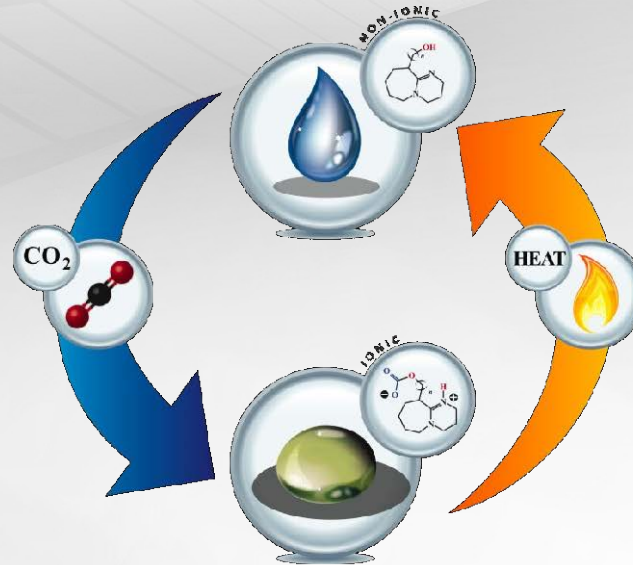




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# Accelerating the development of transformational solvent systems for CO<sub>2</sub> separations

DAVID J. HELDEBRANT  
NETL CO<sub>2</sub> CAPTURE TECHNOLOGY MEETING  
PITTSBURGH, PA  
JUNE 24, 2015

# Pacific Northwest National Laboratory: *Battelle-managed and mission-driven*



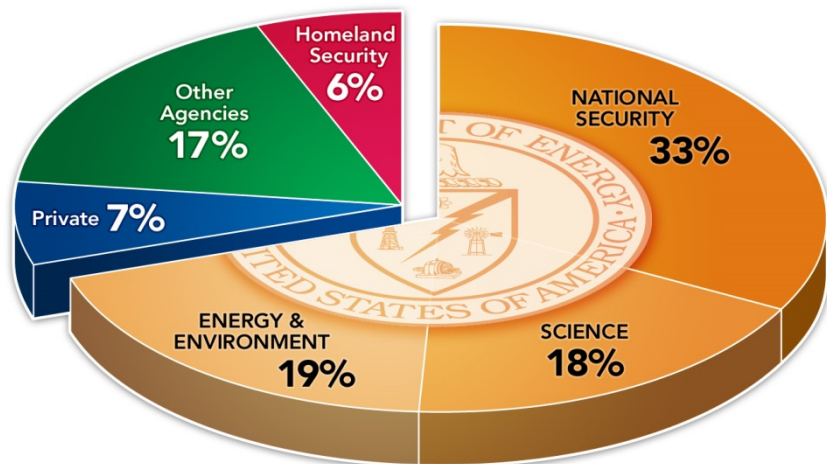
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## FY13 Facts

- ▶ \$936 million in R&D expenditures
- ▶ More than 4,300 staff
- ▶ 2000+ users & visiting scientists
- ▶ 1,168 peer-reviewed publications
- ▶ 36 patents

- ▶ Mission-driven collaborations with government, industry, academia
- ▶ Operated by Battelle since 1965
- ▶ DOE's top-performing lab for 7 years



Interdisciplinary teams at [Pacific Northwest National Laboratory](#) address many of America's most pressing issues in energy, the environment and national security through advances in basic and applied science. For more, visit [PNNL's News Center](#), or follow PNNL on [Facebook](#), [LinkedIn](#) and [Twitter](#).

# Why Water-Lean & Concentrated Solvents?



## Benefits:

- ▶ Reduced reboiler duty from boiling and condensing water
- ▶ Lower sensible heat
- ▶ Different thermodynamic and physical properties
- ▶ May use existing 1<sup>st</sup> gen solvent infrastructure

## Limitations:

- ▶ Some advanced solvents have not yet demonstrated water tolerance
- ▶ Full dehydration impractical
- ▶ Cost challenges with a custom solvent
- ▶ Viscosity increase as a function of CO<sub>2</sub> loading



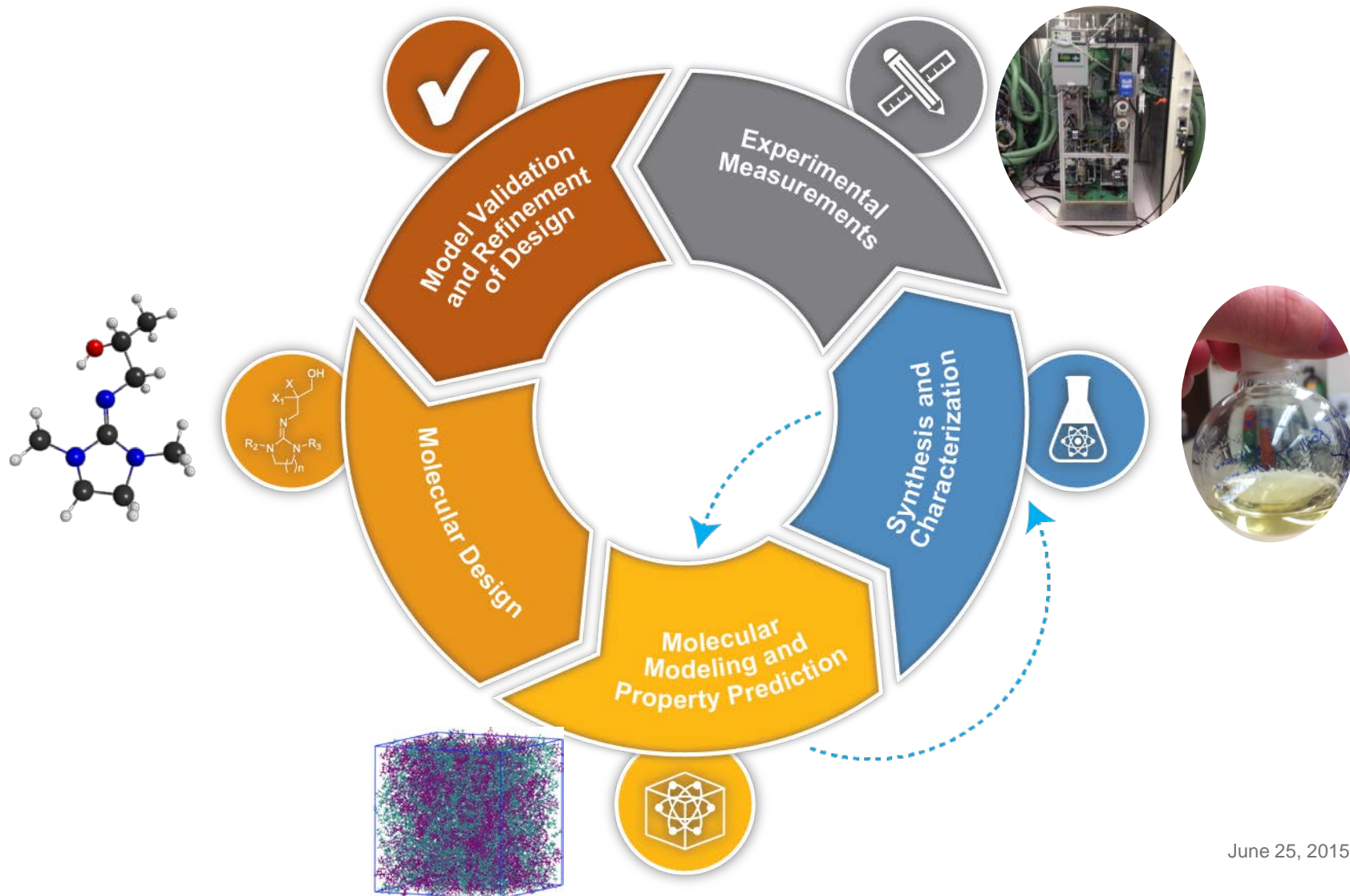
# Overview: Integrating Molecular Design, Synthesis & Testing For Multiple Platforms



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\*Aiding DOE's transformational solvent portfolio address the grand challenge of viscosity



# Project Goals and Objectives

## Goals

- ▶ Develop tools for viscosity prediction and solvent design methodologies for reducing viscosity across all transformational solvent platforms.
- ▶ Develop cost-effective synthesis methodologies to bring solvent costs ~ \$10/kg.
- ▶ Verify the performance of the model, and reduce viscosity of current formulations by >400 cP.
- ▶ Enable advanced solvent designs for advancement up DOE's TRL readiness scale to enable large scale testing and deployment by year 2030.

## Objectives

- ▶ Develop a viscosity model that can predict key solvent physical and thermodynamic properties.
- ▶ Collect necessary additional thermodynamic and kinetic information for a library of compounds.
- ▶ If budget and time permitting use continuous flow testing data to make robust energy and LCOE predictions for a full-scale system, using Aspen Plus™ to model the system.
- ▶ Apply the viscosity model and molecular design principles to other solvents in DOE's post-combustion solvent portfolio.

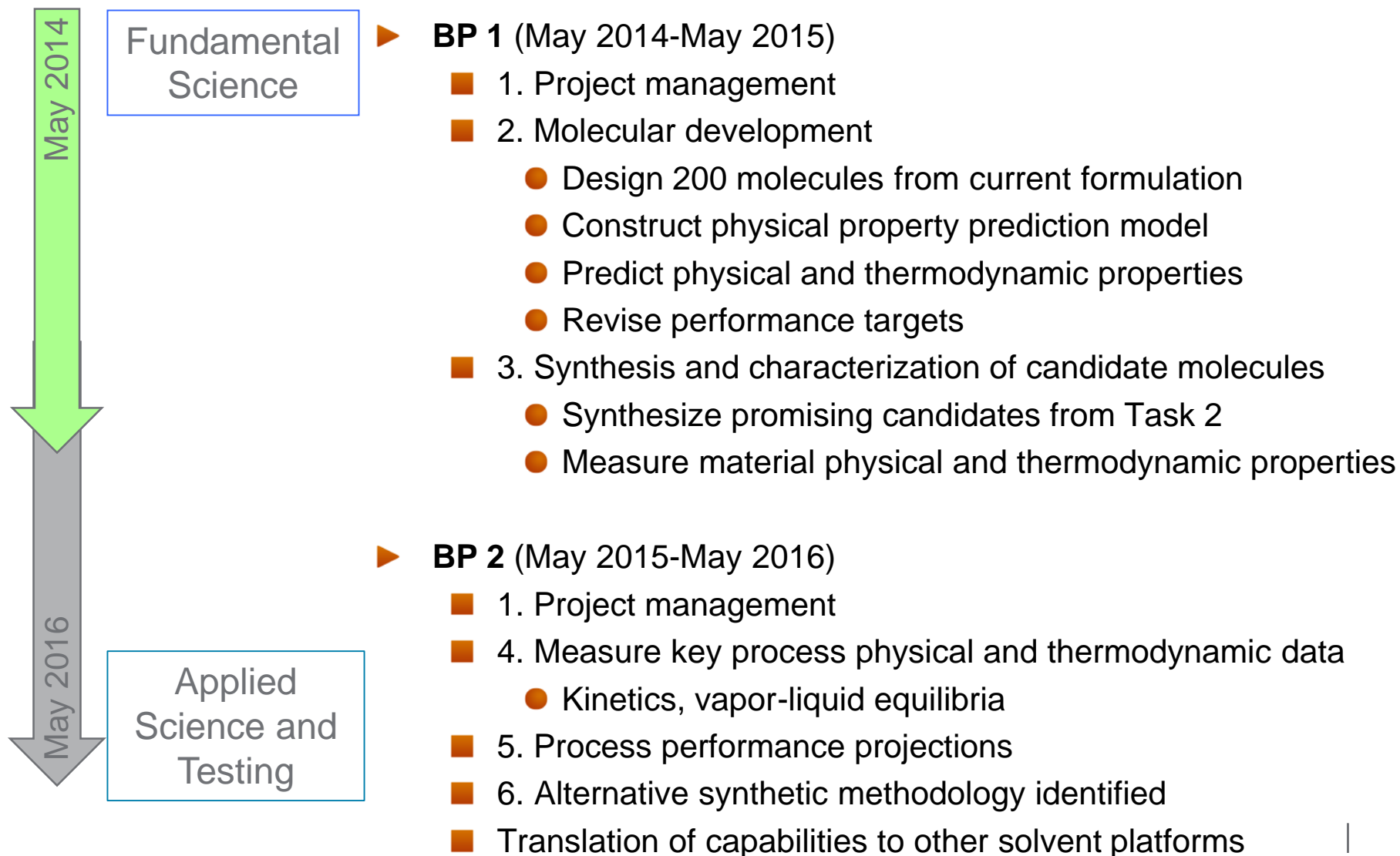
# Project Schedule and Major Tasks



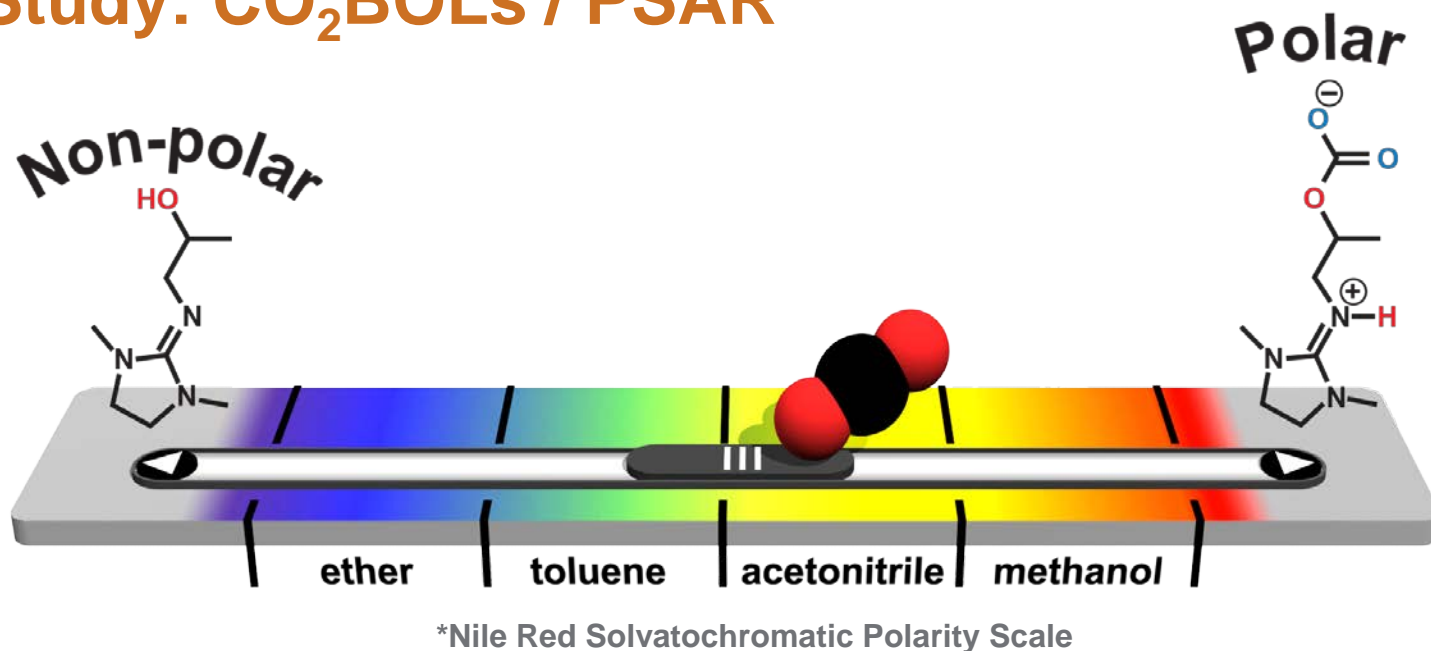
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**Funding: 1.76 million/ 24 months**

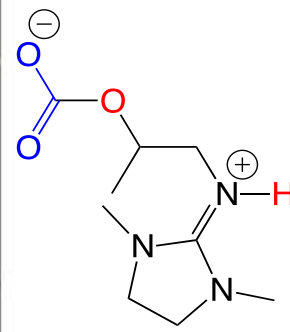
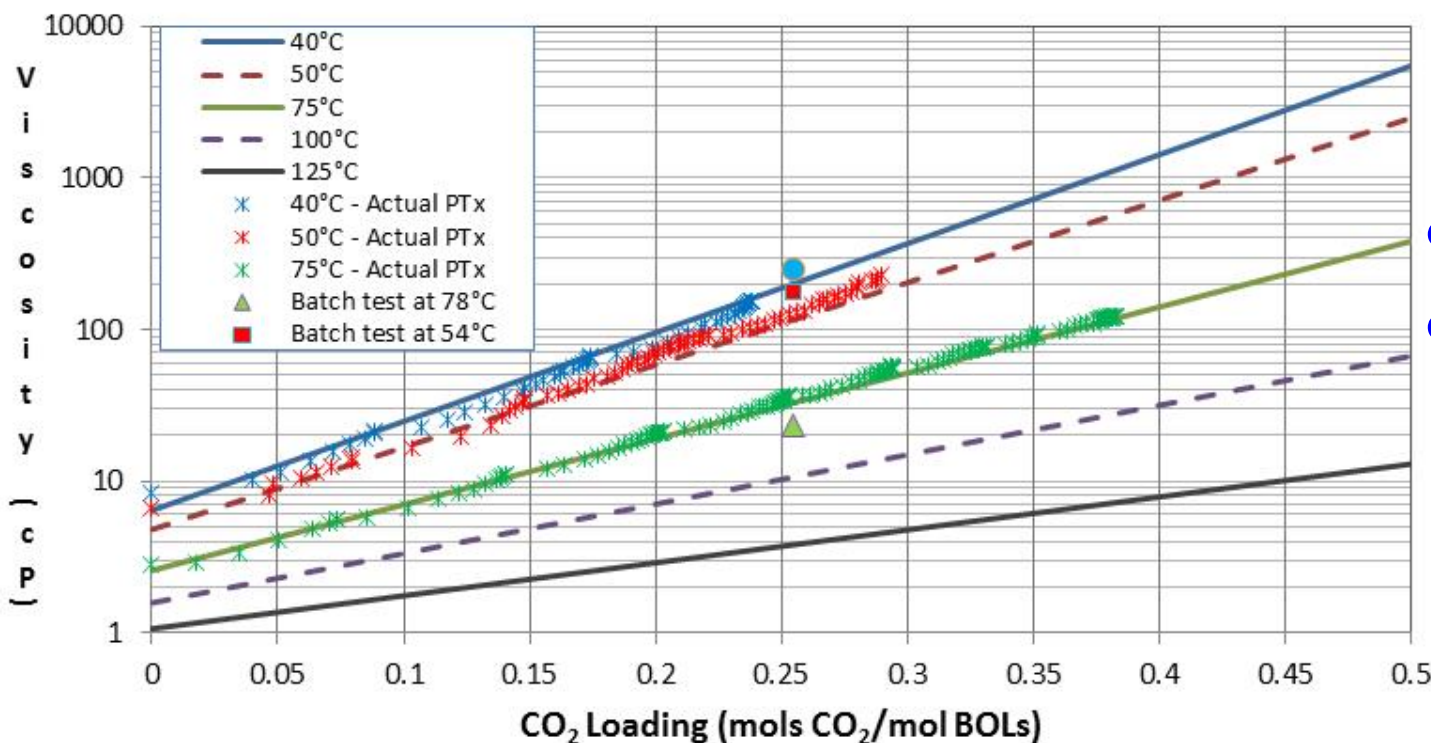
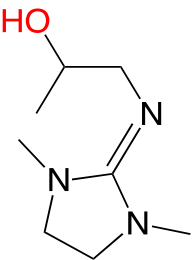


# Case Study: CO<sub>2</sub>BOLs / PSAR



- “Water-lean” organic switchable ionic liquid solvent system
  - Optimal water level in circulating solvent estimated
    - (~5 wt. % water confirmed by simulation)
  - Heat of solution -80 kJ/mol
  - CO<sub>2</sub>BOL material projected at (\$35-70/kg)
- Polarity-Swing Assisted Regeneration
  - Co-injection of non-polar “antisolvent” destabilizes the CO<sub>2</sub>-rich form enhancing CO<sub>2</sub> release.

## Viscosity Correlation for CO<sub>2</sub>-BOLs



- ▶ Points are measured data and lines are model fits
- ▶ Water does not precipitate bicarbonate salts
- ▶ Viscosity with 10% water (worst case loading) has a minor impact
- ▶ Equilibrium model projections of current formulation (0.25 LEAN -0.5 RICH) would be 200-3,000 cP



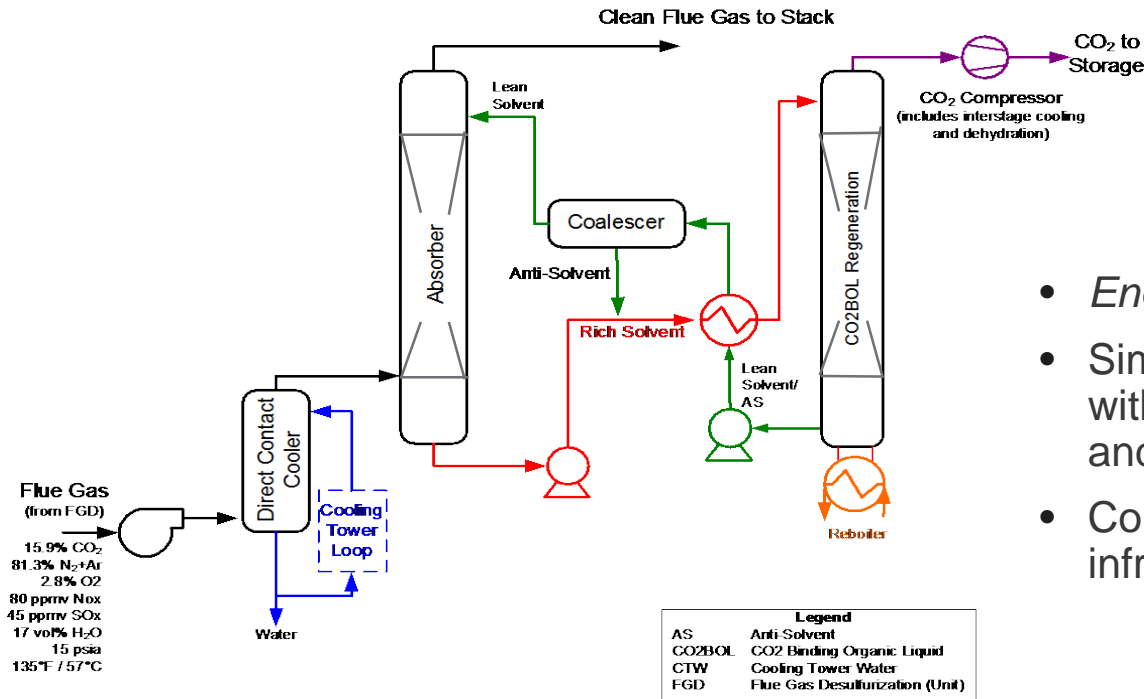
# CO<sub>2</sub>BOL/PSAR Conceptual Configuration



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**FLUOR**<sup>®</sup>



- *Energy. & Env. Sci.* (2013), 6, 2233
- Similar to aqueous amine systems albeit with coalescing tank, antisolvent loop, and water management equipment
- Commercially available equipment and infrastructure

| Legend |                                 |
|--------|---------------------------------|
| AS     | Anti-Solvent                    |
| CO2BOL | CO2 Binding Organic Liquid      |
| CTW    | Cooling Tower Water             |
| FGD    | Flue Gas Desulfurization (Unit) |

## Process Model Results

|   |                                 |
|---|---------------------------------|
| Lean Solution Loading                             | mol CO <sub>2</sub> /mol BOL    |
| Rich Solution Loading                             | mol CO <sub>2</sub> /mol BOL    |
| Delta Loading                                     | mol CO <sub>2</sub> /mol BOL    |
| Lean solution circulation rate                    | kg/hr                           |
| CO <sub>2</sub> removed                           | kg/hr                           |
| lean solution rate per kg CO <sub>2</sub> removed | kg/kg CO <sub>2</sub>           |
| RICH viscosity                                    | cP                              |
| Reboiler Temperature                              | °C                              |
| heat rate   | kcal/kg CO <sub>2</sub> removed |
| heat rate   | btu/lb CO <sub>2</sub> removed  |
| Relative heat rate                                |                                 |

|         | 20 cP Target<br>Equilibrium Case |                  |   |
|---------|----------------------------------|------------------|---|
| Case 2  | Case 4                           | Equilibrium Case |   |
| 0.0807  | 0.0807                           | 0.2615           |   |
| 0.2867  | 0.3339                           | 0.5737           |   |
| 0.206   | 0.2532                           | 0.3122           |   |
| 6004440 | 4878290                          | 4387408          |   |
| 297957  | 297957                           | 299188           |   |
| 20.15   | 16.37                            | 14.66            |   |
| 356     | 577                              | 20               | → |
| 103.8   | 103.6                            | 86               |   |
| 615.5   | 548                              | 442.3            |   |
| 1107.9  | 986.3                            | 796              | → |
| 1       | 0.89                             | 0.72             | → |

Manuscript in  
preparation

# Why CO<sub>2</sub>BOLs as a Case Study

- ▶ Comprehensive data available of all transformational solvents is lacking
  - Complete thermodynamic, kinetic and bench scale data available
  - Water tolerance established (5 wt% steady state)
  - Estimated low evaporative losses
  - Comparable Ecotoxicity (rainbow trout) to MEA
    - CO<sub>2</sub>BOL (180), MEA (150mg/L)
  
- ▶ Process reviewed and guided by the Fluor Corporation
  - New ASPENplus equilibrium and kinetic models constructed by Fluor.
  - Viscosity increases consistent with prior results, but capture performance not impeded as much as anticipated.
  - Current formulation of BOL shows acceptable performance, but less viscous derivatives will show enhanced performance.
  - Prior thermodynamic model projections consistent with observed bench scale performance.
  
- ▶ **Other transformational (water-lean) solvent systems will behave similarly to CO<sub>2</sub>BOLs**

# Applying Molecular Design Towards CO<sub>2</sub> Capture

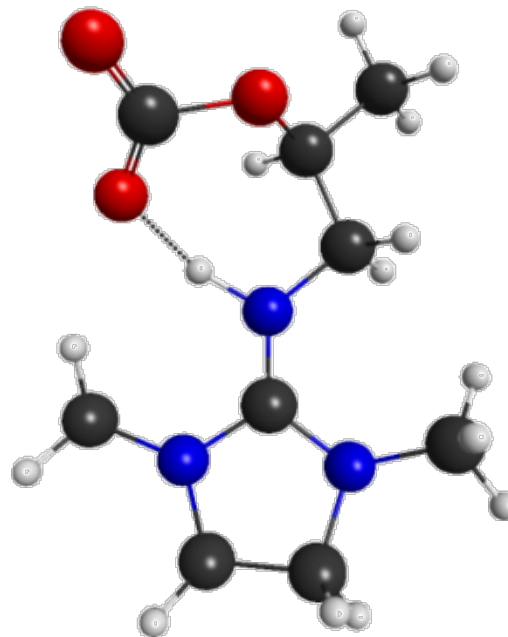
## What we need

### (*specific for each solvent class*):

- ▶ Guanidine-based CO<sub>2</sub>BOLs
  - High basicity needed for >90% CO<sub>2</sub> capture with acceptable solvent recirculation rates
- ▶ Cyclic base core to prevent hydrolysis

## Viscosity Modifying Factors:

- ▶ Steric crowding
- ▶ Fine tuned electronics
- ▶ Cation-anion interactions
- ▶ Effect of hetero-atoms and charge solvation
- ▶ H-bonding orientation and strength



# Applying Molecular Design Towards CO<sub>2</sub> Capture

## What we need

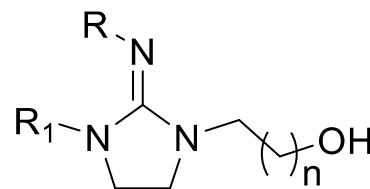
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## Viscosity Modifying Factors:

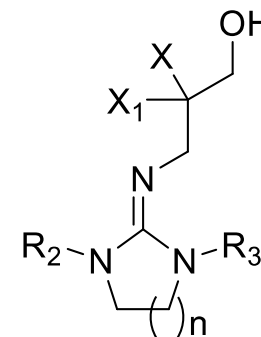
- ▶ Steric crowding
- ▶ Fine tuned electronics
- ▶ Cation-anion interactions
- ▶ Effect of hetero-atoms and charge solvation
- ▶ H-bonding orientation and strength

### Steric Effects



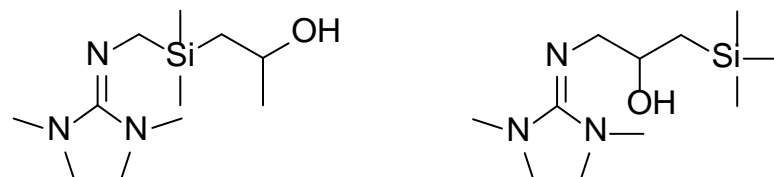
R=Pr, i-Pr, Bu, t-Bu  
R<sub>1</sub>=Me, Et, i-Pr  
with n=1, 2, 3

### Electronic Effects



X and X<sub>1</sub>= F, Cl, CF<sub>3</sub>,  
(EWG) or OMe, CH<sub>2</sub>NMe<sub>2</sub>,  
(EDG) and R<sub>2</sub>=R<sub>3</sub>=Me,  
CF<sub>3</sub>, CF<sub>3</sub>CF<sub>2</sub>, OMe with  
n=1, 2, 3

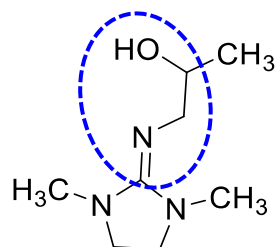
### Charge Solvation (Silane-Based)



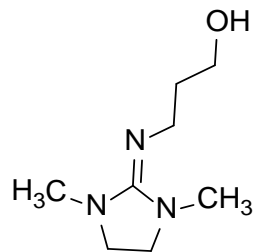
# Integrating Molecular Modeling and Design Towards Liquids for CO<sub>2</sub> Capture

- ▶ Model validation through testing of known compounds
  - Evaluate inter- vs intra-molecular hydrogen bonding effects on viscosity
  - 3-D steric interactions
  - Reduced intermolecular interactions
- ▶ Simulate pure liquids and mixtures at 15%, 25%, and 50% CO<sub>2</sub>, determine viscosity from analysis of trajectories

## Control Molecules & Complexes

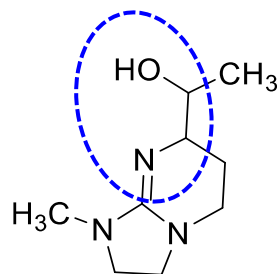


Current best-performing BOL  
Viscosity ~ 200cP at  
0.25 mol %CO<sub>2</sub>

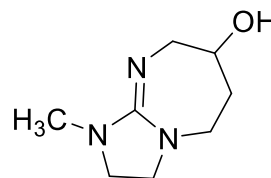


Poor performing BOL  
Viscosity >>1,000 cP at  
0.25 mol %CO<sub>2</sub>

## Trial Molecules & Complexes



- Preserves weights and functional groups of Current BOL (2<sup>nd</sup> amine and alcohol-i.e. similar CO<sub>2</sub> adsorption energy)
- Partially restrict mobility of aliphatic side chain w. 2<sup>nd</sup> ring.
- Favors internal H-Bond.
- May be a more readily synthesizable target.



- Preserves weights and functional groups of Current BOL (2<sup>nd</sup> amine and alcohol, i.e. similar CO<sub>2</sub> adsorption energy)
- Restrict mobility of aliphatic side chain w. 2<sup>nd</sup> ring.
- Hinders internal H-Bond.

# Computational Materials Design

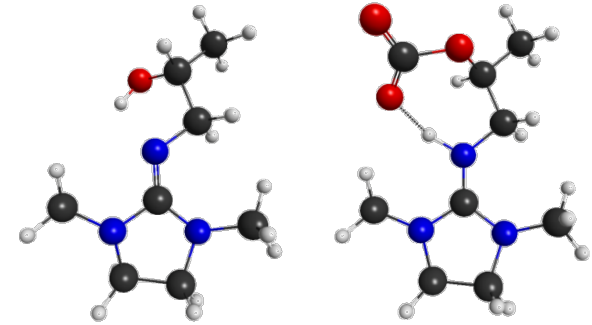


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▶ *Ab Initio* Electronic Structure for Molecular Properties ( $\sim 10^2$ - $10^3$  atoms)

- Accurate description of molecular properties
- Atomic charges and intermolecular contacts
- Reaction energetics: H-bonding, CO<sub>2</sub> absorption energy
- Spectroscopic properties: IR, Raman, NMR



IPADM-2-BOL

CO<sub>2</sub>-loaded  
IPADM-2-BOL

▶ Classical Molecular Dynamics ( $\sim 10^4$ - $10^5$  atoms)

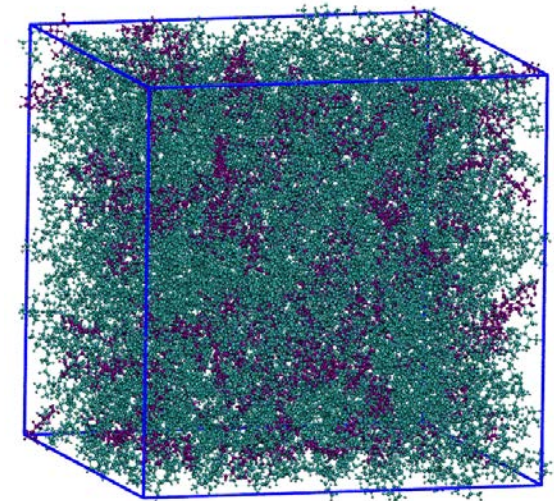
- Accurate description of molecular liquid structure
- Universal OPLS with *ab initio* charges
- Transport properties: diffusion and viscosity
- Viscosity can be directly computed from long simulations (1  $\mu$ s) Codes, Software: GROMACS ([www.gromacs.org](http://www.gromacs.org))

▶ Reduced ordered model capabilities

- Shift through many candidates in short time (few days)

▶ Codes, Software:

- CP2K ([www.cp2k.org](http://www.cp2k.org)),
- NWChem ([www.nwchem.org](http://www.nwchem.org))

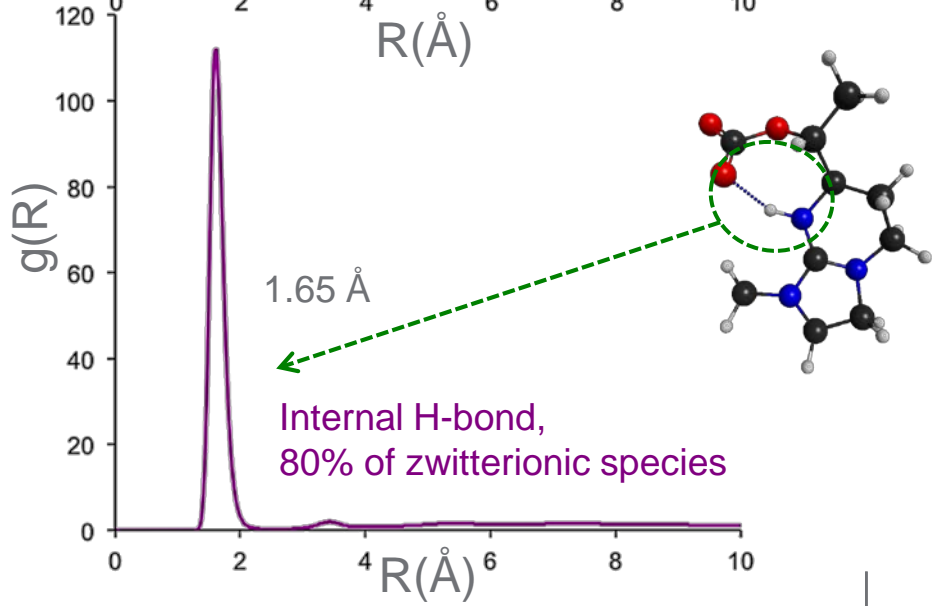
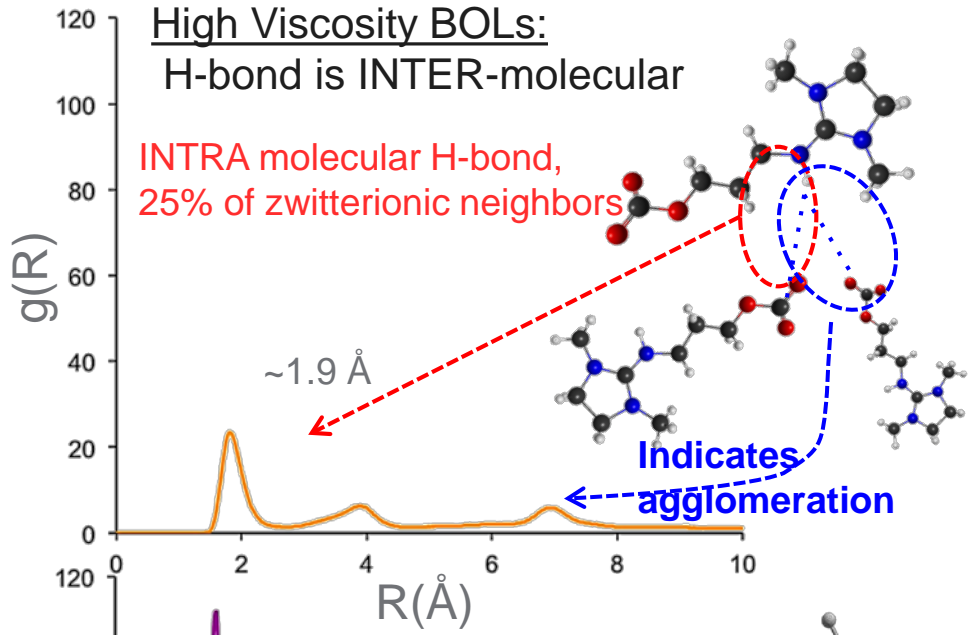
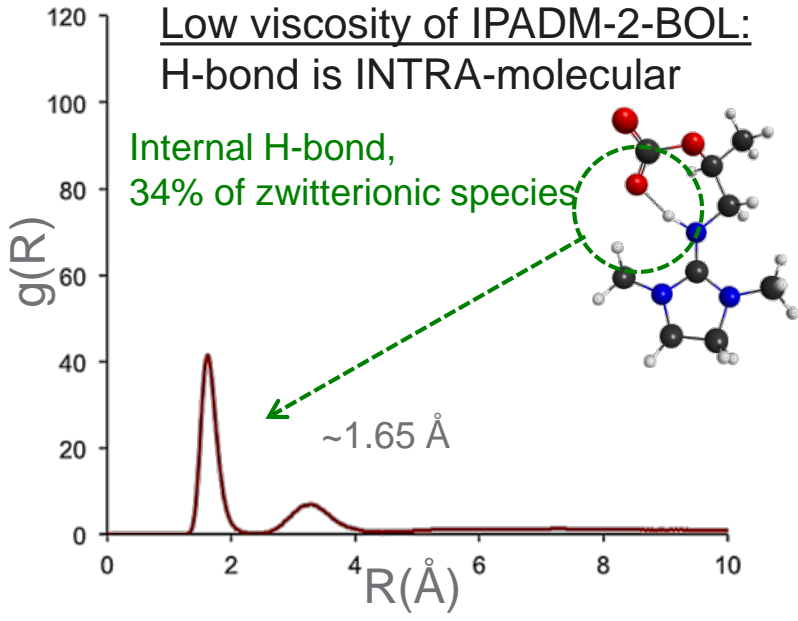


# Molecular-Level Interactions: The Hydrogen Bond

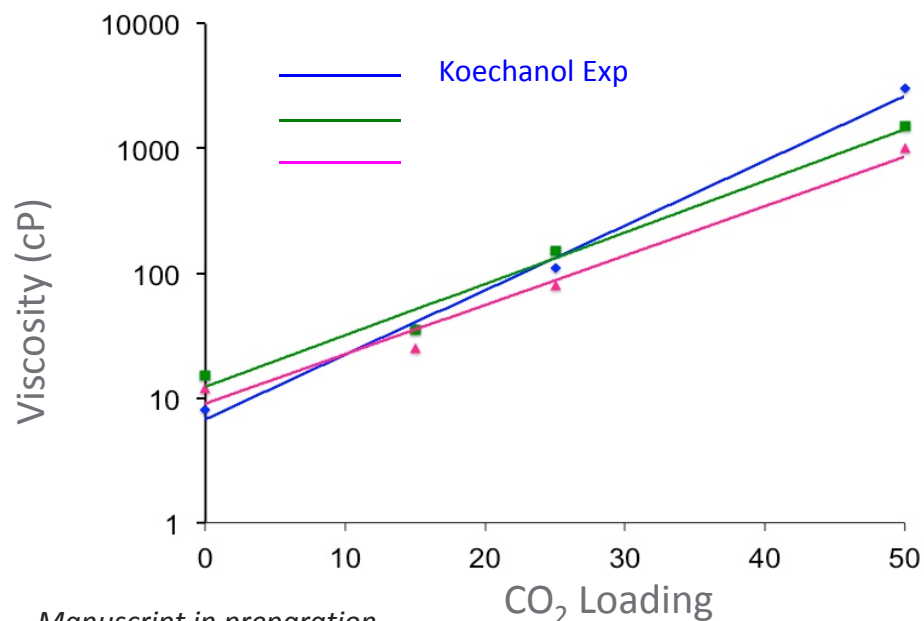
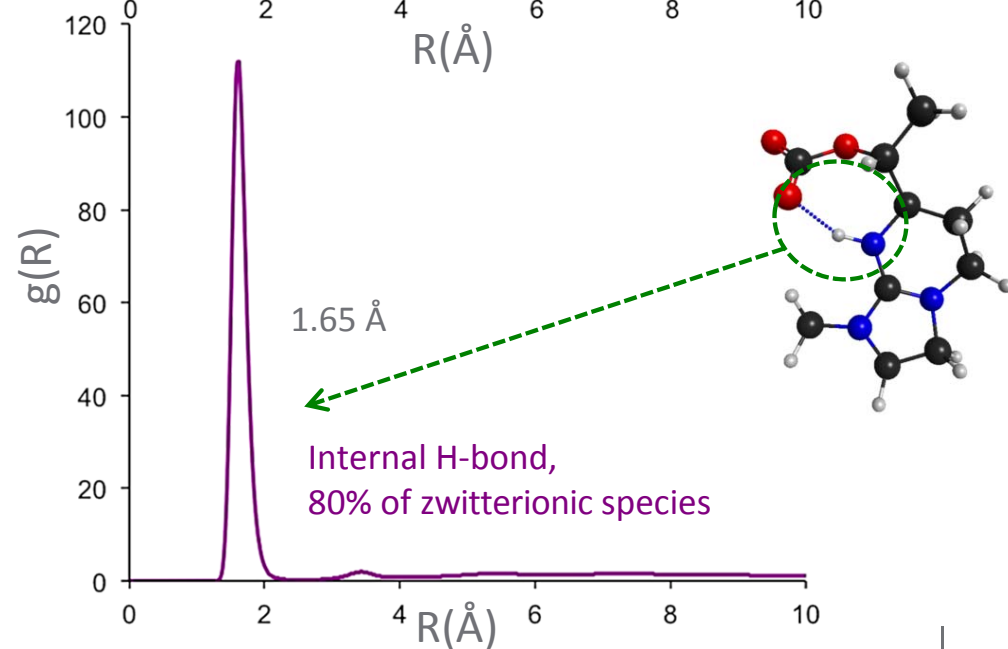
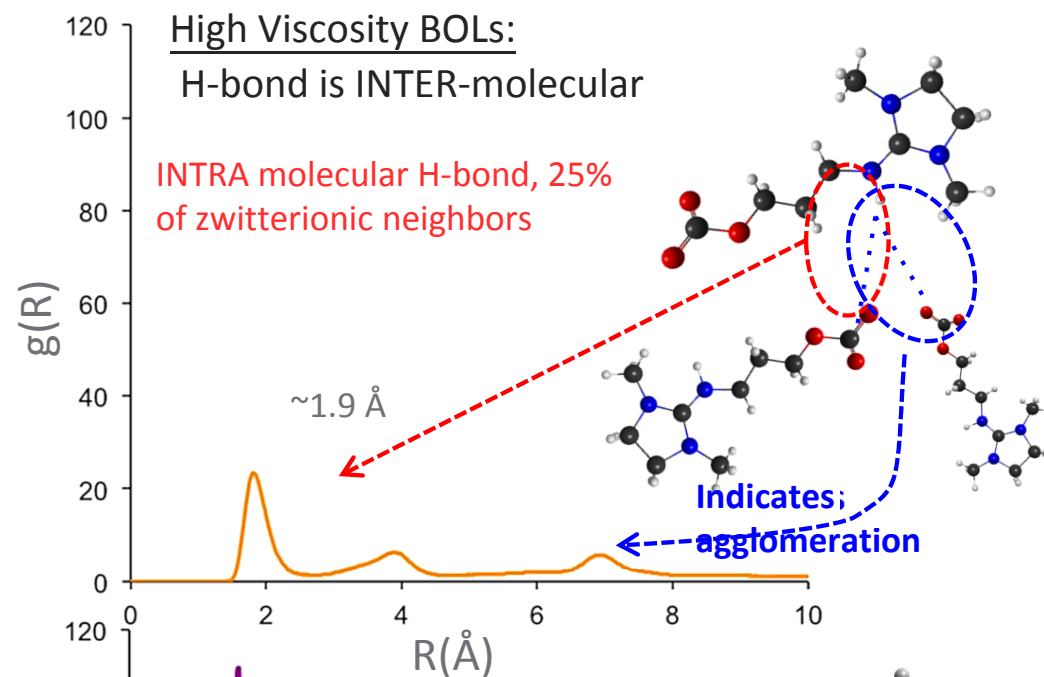
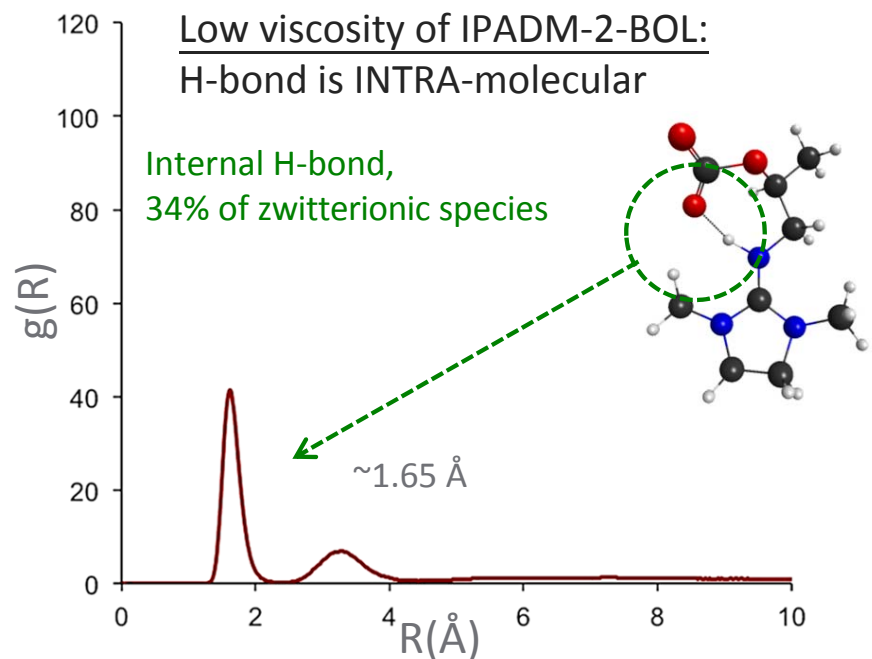


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# Molecular-Level Interactions: The Hydrogen Bond



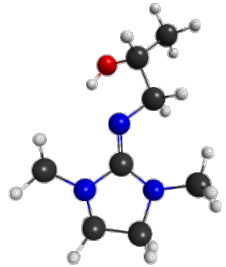


# Validation of the Model With Experimental Data is Critical



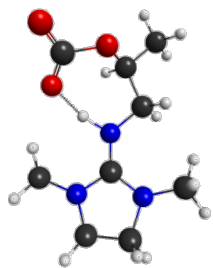
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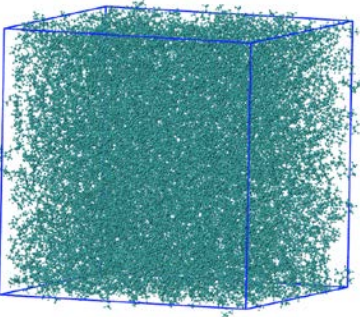
**IPADM-2-BOL**

| System (IPADM-2-BOL)   | Experimental viscosities (cP) | Calculated viscosities from MD (cP) |
|------------------------|-------------------------------|-------------------------------------|
| 0% mol CO <sub>2</sub> | 8                             | 15                                  |
| 15%mol CO <sub>2</sub> | 36                            | 35                                  |
| 25%mol CO <sub>2</sub> | 110                           | 150                                 |
| 50%mol CO <sub>2</sub> | ~3000                         | >1000                               |

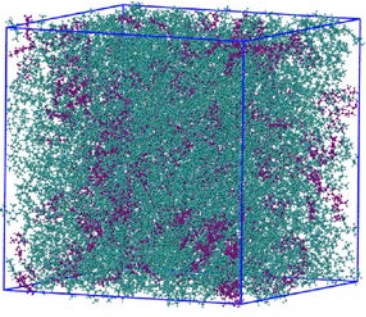


**CO<sub>2</sub>-loaded IPADM-2-BOL**

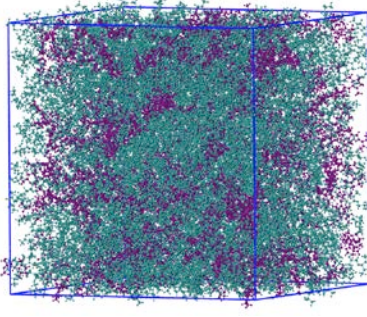
**IPADM-2-BOL (0% CO<sub>2</sub>)**



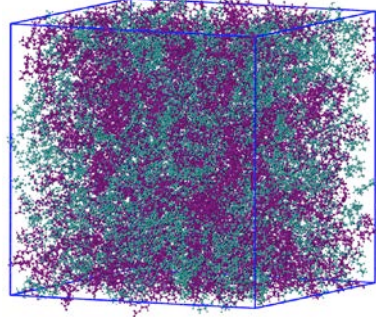
**IPADM-2-BOL (15% CO<sub>2</sub>)**



**IPADM-2-BOL (25% CO<sub>2</sub>)**



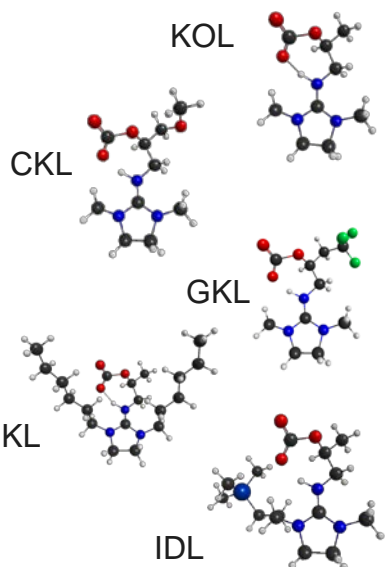
**IPADM-2-BOL (50% CO<sub>2</sub>)**



# Integration of Molecular Modeling and Molecular Design

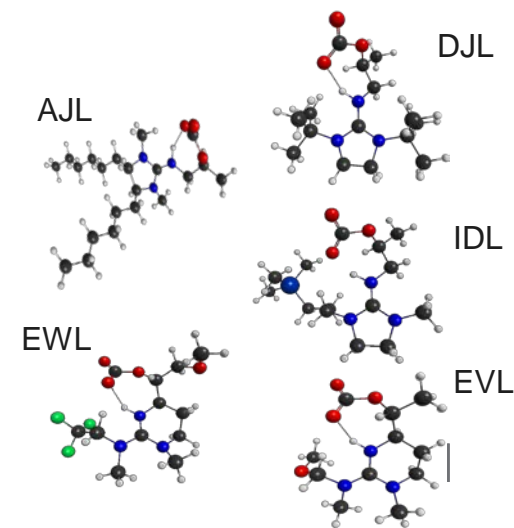
## Validation of model performance with experimental data

| Compound | Pint *<br>(Model predicted) | $\Delta\Delta E$ (kJ/mol)<br>(CO <sub>2</sub> BE) | $\eta$ MD | $\eta$ (cP) (25%)<br>Reduced | Exp        |
|----------|-----------------------------|---|-----------|------------------------------|------------|
| KOL      | 41%<br>(34% MD calculated)  | 0.0   | 150       | 110                          | 110        |
| CKL      | 40%<br>(52% MD calculated)  | 8.3   | 100       | 113                          | $\leq$ KOL |
| GKL      | 43%<br>(34% MD calculated)  | -5.6  | 100       | 104                          | N/A        |
| HKL      | 15%<br>(6% MD calculated)   | 21.9  | 250       | 234                          | N/A        |
| IDL      | 75%                         | 11.7  | N/A       | 35                           | < KOL      |



## Promising targets from validated reduced Model

| Compound | Pint *<br>(Model predicted) | $\Delta\Delta E$ (kJ/mol)<br>(CO <sub>2</sub> BE) | (cP)(25%)<br>Reduced model |
|----------|-----------------------------|---|----------------------------|
| DJL      | 87%                         | 0.8   | 18                         |
| AJL      | 79%                         | 16.2  | 30                         |
| IDL      | 75%                         | 11.7  | 35                         |
| EWL      | 75%                         | -8.2  | 37                         |
| EVL      | 69%                         | -4.1  | 46                         |



# Current Work: Experimental Validation

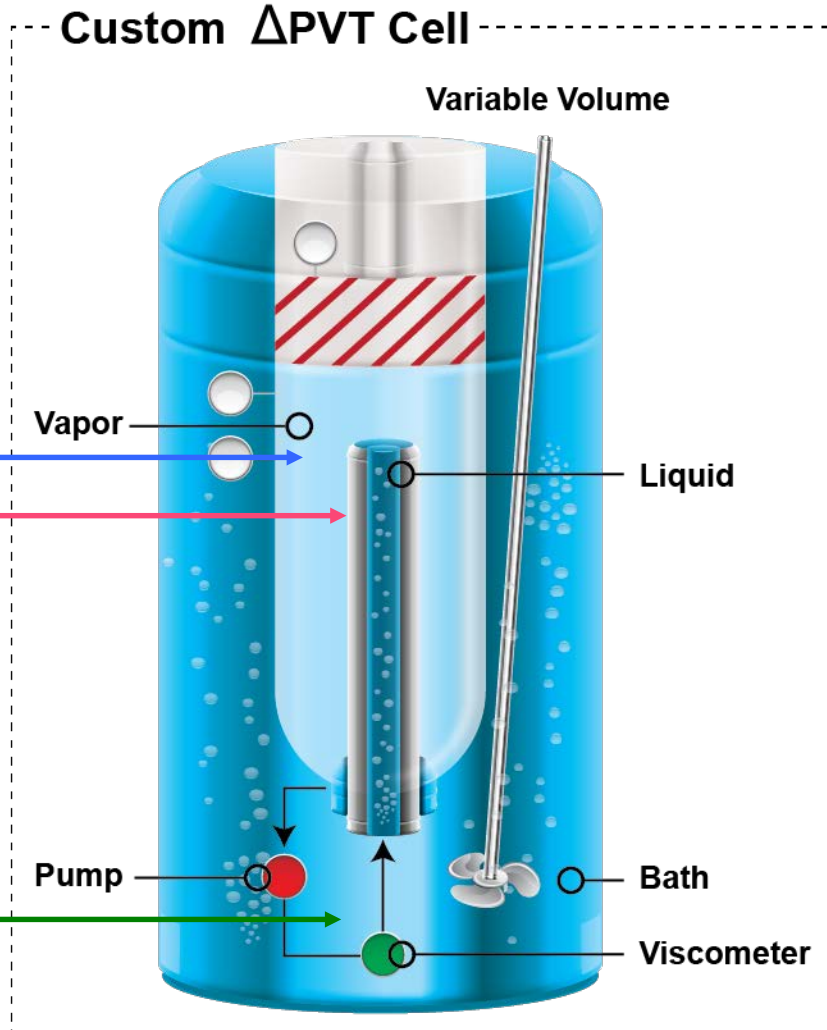


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## Comprehensive data collection equipment for liquid systems

- ▶ Scale-up 5-L synthesis reactor
- ▶ PTx cells (equilibria data)
- ▶ Wetted-wall column (kinetics)
- ▶ Viscometer (transport data)
- ▶ Continuous-flow liquid and sorbent carts (mobile capability for flue gas evaluations)



*Enables equilibrium, kinetic and viscosity measurements on only 20 mL of sample*

# Benefits of Technology to the Program



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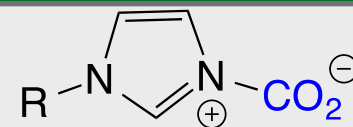
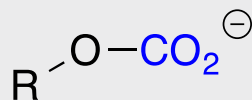
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- An approach that can impact a broad set of materials (solvents)
- Rapid modeling and testing of all CO<sub>2</sub> binding mechanisms
- Detailed understanding of molecular level interactions and how it impacts process performance

## Alkylcarbonate-Derived

## Carbamate-Derived

## Imidazole-Derived



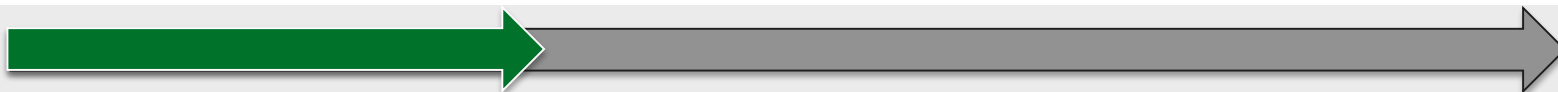
Property

(CO<sub>2</sub>BOLs)

(RILs, Aminosilicones,  
TSILs, Phase-Change)

(imidazole, carbene)

Internal H-Bonding



Molecular Stacking



Steric Crowding



Optimized Thermo-chemistry



**KEY**

Current Work

Projected Translation

# Acknowledgements

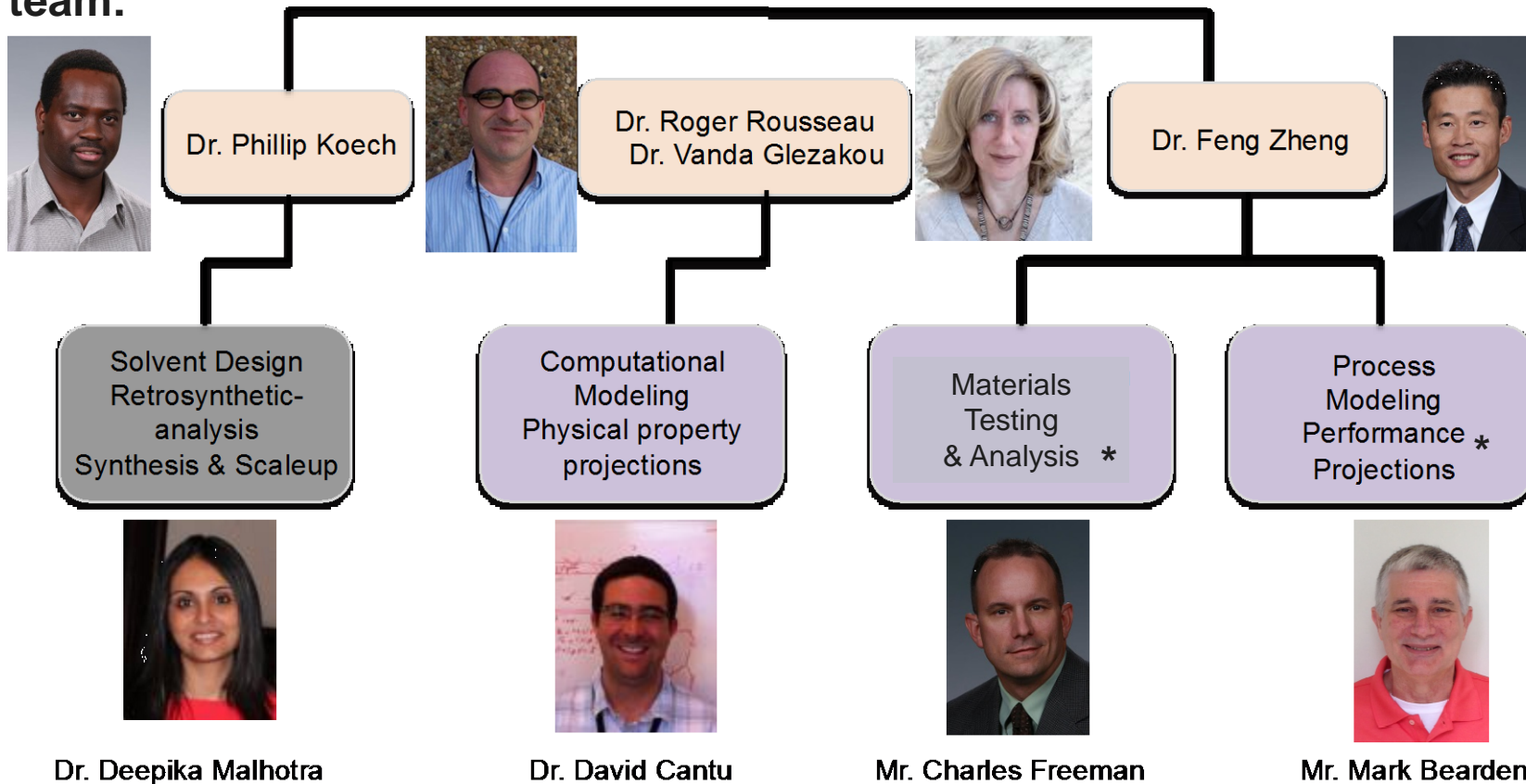


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- ▶ **Funding:** US Department of Energy Office of Fossil Energy
- ▶ **FWP 65872, PM Andy Aurelio**

## PNNL team:



## Collaboration:



\*Advisory process engineering,  
thermodynamics:  
Dr. Paul M. Mathias



Mr. Abhoyjit Bhowan



Dr. Josh Stohlaroff,  
Dr. John Vericella



Prof. Aaron Esser-Kahn