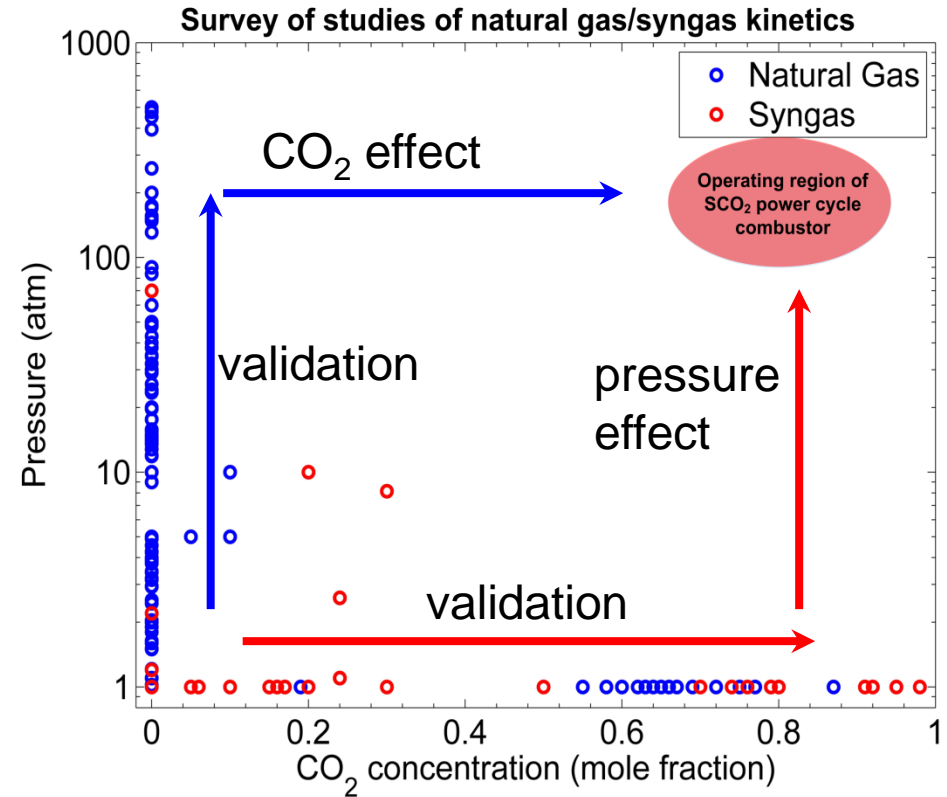
Shock tube is ready and experiments on the way

Task 1 accomplished in year 1

Task 2: Investigation of Natural Gas and Syngas Autoignition in sCO₂ Environment



- Autoignition properties have never been investigated before in region of interest
- This task will investigate critical autoignition properties of natural gas and syngas diluted by CO₂ in region of interest
- Approach for high quality data:
 - Repeat existing experiments for validation
 - Ramp up pressure to study pressure effect
 - Ramp up CO₂ dilute concentration to study CO₂ dilution effect



A new regime to explore!

e.g.:

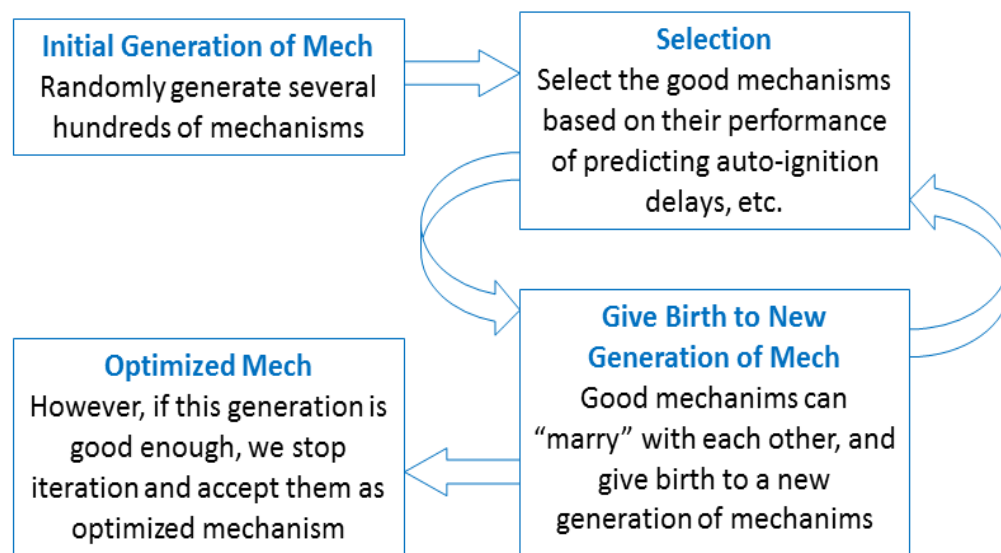
E.L. Petersen, et al, Symp. Combust., 1996(26), 799-806

S. Vasu, et al, Energy Fuels, 2011(25), 990-997

Task 3: Development of a Compact and Optimized Chemical Kinetic Model for sCO₂ Oxy-combustion



- Develop an optimized, validated and compact chemical kinetic mechanism
- Employ the optimized mechanism in LES to study combustion stability
- Approach: optimize chemical kinetic mechanism based on experimental data obtained in task 2.
- Explore other methodology: Bayesian optimization for better optimization



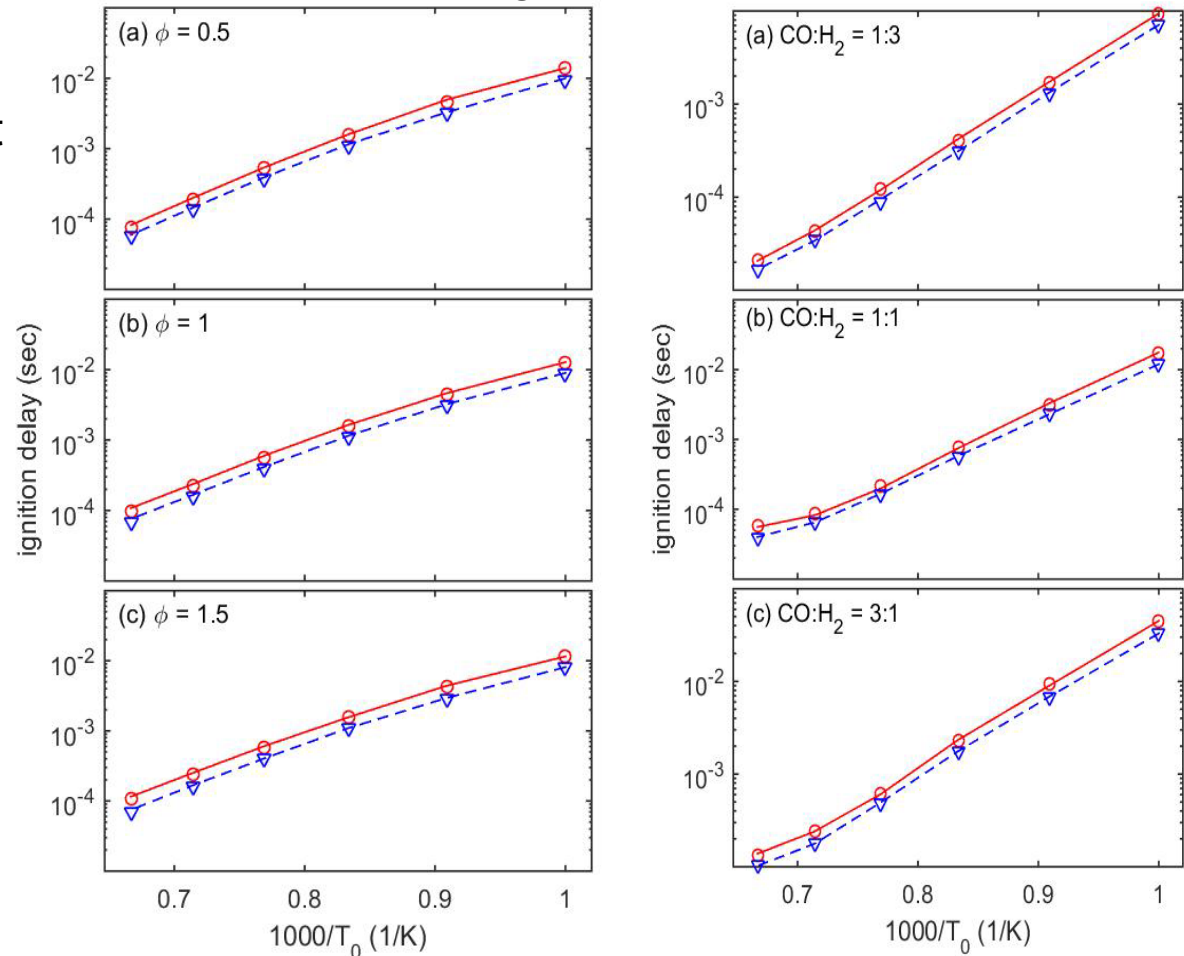
Flow chart of using Genetic Algorithm to optimize chemical kinetic mechanisms

Task 3: Development of a Compact and Optimized Chemical Kinetic Model for sCO₂ Oxy-combustion



- Comparing to existing high pressure autoignition delay data, USC Mech II (111 species) has the best agreement¹. So it is used as a starting point for future optimized mechanism
- A 27 species reduced mechanism² for natural gas (CH₄/C₂H₆) and syngas (CO/H₂) is developed
- Comparison of the results from reduced (marker) and detailed mech (line). Solid lines (p = 200atm), dashed line (p = 300atm)

Autoignition



92.5% CO₂ diluted natural gas/O₂ (CH₄:C₂H₆=95:5)

92.5% CO₂ diluted syngas gas/O₂ ($\phi=1$)

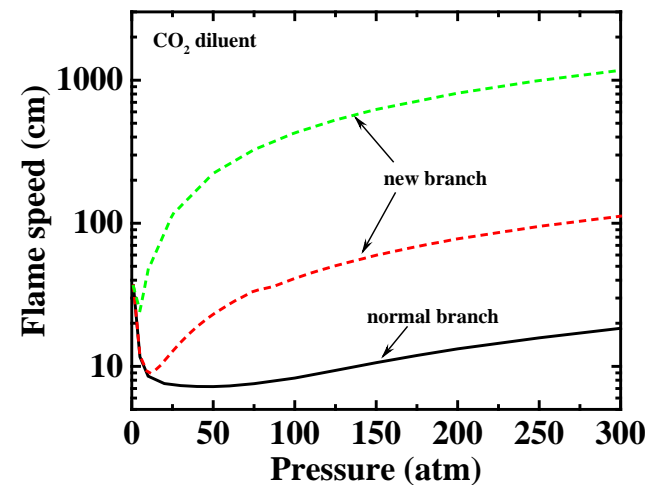
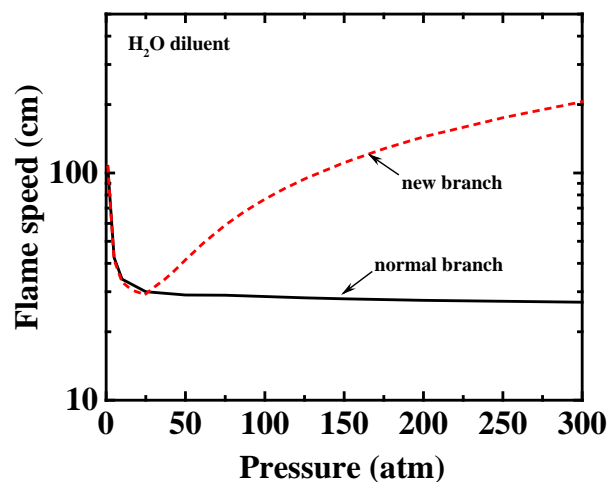
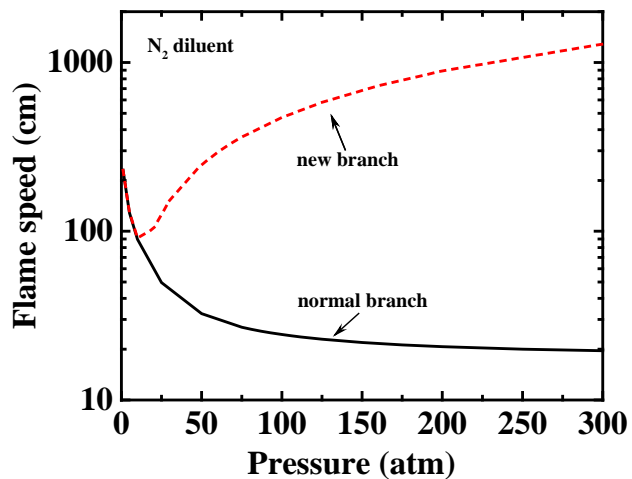
1. A. McClung, DE-FE0024041 Q1FY15 Research Performance Progress Report, SwRI

2. S. Coogan, X. Gao, W. Sun, Evaluation of Kinetic Mechanisms for Direct Fired Supercritical Oxy-Combustion of Natural Gas, TurboExpo 2016

Task 3: Development of a Compact and Optimized Chemical Kinetic Model for sCO₂ Oxy-combustion



- 1D Chemkin calculation with reduced model (only USC II converges)
- flame speeds at different pressure conditions of stoichiometric CH₄/O₂ with 80% diluent at 1000 K initial temperature



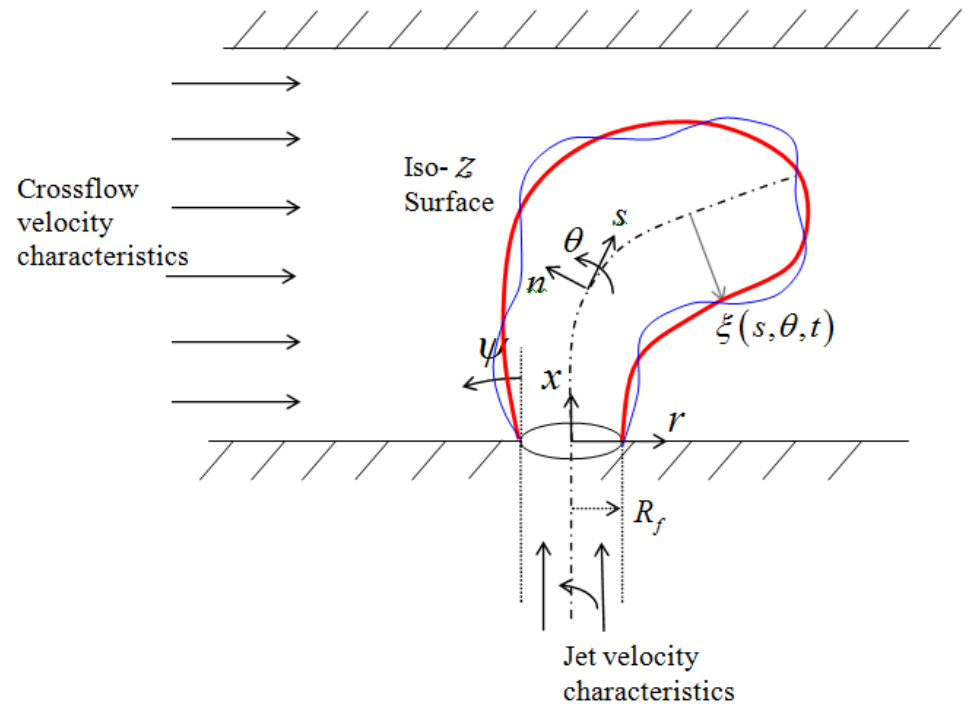
- Multiple solutions when $P > 25$ atm
- At 300 atm, how fast flame propagates? What will be observed in experiments and LES?
- Large flame speed: pulsating flame? Small flame speed: blow out?

Critical for combustor design

Task 4: Analytical modeling of Supercritical Reacting Jets in Crossflow



- Physics based models of reacting jet in crossflow (JICF)
 - Connect flow dynamics to flame dynamics
 - Modeling explicit flame position dynamics
- Understanding flow dynamics of a jet in crossflow



Analytic model of jet in crossflow



Challenges of Task 4

- Flame response modeling

- Majority of past work has addressed models for premixed flames
 - Explicit governing equations describing dynamic flame surface evolution (e.g., G equation)
- Non-premixed flames not well studied
 - mixture fraction framework, implicit representation of the flame
 - No explicit governing equations for flame position

- Challenges

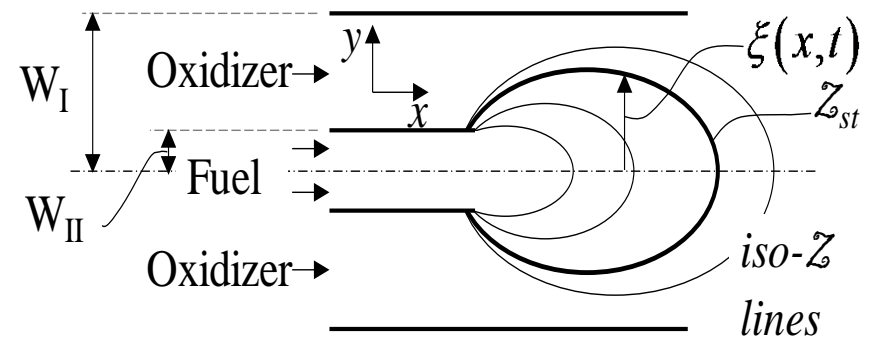
- Using governing equation for a full-field quantity (mixture fraction) to develop a governing equation for a given iso-contour of the mixture fraction solution
 - Boundary conditions are important => affect flame
 - Results in complicated non-linear governing equations, that require physics based simplifications
- Flow dynamics for a jet in cross-flow are not easily understood or modeled
 - Requires detailed understanding of flow from experiments and LES
 - Developing an analytical representation of flow for use in analytical models

Modeling Flame Surface Dynamics

- The non-premixed flame is modeled using the Burke-Schumann framework
 - Governing equation based on the mixture fraction formulation
 - assuming fast chemistry but equal diffusivities

$$\frac{\partial Z}{\partial t} + \mathbf{u} \cdot \nabla Z = \nabla \cdot (\mathcal{D} \nabla Z) \quad Z \equiv Y_{\text{Fuel}} + \left(\frac{1}{\varphi_{ox} + 1} \right) Y_{\text{Prod}}$$

- Flame location is based on the stoichiometric mixing of fuel and oxidizer
 - Stoichiometric iso-contour of mixture fraction field ($Z = Z_{st}$)
 - Example: simple ducted non-premixed flame with co-flowing fuel/oxidizer





Analytical Modeling Strategy

$$\frac{\partial \mathcal{Z}}{\partial t} + \mathbf{u} \cdot \nabla \mathcal{Z} = \nabla \cdot (\mathcal{D} \nabla \mathcal{Z})$$

- The mixture fraction and flow-field can be decomposed into steady mean (subscript 0) and unsteady perturbations (subscript 1)

- $u_i = u_{i,0} + u_{i,1}$; $\mathcal{Z} = \mathcal{Z}_0 + \mathcal{Z}_1$

- Decomposes governing equations into separate equations for steady state and dynamics (unsteady state)

$$(\mathbf{u}_0 \cdot \nabla) \mathcal{Z}_0 = \mathcal{D} (\nabla^2 \mathcal{Z}_0)$$

$$\frac{\partial \mathcal{Z}_1}{\partial t} + (\mathbf{u}_0 \cdot \nabla) \mathcal{Z}_1 - \mathcal{D} (\nabla^2 \mathcal{Z}_1) = -(\mathbf{u}_1 \cdot \nabla) \mathcal{Z}_0$$

- Solutions provide description of complete mixture fraction field



Iso-surface dynamics

- In a frame of reference (Lagrangian representation) fixed to the iso-surface, the material derivative vanishes

$$\left. \frac{DZ}{Dt} \right|_{Z=Z_{st}} = 0$$

- In the observer fixed frame of reference, the equation translates to:

$$\left. \frac{\partial Z}{\partial t} \right|_{Z=Z_{st}} + \left(\mathbf{u}_f \cdot \nabla Z \right) \Big|_{Z=Z_{st}} = 0$$

- The front velocity (u_f) is a combination of the ambient flow and the inherent front propagation velocity:

$$\left. \frac{\partial Z}{\partial t} \right|_{Z=Z_{st}} + \left(\mathbf{u} \cdot \nabla Z \right) \Big|_{Z=Z_{st}} = s_f(Z_{st}) \left| \nabla Z \right|_{Z=Z_{st}} \quad s_f(Z_{st}) = \frac{\nabla \cdot (\mathcal{D} \nabla Z) \Big|_{Z=Z_{st}}}{\left| \nabla Z \right|_{Z=Z_{st}}}$$

- The equation is valid only at the stoichiometric iso-surface and the front speed is a function of the stoichiometric mixture fraction.



Front Propagation Velocity

- Since governing equation at iso-surface is not valid anywhere else, the following transformation applies

$$Z - Z_{st} = \xi(x, t) - y \quad \frac{\partial \xi}{\partial t} + u \frac{\partial \xi}{\partial x} - v = s_f(Z_{st}) \sqrt{1 + \left(\frac{\partial \xi}{\partial x}\right)^2}$$

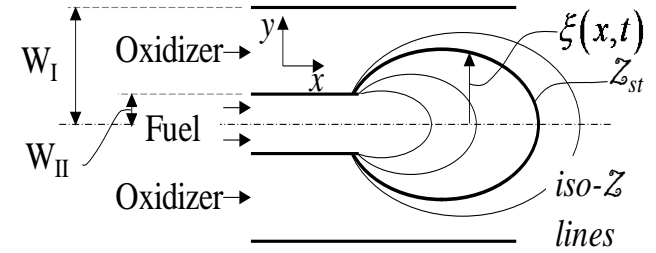
- Transformation does not apply to front-speed (relationship derived from a full-field mixture fraction governing equation)

- Front-speed obtained from iso-surface solution ($Z = Z_{st} = g(x, \xi, t)$)

$$s_f \sqrt{1 + \left(\frac{\partial \xi}{\partial x}\right)^2} = \left(\frac{\mathcal{D} \left(\frac{\partial_{\xi x} g}{\partial_{\xi} g} \right)}{u_D(x, \xi)} \frac{\partial \xi}{\partial x} + \mathcal{D} \frac{\partial^2 \xi}{\partial x^2} - \frac{\mathcal{D} \left(\frac{\partial_{\xi \xi} g}{\partial_{\xi} g} \right)}{s_D(x, \xi)} \left[1 - \left(\frac{\partial \xi}{\partial x}\right)^2 \right] \right)$$

Properties of Position Dynamics PDE

$$\frac{\partial \xi}{\partial t} + (u - u_D(x, \xi)) \frac{\partial \xi}{\partial x} - \nu = \mathcal{D} \frac{\partial^2 \xi}{\partial x^2} - s_D(x, \xi) \left[1 - \left(\frac{\partial \xi}{\partial x} \right)^2 \right]$$



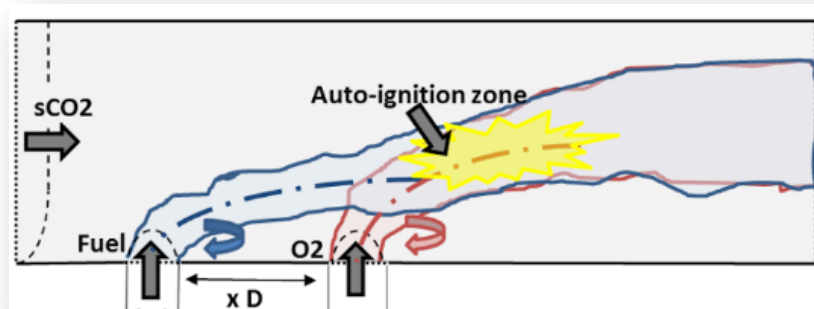
- **Non-linear wrinkle convection**
 - Flow based convection as well as position-coupled diffusion based convection
- **Linear term from “Diffusion” of wrinkles**
 - Similar to stretch effects in premixed flames (i.e. stretch correction to flame speed)
- **Non-linear term from diffusion**
- **Boundary conditions**
 - physics required input from full-field mixture fraction solutions (diffusion wave transport & non-linear diffusion term)
 - Stems from the fact that boundary conditions (at inlet, walls etc.) need to be accounted for in “reduced” governing equation for flame position



Future Directions for Task 4

- Linearization of position dynamics governing equation
 - Steady state governing equation
 - Flame wrinkle governing equation
- Application of position dynamics to reacting jet in crossflow configuration
- Identification of key control parameters
- Spatially integrated total heat release dynamics
- Comparisons with real reacting jets in crossflow

Task 5: LES Studies of Supercritical Mixing and Combustion



Baseline model
NOT actual design

- Systematic variation of design parameters
 - Momentum ratios for fuel and oxygen, number of jets
 - Size and spacing of injectors
 - Fuel upstream of oxidizer jet
 - Flow rates
- Computational modeling may be more cost effective but include its own challenges
 - Autoignition kinetics (large uncertainty, maybe wrong)
 - Turbulence-chemistry closure
 - Real gas effects



Task 5: LES Studies of Supercritical Mixing and Combustion

- Pressure: 300 bar
- ~90 % CO₂ concentration
- Inlet temperature: 1100K
- All incoming fluids are Supercritical
 - O_{2c} (50 bar, 155 K),
 - CO_{2c} (77 bar, 304 K),
 - CH_{4c} (46 bar, 190 K)
- Reduced Kinetics needed

Mechanism	Species	Steps
USC II	111	784
Reduced ¹	27	150
Jones-Lindstedt ²	7 (6*)	4

¹Coogan et al., ASME Turbo Expo (2016)

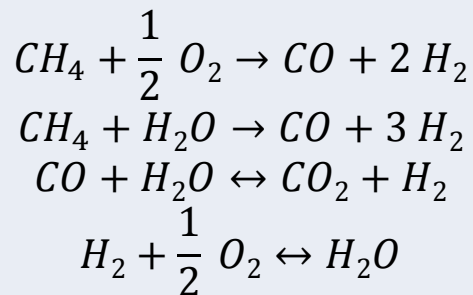
²Jones & Lindstedt, Comb Fl. (1988)

* Does not include N₂

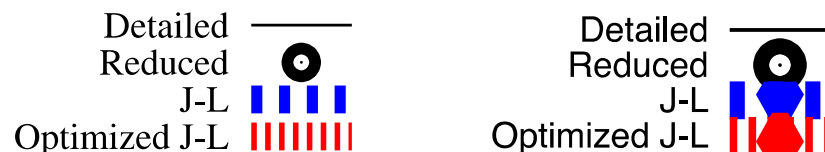
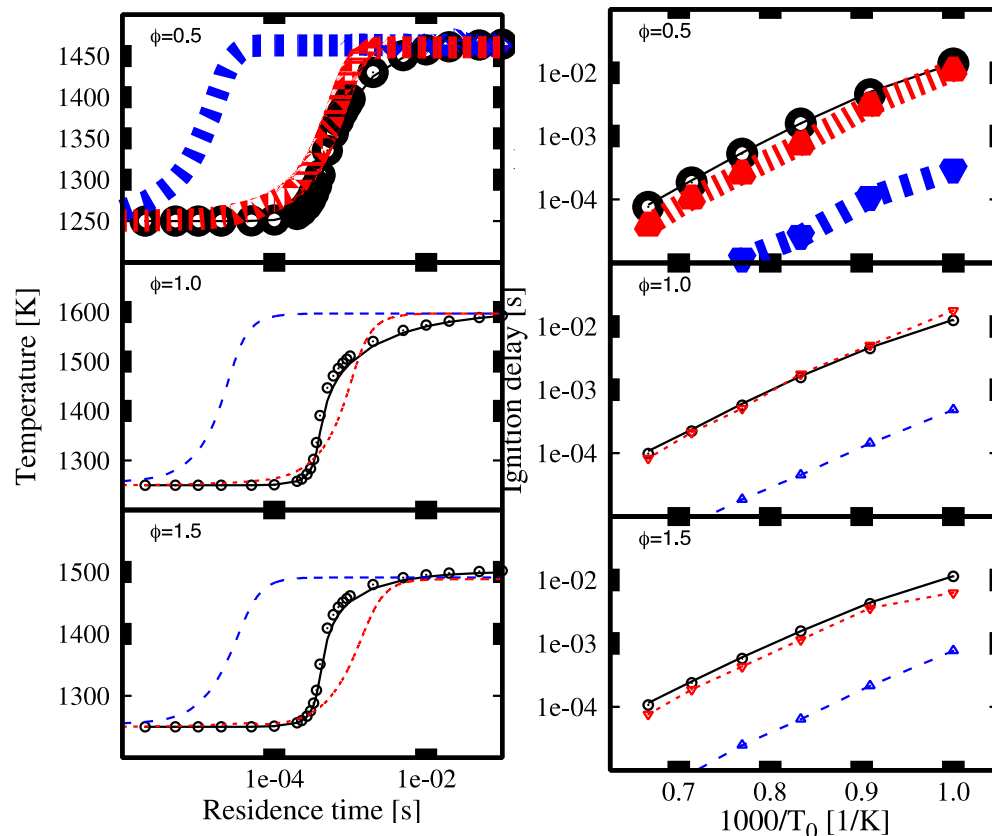
Parameters	Value
P _{ref}	300 bar
T _{cross}	1100 K
U _{cross}	50 m/s
T _{jets}	300 K
J _{Ox}	20
J _F	18.4
D _F /D _{Ox}	0.6
Channel length	75 D _{ox}
Re _{JOx} , Re _{JF} , Re _{CO2}	4.4 x 10 ⁵ , 7.8 x 10 ⁵ , 1.5 x 10 ⁶

Modified Jones-Lindstedt (J-L) Mechanism

- Quick assessment
- Only CH_4 , O_2 , CO , H_2 , H_2O , CO_2
- modified to predict T_{ad} and ignition



Step Number	A (Original)	A (Modified)
1	4.4×10^{11}	1.1×10^{10}
2	3.0×10^8	7.21×10^6
3 (forward)	2.75×10^9	6.6×10^7
3 (backward)	8.0×10^{10}	1.91×10^9
4 (forward)	6.8×10^{15}	1.63×10^{14}
4 (backward)	7.1×10^{17}	1.70×10^{16}





Numerical Methodology

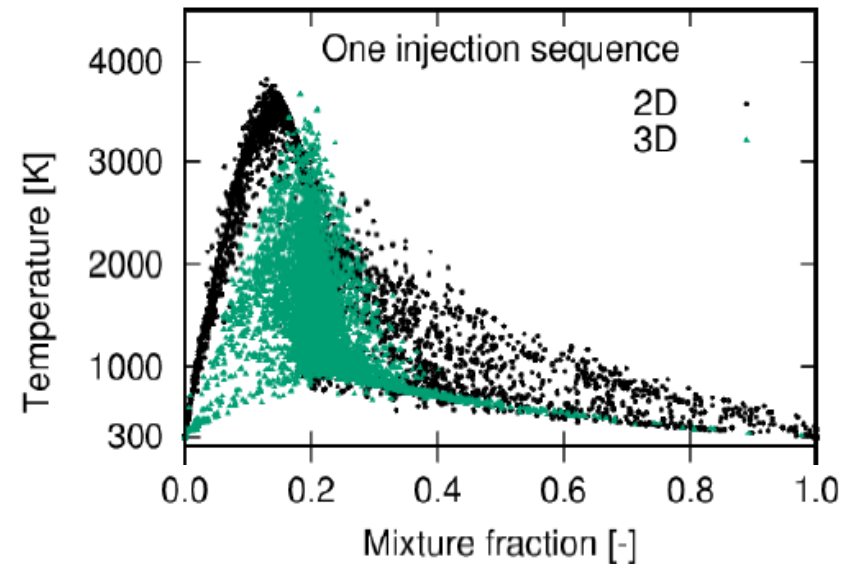
- **LESLIE**; a multi-species compressible flow solver¹:
 - 3D Adaptive Mesh Refinement finite-volume solver
 - Mesh adapted and then frozen once solution settles down
 - 2nd order Predictor-Corrector with artificial dissipation
 - Time integration: 2nd order explicit
 - Characteristics based boundary conditions
 - **Chung's transport** with **Peng Robinson Real Gas** EOS
 - Thermally perfect gas EOS used for comparison
- Subgrid-scale (SGS) closures:
 - Momentum, energy & scalar subgrid fluxes: One-equation model turbulent kinetic energy² model used for closure
 - Kinetics computed using filtered variables

¹Genin & Menon, AIAA J., 48, 2010; ²Kim & Menon, I. J. Numer. Meth. Fluids, 31, 1999

2D/3D Preliminary Investigations: Flame Structure



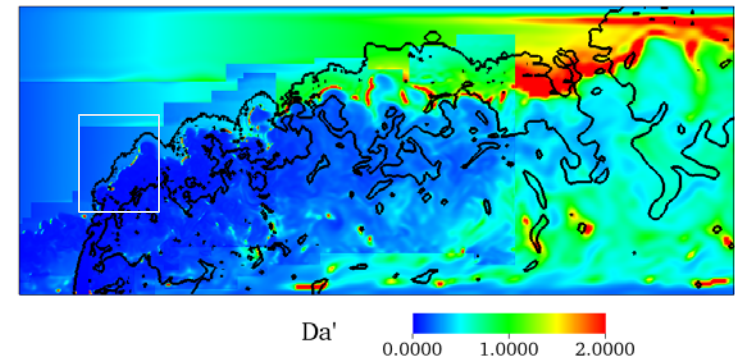
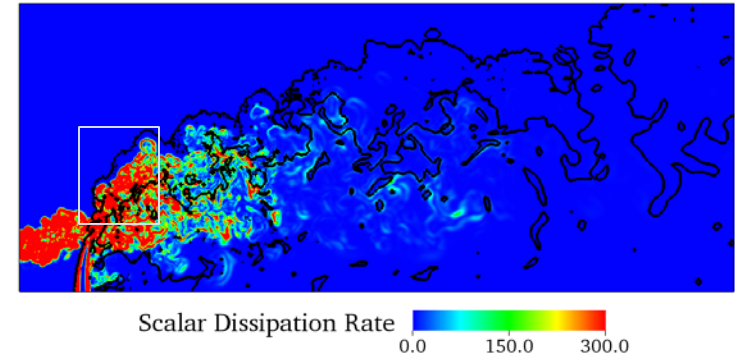
- Flame anchoring very different:
 - 2D: flame anchoring occurs on jets
 - 3D: Lifted flame anchored on oxidizer jet
 - engulfment and jet wake effects
- Differences in combustion regime:
 - 2D: reaction occurs in **rich** regime
 - 3D: **reaction occur close to stoichiometry and on lean side**
- 3D needed for accuracy:
 - CPU cost severe for multi-block grid
 - 32/65/90M for single/two/three
 - Use AMR as alternative approach
 - Cost effective and refined
 - Structured grid for high accuracy



Combustion regime
and flame structure

Non-Reacting: Analysis of Scalar Mixing

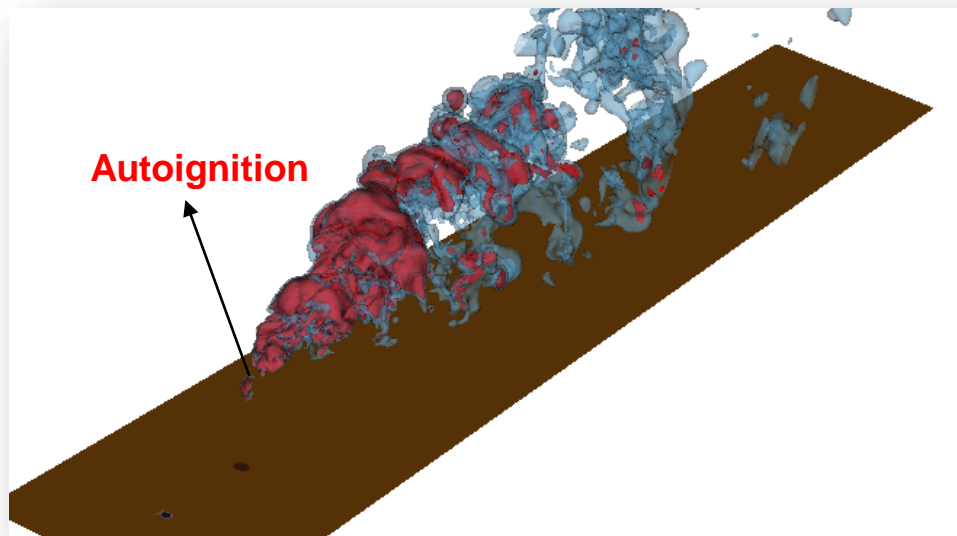
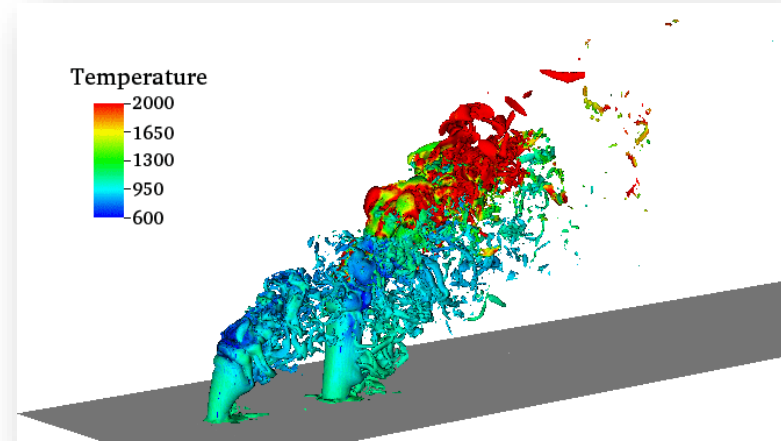
- Flow must have enough time for fuel and oxidizer to mix and then ignite (T is high enough)
- Da' : ranges from $\ll 1$ to $O(1)$
- Iso-lines represent the stoichiometric mixture fraction value
- The boxed regions:
 - Near stoichiometric with low S.D.R.
 - Possible auto-ignition region
 - Kinetics controlled



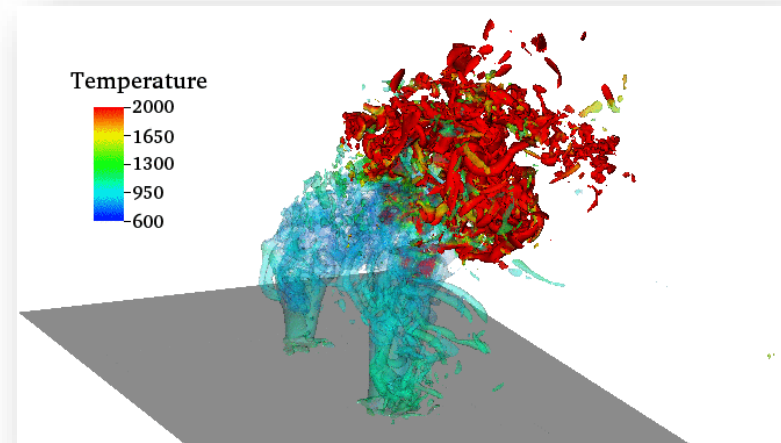
$$Da' = \frac{\tau_{mix}}{\tau_{ignition\ delay}}$$

Instantaneous Reacting Flow Features

- Autoignition close to predicted location based on mixing
- Autoignition occurs slightly downstream of the oxidizer jet towards lean side
- Autoignition with lifted flame structure

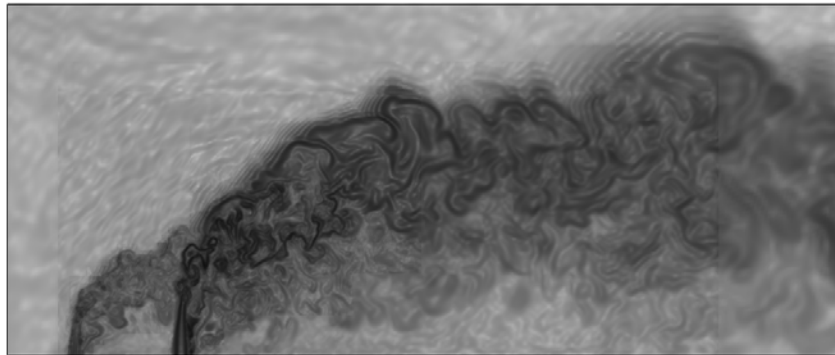


Temperature iso-surface (2100 K, 1500 K)



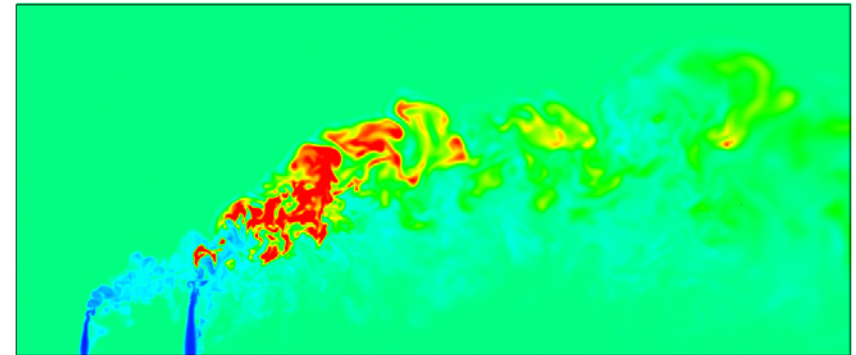
Vorticity magnitude colored by temperature

Instantaneous Reacting Flow Features



Schlieren 1 5 8 12 16

Schlieren

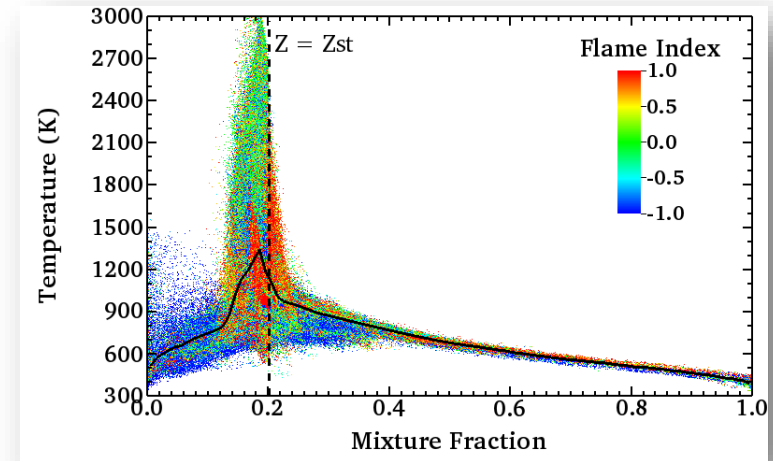
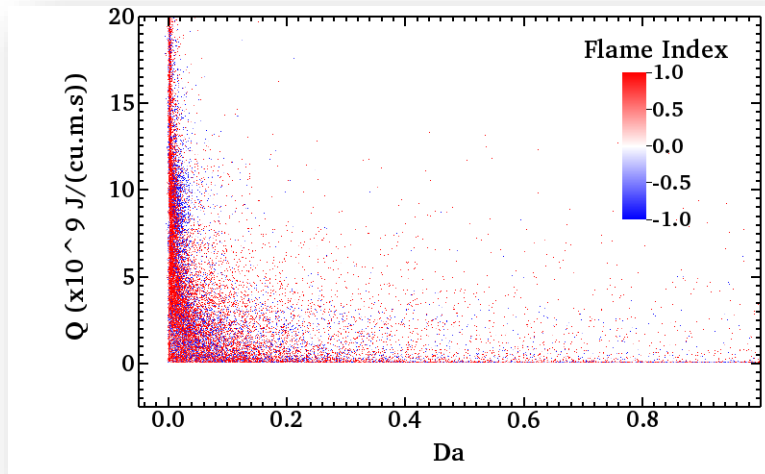


Temperature 300 850 1400 1950 2500

Temperature

- Large density gradient (Schlieren: log of density gradient)
- Mixing of fuel and oxidizer followed by ignition in lifted regions
- Autoignition in hot kernels where fuel mixes with oxidizer
 - Finite-size kernel but no continuous flame structure
- Autoignition sensitive to many parameters: mixing time, kinetics, local scalar dissipation rate, etc.

Instantaneous Flame Structure



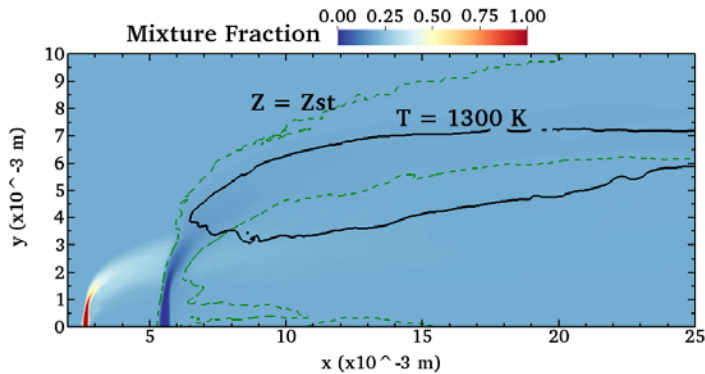
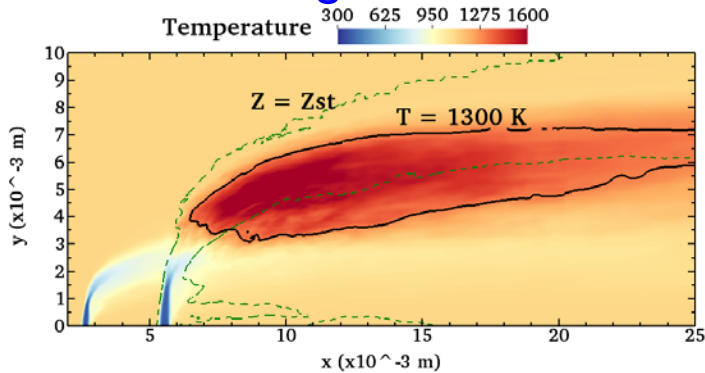
Heat release rate v/s Damkohler number

Temperature v/s mixture fraction

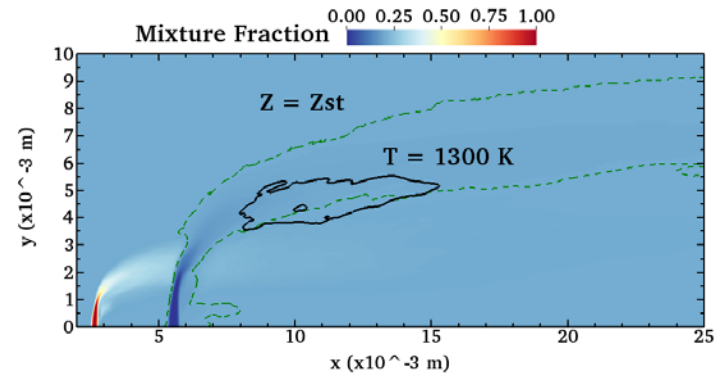
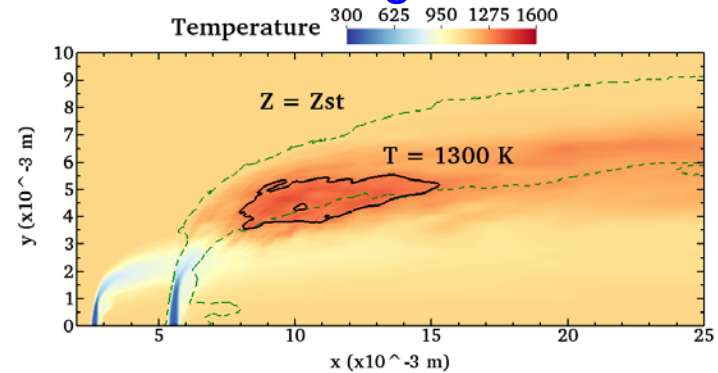
- $Da \ll 1$ (flow property resolved, slow chemistry)
- Multi-mode combustion after ignition
 - Flame Index is positive (premixed) & negative (non-premixed)
 - Most of burning occurs under lean conditions
- Compressibility factor shows marginal variations (is PG OK?)

Effect of Compressibility

Real gas EOS



Perfect gas EOS

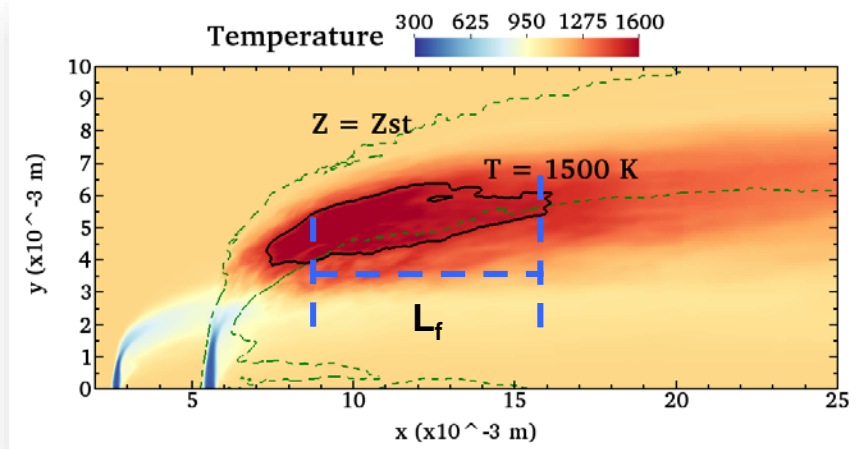


- Both cases simulated at same operating conditions
- Reduced jet penetration with perfect gas EOS in comparison to Peng Robinson EoS – clearly shows RG effects
- Heat release also decreased with perfect gas EOS

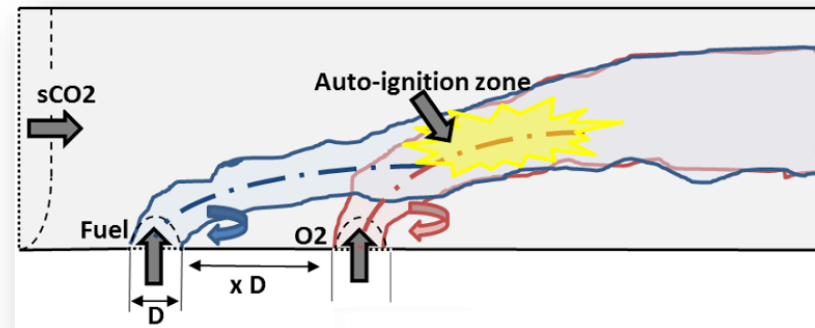
Flame Length and Combustion Efficiency

- Combustion is not efficient
- Combustion efficiency estimated as:

$$\eta = 100 \times \frac{\dot{m}_{f,in} - \dot{m}_{f,out}}{\dot{m}_{f,in}} \sim 49\%$$
- Flame length, $L_f \sim 14.5 D_{ox}$
 - estimated as intersection of $Z = Z_{st}$ and $T = 1500 \text{ K}$
- η needs to be improved
 - Inflow realistic turbulence
 - Modify J and jet spacing
 - Mass flow rate changes
 - Jet-staging and distributed mixing
 - Inflow swirl
- More studies needed and underway



Temperature overlaid with stoichiometry line





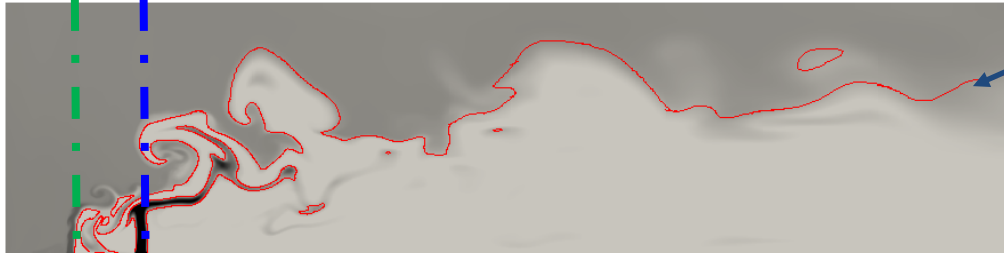
2D Preliminary Investigation: Density

Injection sequences

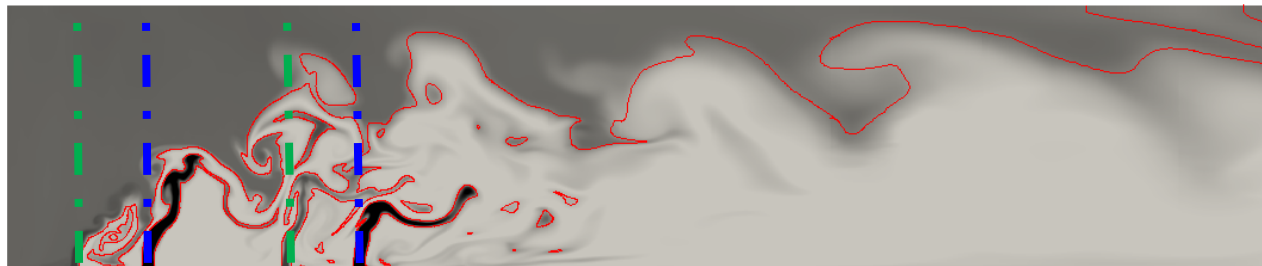
CH₄ O₂

T = 1200 K

One



Two

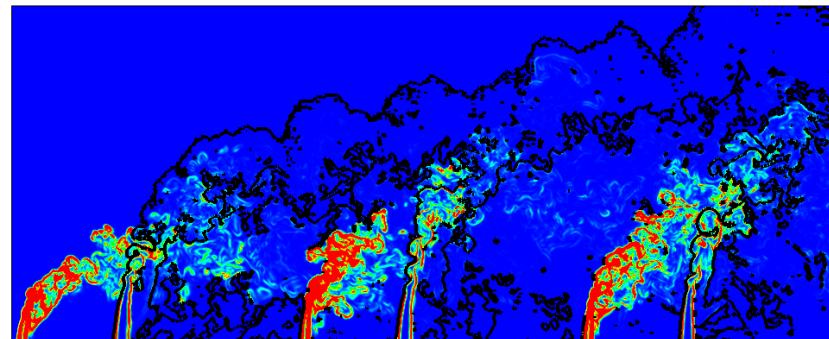
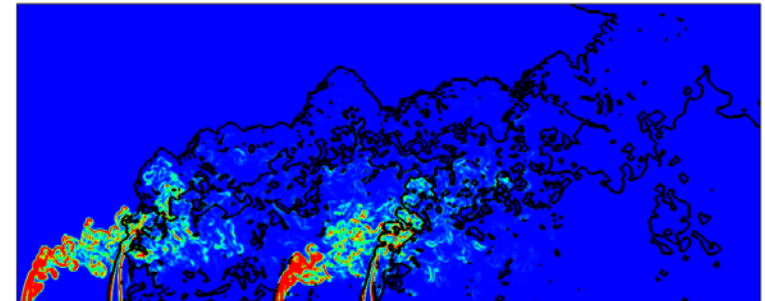
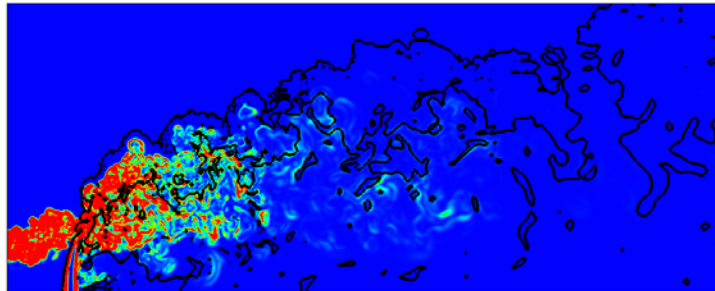


Three



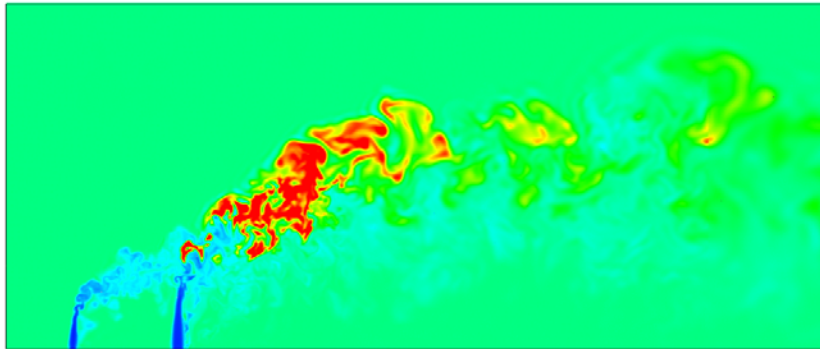
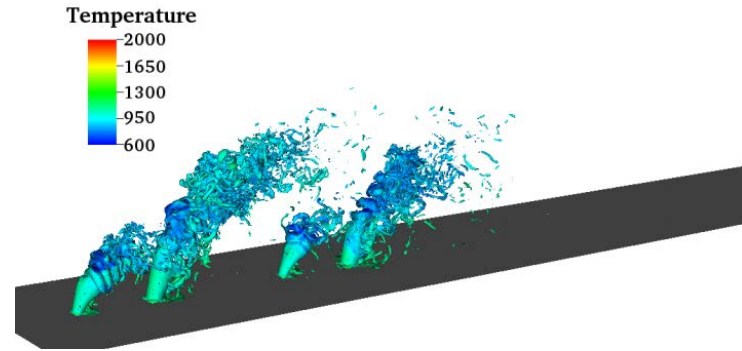
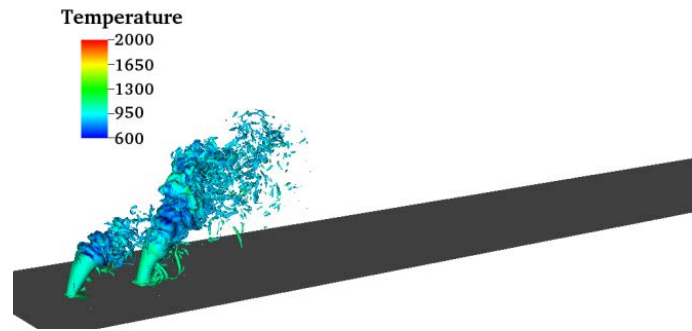
1st sequence 2nd sequence 5.000e+01 300 450 600 8.600e+02

Multi-Jet Mixing with Real Gas

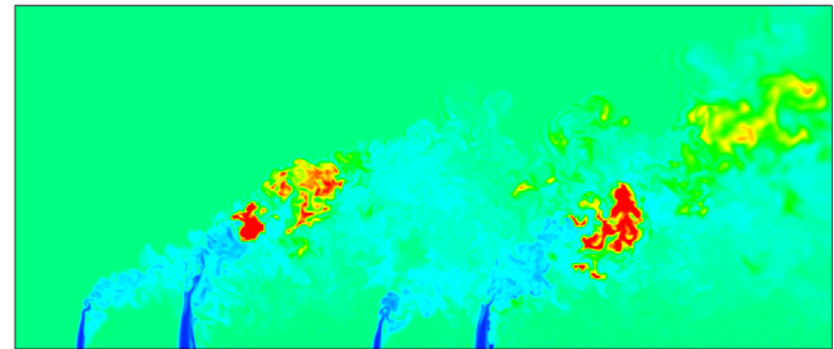


- 1-set, 2-set and 3-set show differences in mixing and locations of low SDR
- Possible interactions due to acoustic waves in subsonic
- Multiple JICF configurations may all be unique

Autolgnition and Blow out



Temperature 300 850 1400 1950 2500



Temperature 300 850 1400 1950 2500

- Limitations of kinetics
- Influence of upstream acoustic waves



Future Directions for Task 5

- Future studies to focus on
 - Effect of chemical kinetics – employ more detailed kinetics
 - Locations and injection strategies for fuel and oxygen non-reacting mixing studies with different injector locations to determine how to increase the low SDR regions (autoignition)
 - 1D LEM to handle all flame regimes
- Challenges
 - reliable mixing rules and kinetics
 - SGS closure for high Re multi-mode combustion (how to dynamically switch between different combustion regimes)



Summary of Year 1 Achievement

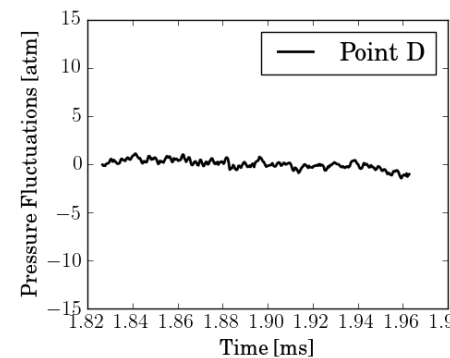
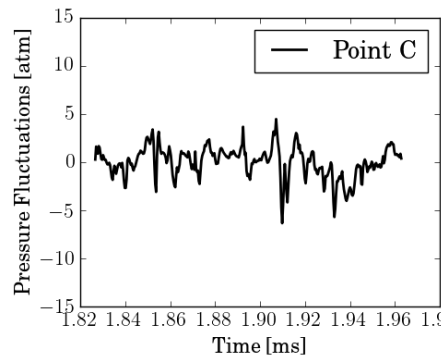
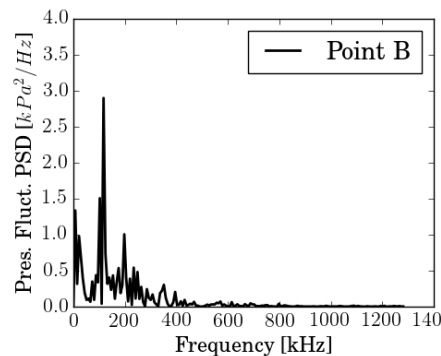
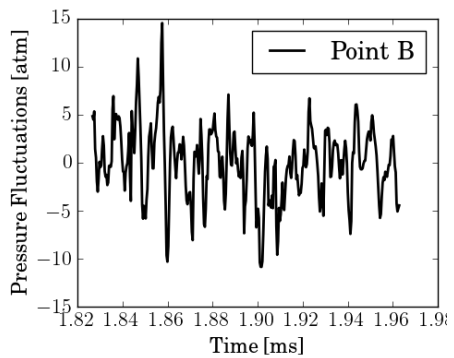
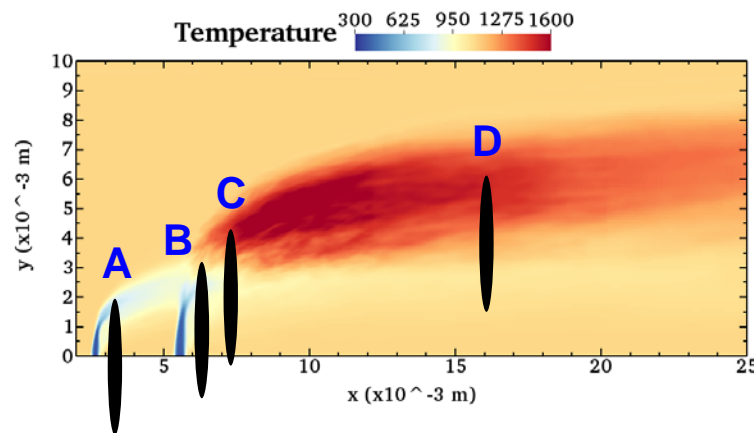
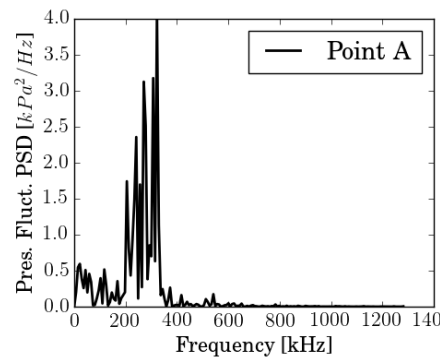
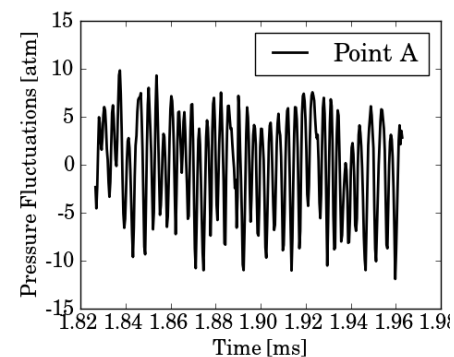
- High pressure shock tube developed
- Reduced kinetic model with 27 species for natural gas and syngas
- Governing equation developed for theoretical frame work
- LES investigation of JICF
 - Real gas effect
 - 3D effect
 - Deficiency of kinetics, insight to combustor design

Thank you!
&
Questions?

Acknowledgement:

UTSR Project: DE-FE0025174; PM: Seth Lawson

Analysis of Pressure Fluctuation

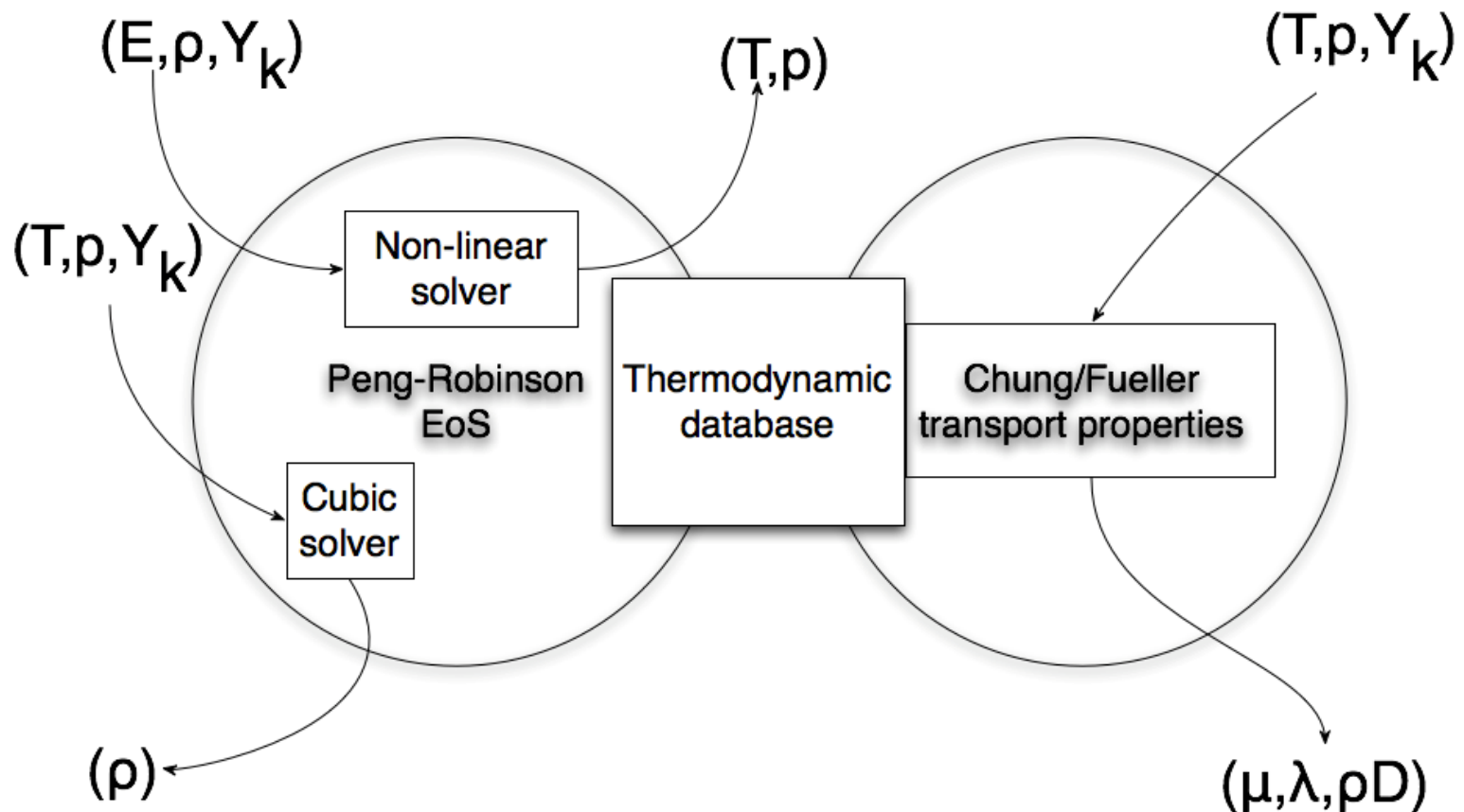


- Pressure at various locations (Autoignition location C)
- At A and B ~ 3-5% fluctuations due jet interacting with cross flow
 - St of peak frequencies range from 0.1 – 1.1 (~ jet preferred modes)
- At C and D, the fluctuations are purely indicative of turbulent fluctuations

Task 5: LES Studies of Supercritical Mixing and Combustion



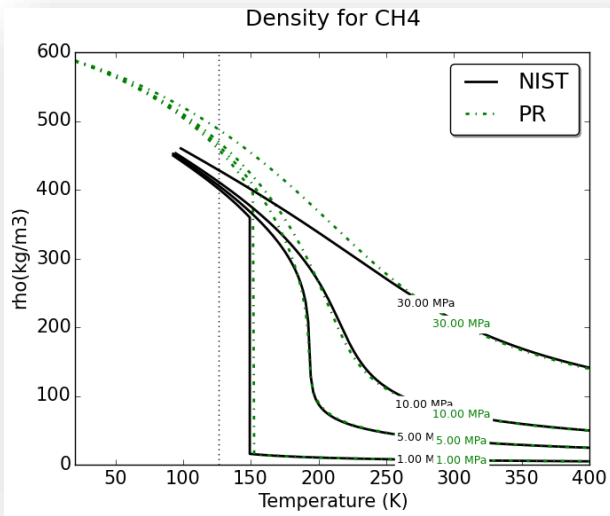
Real gas framework



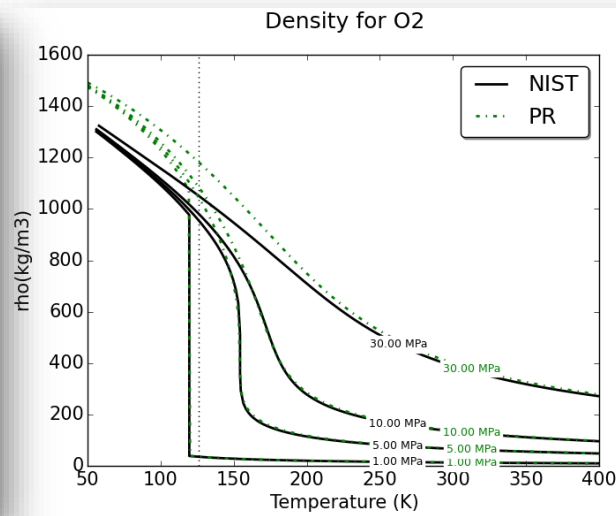


Modeling Under Supercritical Conditions

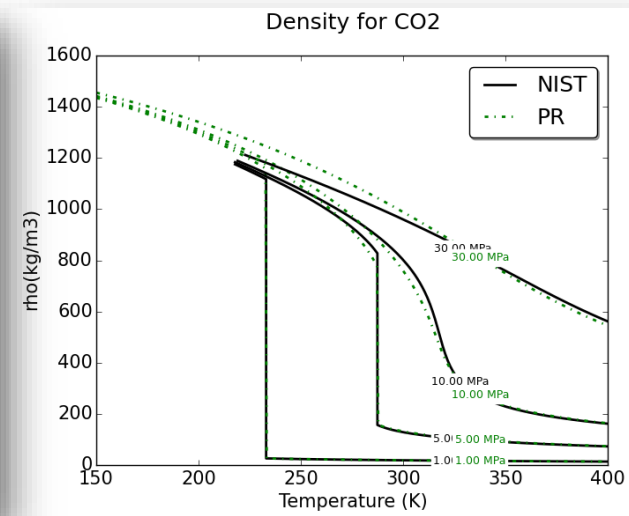
- Fluid properties assessed for methane, oxygen and carbon dioxide against reference NIST database
- Reasonable agreement for a wide range of operating conditions
- Peng Robinson cubic EoS is adequate for present study



Methane



Oxygen



Carbon dioxide