



# Model-Based Sensor Placement for Component Condition Monitoring and Fault Diagnosis in Fossil Energy Systems

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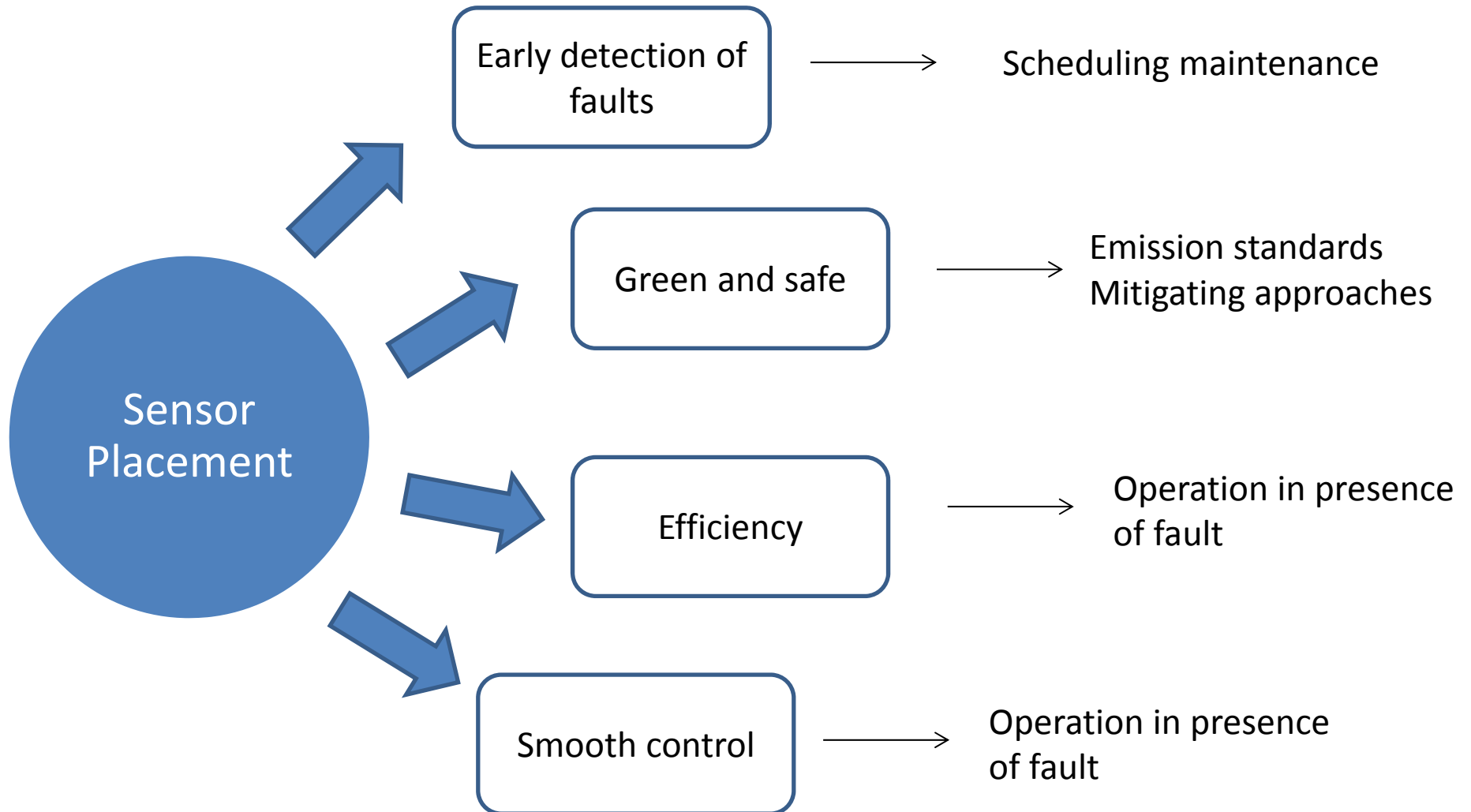
# Sensor Network Design (SND) Problem

- Which variable to measure and where (if spatial variation is considered)
- Which physical sensors (with different properties, cost) should be used
- How many sensors (hardware redundancy) should be used for measuring a variable
- What should be a frequency of sampling for different variables
- Maintenance policies

**Design as well as retrofit problem**



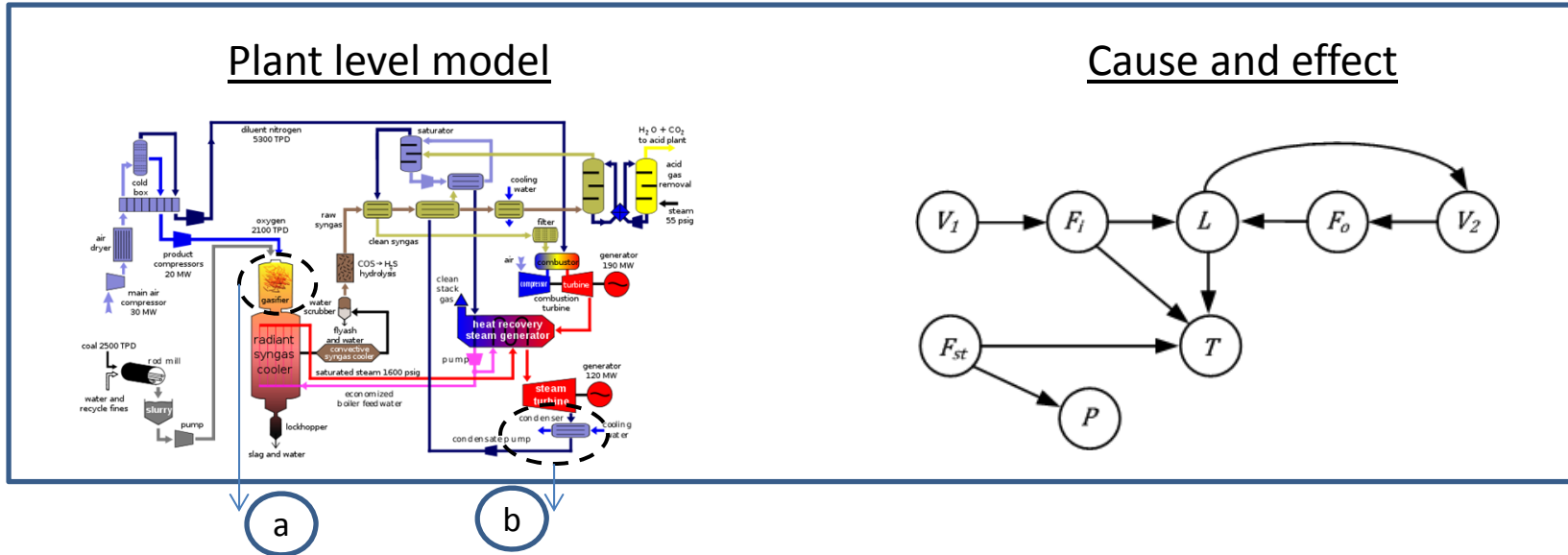
# Motivation



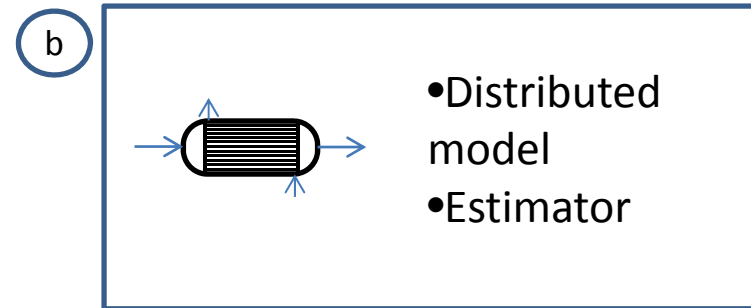
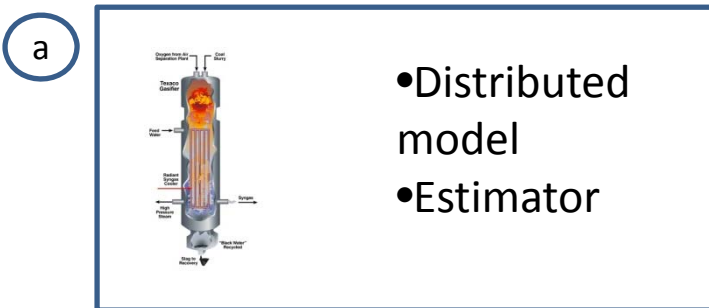


# Two-Tier Approach

## Tier 1 – Plant level



## Tier 2 – Equipment Level

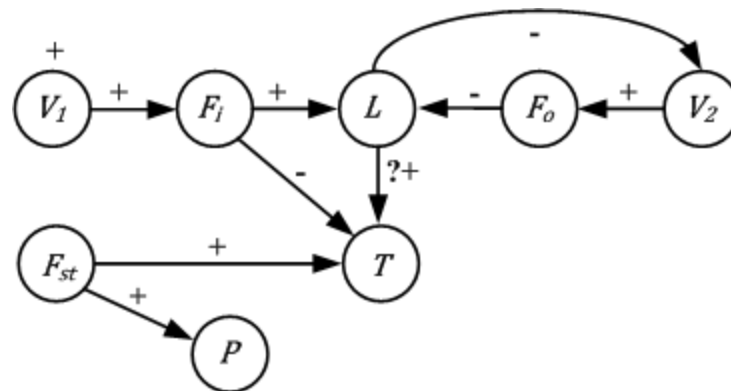




# **Plant Level Sensor Placement: Qualitative Graph-Based Approaches**



# Graph-Based Approaches



**DG** representation:

**SDG** representation

- Only arrows
- $\{0,1\}$  Matrix: Response to faults
- Numerically: Change > Threshold

- Arrows and signs
- $\{-1,0,1\}$  Matrix: Response and direction to faults
- Numerically: Change > Threshold

## Result

- $M$  faults  $\times$   $N$  variable matrices for each algorithm



# Integer Programming

## Objective function

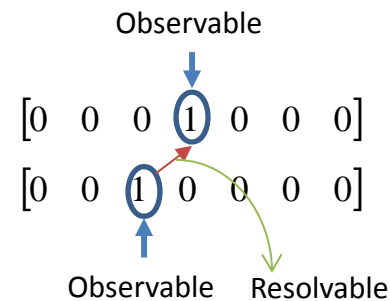
- minimize sensor network cost

$$\min f = \sum_j^N w_j x_j$$

$$x = \text{binary}$$

## Constraint

- Observability: Observe faults
- Resolution: Distinguish faults



$$Ax^T \geq b \quad A = \begin{bmatrix} 1 & 0 & 0 & 1 & \dots & 1 \\ 0 & 0 & 1 & 1 & \dots & 1 \\ \vdots & \vdots & \vdots & \vdots & \ddots & \vdots \\ 0 & 1 & 0 & 1 & \dots & 1 \end{bmatrix}_{M \times N} \quad \& \quad x_1 + x_2 + x_3 + \dots + x_N \geq 1 \quad b = \begin{bmatrix} 1 \\ 1 \\ \vdots \\ 1 \end{bmatrix}_{M \times 1}$$

## Decision variables

- Binary  $\rightarrow$  "1": Variable measured      "0": Variable not measured
- Weight  $\rightarrow$  Cost of measuring sensor



# Fault Evolution Sequence Algorithm

- Enhance DG and SDG for fault resolution
- $\{-1,0,1\}$  Matrix: Fault evolution sequence algorithm
- Compare sequence of responding sensors
- Pair the sensors and compare

Fault	Sequence	Pairs
F1	$S_1 S_3 S_2 S_4$	$\{S_1, S_3\}$ $\{S_1, S_2\}$ $\{S_1, S_4\}$ $\{S_3, S_2\}$ $\{S_3, S_4\}$ $\{S_2, S_4\}$
F2	$S_1 S_2 S_3 S_4$	$\{S_1, S_3\}$ $\{S_1, S_2\}$ $\{S_1, S_4\}$ $\{S_2, S_3\}$ $\{S_3, S_4\}$ $\{S_2, S_4\}$

Base pairs:  $\{S_1, S_2\}$   $\{S_1, S_3\}$   $\{S_1, S_4\}$   $\{S_2, S_3\}$   $\{S_2, S_4\}$   $\{S_3, S_4\}$

- If Pair  $\subseteq$  Base pair :
  - Same sequence: "1"
  - Reverse sequence: "-1"
- If Pair  $\not\subseteq$  Base Pair : "0"





# Magnitude Ratio Algorithm

- Enhance DG & SDG for fault resolution
- $\{-1,0,1\}$  Matrix: Magnitude ratio

Fault	Sensor direction	
	$S_1$	$S_2$
$F_1$	+1	-1
$F_2$	+1	-1

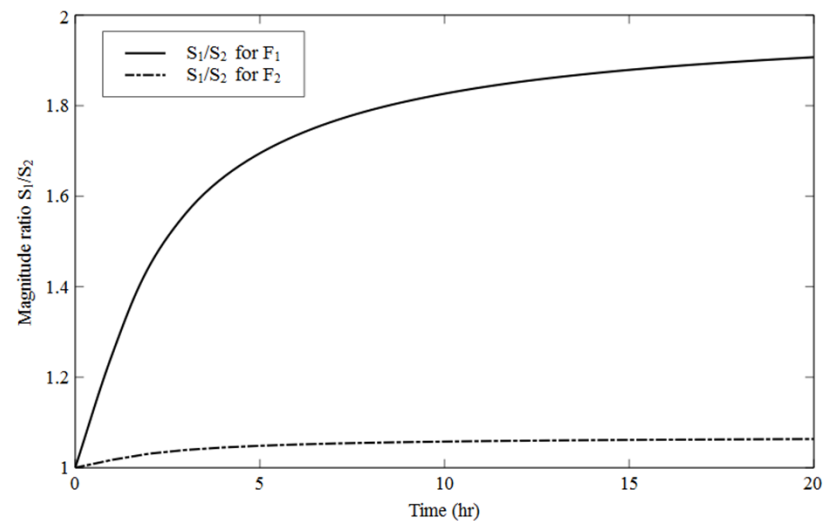
A = Normalized measurement ratios for  $F_1$ :  $S_1/S_2$

B = Normalized measurement ratios for  $F_2$ :  $S_1/S_2$

➤  $A \gg B$  : "1"

➤  $B \gg A$  : "-1"

➤  $A \cong B \cong 1$  : "0"





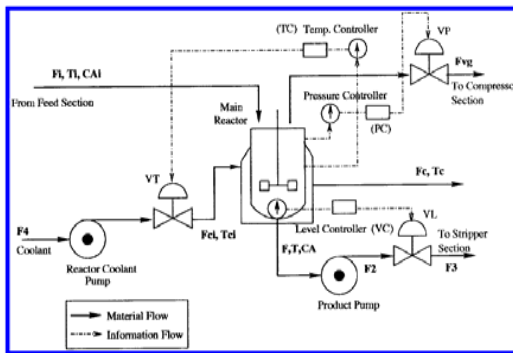
# Results



## Weights in optimization problem: Cost of sensors

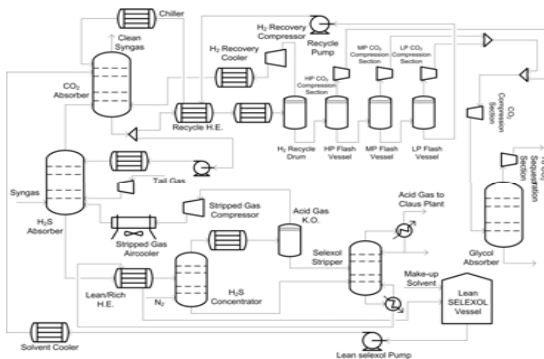
Sensor type	Cost	Accuracy
Temperature	0.1	2 °F
Pressure	0.5	3% of span
Flow	1	4% of span
Level	1	1 inch
Concentration	10	0.01

## CSTR system



- 10 Faults
- 7 Sensors

## SELEXOL process



- 14 Faults
- 25 Sensors

Algorithms	Network cost	Irresolvable
SDG	10.7	1 fault
FES	0.7	1 fault $\subseteq$ SDG
MR	0.7	[ ]
FES & MR	0.7	[ ]

Algorithms	Network cost	Irresolvable
SDG	22.3	1 fault
FES	22.2	[ ]
MR	22.1	[ ]
FES & MR	22	[ ]

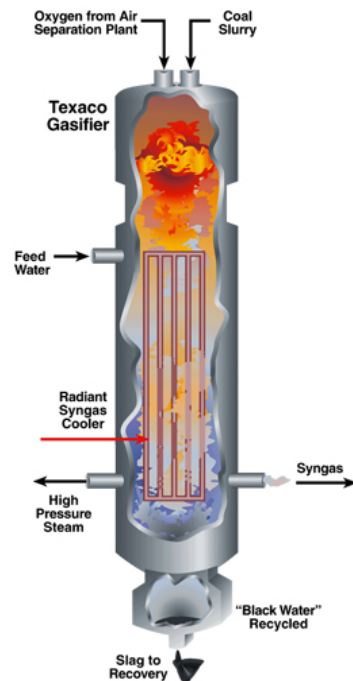


# **Equipment Level Sensor Placement: Model-Based Quantitative Approach**

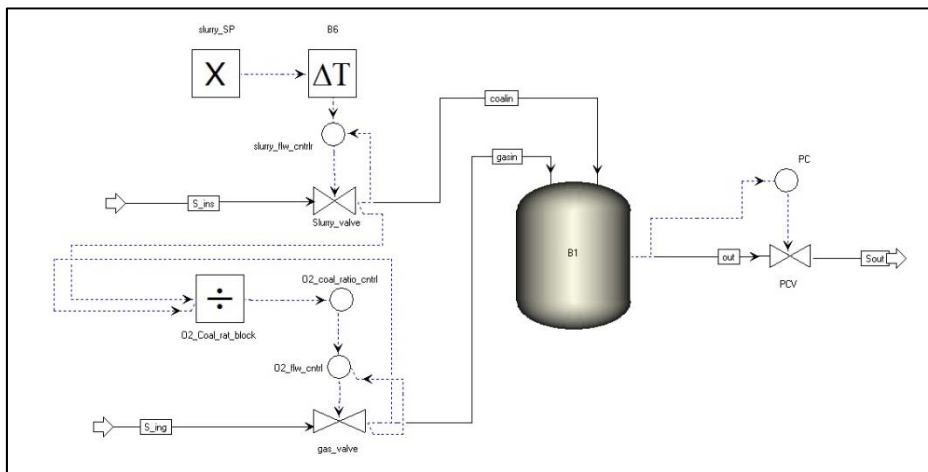
- 1. Gasifier**
- 2. Water-Gas Shift Reactor**



# Slagging Gasifier



- Gasifier operates at temperatures of about 1200-1600°C
- Liquid slag flows on walls and is collected at bottom
- Slagging gasifier model required for fault simulation



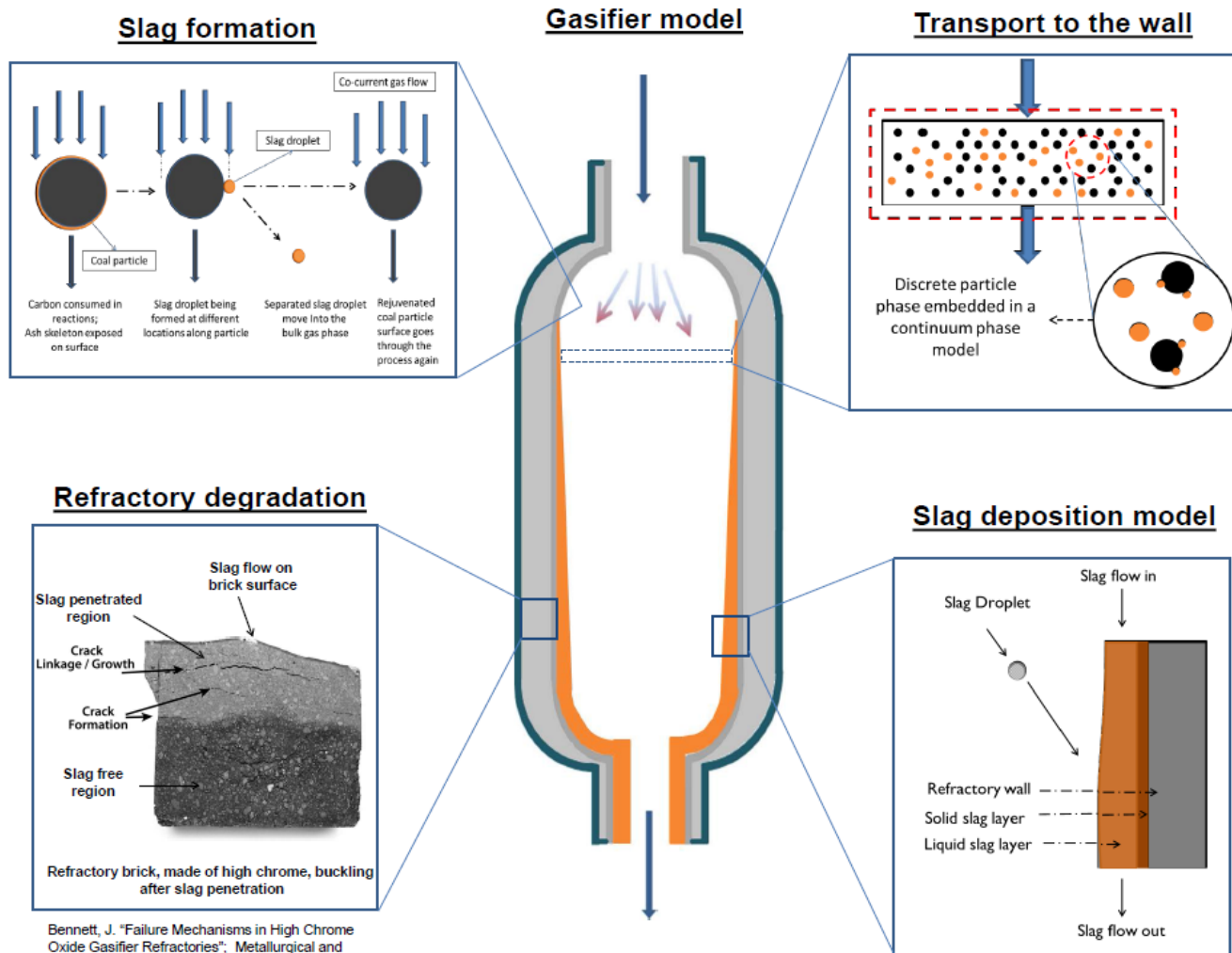
## Two faults of interest in the gasifier

1. Slag layer thickness

2. Refractory degradation



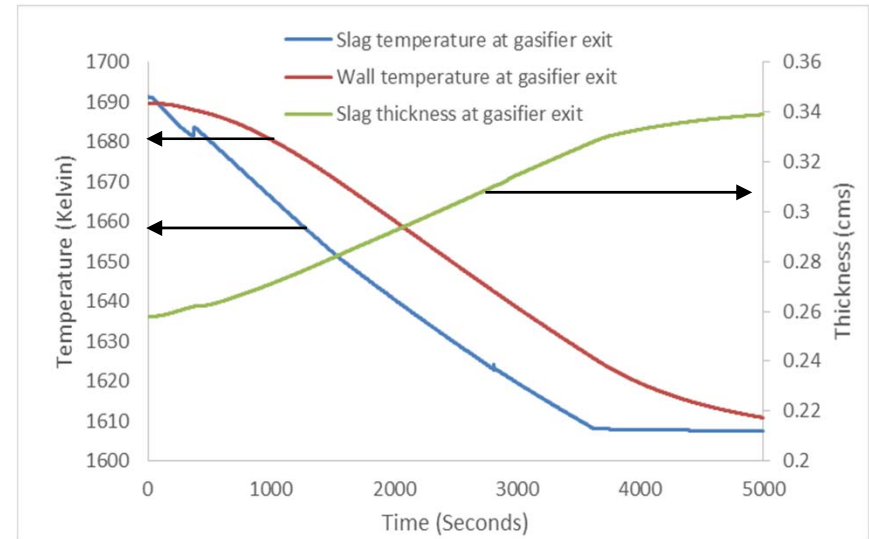
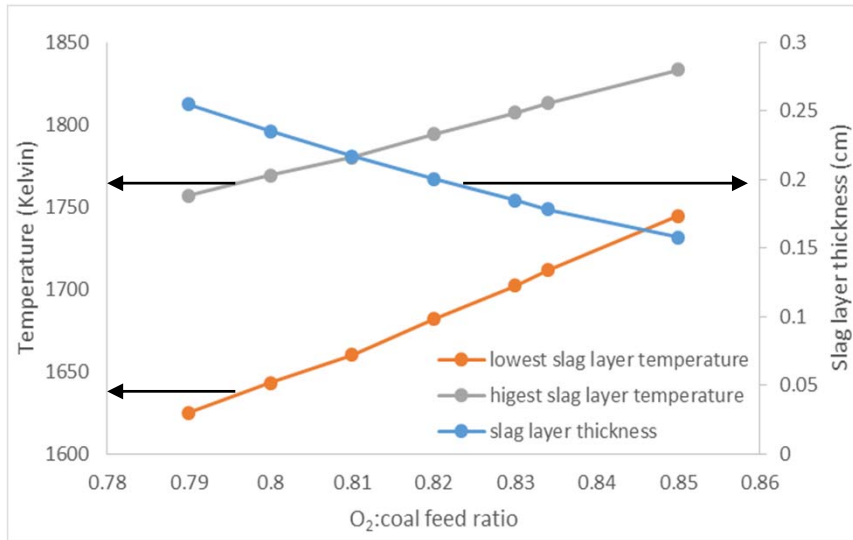
# Model Development for Condition Monitoring



Bennett, J. "Failure Mechanisms in High Chrome Oxide Gasifier Refractories"; Metallurgical and Materials Transactions; 2011, 42, 4, pp. 888 - 904



# Effect of Operating Conditions

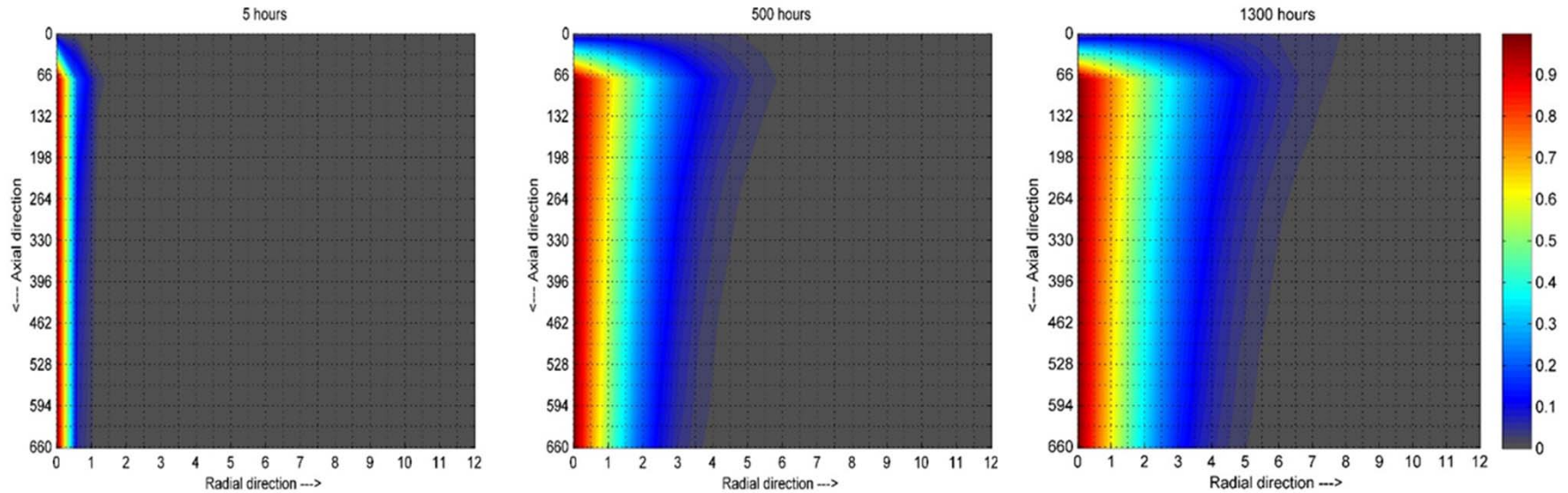


- Thickness increases by 75% for change in O<sub>2</sub>:coal ratio from 0.79 to 0.85
- High slag temperature can accelerate the slag penetration into the refractory brick leading to faster spalling
- Low slag temperature can result in solidification of slag, leading to clogging and reduced volume for reactions

- Coal feed changed from Illinois #6 to Pittsburgh #8 coal in 1 hour
- Slag layer increases in thickness by about 30%
- Slag layer temperature approaches critical viscosity temperature if O<sub>2</sub>/coal ratio not adjusted, could lead to solidification



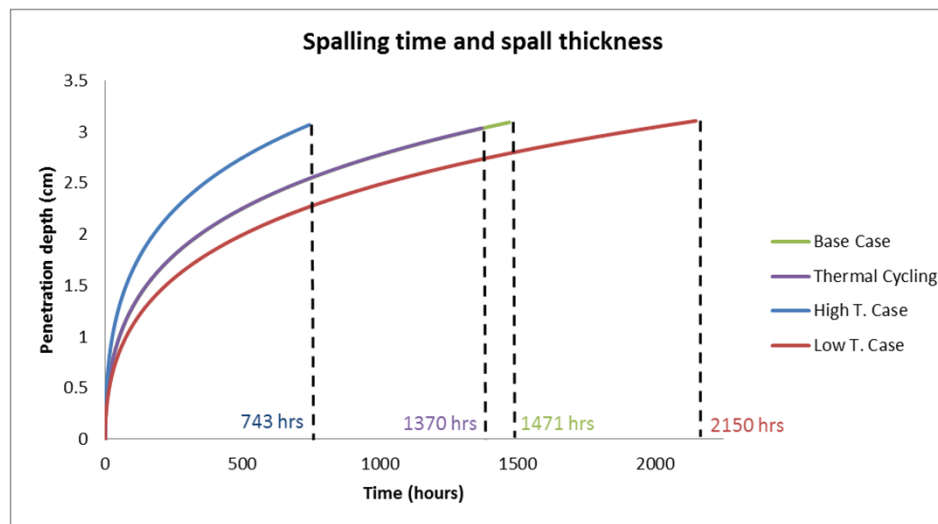
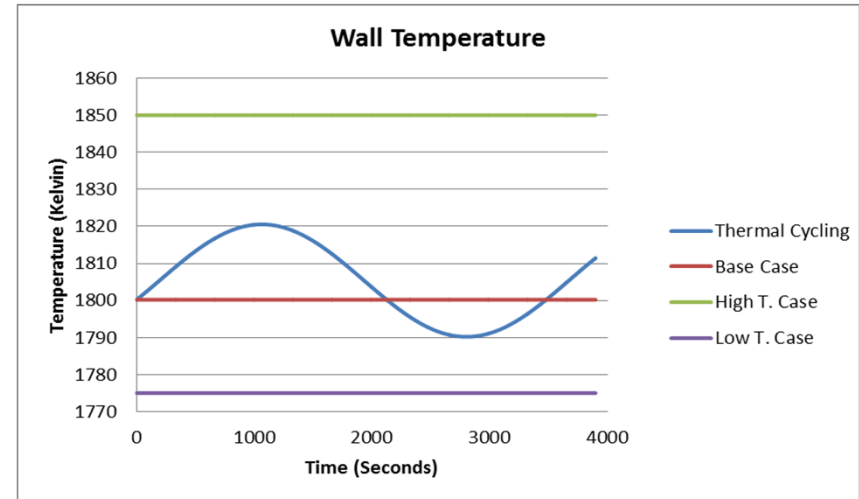
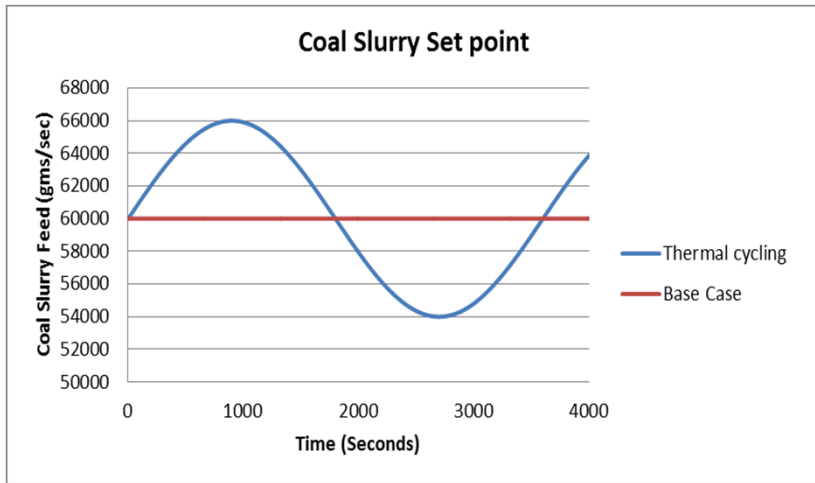
# Slag Penetration



- Temperature decreases with depth
- Diffusivity is a strong function of temperature
- As slag penetrates, penetration rate slows down due to decrease in effective diffusivity and due to increasing radius



# Refractory Degradation





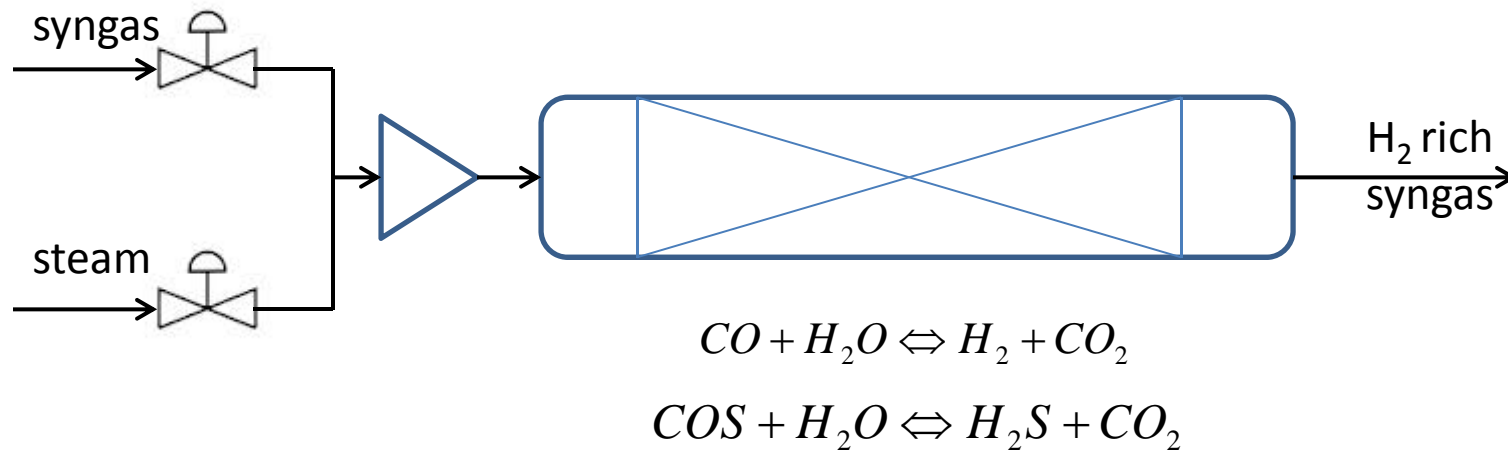


# Equipment level sensor network design

## 2. Water gas shift reactor



# Sour Water-Gas Shift Reactor (SWGSR)



## Model

- 1<sup>st</sup> principle, 1-D, PDAE model developed
- Reaction kinetics: data reconciliation

## Application

- Simulate faults: catalyst deactivation
- Fault estimation: State estimation techniques

- Search space for measurement model is large ( $>2^{176}$ )
- Evolutionary algorithm can help us surf the space to find optimal model

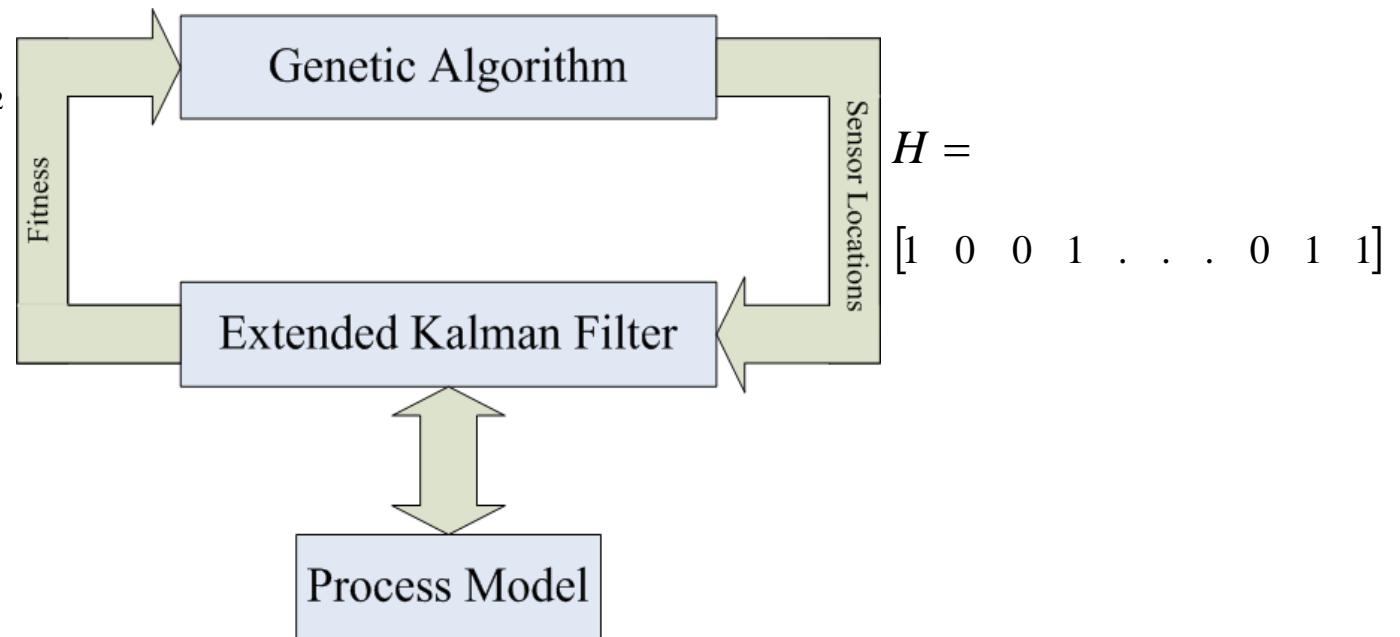
**Genetic Algorithm!**



# SND Framework for WGSR

$$e_{total} = \sum_{i=1}^N (x_{estimate,i} - x_{actual,i})^2$$

$$Fitness = e^{-e_{total}}$$



$$\dot{x} = f(x, z)$$

$$g(x, z) = 0$$



# Estimation Technique



- **State estimation**
  - Non-linear model
  - Differential and algebraic equations (DAE)
- **Estimator must handle**
  - Non-linearity : Nonlinear model
  - DAE systems : DAE model
  - Constraints : Sum of mole/mass fractions = 1
  - Uncertainty in both differential and algebraic variables : Ergun Eq.

$$x_{k+1} = x_k + \int_{k\Delta t}^{(k+1)\Delta t} f(x(t), z(t)) dt + G\omega_{k+1}$$

$$g(x_{k+1}, z_{k+1}) = \gamma_{k+1}$$

$$y_{k+1} = h(x_{k+1}, z_{k+1}) + v_{k+1}$$

$$\omega \sim N(0, Q) \quad \gamma \sim N(0, W) \quad v \sim N(0, R)$$

$$\text{subject to : } Ex_{k+1}^{aug} = b$$

**A modified EKF is proposed!**



# Modified EKF

- **Propagation**

- ✓ States: Propagated by integrating nonlinear DAE solvers
- ✓ Error covariance matrix is propagated by using linearized DAE model

$$\begin{array}{ccc}
 \dot{x} = Ax + Bz & \xrightarrow{\text{Algebraic equations are not differentiated}} & \dot{x} = (A - BD^{-1}C)x \\
 Cx + Dz = 0 & & z = -D^{-1}Cx
 \end{array}
 \longrightarrow
 \begin{array}{l}
 x(k+1) = \phi x \\
 z = -D^{-1}Cx
 \end{array}$$

- ✓ Error covariance: Error covariance matrix split between differential and algebraic states

$$P_{k+1|k} = \begin{bmatrix} P_{k+1|k}^{xx} & P_{k+1|k}^{xz} \\ P_{k+1|k}^{zx} & P_{k+1|k}^{zz} \end{bmatrix} = \begin{bmatrix} \phi P_{k|k}^{xx} \phi^T + GQG^T & P_{k+1|k}^{xx} (D^{-1}C)^T \\ (D^{-1}C)P_{k+1|k}^{xx} & (D^{-1}C)P_{k+1|k}^{xx} (D^{-1}C)^T + W \end{bmatrix}$$

- **Correction**

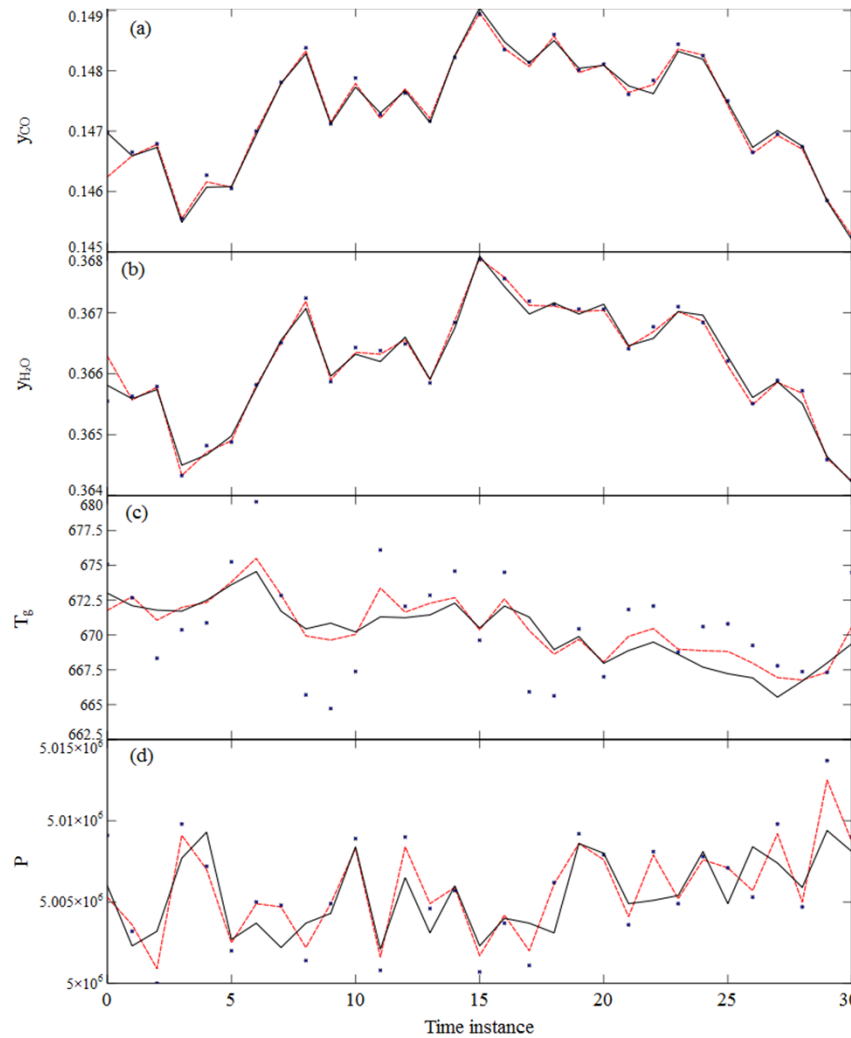
- ✓ Solve optimization problem

$$\min_{\hat{x}_{k+1|k+1}^{aug,c}} = \left( \hat{x}_{k+1|k+1}^{aug,c} - \hat{x}_{k+1|k}^{aug} \right)^T P_{k+1|k}^{-1} \left( \hat{x}_{k+1|k+1}^{aug,c} - \hat{x}_{k+1|k}^{aug} \right) + \left( y_{k+1} - C\hat{x}_{k+1|k+1}^{aug,c} \right)^T R^{-1} \left( y_{k+1} - C\hat{x}_{k+1|k+1}^{aug,c} \right)$$

$$\text{subject to : } E\hat{x}_{k+1|k+1}^{aug,c} = b$$



# Modified EKF - Estimation



RMSE	
Measured data	Estimate
$1.029 \times 10^{-4}$	$0.891 \times 10^{-4}$
$1.031 \times 10^{-4}$	$0.874 \times 10^{-4}$
$4.9 \times 10^{-3}$	$1.7 \times 10^{-3}$
$4.847 \times 10^{-4}$	$3.994 \times 10^{-4}$

Actual (-), measured (\*) and estimated (- -) at middle of the reactor



# Computational Complexity

- Each generation of GA
  - Population : 16 Individual
  - Each individual (Measurement model) : EKF estimation
  - EKF is simulated for 20 sample instant ; 20 times nonlinear process model is numerically integrated
  - 320 times nonlinear process model is numerically integrated
- Each generation takes  $\approx$  40 seconds in parallel in HPCC
  - 10K generation  $\approx$  5 days
- How to reduce the computation time?
  - Optimize the code ✓
  - Run in parallel ✓
  - Use of simplified model



## Simplification of WGSR model

- **Scaling analysis** of current WGSR model identifies following
  - ✓ Conduction phenomenon can be negligible
  - ✓ Species balance equations can be quasi steady
  - ✓ Catalyst and gas phase temperatures can be made equal
- Number of species balance equations can be reduced using stoichiometric relations





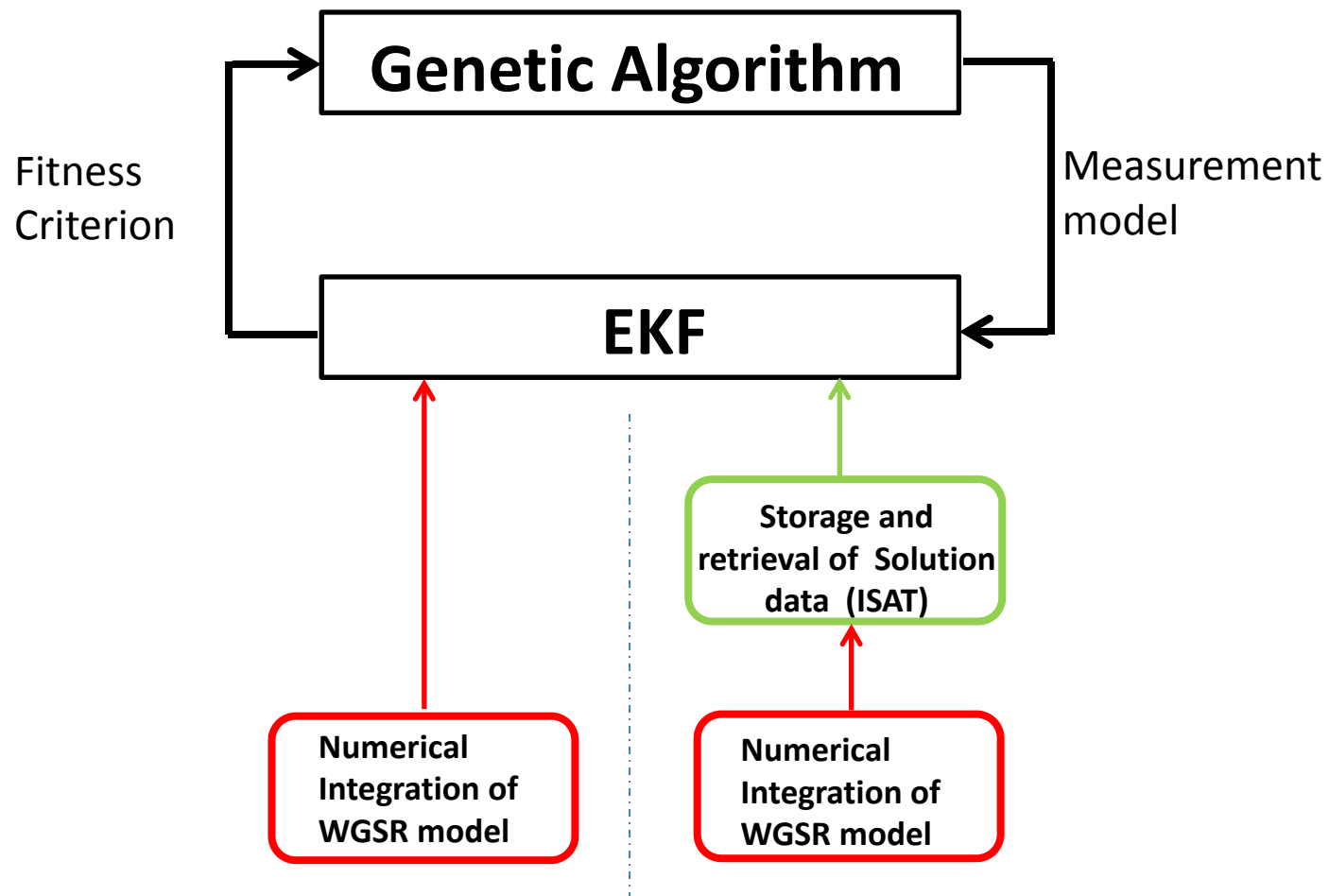
## Original vs. Simplified Model

Properties	Original model	Simplified model
No. of PDEs	8	1
No. of ODEs	1	3
No. of algebraic equations	0	4
Types of PDE solved	Parabolic	First order hyperbolic
Steady state simulation time, sec	75	1
Dynamic simulation time, sec	110	40



# In-Situ Adaptive Tabulation (ISAT)

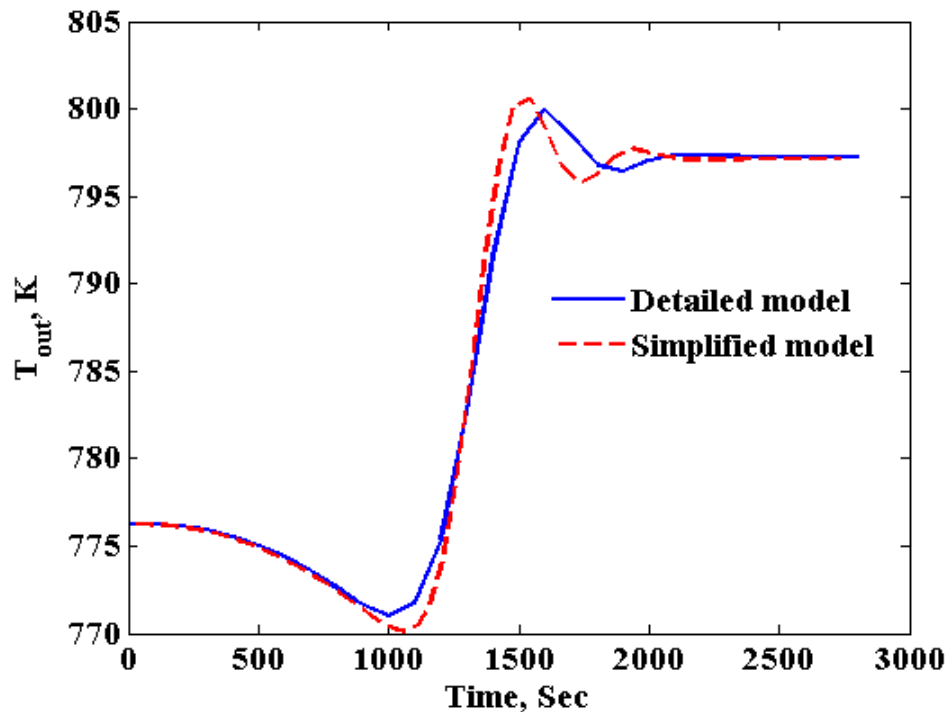
Use of storage and retrieval approach such as ISAT is investigated for computational efficiency





# Simulation Results

## Dynamic response for step up in inlet temperature



## Computational efficiency per sample time

- Numerical simulation: **0.7 sec**  
(Detailed model)
- Numerical simulation: **0.12 sec**  
(Simplified model)
- ISAT (Retrieval): **0.0027 sec**



# Plant-Wide Sensor Placement



# SND for Large Networks

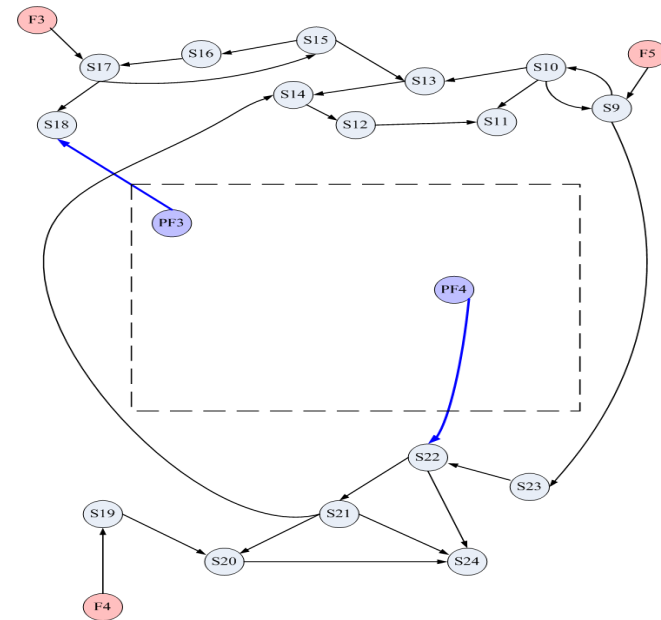
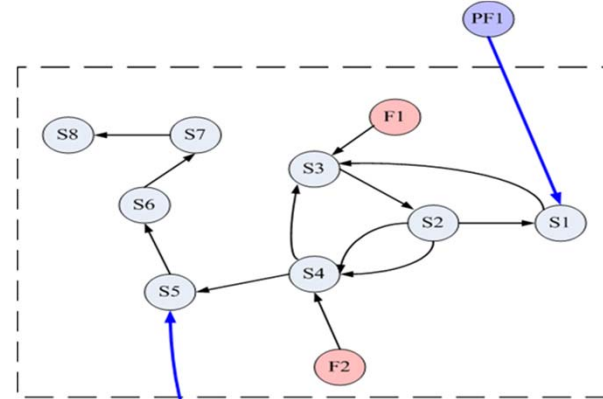
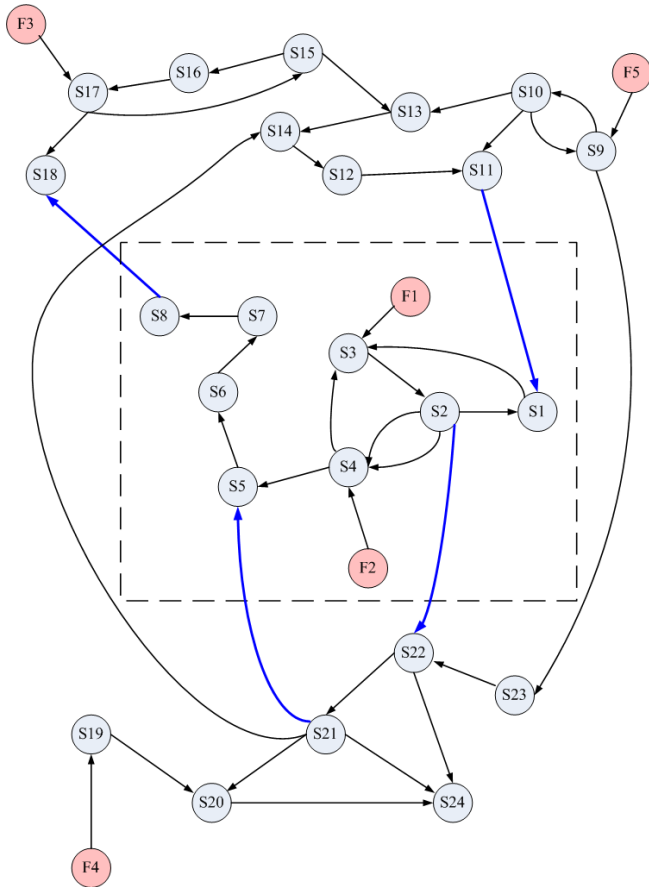
- Large networks
  - Many state and fault nodes
- Sensor placement for fault diagnosis
  - Might become computationally complex
    - Resolution problems because of the nested symmetric difference operations in graph-based approaches
  - Difficult to nest models of different level of granularity such as graph models, and PDE models

## Decomposition Strategy

- Decomposition of the large network to sub-networks
- Definition of pseudo-faults to avoid solution iteration between sub-networks



# Decomposition Approach



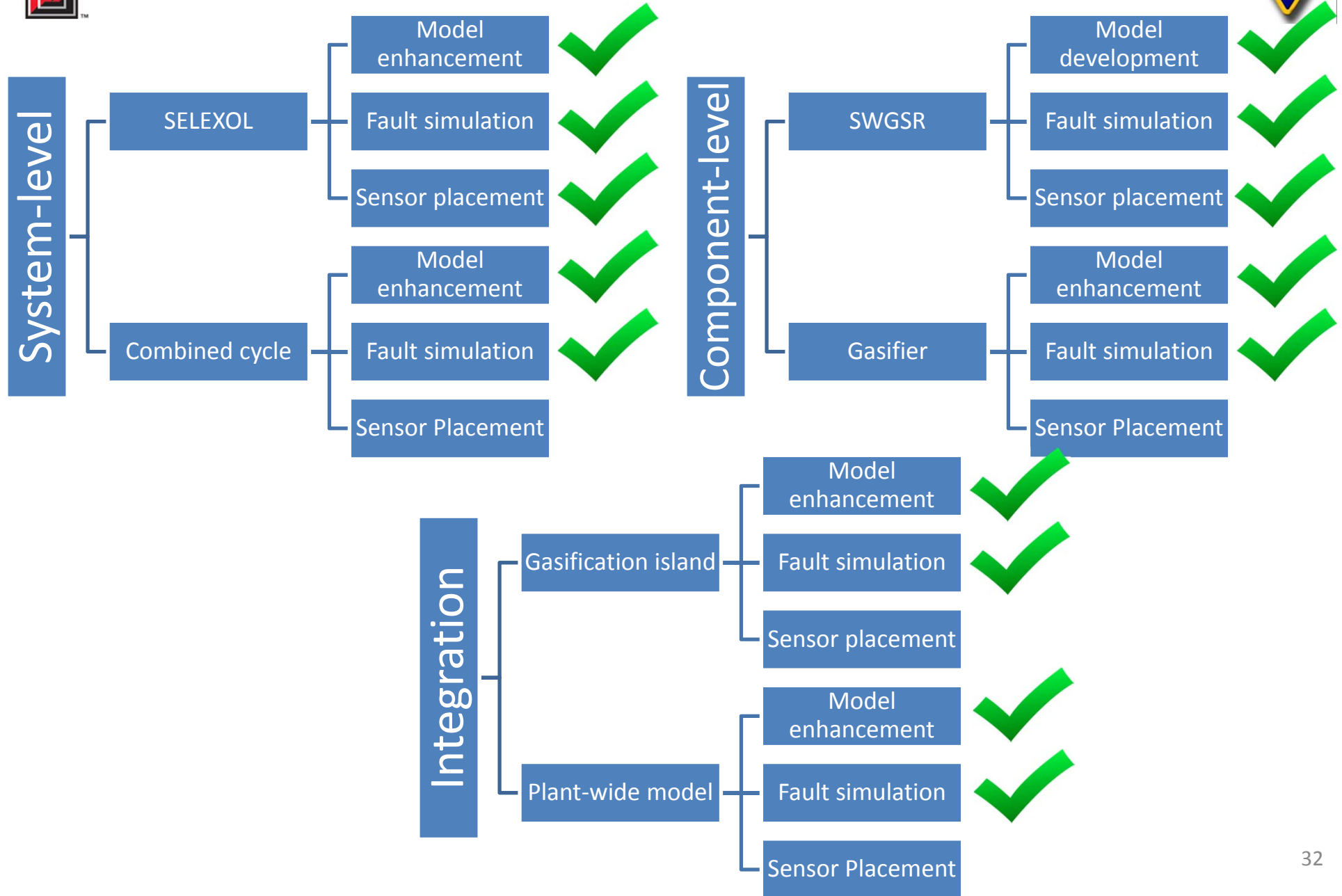


## Solution Characteristics - Decomposition

- Expected high computational enhancements for largely naturally partitionable systems
- Forced partitioning can result in large number of pseudo-faults
- Sub-networks can use models of different levels of granularity
  - Graph, Algebraic, ODE, PDE
- Optimal sub-network partitions
  - Specialize k-way partitioning, sub-modular function approaches for the sensor placement problem



## Current status







## Future work

- Complete SND for the combined cycle unit
- Synthesize sensor network for the gasifier using a reduced order model
- Use the simplified model and ISAT approach for the sensor network design of SWGSR
- Perform two tier sensor placement using the proposed decomposition approach



# Acknowledgement

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- Parham Mobed (TTU), Jeevan Maddala (TTU), Pratik Pednekar (WVU)



Thank You