



Biogasification Panel

2015 Gasification Systems and Coal & Coal-Biomass Workshop

Morgantown, WV
August 11th, 2015



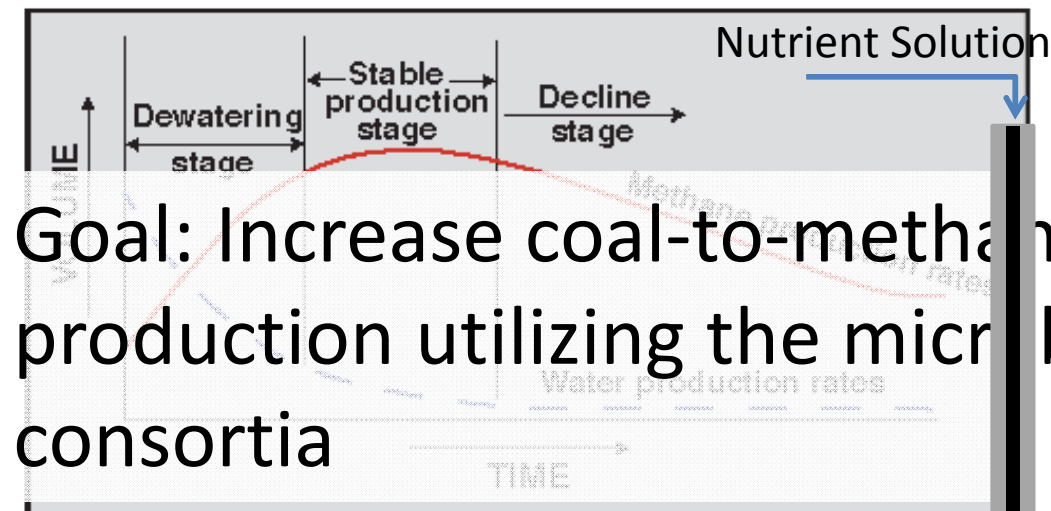
U.S. DEPARTMENT OF
ENERGY

National Energy
Technology Laboratory

Panelists

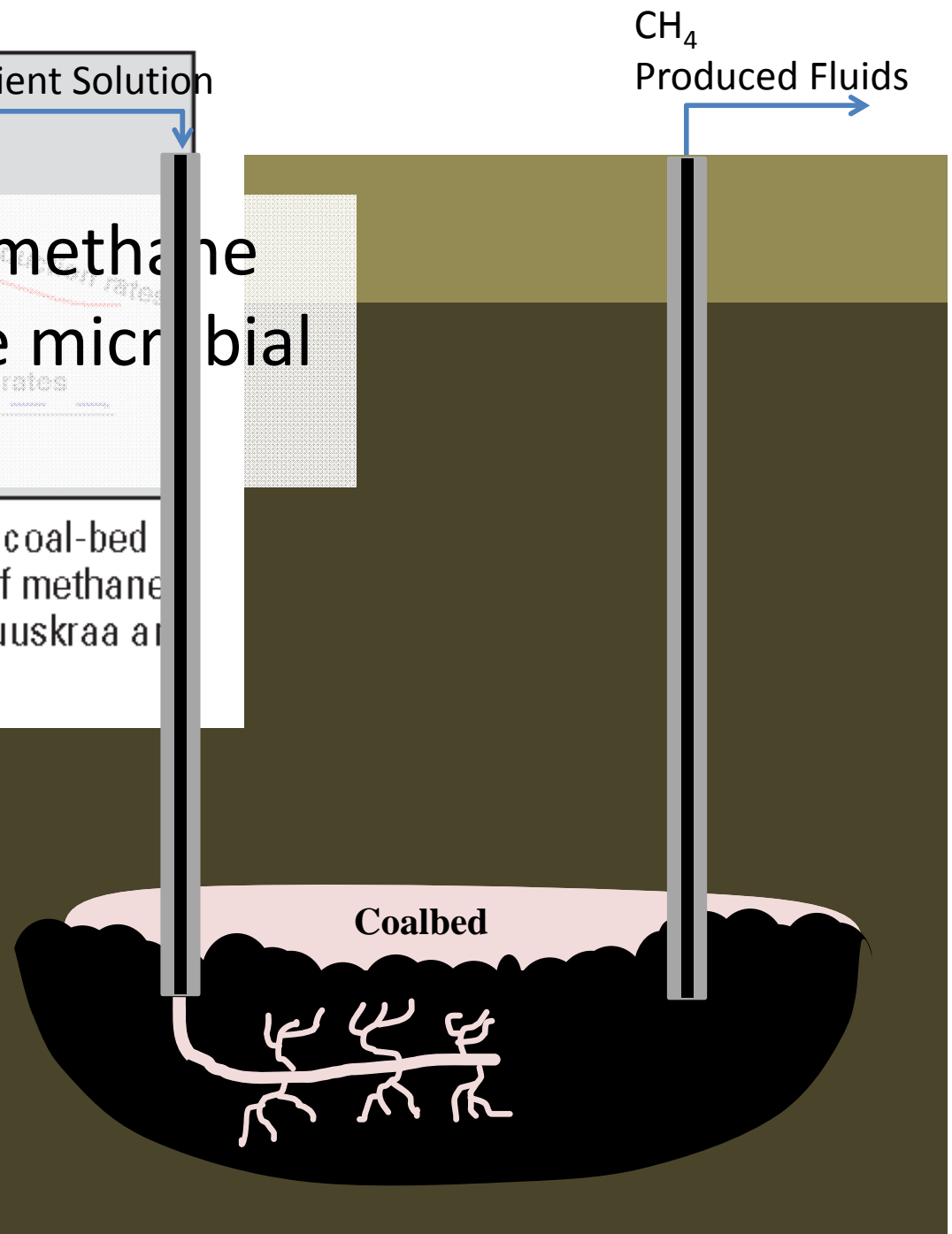


- Djuna Gulliver, Ph. D. (Moderator) – NETL-DOE
- Yael Tucker, Ph. D. – NETL-DOE
- Prof. Yanna Liang, Ph. D., P.E. – Southern Illinois University
- Prof. Matthew Fields, Ph. D. – Montana State University
- Prof. Taylor Sparks, Ph. D. – University of Utah

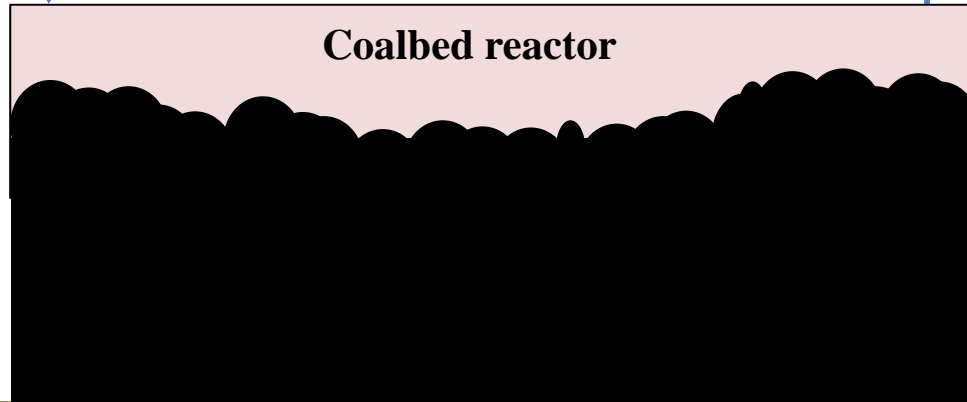


Goal: Increase coal-to-methane production utilizing the microbial consortia

Figure 2. Typical production curves for a coal-bed methane well showing relative volumes of methane and water through time. Modified from Kuuskraa and Brandenburg (1989).



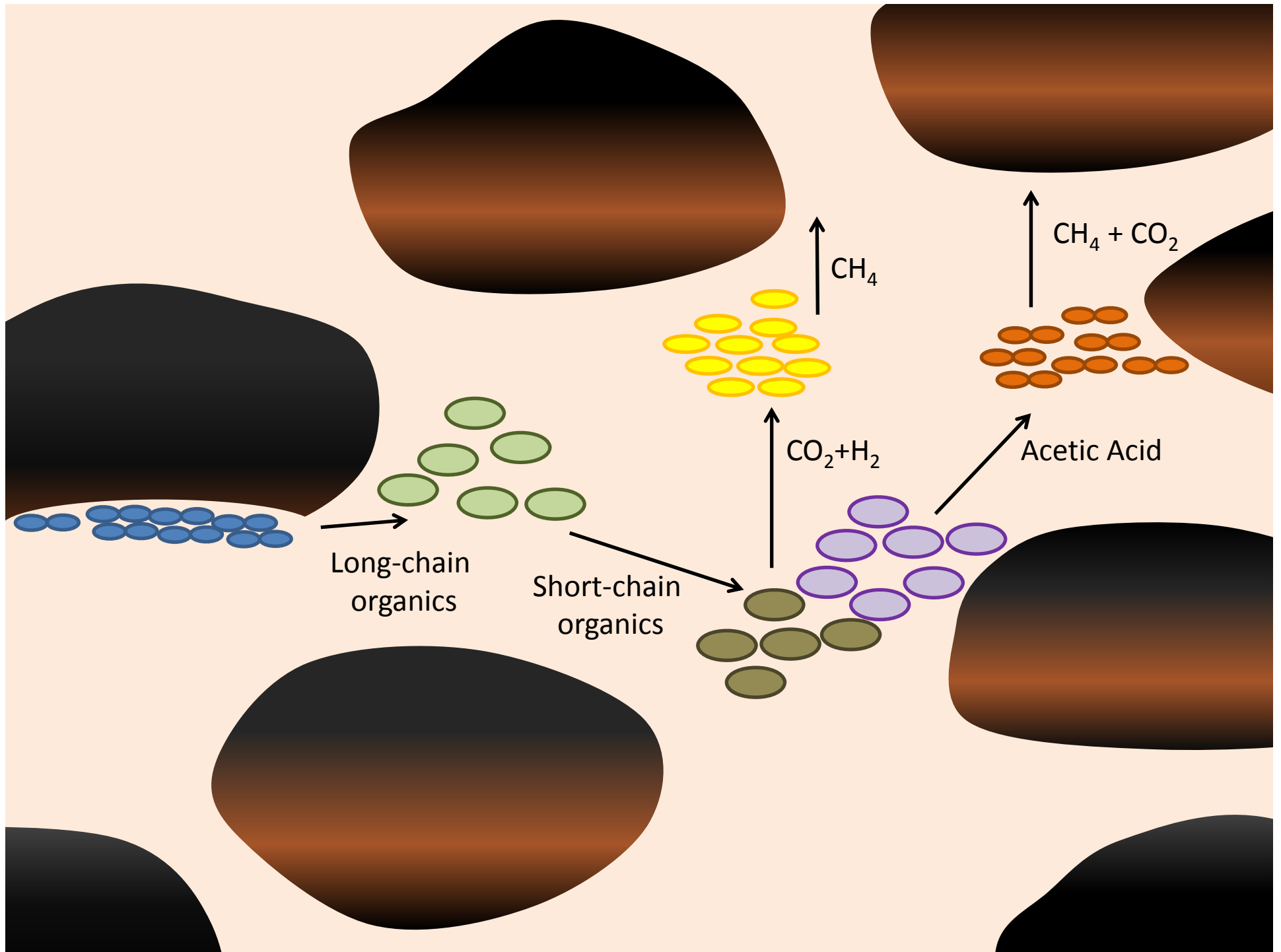
Nutrient Solution



Coalbed reactor

CH₄







Biogasification

Yael Tarlovsky Tucker - Genetics/ Microbiology

Djuna Gulliver - Environmental Engineering

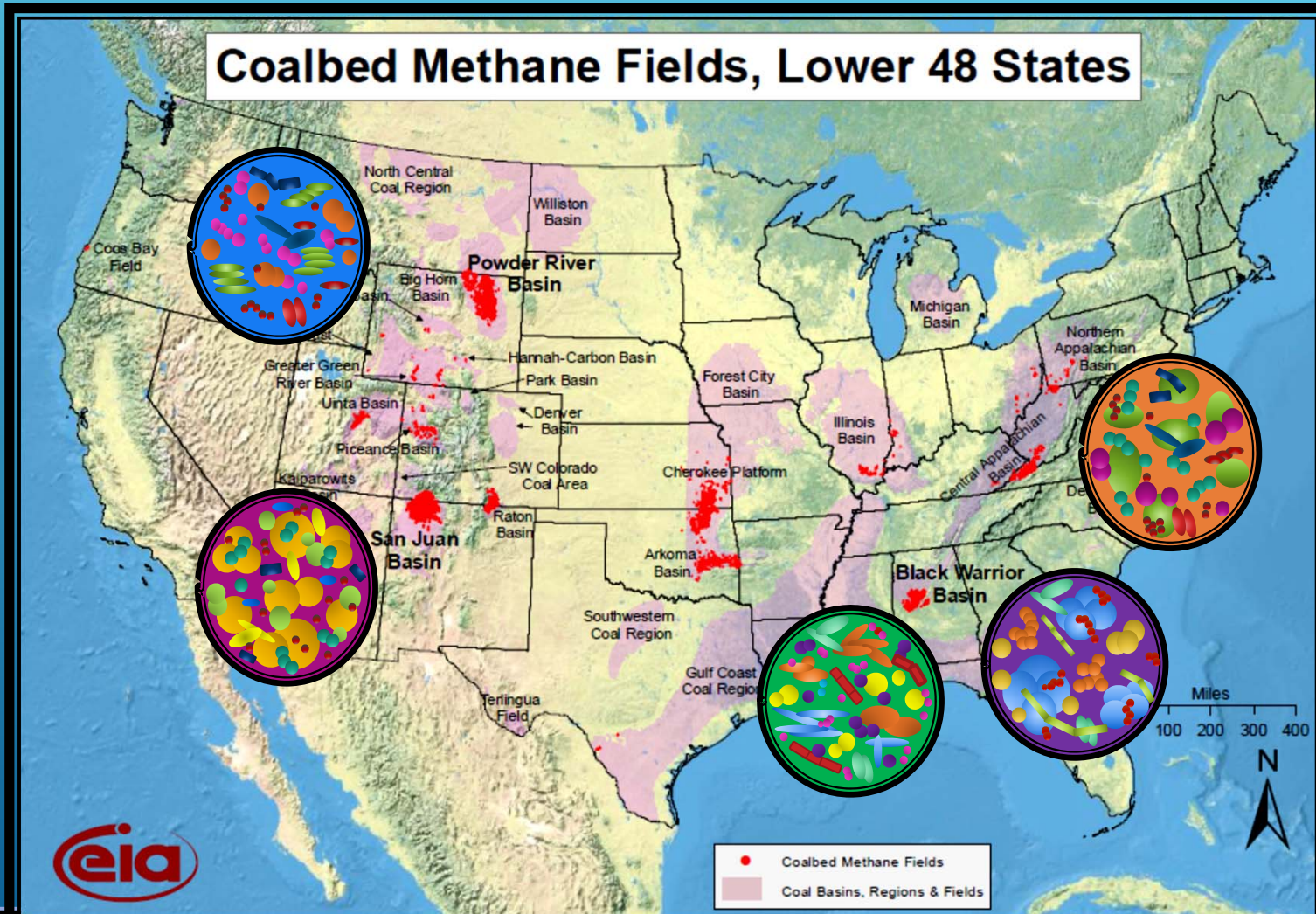
Mark McKoy - Geology

Engineered Natural Systems Division

August 11, 2015

GENETIC CHARACTERIZATION OF MICROBIAL COMMUNITIES IN "UN-MINEABLE" COALS

At NETL, our initial goal will be to characterize the native microbial communities across different basins in the United States in reference to chemical composition, and geologic characteristics of different reservoirs.

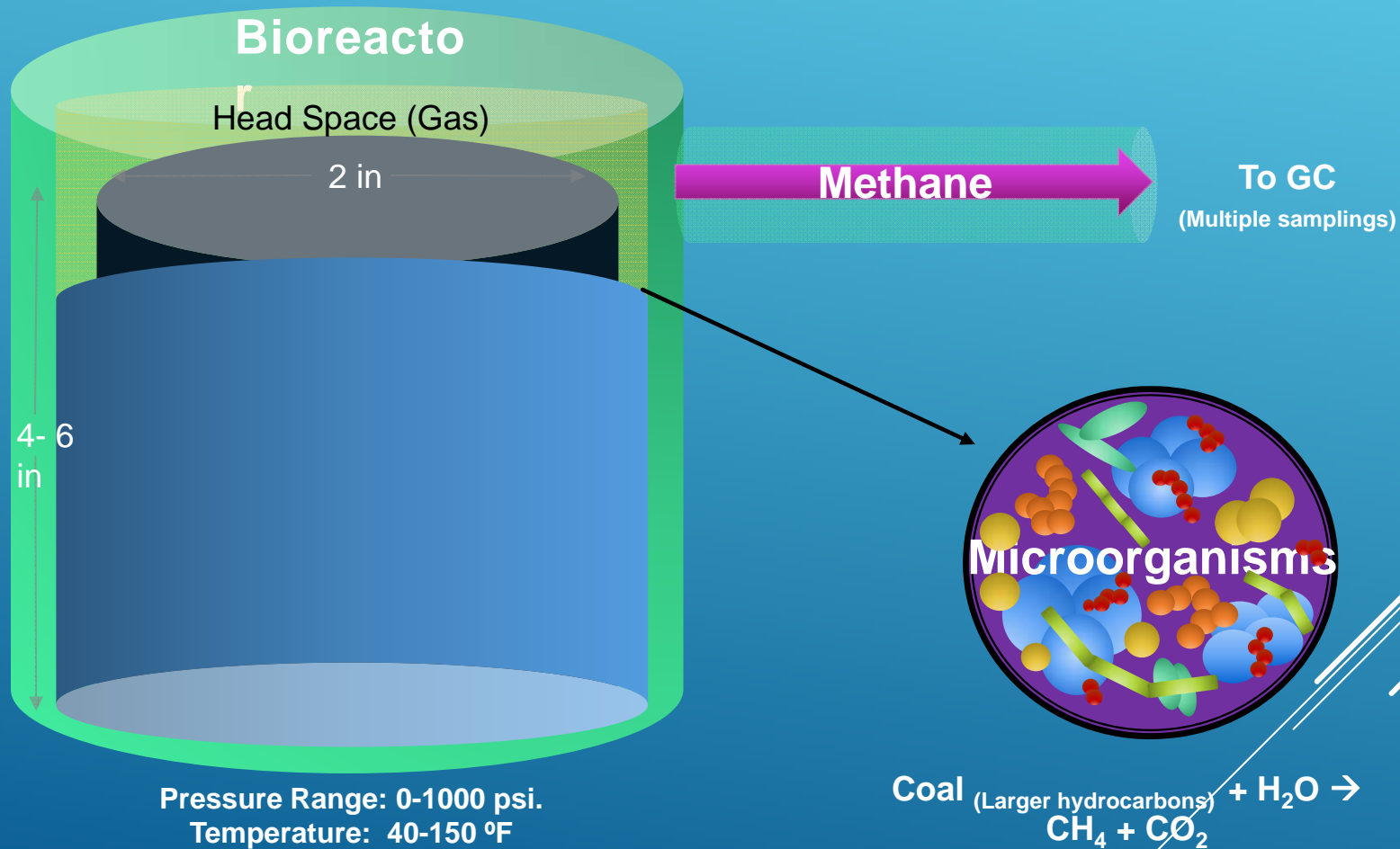


Source: Energy Information Administration based on data from USGS and various published studies
Updated: April 8, 2009



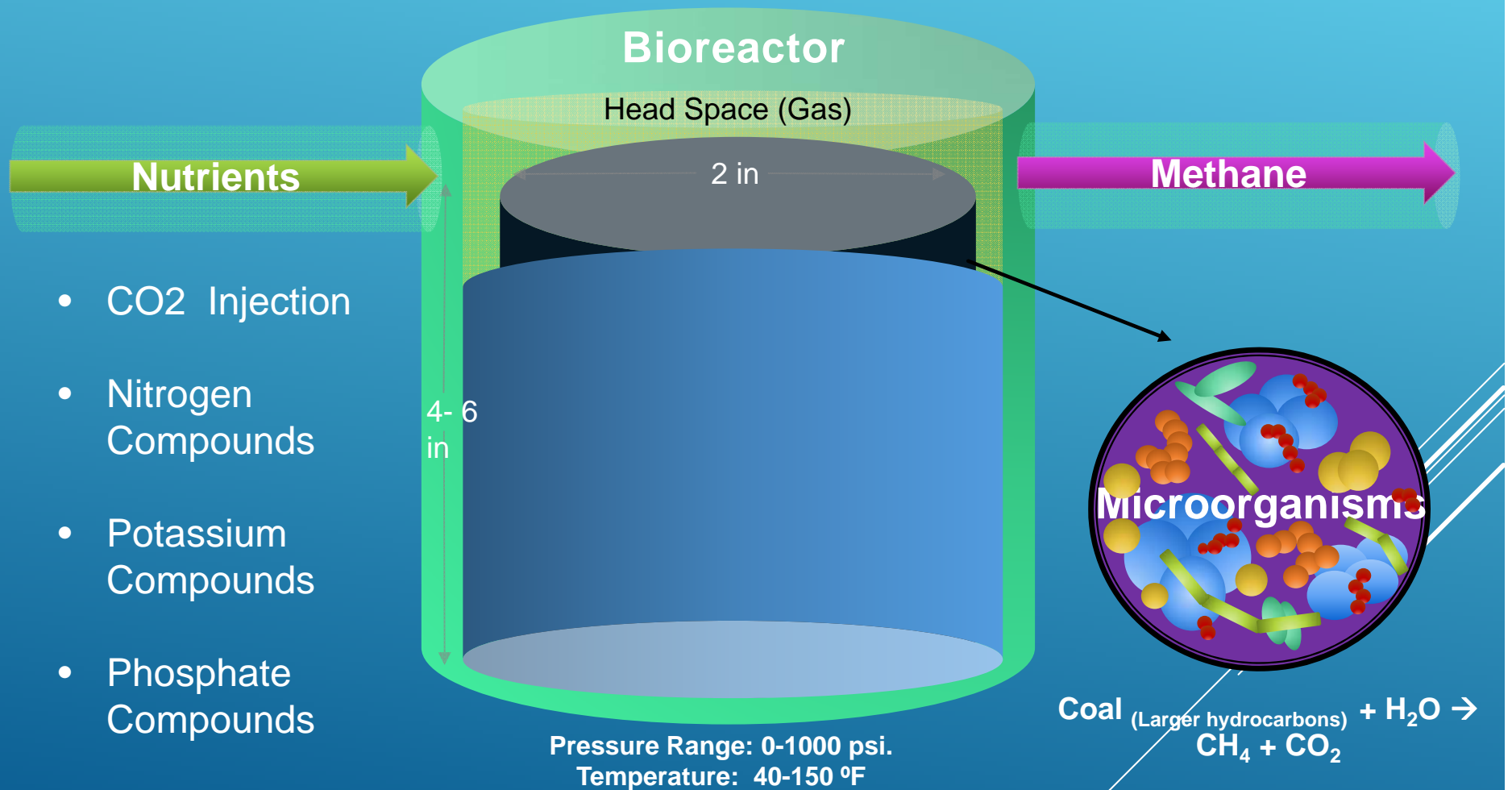
ASSESSMENT OF NATURAL BIOGENIC GENERATION POTENTIAL

In combination to any production values acquired from any coals from coalbed methane reservoirs, natural methane potential will then be assessed using bench-top bioreactors. We will then compare this to the microbial, chemical, and geological characteristics and strive to understand their relationship.



NUTRIENT ENHANCEMENT TESTS

This information will then be utilized to work with the natural consortia and complement their environment with inexpensive nutrients that may be limiting methane production in each reservoir. Together, these tests should help us find an inexpensive solution for enhancing the natural methane production potential several types of unmineable coals.



FUTURE DIRECTIONS

Once we develop a series of nutrients that enhance methane production in our bioreactors, we will progress to a field demonstration where nutrients will be pumped into reservoirs. These test sites may include existing depleted coalbed methane wells or greenfield sites new to coalbed methane production.



Nutrients

Microorganisms

Methane

Un-mineable Coal

Optimized microbial conversion of
bituminous coal to methane for
in situ and *ex situ* applications

Yanna Liang, Ph.D., P.E.

08-11-2015

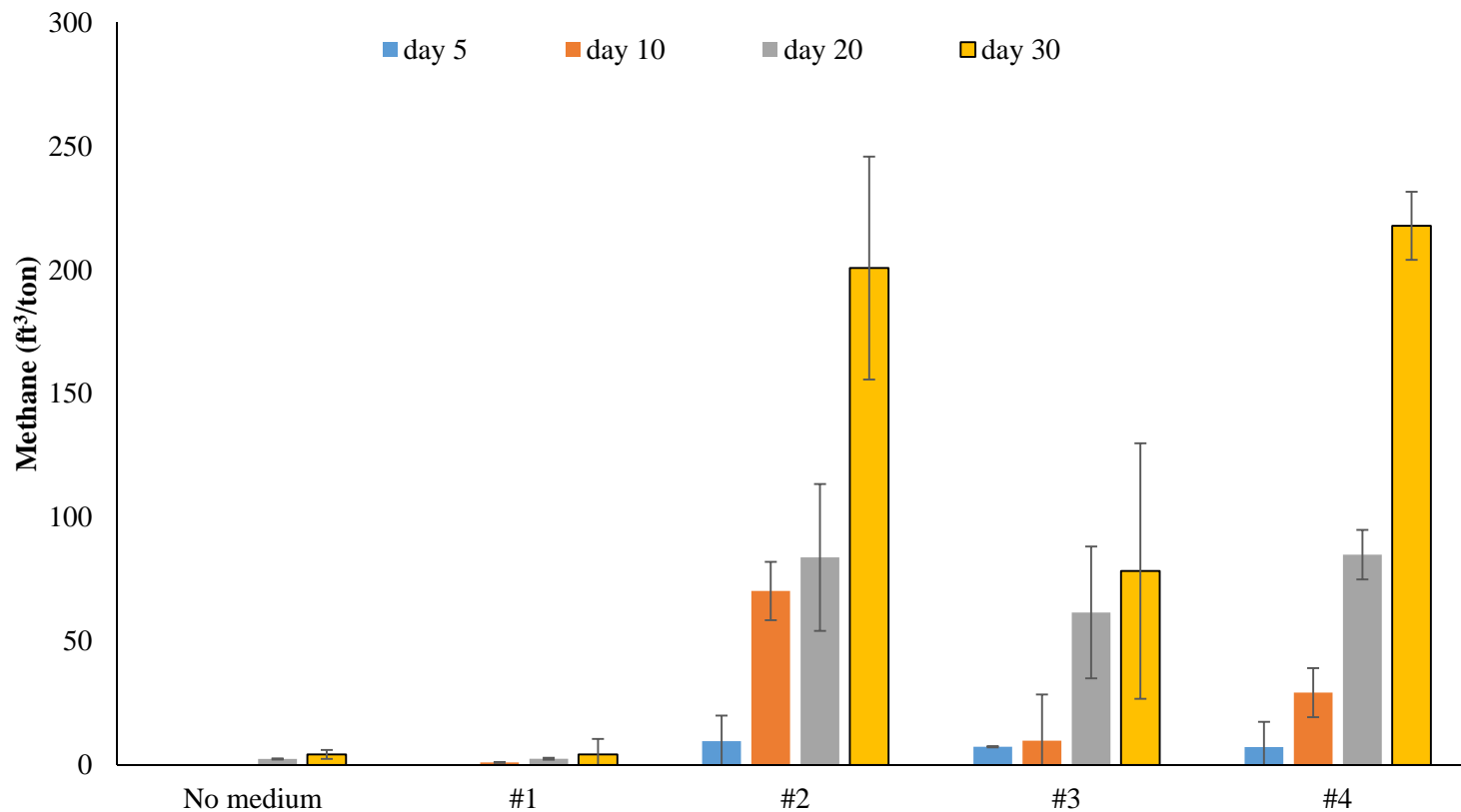
Overall Objectives

- 1) Optimize methane production from bituminous coal through biogasification
- 2) Demonstrate feasibility of the developed technology for *ex situ* and *in situ* applications

Tasks

- Task 1.0 : Project Management, Planning and Reporting
- Task 2.0: Simplify the composition of the nutrient medium
- Task 3.0: Investigate individual and interactive effects from different parameters
- Task 4.0: Maximize methane productivity in a fed-batch system
- Task 5.0: Bioconversion under pressurized conditions
- Task 6.0: Ecological Considerations of the Proposed Process
- Task 7.0: Economic Analysis of the Proposed Process

Comparison of nutrient solutions



#1: General medium for anaerobic bacteria

#2: Medium for methane-producing methanogens

#3: Simplified medium based on #2

#4: Trypticase soy broth based medium

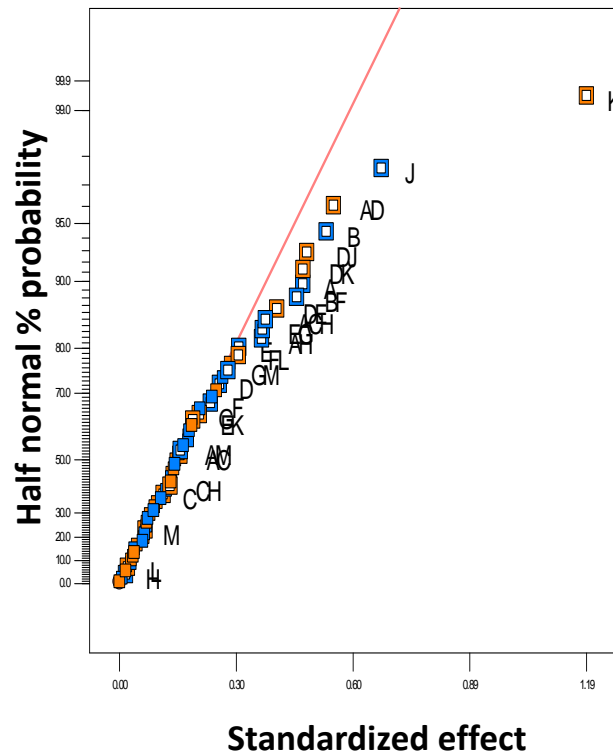
Nutrient solution #2: screening significant parameters

Number	Particle size	Temp.	Inoculum size	Coal loading	pH	Mixing	CoM	Triton X	SDS	Ethanol	2-Propanol	Sodium formate	Methane Prod.	Methane
	(mm)	°C	(mL)	(g)		(rpm)	(mL)	(µL)	(µL)	(µL)	(µL)	(g)	(ft ³ /ton)	(%)
11	<0.074	40	10	35	8	100	0	1.98	30	0	0	0.34	4.50	7.5
6	<0.074	40	10	35	6	100	0	1.98	50	0	382.3	0	5.06	10
3	0.074-0.42	28	5	10	8	0	0.25	3.3	50	0	382.3	0.34	7.80	3
55	0.074-0.42	40	5	35	6	100	0	3.3	50	0	0	0.34	10.50	15.2
36	<0.074	28	10	10	8	0	0.25	1.98	50	0	0	0	18.64	7
24	0.074-0.42	40	5	35	8	100	0	3.3	30	0	382.3	0	20.14	24
51	<0.074	40	5	35	8	0	0.25	1.98	50	0	382.3	0.34	20.15	24
48	0.074-0.42	28	10	10	8	100	0	3.3	30	0	0	0.34	21.18	9.4
2	0.074-0.42	40	10	35	6	0	0.25	3.3	30	0	382.3	0.34	23.83	27
34	<0.074	40	5	35	6	0	0.25	1.98	30	0	0	0	23.83	19
5	<0.074	40	5	10	8	100	0.25	3.3	30	0	0	0.34	24.64	9.2
1	0.074-0.42	40	5	10	8	100	0	1.98	50	292	382.3	0.34	25.63	10.3
53	0.074-0.42	40	5	10	8	0	0	1.98	50	0	0	0	26.93	10.3
54	0.074-0.42	40	5	10	6	100	0	1.98	30	292	0	0	29.98	10
44	<0.074	28	5	35	8	0	0	3.3	50	0	0	0	30.38	29
27	0.074-0.42	28	5	10	8	100	0.25	3.3	50	292	0	0	31.97	12.3
31	0.074-0.42	40	10	10	6	100	0.25	1.98	50	0	0	0.34	33.87	14
57	0.074-0.42	40	5	35	6	0	0	3.3	50	292	382.3	0	37.34	41
26	0.074-0.42	28	5	35	6	100	0.25	1.98	50	0	382.3	0	38.61	38
4	0.074-0.42	28	10	10	6	0	0	3.3	50	292	0	0.34	39.45	14
45	0.074-0.42	28	5	35	8	100	0.25	1.98	30	0	0	0.34	46.53	42
33	0.074-0.42	28	10	10	6	100	0	3.3	50	0	382.3	0	46.78	19
10	0.074-0.42	40	10	35	8	0	0.25	3.3	50	0	0	0	48.19	40
19	0.074-0.42	28	10	35	6	0	0	1.98	30	0	0	0	51.04	41
15	0.074-0.42	40	10	35	8	100	0.25	3.3	50	292	382.3	0.34	52.11	38
17	0.074-0.42	40	10	10	8	100	0.25	1.98	30	0	382.3	0	54.86	19.2
58	<0.074	28	5	10	6	0	0	1.98	50	292	382.3	0	57.18	21
42	<0.074	28	10	35	8	100	0.25	3.3	30	0	382.3	0	59.92	44
63	<0.074	40	5	10	6	100	0.25	3.3	50	0	382.3	0	65.51	21
7	<0.074	40	10	10	8	100	0	3.3	50	292	0	0	65.63	18
18	0.074-0.42	28	10	35	8	0	0	1.98	50	0	382.3	0.34	68.15	69
52	0.074-0.42	28	10	10	8	0	0	3.3	30	292	382.3	0	69.24	28
38	<0.074	28	5	35	6	0	0	3.3	30	0	382.3	0.34	73.45	50
12	0.074-0.42	40	5	10	6	0	0	1.98	30	0	382.3	0.34	74.31	25
49	<0.074	40	10	10	8	0	0	3.3	50	0	382.3	0.34	75.52	25
39	<0.074	28	10	35	6	100	0.25	3.3	50	0	0	0.34	77.84	51
41	<0.074	28	10	10	8	100	0.25	1.98	50	292	382.3	0.34	84.63	27
61	<0.074	28	5	35	6	100	0	3.3	30	292	0	0	97.60	51
47	<0.074	28	5	10	6	100	0	1.98	50	0	0	0.34	100.99	35
13	0.074-0.42	40	10	10	6	0	0.25	1.98	50	292	382.3	0	102.52	34
25	<0.074	40	10	35	8	0	0	1.98	30	292	382.3	0	105.36	65
64	0.074-0.42	28	5	10	6	0	0.25	3.3	30	0	0	0	125.48	34
37	0.074-0.42	28	5	35	6	0	0.25	1.98	50	292	0	0.34	126.35	69
21	<0.074	40	5	35	6	100	0.25	1.98	30	292	382.3	0.34	131.10	76
28	<0.074	40	5	35	8	100	0.25	1.98	50	292	0	0	141.39	61
32	0.074-0.42	40	10	10	8	0	0.25	1.98	30	292	0	0.34	142.04	36
59	<0.074	40	10	35	6	0	0	1.98	50	292	0	0.34	186.12	50
40	0.074-0.42	28	10	35	8	100	0	1.98	50	292	0	0	193.19	62
14	<0.074	40	5	10	6	0	0.25	3.3	50	292	0	0.34	193.31	38
62	0.074-0.42	40	10	35	6	100	0.25	3.3	30	292	0	0	203.35	58
23	0.074-0.42	40	5	35	8	0	0	3.3	30	292	0	0.34	214.43	66
46	<0.074	40	5	10	8	0	0.25	3.3	30	292	382.3	0	224.98	46
30	<0.074	28	10	35	6	0	0.25	3.3	50	292	382.3	0	230.48	74
43	0.074-0.42	28	5	35	8	0	0.25	1.98	30	292	382.3	0	231.13	73
22	<0.074	28	5	35	8	100	0	3.3	50	292	382.3	0.34	242.64	69
9	<0.074	28	10	35	8	0	0.25	3.3	30	292	0	0.34	243.20	66
20	<0.074	28	5	10	8	100	0	1.98	30	0	382.3	0	255.35	55
8	<0.074	28	10	10	6	0	0.25	1.98	30	0	382.3	0.34	263.26	60
35	0.074-0.42	28	10	35	6	100	0	1.98	30	292	382.3	0.34	264.44	77
60	<0.074	40	10	10	6	100	0	3.3	30	292	382.3	0.34	335.85	15
50	<0.074	40	10	10	6	0	0	3.3	30	0	0	0	336.64	52
56	0.074-0.42	28	5	10	6	100	0.25	3.3	30	292	382.3	0.34	514.93	76
16	<0.074	28	10	10	6	100	0.25	1.98	30	292	0	0	880.13	64
29	<0.074	28	5	10	8	0	0	1.98	30	292	0	0.34	979.43	76

Half normal probability plot for methane productivity (ft³/ton)

Design-Expert® Software
Ln(Methane yield)

Shapiro-Wilk test
W-value = 0.984
p-value = 0.860
A: Particle size
B: Temperature
C: Inoculum size
D: Solid loading
E: pH
F: Mixing
G: Coenzyme M
H: Triton X-100
J: SDS
K: Ethanol
L: 2-Propanol
M: Sodium formate
■ Positive Effects
■ Negative Effects



Effect from different parameters

Term	Standardized Effect	Sum of squares	% Contribution
A-Particle size	-0.469	3.516	4.310
B-Temperature	-0.529	4.469	5.478
C-Inoculum size	0.112	0.201	0.246
D-Solid loading	-0.256	1.046	1.282
E-pH	-0.305	1.493	1.830
F-Mixing	-0.233	0.866	1.061
G-Coenzyme M	0.205	0.669	0.820
H-Triton X-100	-0.016	0.004	0.005
J-SDS	-0.669	7.162	8.778
K-Ethanol	1.19305	22.774	27.913
L-2-Propanol	0.0209669	0.0070338	0.009
M-Sodium formate	0.0659437	0.0695771	0.085

ANOVA test

ANOVA for selected factorial model
Analysis of variance table [Partial sum of squares - Type III]

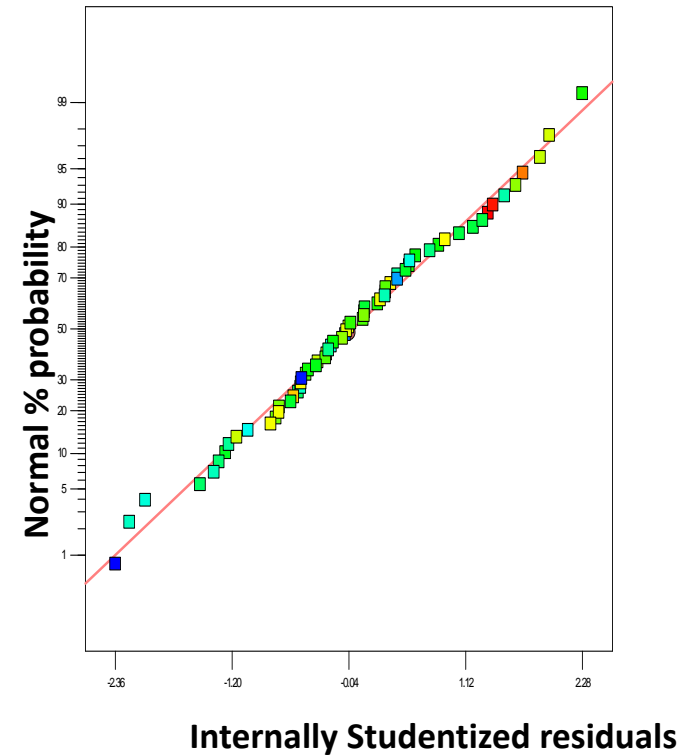
Source	Sum of Squares	df	Mean Square	F Value	p-value Prob > F	
Model	70.92	26	2.73	9.46	< 0.0001	significant
A-Particle size	3.52	1	3.52	12.2	0.0013	
B-Temperature	4.47	1	4.47	15.5	0.0004	
C-Inoculum size	0.2	1	0.2	0.7	0.4092	
D-Solid loading	1.05	1	1.05	3.63	0.0646	
E-pH	1.49	1	1.49	5.18	0.0287	
F-Mixing	0.87	1	0.87	3	0.0914	
G-Coenzyme M	0.67	1	0.67	2.32	0.1361	
H-Triton X-100	4.07E-03	1	4.07E-03	0.014	0.906	
J-SDS	7.16	1	7.16	24.84	< 0.0001	
K-Ethanol	22.77	1	22.77	79	< 0.0001	
L-2-Propanol	7.03E-03	1	7.03E-03	0.024	0.8767	
M-Sodium formate	0.07	1	0.07	0.24	0.6261	
AC	0.39	1	0.39	1.34	0.2549	
AD	4.79	1	4.79	16.61	0.0002	
AH	2.11	1	2.11	7.33	0.0102	
AM	0.39	1	0.39	1.35	0.2536	
BF	3.28	1	3.28	11.39	0.0017	
CH	0.27	1	0.27	0.93	0.3409	
DE	2.59	1	2.59	8.99	0.0048	
DJ	3.67	1	3.67	12.73	0.001	
DK	3.52	1	3.52	12.21	0.0013	
EG	2.13	1	2.13	7.4	0.0099	
EK	0.56	1	0.56	1.96	0.17	
FL	1.48	1	1.48	5.13	0.0294	
GM	1.23	1	1.23	4.28	0.0455	
ACH	2.23	1	2.23	7.73	0.0085	
Residual	10.67	37	0.29			
Cor Total	81.59	63				

The Model F-value of 9.46 implies the model is significant. There is only a 0.01% chance that a "Model F-Value" this large could occur due to noise.

Normal plot of residuals

Design-Expert® Software
Ln(Methane yield)

Color points by value of Ln(Methane yield):
6.88697
1.50432

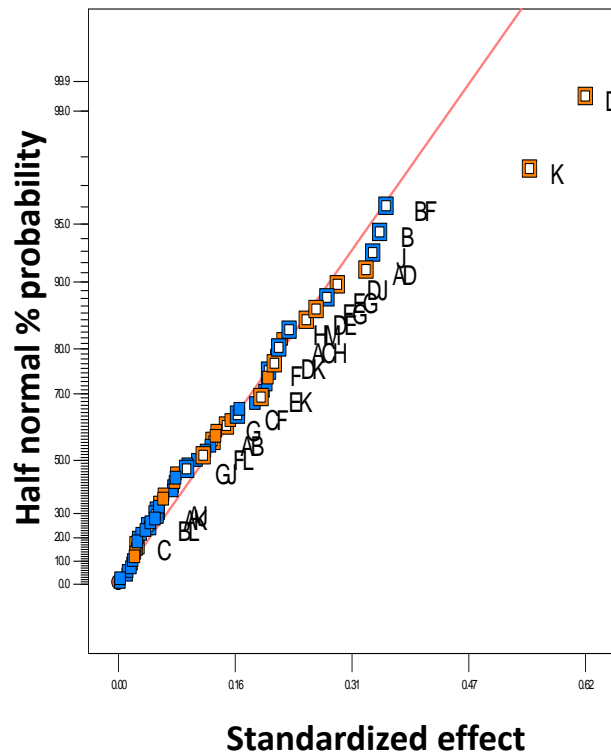


Half normal probability plot for methane content (%)

Effect from different parameters

Design-Expert® Software
Ln(Methane content)

Shapiro-Wilk test
W value = 0.986
p value = 0.290
A: Particle size
B: Temperature
C: Inoculum size
D: Solid loading
E: pH
F: Mixing
G: Coenzyme M
H: Triton X-100
J: SDS
K: Ethanol
L: 2-Propanol
M: Sodium formate
■ Positive Effects
■ Negative Effects



Term	Standardized Effect	Sum of squares	% Contribution
A-Particle size	-0.195	0.608	1.726
B-Temperature	-0.350	1.955	5.547
C-Inoculum size	0.025	0.010	0.029
D-Solid loading	0.625	6.240	17.703
E-pH	-0.199	0.631	1.790
F-Mixing	-0.201	0.647	1.834
G-Coenzyme M	0.145	0.335	0.951
H-Triton X-100	-0.073	0.086	0.244
J-SDS	-0.340	1.853	5.257
K-Ethanol	0.550	4.841	13.733
L-2-Propanol	0.131	0.275	0.780
M-Sodium formate	-	0.0023	0.007

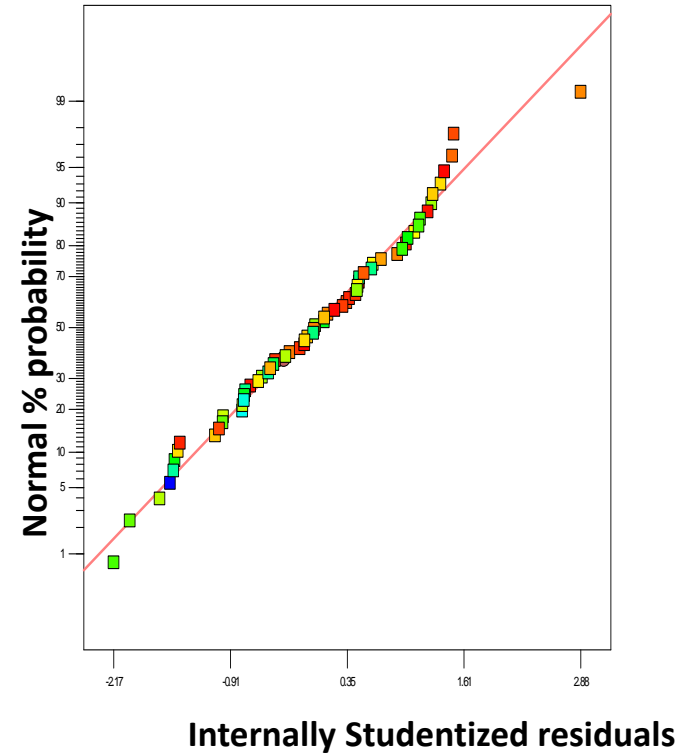
ANOVA test

Source	Sum of Squares	df	Mean Square	F Value	p-value Prob > F
Model	31.25	32	0.98	7.58	< 0.0001 significant
A-Particle size	0.61	1	0.61	4.72	0.0376
B-Temperature	1.96	1	1.96	15.17	0.0005
C-Inoculum size	0.01	1	0.01	0.079	0.7803
D-Solid loading	6.24	1	6.24	48.4	< 0.0001
E-pH	0.63	1	0.63	4.89	0.0345
F-Mixing	0.65	1	0.65	5.02	0.0324
G-Coenzyme M	0.34	1	0.34	2.6	0.117
H-Triton X-100	0.086	1	0.086	0.67	0.4198
J-SDS	1.85	1	1.85	14.37	0.0007
K-Ethanol	4.84	1	4.84	37.55	< 0.0001
L-2-Propanol	0.27	1	0.27	2.13	0.1544
M-Sodium formate	2.37E-03	1	2.37E-03	0.018	0.8931
AB	0.26	1	0.26	1.99	0.1679
AC	0.64	1	0.64	4.98	0.0331
AD	1.76	1	1.76	13.62	0.0009
AH	0.54	1	0.54	4.15	0.0502
AJ	0.044	1	0.044	0.34	0.5636
AK	0.041	1	0.041	0.32	0.577
BF	2.05	1	2.05	15.92	0.0004
BL	0.027	1	0.027	0.21	0.6531
CF	0.41	1	0.41	3.16	0.0853
CH	0.059	1	0.059	0.46	0.5043
DE	1.01	1	1.01	7.85	0.0087
DJ	1.37	1	1.37	10.66	0.0027
DK	0.7	1	0.7	5.41	0.0267
EG	1.25	1	1.25	9.67	0.004
EK	0.58	1	0.58	4.53	0.0414
FG	1.12	1	1.12	8.69	0.006
FL	0.21	1	0.21	1.6	0.215
GJ	0.13	1	0.13	1.04	0.3158
HM	0.84	1	0.84	6.48	0.0161
ACH	0.74	1	0.74	5.72	0.023
Residual	4	31	0.13		
Cor Total	35.25	63			

Normal plot of residuals

Design-Expert® Software
Ln(Methane content)

Color points by value of
Ln(Methane content):

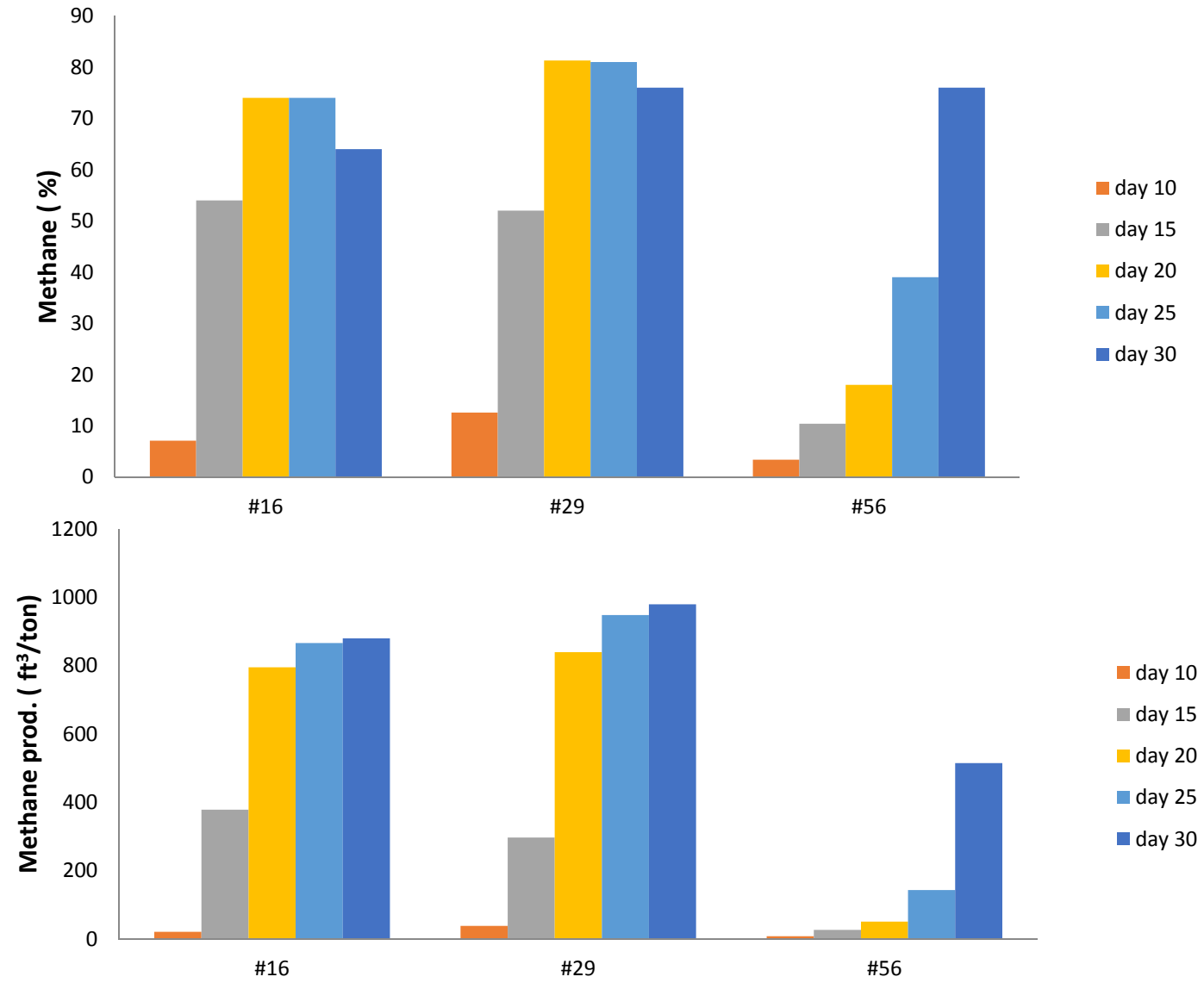


Current status

An optimization experiment is underway.

1. Temperature range: 28-32°C
2. Particle size: < 0.074 mm
3. Coal loading: < 700 g/L
4. Ethanol content: 100-300 mM

Time series data



Current challenges

Ex situ:

1. How to sustain methane release over time?
2. How to maximize coal conversion?

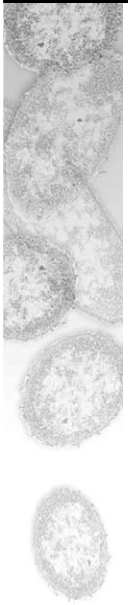
In situ:

1. How to deliver the nutrient solution?
2. How to determine the time interval for nutrient supplementation?

Acknowledgement

Department of Energy: DE-FE0024126

- Dr. Satya Harpalani
- Dr. Stephen Park
- Dr. Chunjie Xia
- Ji Zhang
- Rohit Pandey



Optimization, Scale-up, and Design of Coal-Dependent Methanogenesis in Preparation for *in situ* Field Demonstration



Prof. Matthew W. Fields
Center for Biofilm Engineering
Energy Research Institute

Assit. Prof. A. Phillips
R. Hiebert
Prof. L. Spangler
Prof. A. Cunningham
Prof. R. Gerlach

Dr. W. Orem, USGS
Dr. B. Lomans, Shell Global

Project Goal and Objectives

1 y project to mature *in situ* bio-gasification technologies for use in future field tests.

- Enhance traditional CBM production rates
- Shorten time needed to re-generate CBM fields
- Mitigate environmental impacts
- Increase longevity of existing infrastructure
- Provide essential data for resource estimations

Specific Objectives:

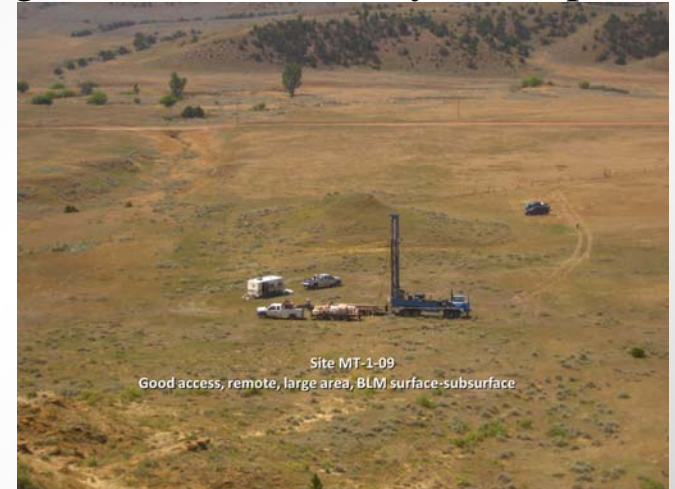
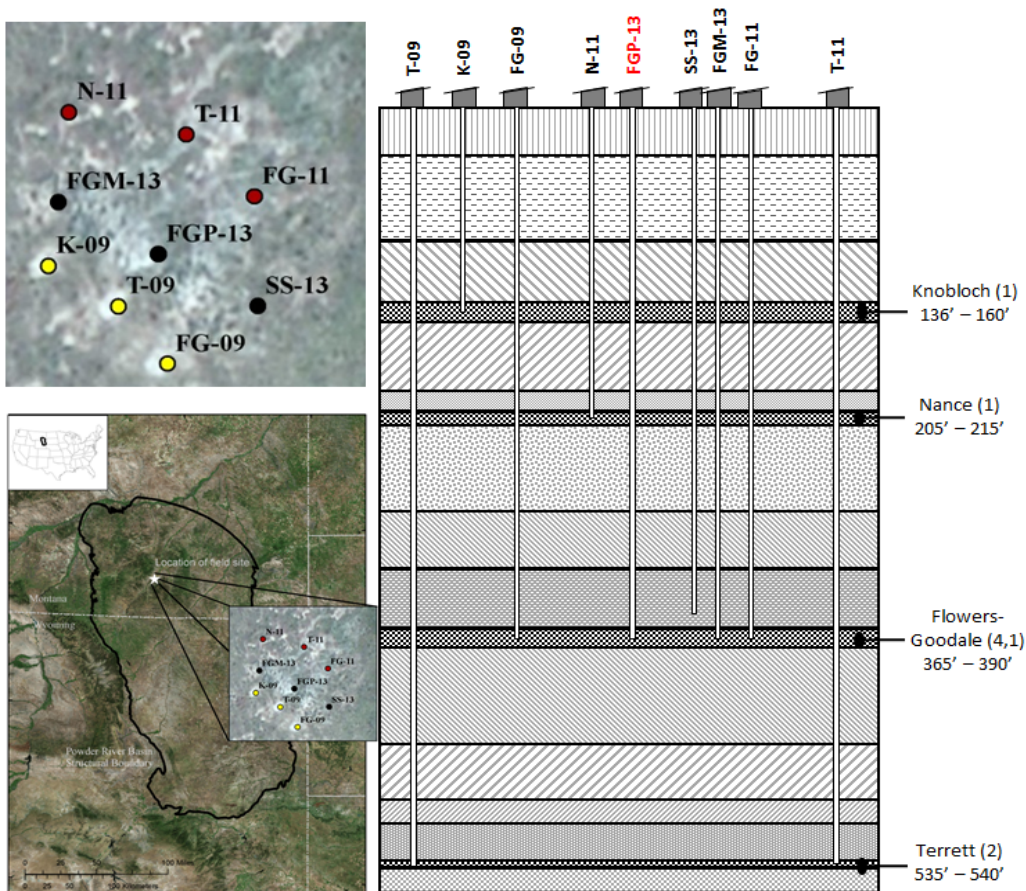
Objective 1. Evaluate time-delay to methane production post-stimulation during meso-scale injections

Objective 2. Complete site characterization

Objective 3. Evaluate and design potential field demonstration and economic analysis at the USGS Birney Test Site in the Powder River Basin

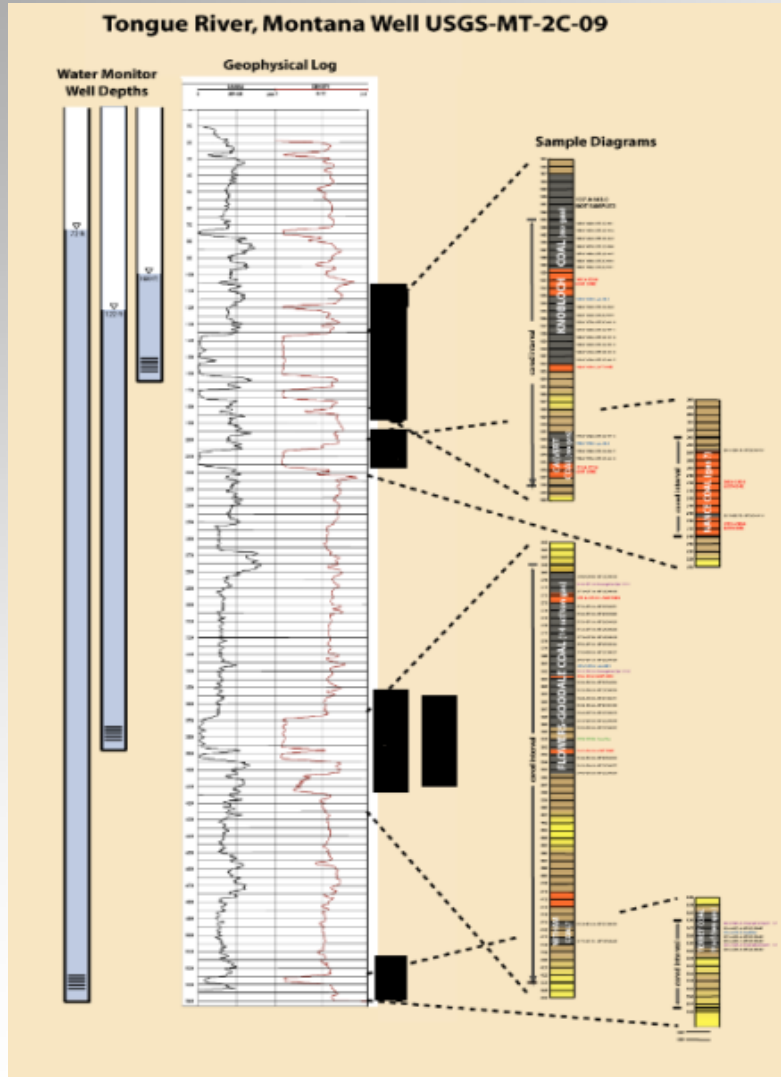
Test Design Program with On-going Research & Collaboration

Target field site (USGS Birney Test Site) already under development by USGS in the PRB in collaboration with MSU. Drilling, logging, coring, and hydrologic tests have already taken place providing a data rich environment for the field test design.



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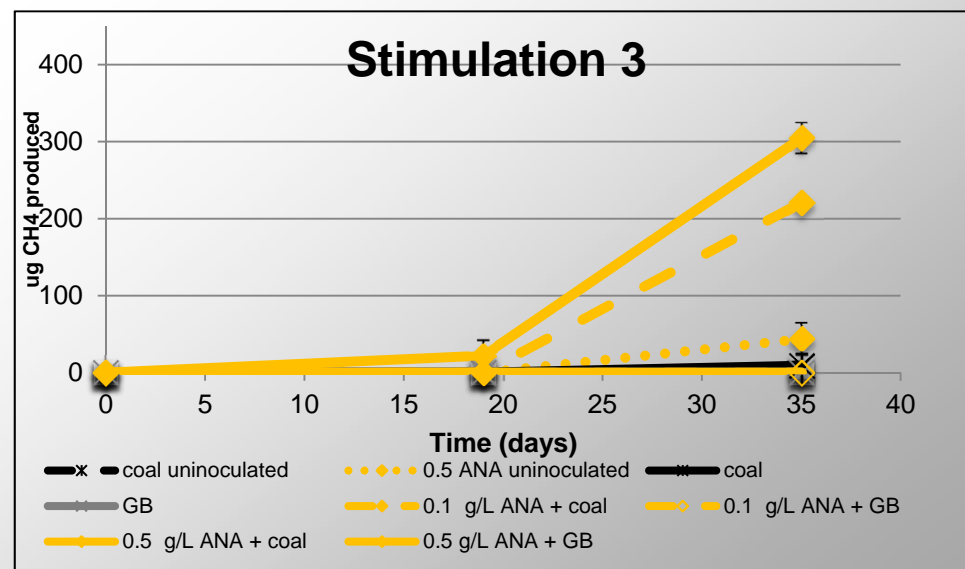
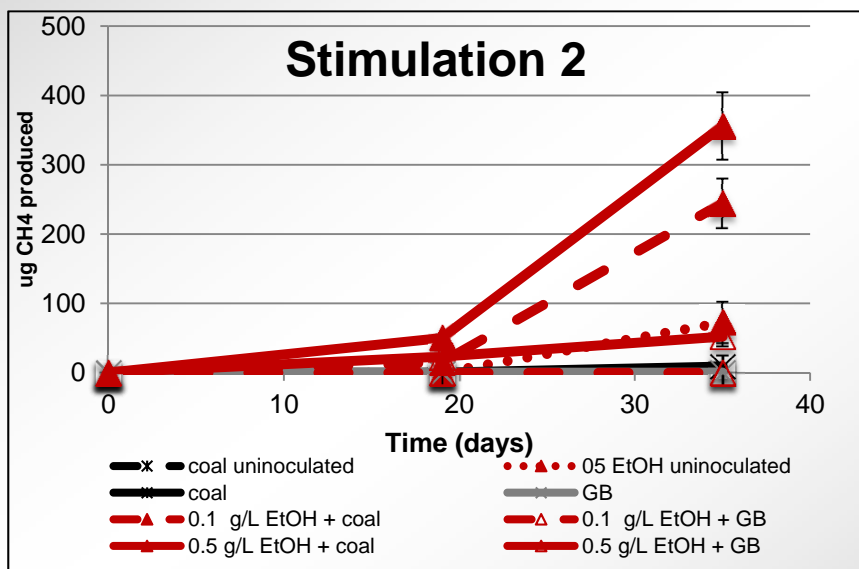
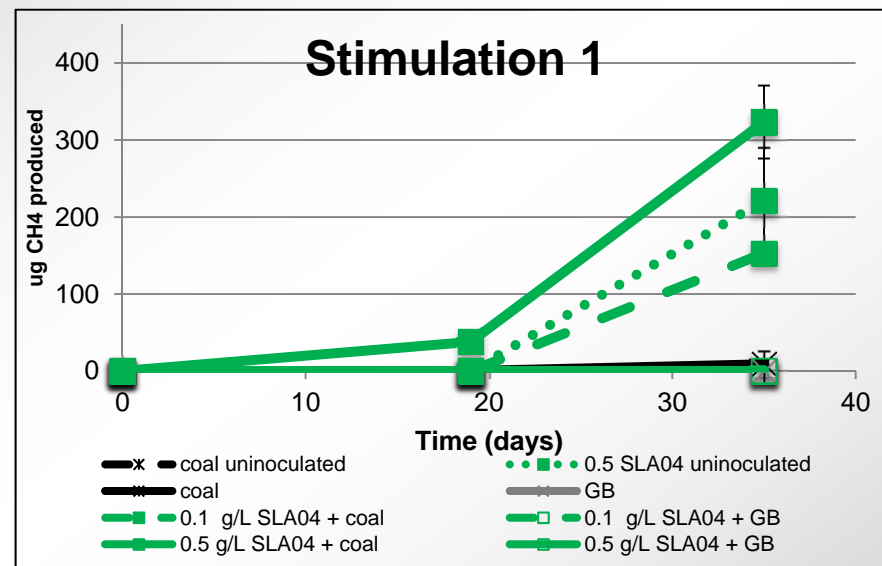
Microbiology



Formation water, coal, and microbial communities extracted from coal surfaces from the target field site

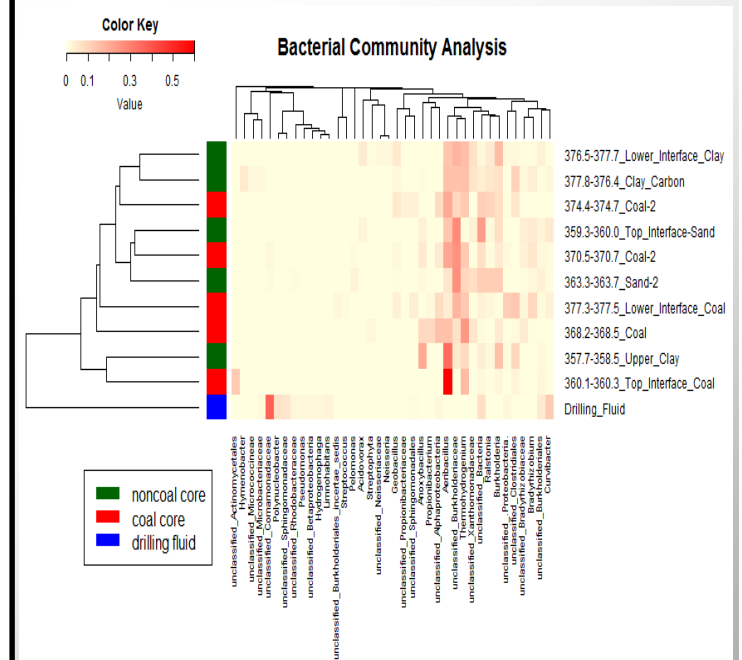
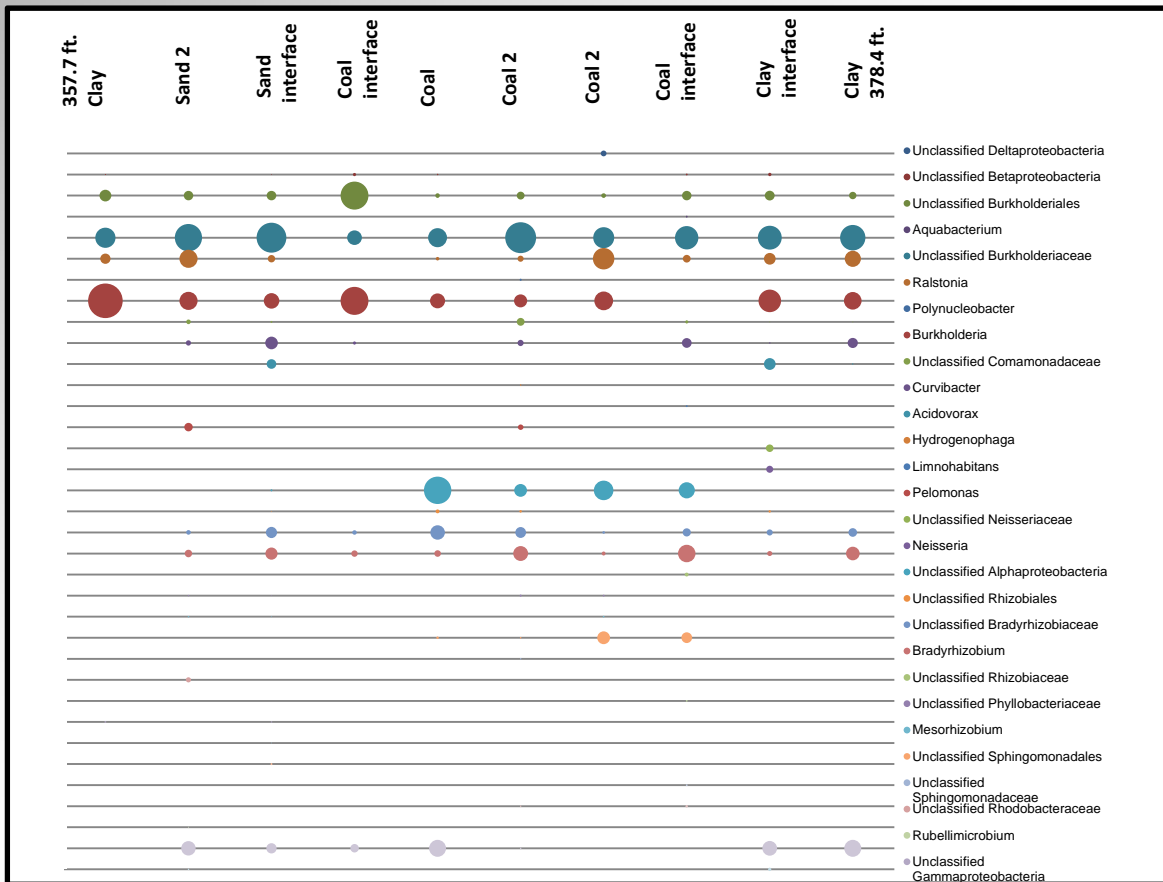


Long term bench-scale enrichments that display coal-dependent methanogenesis with various stimulants



Microbial Genomics

In addition to collaboration with the USGS, we are collaborating with Shell Global Solutions International BV. Shell will perform metagenomic sequencing on coal samples obtained from the USGS field site thereby providing extensive characterization of the microbial communities in the coal beds targeted for later field tests.



Bench- and Meso-Scale Pressure Vessels

High pressure flow through test systems that allow for the study of cores at the 2.5 cm, 5 cm, and 75 cm diameter scales. The meso-scale high pressure vessel is equipped with a custom designed switchboard that allows for the sampling of fluids from the vessel while maintaining the pressure.



Porous Media Reactor

We will use a porous media reactor constructed of a stainless steel top and bottom plate and a stainless steel mesh screen that surrounds the circumference of the reactor.



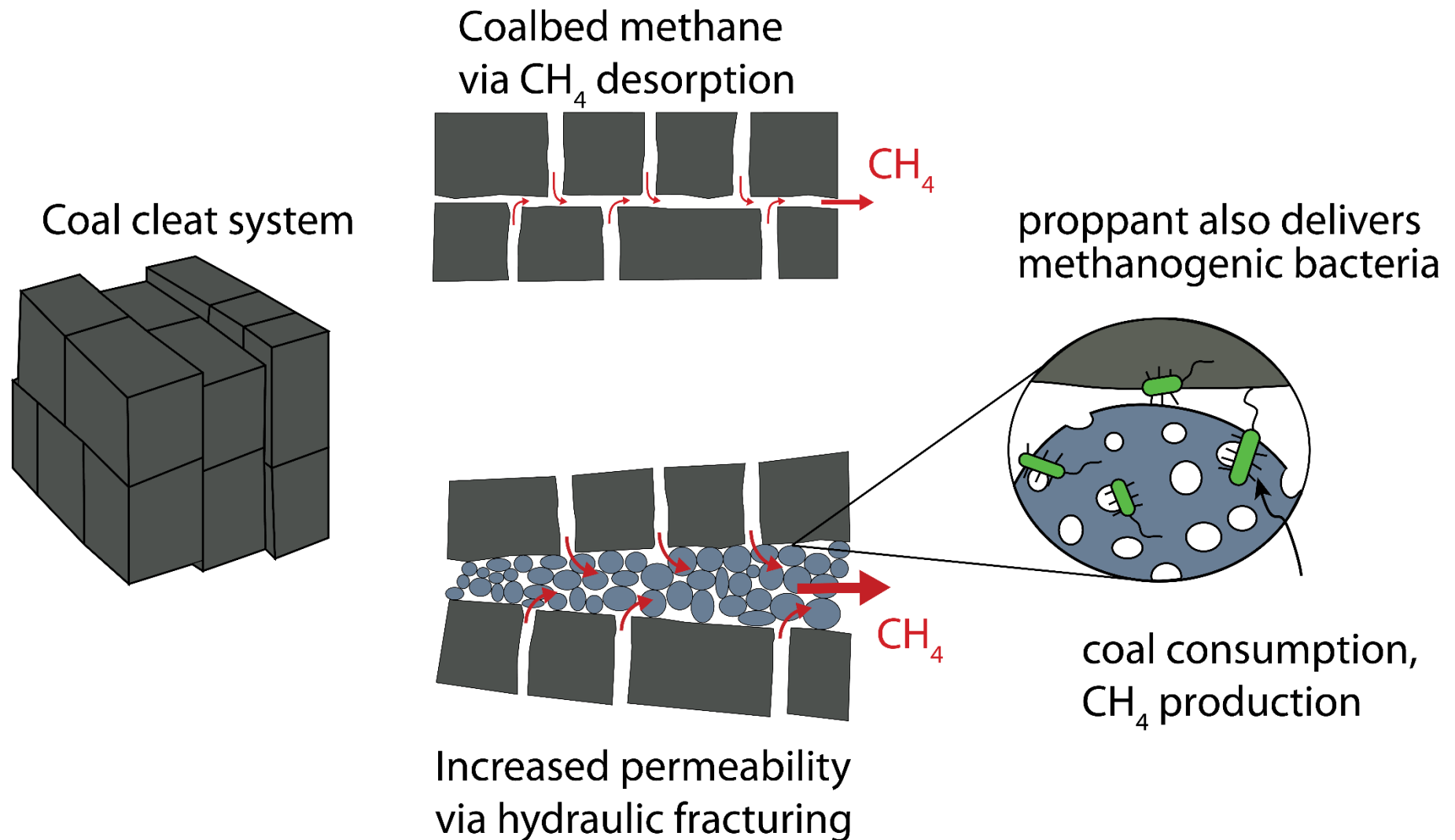
Ceramic Proppant Design for In-Situ Microbially Enhanced Methane Recovery

Award DE-FE0024088

Taylor D. Sparks
Assistant Professor of Materials Science and Engineering
University of Utah

8/11/2015 DOE C&CBTL Workshop, Morgantown WV

Microbes can be used to enhance coalbed methane recovery



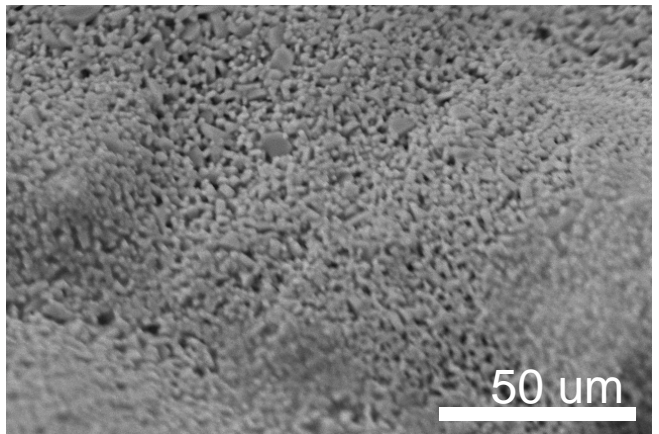
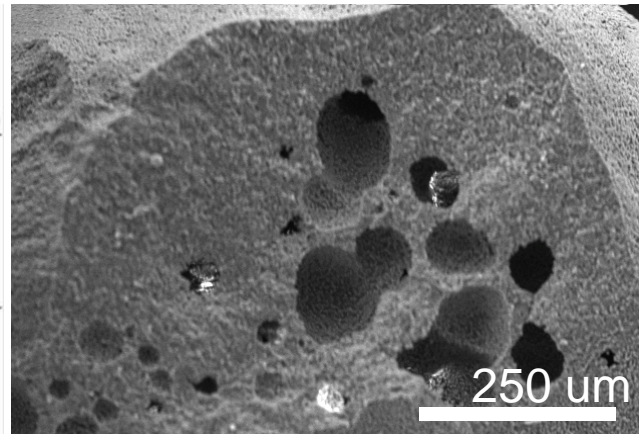
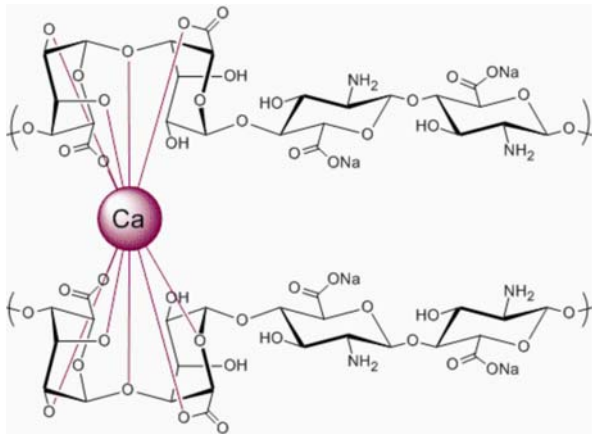
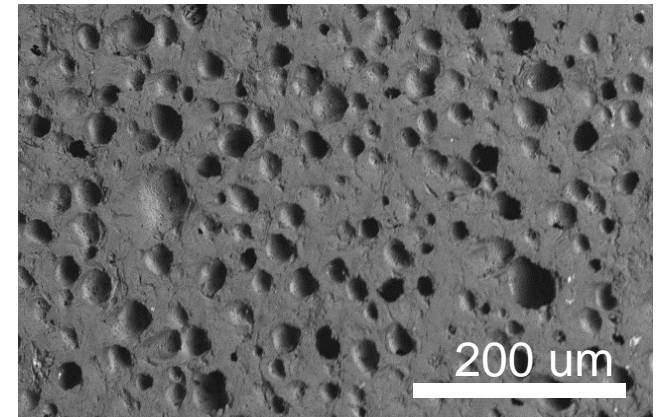
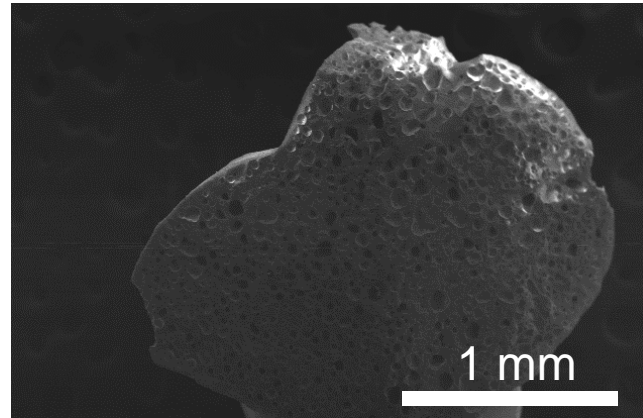
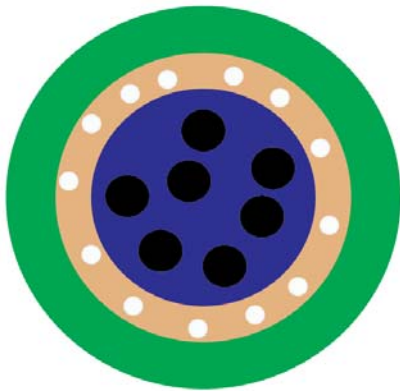
Microbes can either

- (1) consume coal reservoir to generate more methane, or
- (2) remove coal fines in proppant bed to enhance conductivity

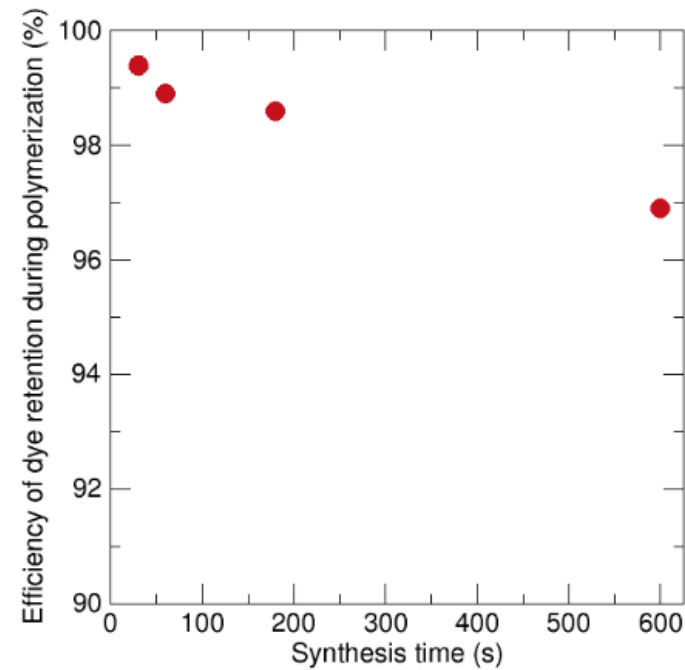
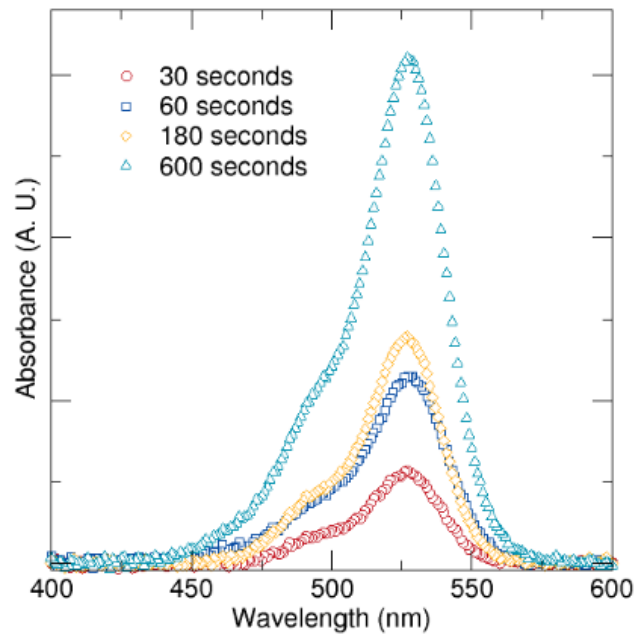
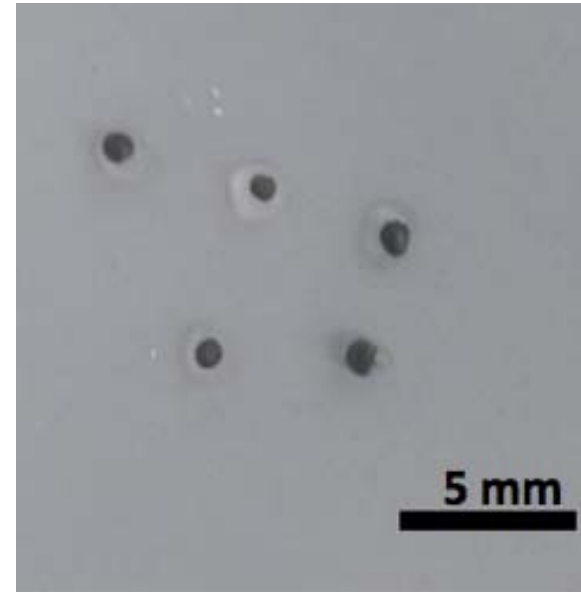
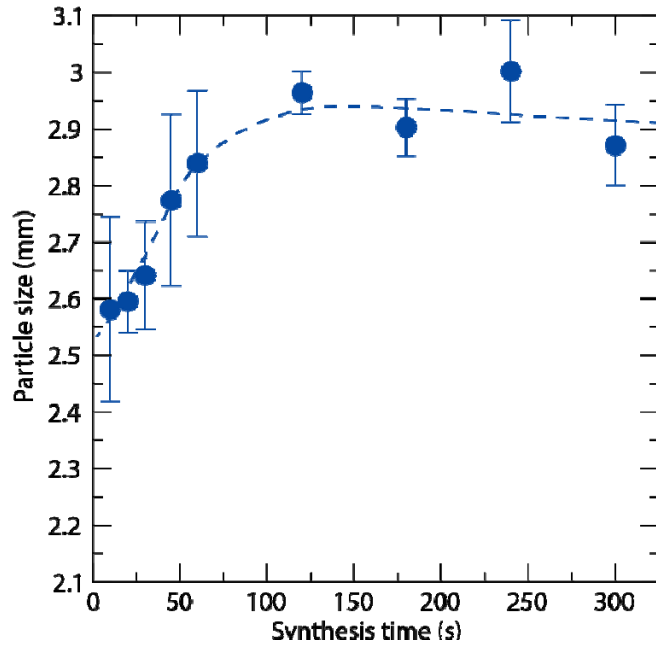
Proppant must be redesigned for low density and microbial loading

Combined high temperature sinter / reduction step

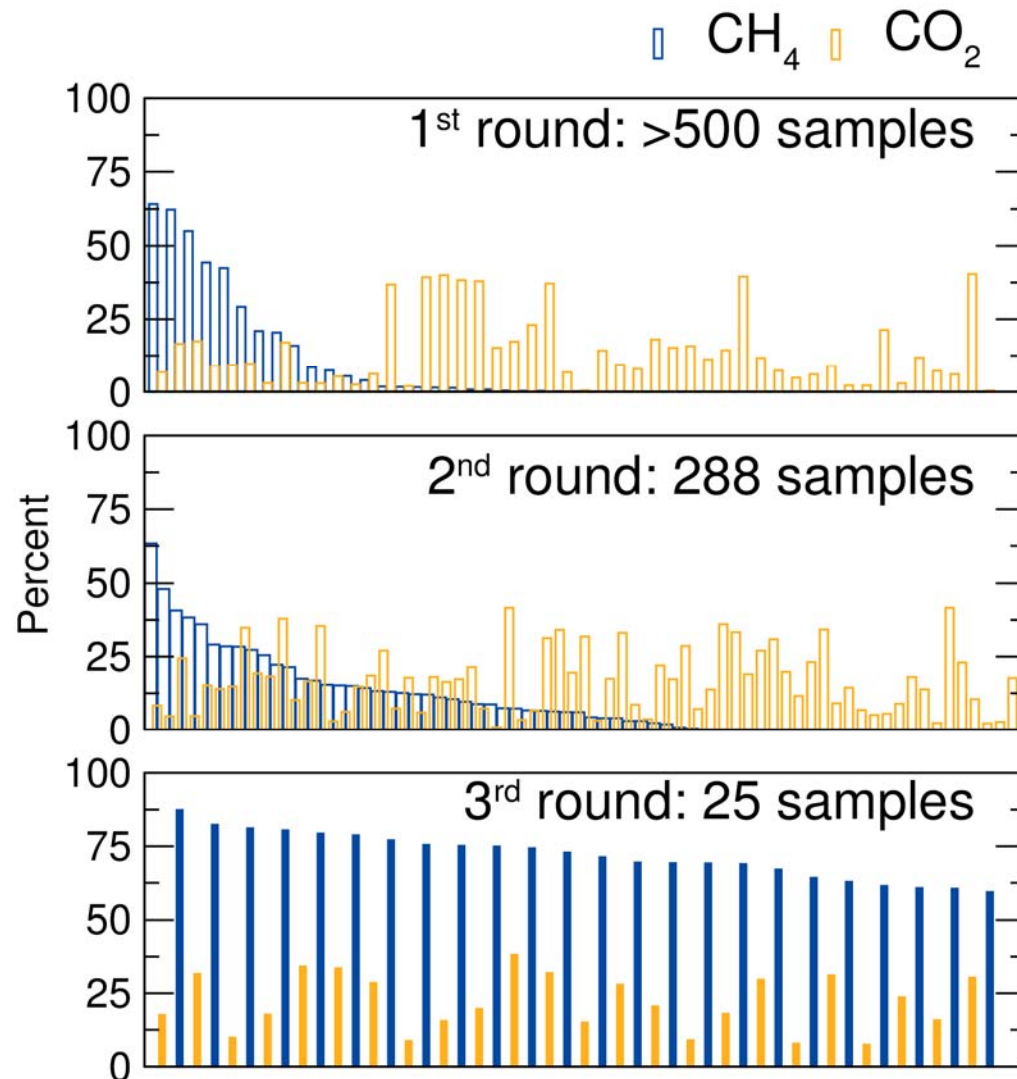
- 35-70 diameter inner pores
- 5-10 diameter outer pores
- Bulk density was 1.5 g/cm^3
- Strength testing underway



Encapsulation process retains molecules impregnated into proppant



Hundreds of microbial experiments performed to find optimum



Controlled variables:

- Bacteria source (14)
- Initial nutrients (6)
- Coal source (4)
- Growth conditions (3)

Statistical analysis applied to determine which variables had highest impact.

Best consortia have been isolated and cultured for proppant impregnation and reactor testing.

Initial results suggest microbial approach is feasible

Synthesis of lightweight proppant with hierarchical porosity is possible with inexpensive materials and scalable process.

Polymer encapsulation was successful using inexpensive lactate alginate polymerization. Thickness and dye retention was calibrated.

Microbial consortia with high methane yield have been identified.

Optimal microbial nutrients, initial and final growth conditions identified for four common coal sources.

To be done still...

Strength and conductivity testing with proppant and encapsulated proppant.

Bacterial loading into proppant and time-dependent methanogenesis measurements.

Reactor level proof-of-concept demonstration.



Questions?



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Biogasification – Field Site Deployment Goals and Challenges

August 11th, 3:00-5:00 pm
Ballroom 4



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