



# OPTIMIZING THE COSTS OF SOLID SORBENT-BASED CO<sub>2</sub> CAPTURE PROCESS THROUGH HEAT INTEGRATION

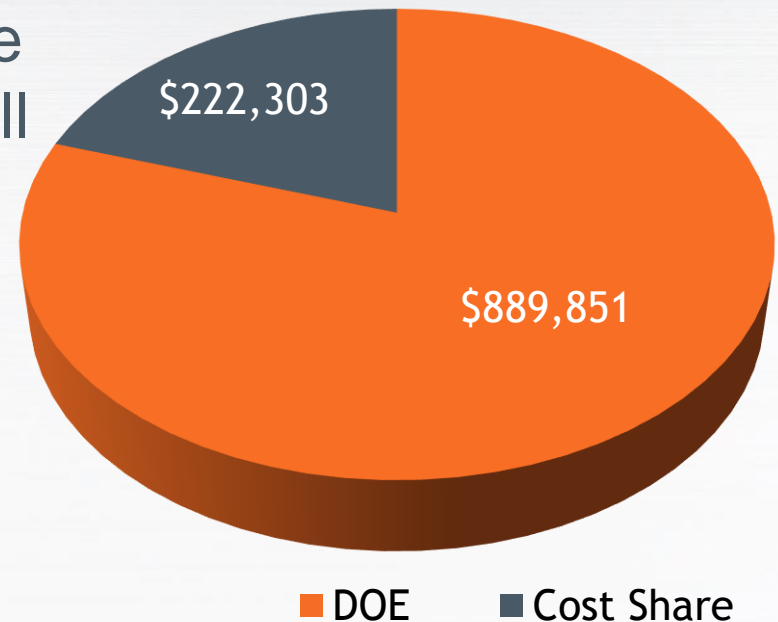
ADA-ES, Inc. NETL Contractor's Meeting  
June 25, 2015

DE-FE0012914

# Project Funding, Objective, and Timeline



- ▶ The overall objective: reduce the energy penalty and/or the overall levelized cost for solid sorbent-based CO<sub>2</sub> capture
- ▶ Outcome: progress towards meeting the overall DOE Carbon Capture Program performance goals



*Cooperative Agreement (Award No. DEFE001291)*

*Administered by DOE-NETL: Project Manager Bruce Lani*

*Project Duration: Nov 2014 - Dec 2015*

# Project Team



- DOE - NETL

- Project Sponsor



- ADA-ES, Inc.

- Project Management
- Technology Selection and Integration
- Techno-Economic Assessment
- Project Cost Share



- Technip Stone and Webster Process Technology with Dorr Oliver Division

- Conceptual Process
- Detailed Engineering, Design, and Costing
- Experience w/ multiple types of FB reactor designs (single, multibed, heat exchanger)



- Solex Thermal Science

- Experience w/ Moving Bed Heating and Cooling
- Thermal Modelling & Costing
- 400 Installations in 23 countries
- Project Cost Share



- Lehigh University Energy Research Center

- Broad Process Modelling Capabilities w/ ASPEN
- Conceptual Process Design
- Techno-Economic Assessment
- Project Cost Share



# Project Scope

- ▶ Evaluate options to reduce plant heat rate and LCOE associated with ADAsorb™ implementation through:
  - Heat integration with plant
  - Cross heat exchanger
- ▶ Assess two cross heat exchanger designs
  - Laboratory testing
  - Preliminary design
  - Preliminary techno-economics

# Project Schedule

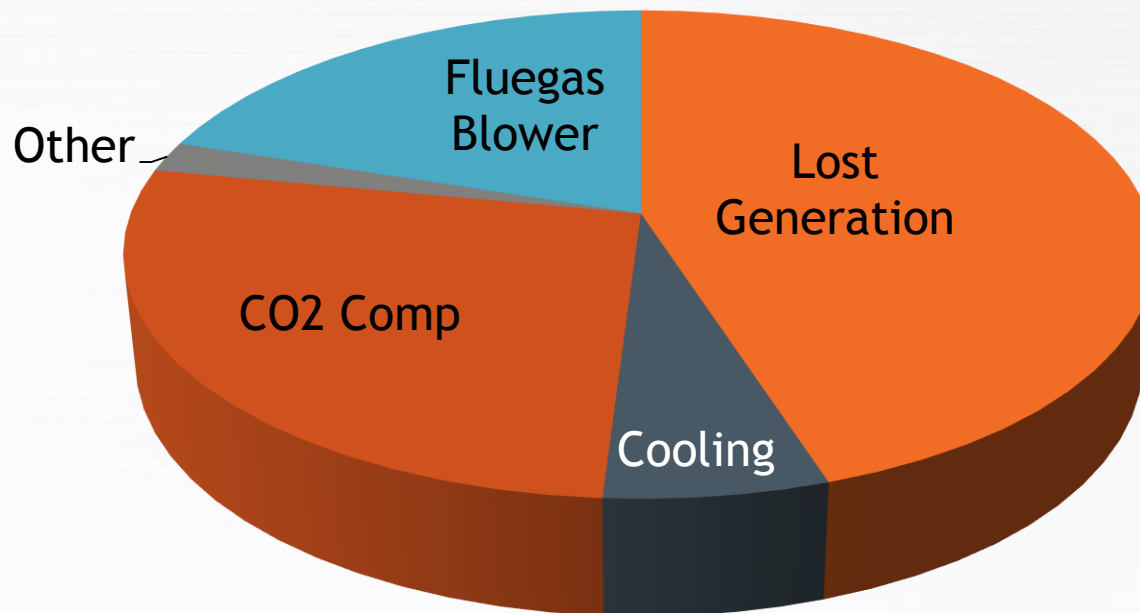


<b>Task Description</b>	<b>Schedule</b>
<b>Bench Scale Testing: Moving Bed</b>	April-July 2014
<b>Modeling: Moving Bed</b>	July 2014
<b>Design Integration: Fluidized Bed</b>	July 2015
<b>Heat Integration and Optimization: Economic Sensitivity Analysis</b>	Feb '14 - August '15
<b>Techno-Economic Assessment</b>	July - Dec 2015

# Breakdown of Estimated Parasitic Load



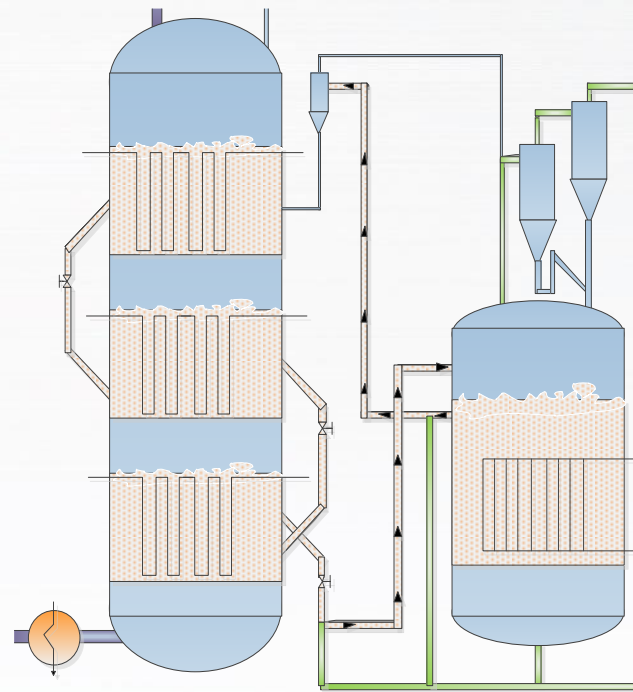
DOE Case 10 Analysis, ADA<sup>Asorb</sup>™ without heat integration



# ADASorb™ System Adsorber-Regen



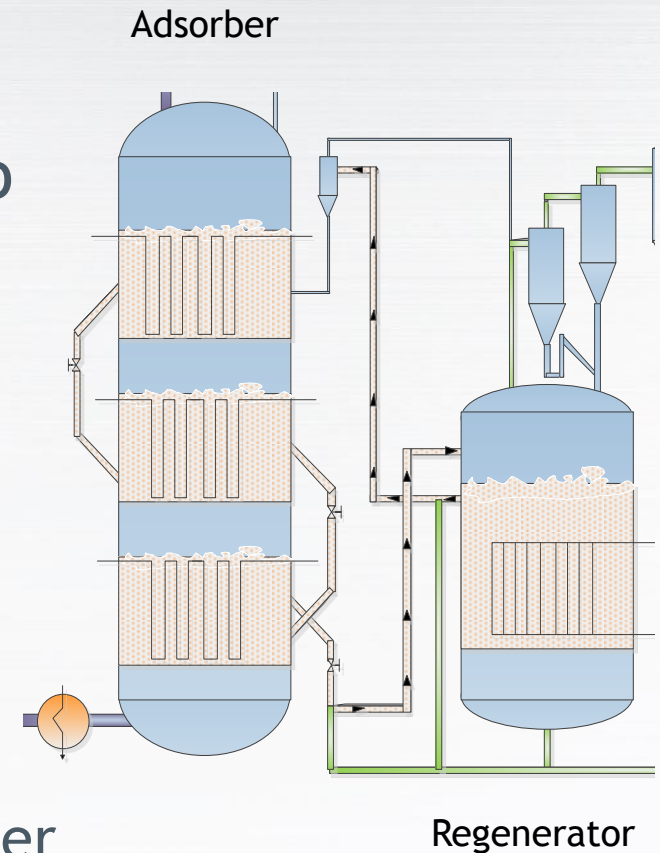
Adsorber



Regenerator

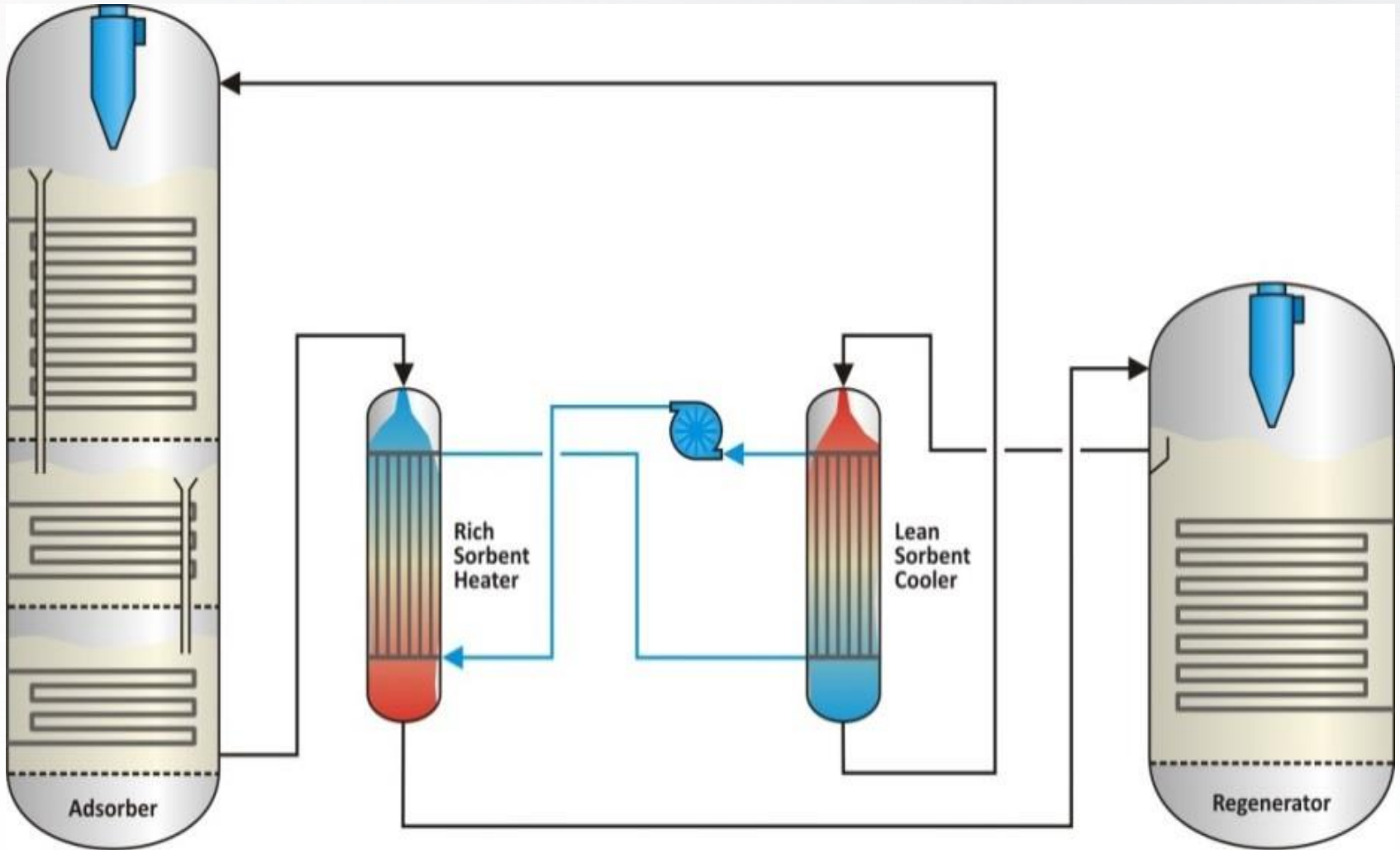
# Benefits of Incorporating a Cross Heat Exchanger

- ▶ Sensible Heat Recovery
- ▶ Reduced Adsorber Pressure Drop
  - Sorbent is currently cooled in top adsorber bed
  - Reduced cooling requirements → smaller bed → reduced flue gas blower power → reduced thermal regeneration input & cooling duty
- ▶ Reduced Regenerator Pressure Drop
  - Sorbent enters regenerator at higher temperature. Less heat transfer surface required

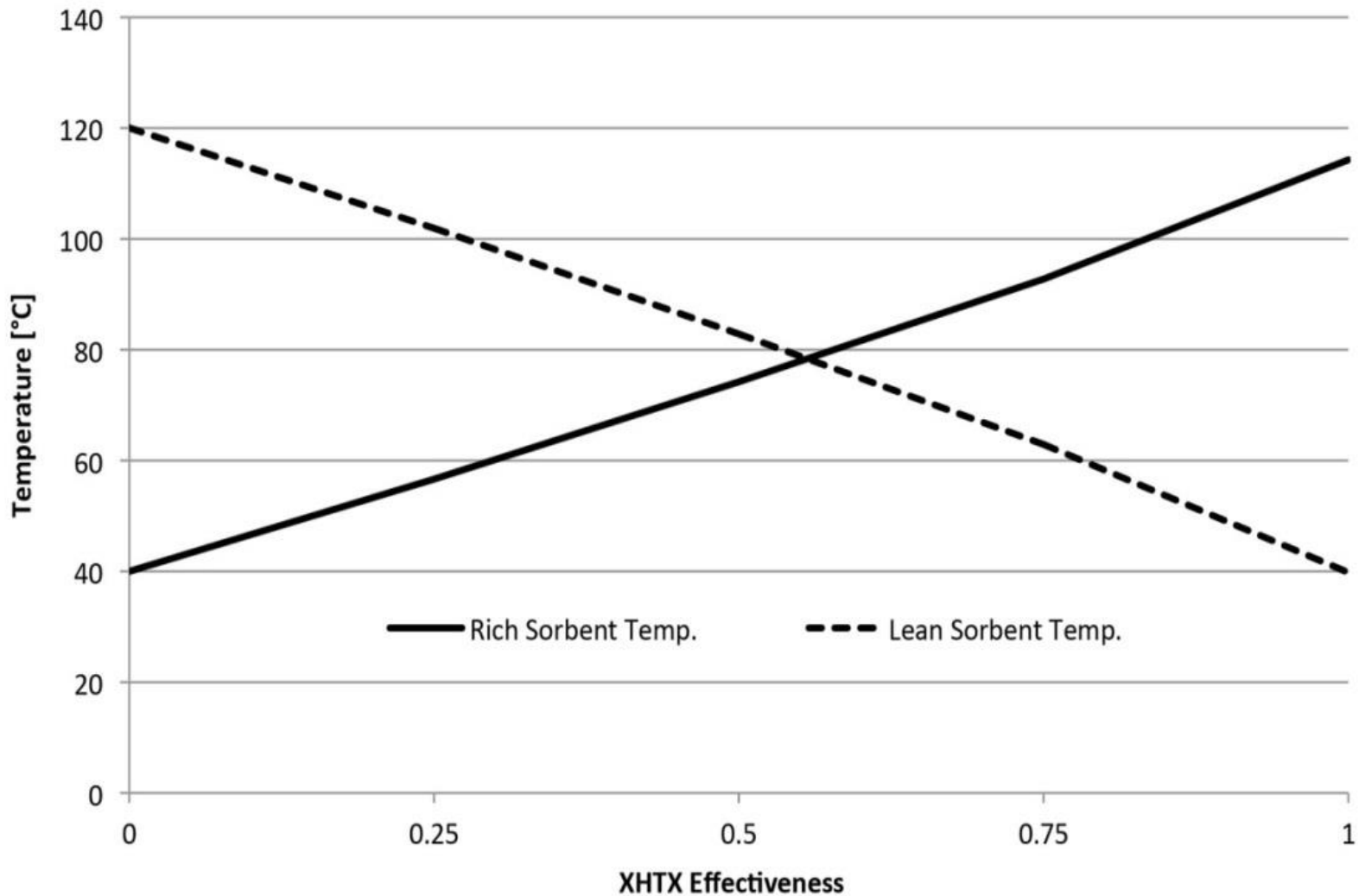




# Cross Heater Exchanger Concept



# Cross Heat Exchanger Effectiveness (Actual Heat transfer/Max Heat transfer)



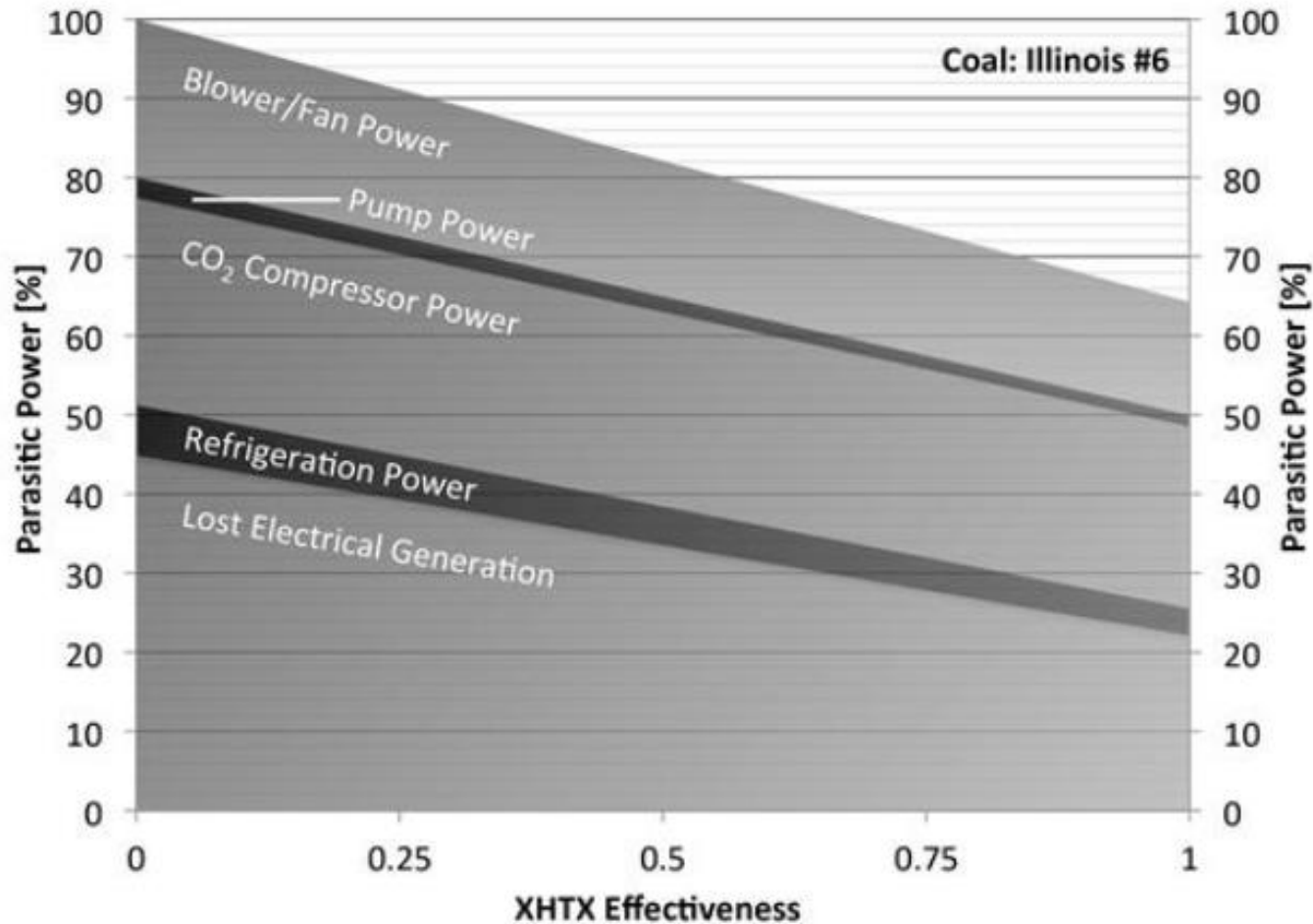
## Heat Rate vs Efficiency

- ▶ Power Plant Efficiency = Power Out/Fuel In
- ▶ Heat Rate = Fuel In/Power Out
- ▶ Heat Rate = 1/Efficiency

# Reduction of Net Unit Heat Rate as Function of Effectiveness of an Idealized Cross Heat Exchanger

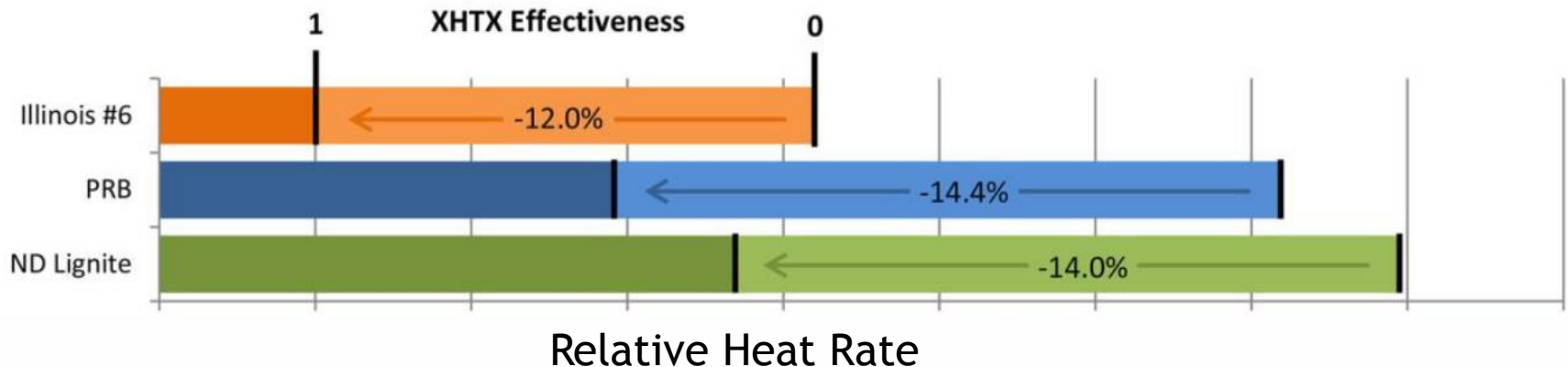


# Effect of Cross Heat Exchanger Effectiveness on Parasitic Power Losses



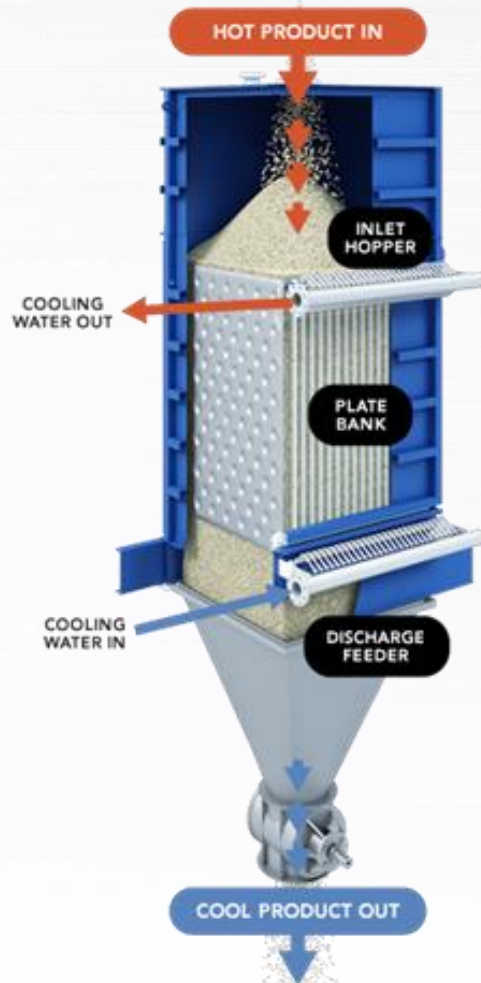
# Impact of Cross Heat Exchanger

- ▶ Significant improvements in process efficiency can be achieved.
- ▶ Pressure drop reduction of approximately 1.3 psi may be realized reducing the blower requirements for the adsorber.
- ▶ Total CO<sub>2</sub> capture (mass) is reduced
- ▶ Gross/Net generation ratio is substantially improved



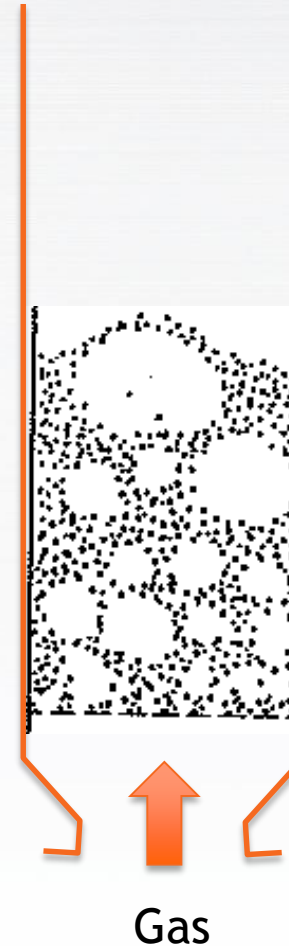
# Cross Heat Exchanger Design Options

## Moving Bed



Courtesy of Solex

## Fluidized Bed



# Moving Bed Advantages

- ▶ Reduced blower requirements: little or no fluidizing gas is necessary
- ▶ Counter-Current flow between solids and heat transfer media
  - possible to achieve an aggressive approach temperature and high heat recovery using only two moving beds per CO<sub>2</sub> capture train (one moving bed for heating and one for cooling)
- ▶ *Note: Heat transfer coefficient of a sorbent in a moving bed will be lower than that of the same sorbent in a fluidized bed*



# ADA and Solex Bench Scale Testing Results



## Successful Bench Scale Test

- Sorbent heated and cooled with the heat exchanger through process range (40-120<sup>0</sup>C)
- Sorbent flow smooth and consistent, no bridging between plates observed
- Minor bridging observed at the outlet of the exchanger. Proved to be manageable

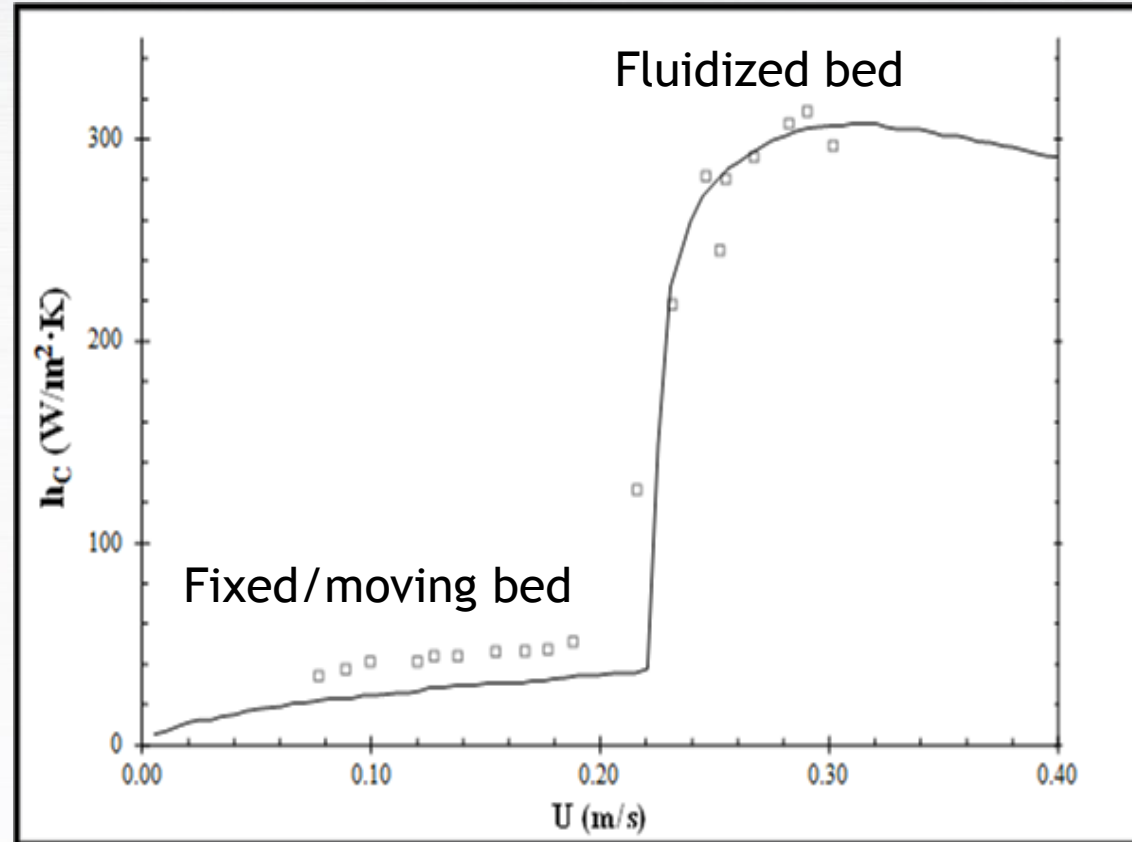


# Benefits of Fluidized Beds

- ▶ Good heat and mass transfer
- ▶ Equipment components have been demonstrated successfully on the required scale
- ▶ Industry process scalability knowledge

But . . .

- ▶ Higher pressure drop
- ▶ More complicated operation



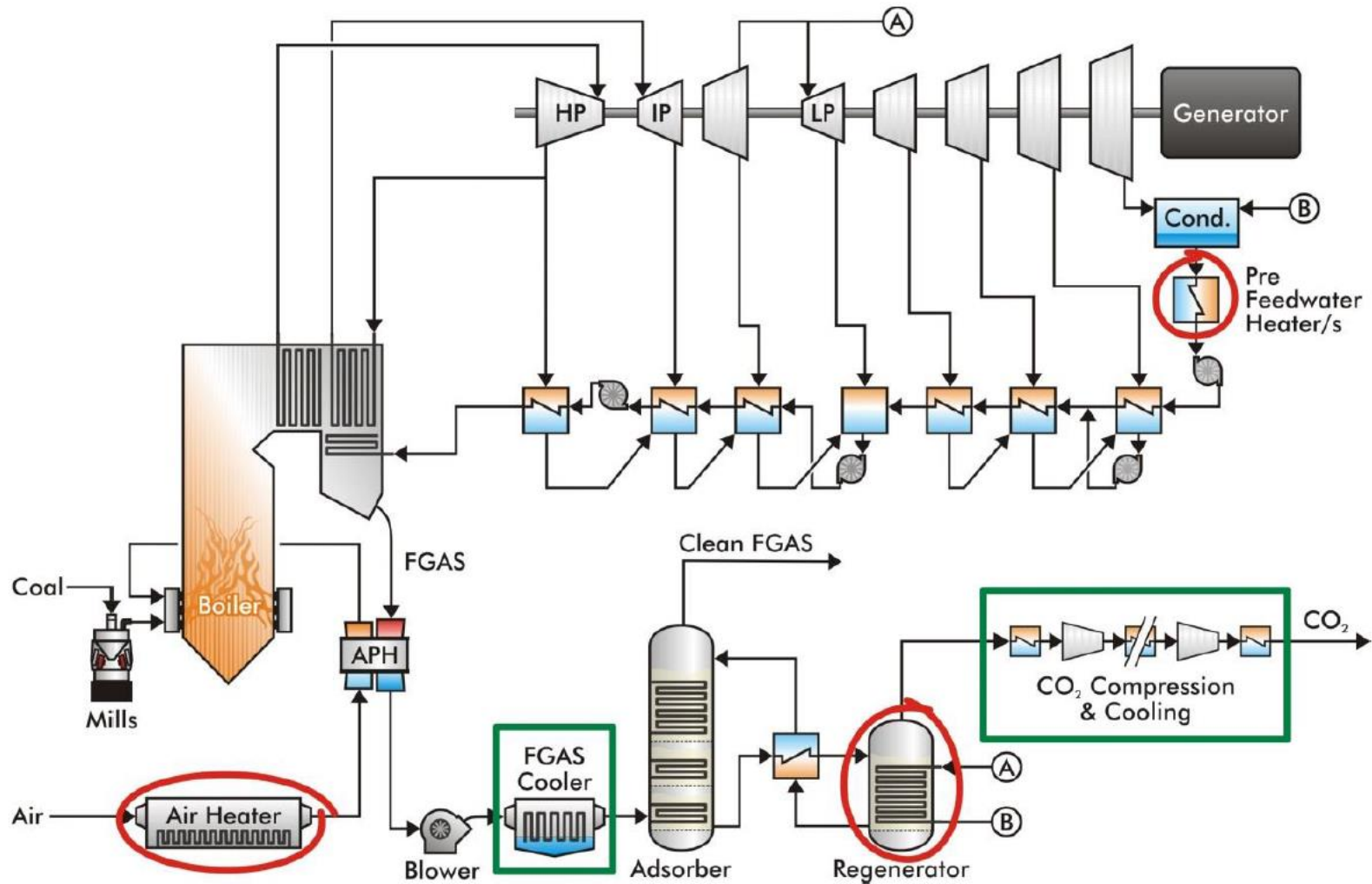
*J.F. Davidson, "Fluidization" 1985*

# Cross Heat Exchanger Preliminary Assessment



- ▶ Solex downward flow moving bed
  - Completed lab tests and modeling using Solex custom software
  - Preliminary design has promising technical and economic potential
- ▶ Technip fluidized bed
  - Initial assessment indicates design is not a practical approach

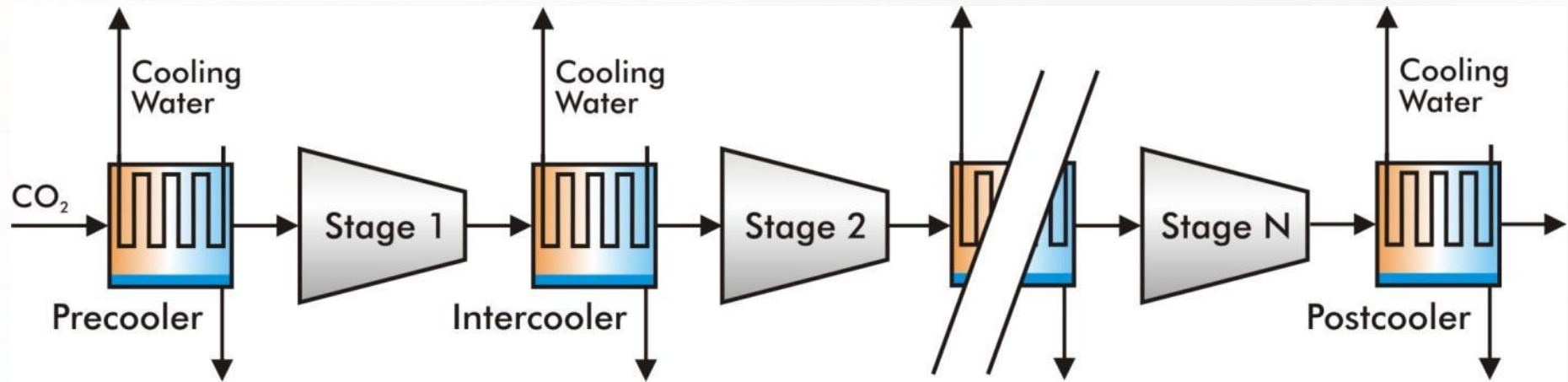
# Sources and Sinks for Waste Heat



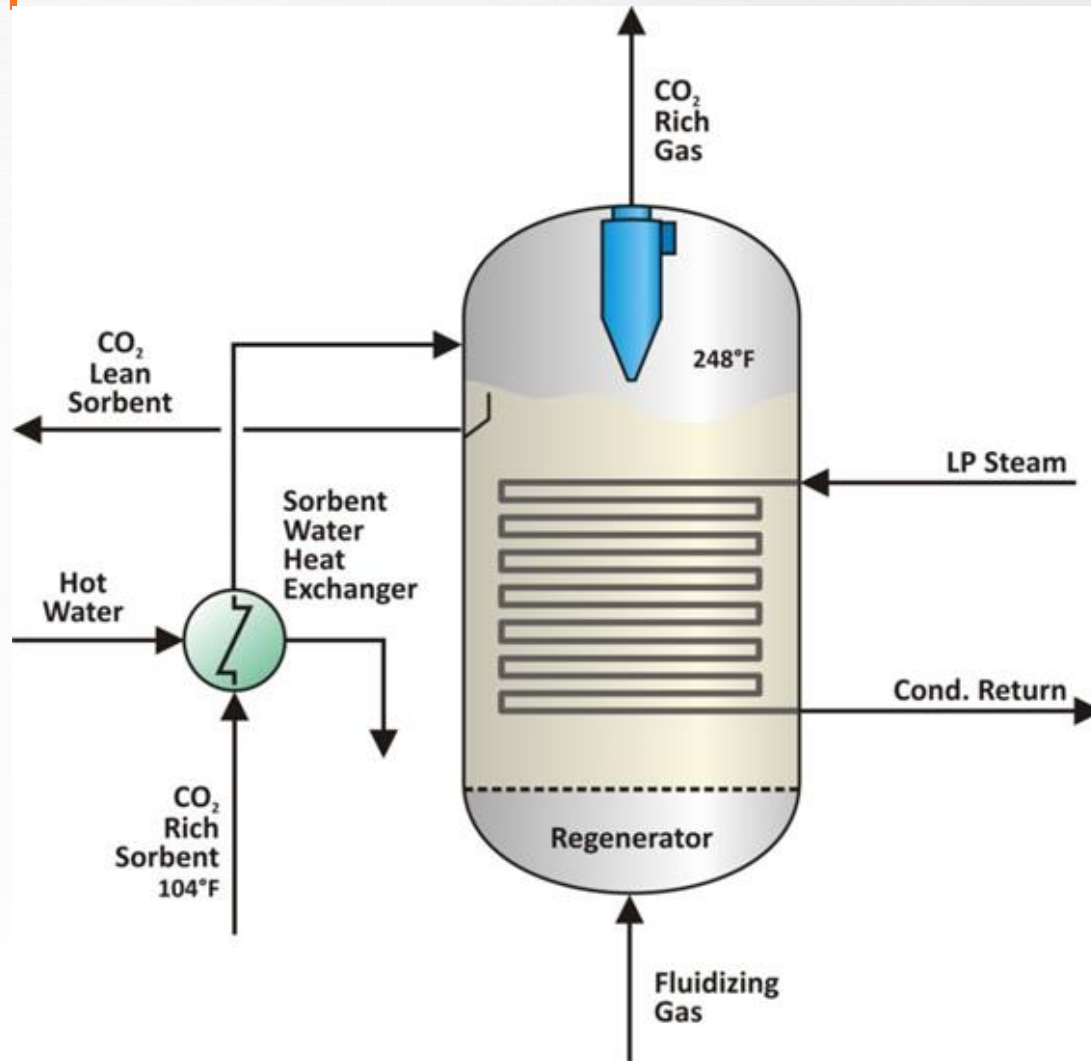
Lehigh Model

Advancing Cleaner Energy

# CO<sub>2</sub> Precooler & Compressor Intercoolers



# Sorbent Regenerator with Heat from Steam Turbine Extraction, CO<sub>2</sub> Cooler and CO<sub>2</sub> Compressor



# Predicted Impacts of Waste Heat Integration and Cross Heat Exchanger on Net Unit Heat Rate with Illinois #6 Coal



Case	$\Delta$ HR [%]
BASE	0
(1)	-0.96
(2)	-6.86
(1,2)	-7.36
(1,2,4)	-15.02

(1) Flue Gas Cooler Heat Integration

(2) CO<sub>2</sub> Cooler & CO<sub>2</sub> Compressor Intercooler Heat Integration

(3) Optimal Adsorber and Regenerator Operating Temperatures

(4) Addition of Cross Heat Exchanger (Effectiveness of 1.0)

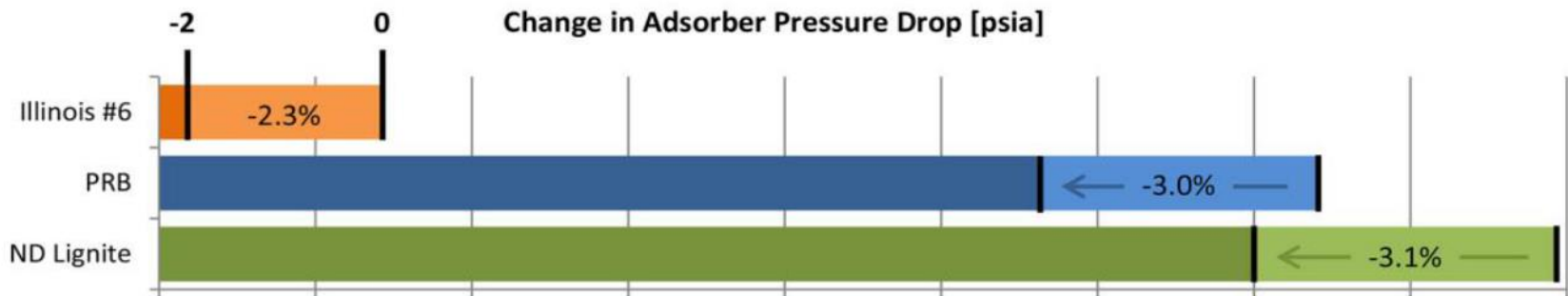
*Lehigh Model Results*

**Advancing Cleaner Energy**

# Other Key Improvements

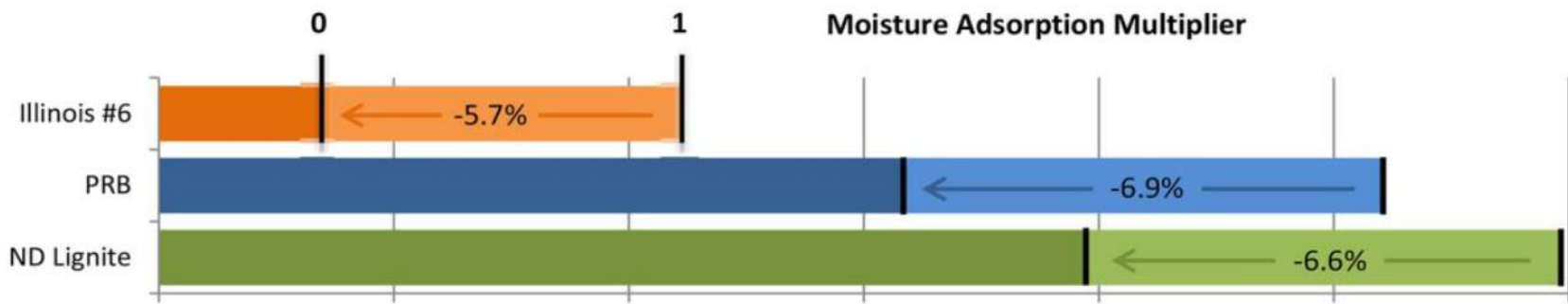
## ▶ Flue Gas Blower

- Accounts for between 25 to 28 percent of the parasitic power



Relative Heat Rate

## ▶ Sorbent moisture adsorption characteristics



Relative Heat Rate

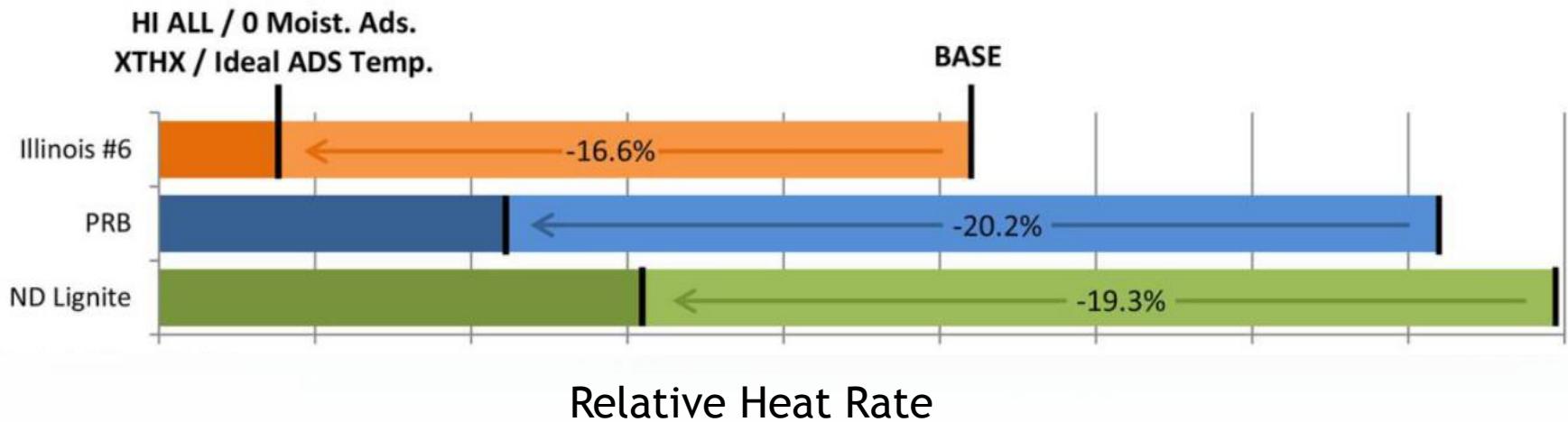
Lehigh Model Results

Advancing Cleaner Energy



# Combining Benefits

- ▶ Combining waste heat integration, eliminating sorbent moisture adsorption, incorporating a cross heat exchanger and optimizing adsorption temperature can have significant impacts on heat rate for plants using an ADA**Asorb**<sup>™</sup> capture system



# Additional Potential Improvements

- ▶ Develop sorbents with lower moisture uptake and lower temperature swing (Regen T- Adsorb T)
- ▶ ADAorb™ Capture System re-design to reduce fan power requirements (pressure drop)

# Summary



- ▶ Sensible heat recovery has the potential to substantially decrease net unit heat rate and reduce parasitic load based upon modeling results
- ▶ Modeling results have provided significant guidance on improving heat rate
- ▶ Initial design results of fluidized bed heat exchangers indicated that operating complexity and parasitic load outweighs benefits
- ▶ Further techno-economic analysis is required to determine whether the process benefits outweigh the cost of integrating a moving bed heat exchanger



Questions?

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