

Pressurized Testing of Solid Oxide Fuel Cells

**16th Annual Solid Oxide Fuel Cell
(SOFC) Workshop**

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**Naval Undersea Warfare Center
Division Newport**

The Naval Undersea Warfare Center is the United States Navy's full-spectrum research, development, test and evaluation, engineering, and fleet support center for submarines, **autonomous underwater systems**, and offensive and defensive weapon systems associated with Undersea Warfare. (SECNAVINST)

A Navy Core Equity – A National Asset

- **Introduction**
- **Unmanned Undersea Vehicles (UUVs)**
- **Why Pressurized Operation?**
- **Test Facilities**
 - **Pressure Vessel (PV)**
 - **SOFC Test Stand**
- **Stack Test Results**
 - **Ambient**
 - **Pressure**
- **Summary**

- **The Navy has a need for air-independent advanced electric power sources with high energy storage that will replace batteries in unmanned undersea vehicles (UUV) applications**
- **A typical UUV power source will consist of a planar SOFC stack(s), fuel processor, carbon dioxide scrubber, BoP components and fuel / oxidant storage vessels.**
- **SOFCs offer several distinct advantages over battery technology**
 - **Greater specific energy**
 - **Ability to utilize energy-dense fuels**
 - **Self-sustaining operation**
 - **“Gas and go” capability allows UUV to be quickly re-deployed**
- **Although planar SOFC stacks have demonstrated the highest efficiency and power density, concerns remain regarding their robustness, gas leakage, and long-term seal durability**
- **Pressurized operation should help mitigate these issues**



EMATT



MK30 MOD 2



MK30 MOD 1



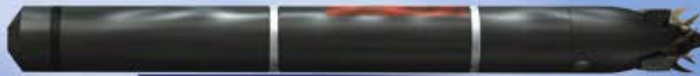
REMUS



MARV



2100V



NMRS



MRUUV FLT1



LMRS



MRUUV FLT2



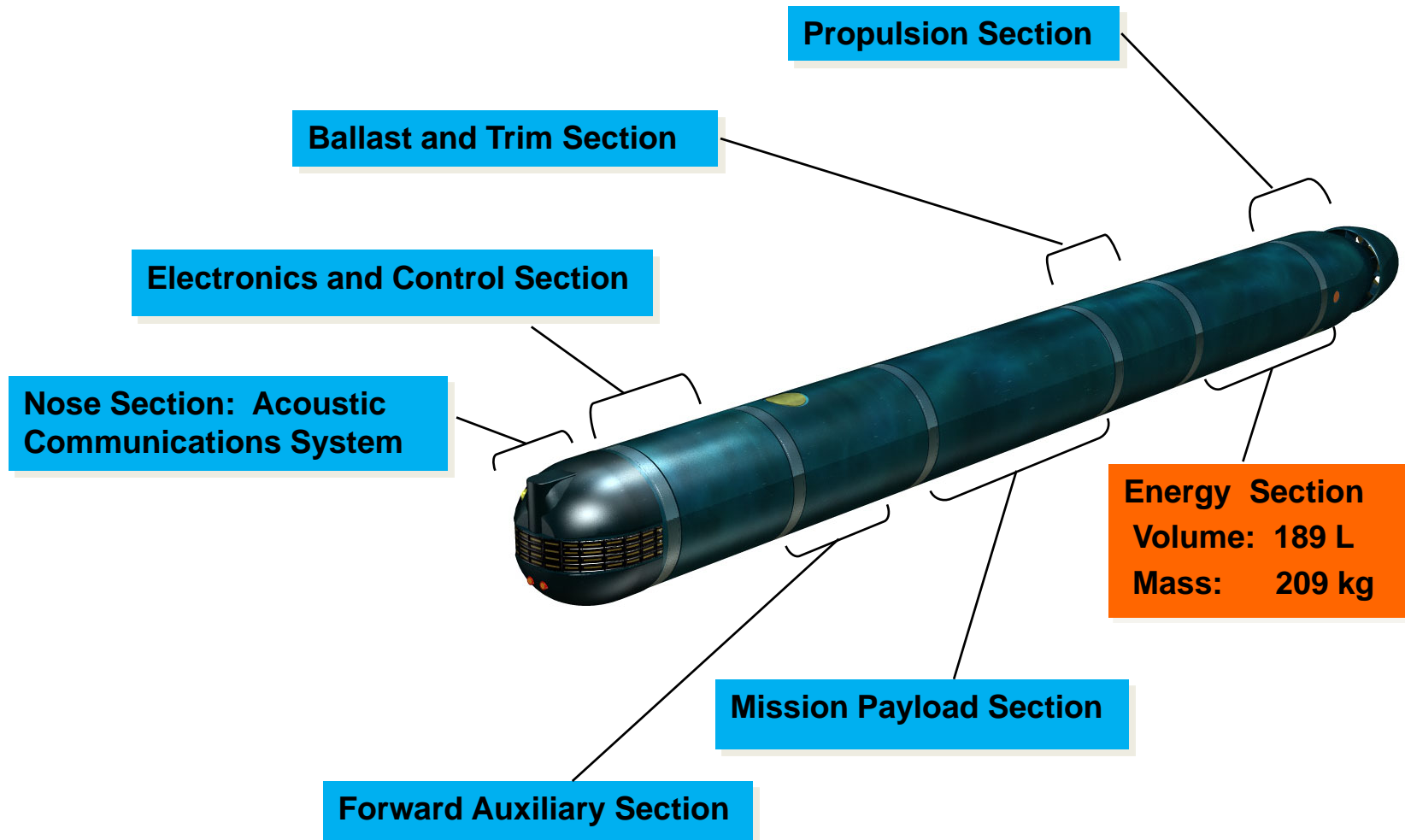
MTV



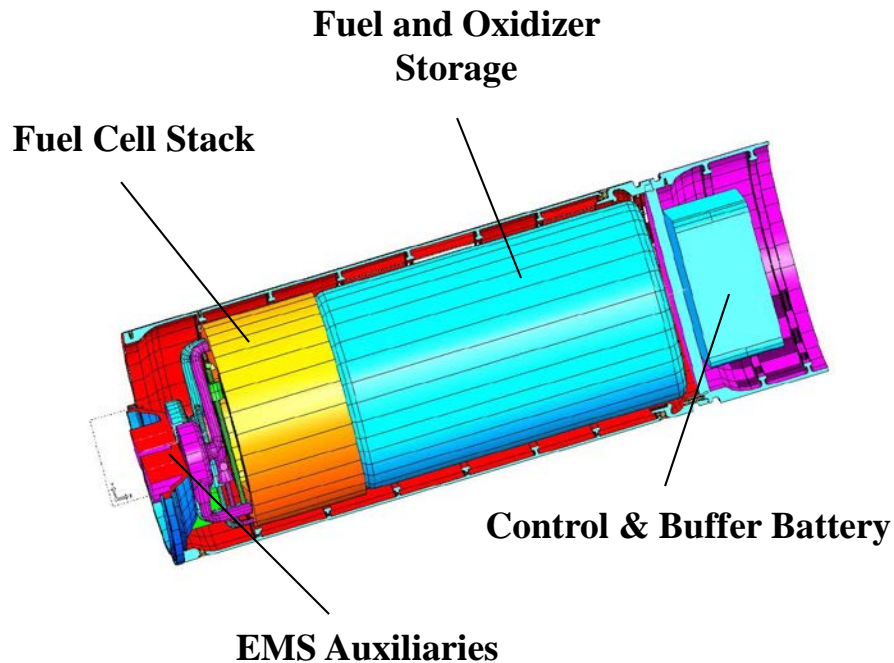
MANTA

Autonomous Undersea Vehicles

Conceptual 21-inch Diameter UUV



UUV Energy Section with Fuel Cell



Potential Benefits:

- Longer UUV missions as a result of higher energy density
- Reduced down time between missions
- Decreased cost and increased safety versus lithium batteries
- Use of hydrocarbon fuels or even biodiesel

Fuel

- Hydrogen
 - compressed gas
 - cryogenic liquid
- Hydrocarbons
 - light ($C_1 - C_4$)
 - liquid (JP-8, diesel)
- Hydrogen-containing cpds
 - $LiAlH_4$
 - $NaBH_4$
 - Mg_2Ni (intermetallic)

Oxidizer*

- Oxygen
 - compressed gas
 - cryogenic liquid
- Hydrogen peroxide (H_2O_2)
- Oxygen-containing cpds
 - $KClO_4$
 - MnO_2

*** Air-independent operation**

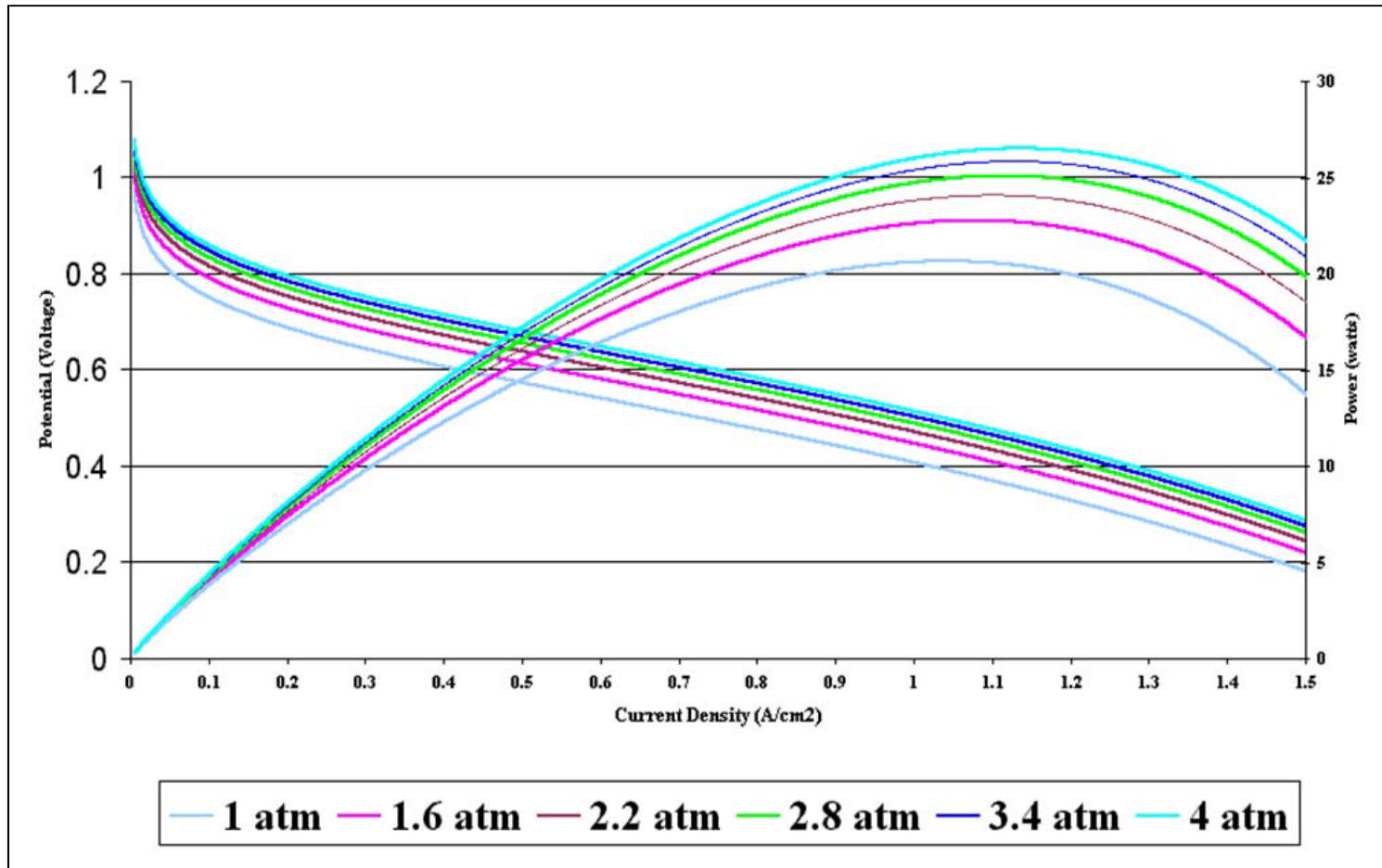
Why Pressurization?

Increase system performance, reduce SOFC losses

- SOFC voltage increases at higher pressures $E = E_0 + \frac{RT}{nF} \ln \left(\frac{p_{H_2} p_{O_2}^{1/2}}{p_{H_2O}} \right)$
- Stack efficiency enhanced by ~ 3%, due primarily to Nernstian and kinetic effects
- System efficiency associated with system level energy storage improves an estimated 7%
 - Lower parasitic power losses for recycling fuel and oxidant streams
 - Carbon dioxide sequestration is facilitated
 - Reduced plumbing requirements (e.g. circulation pump for anode recycle)
- Seal integrity maintained
 - High differential pressures between anode and cathode or process gas and atmosphere can cause seal between cells to fail.
 - Balance external stack pressure with process gas pressure to minimize driving force for gas leakage.

Enhanced efficiency increases system reliability and mission duration

Increased Performance



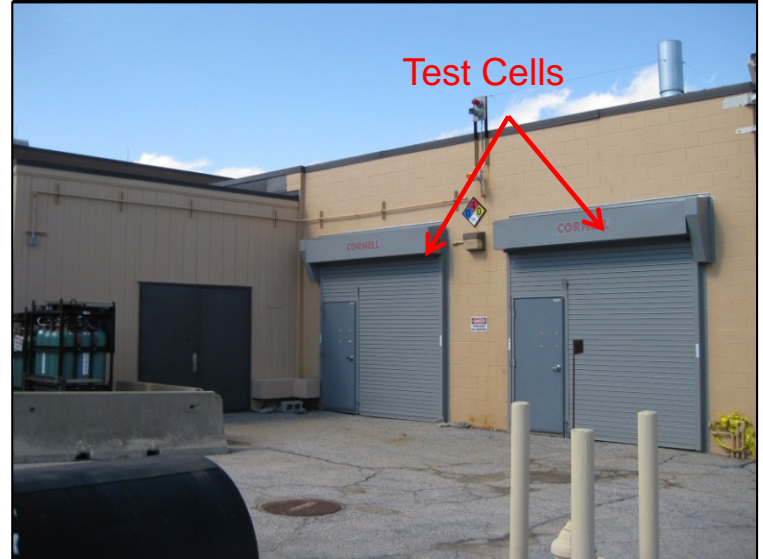
Goals

- Evaluate SECA-sponsored SOFC stacks at elevated pressure
- Construct test stand for pressurized testing of planar stacks
- Operate at elevated pressure to increase system performance and stack reliability
 - Implement algorithms for automated regulation of temperature and pressure set point tracking
 - Control three zones (anode, cathode and ambient (pressure vessel) in order to minimize pressure differentials across stack components

Test Objectives

- Establish performance of SOFC stack at ambient pressure
- Demonstrate enhanced performance at elevated pressure with air
 - Examine effects of pressure (up to 45 psia) on voltage and efficiency
 - Monitor any gas leakage as a function of operating pressure
- Extend pressurized testing to include oxygen as the oxidant

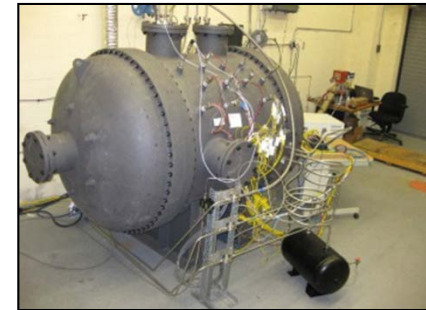
- **Air Independent Propulsion (AIP) test facility at NUWCDIVNPT for long duration testing of electrical energy sections for UUVs**
 - High and low temperature fuel cells
 - Pressurized fuel cell testing
 - Motors/Power electronics
 - Engines/Power systems (Stirling)
 - Reactant delivery systems



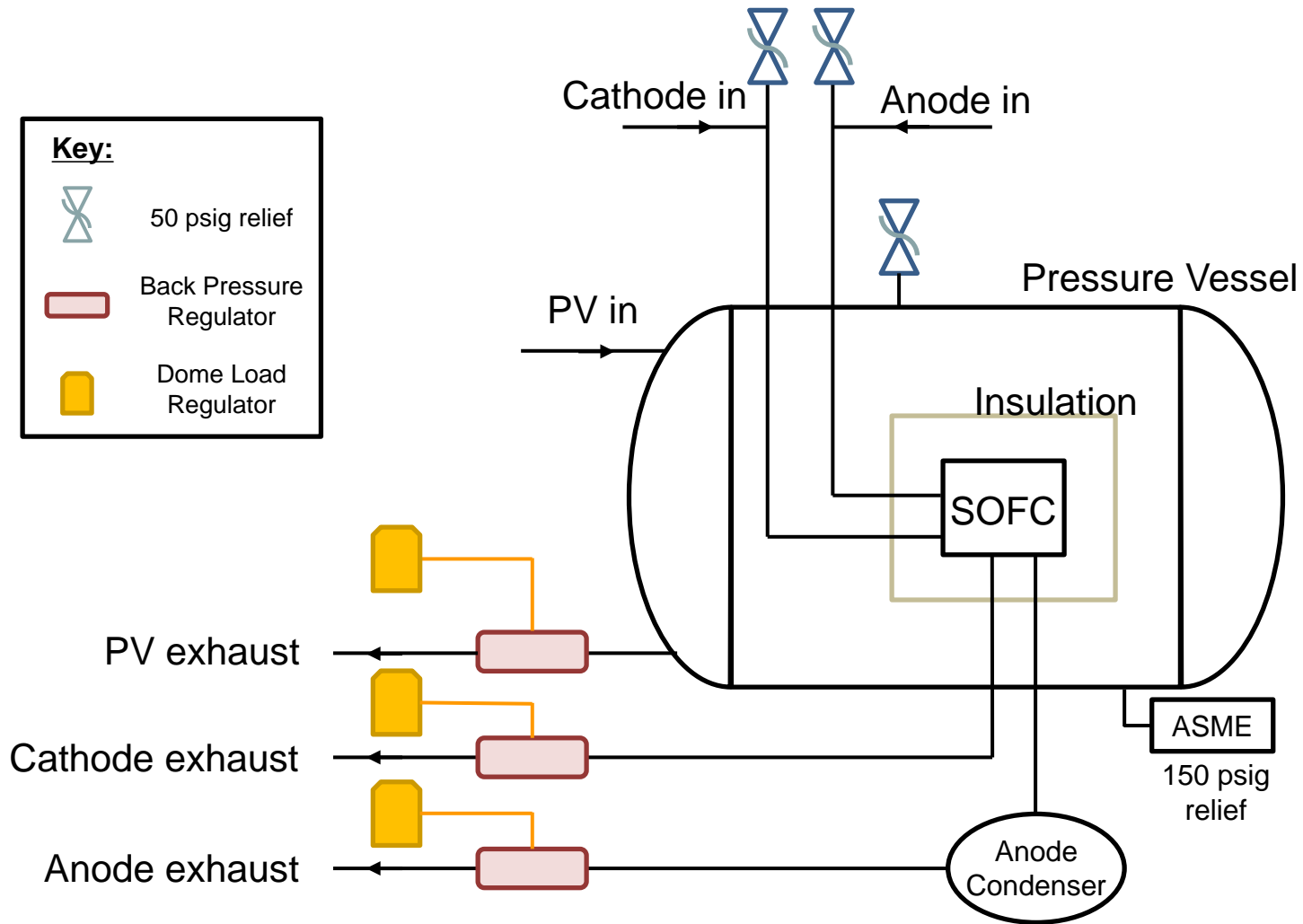
Remote operation from central control room

Pressure Vessel

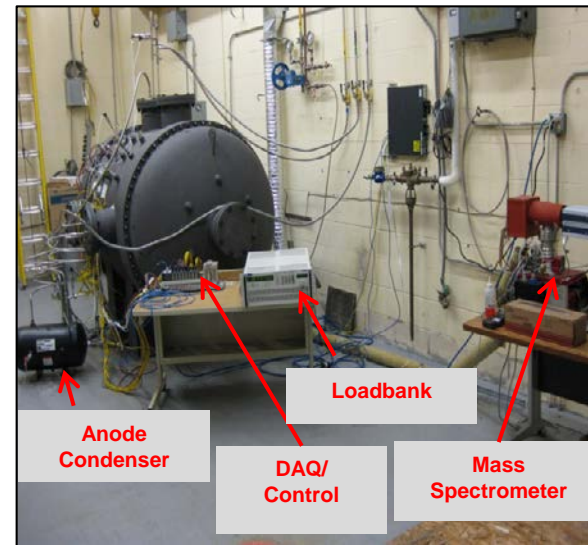
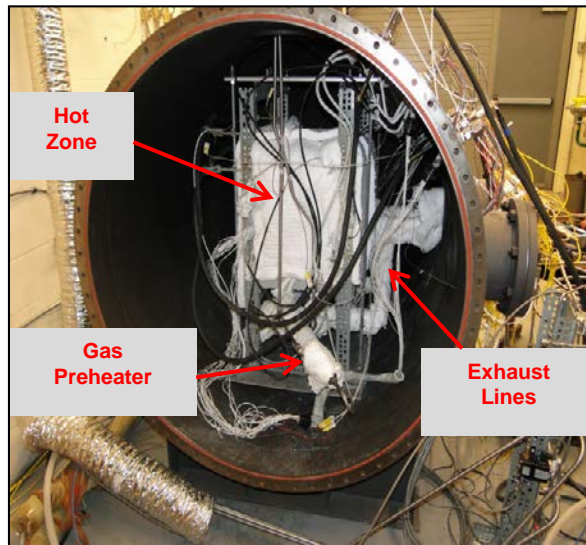
- Carbon steel pressure vessel (50-in ID) rated to 150 psig at 250°C
- ASME-rated relief valve (0.5-in ID)
 - Protects integrity of the pressure vessel (PV)
 - Will not re-close once it has opened
- Supplemental relief valves (0.25-in ID)
 - Installed on anode inlet, cathode inlet and PV
 - Pre-set for each specific test to prevent over-pressurization
- Equilibar® back pressure regulators
 - Installed on the exhaust of each pressurized zone (anode, cathode and PV)
 - Automatically open in case of abort condition or power loss
- Gas flow
 - Capacity up to 700 SLPM total flow in
 - Gas composition sampled via mass spectrometer (MS)
- Temperature monitored in process lines and pressure vessel



Pressure Vessel Schematic

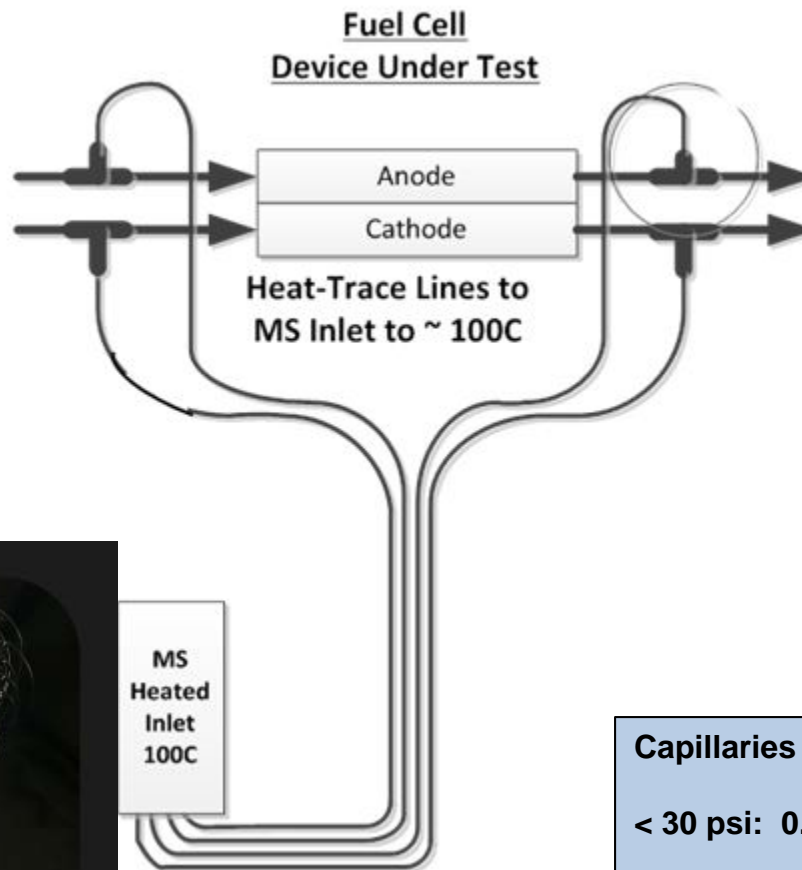


Pressurized SOFC Test Stand



- **50" ID carbon steel pressure vessel rated to 150 psig at 250°C**
- **Hot box consisting of four heating elements constructed around stack**
- **Inline heaters for preheating anode and cathode reactant gases**
- **Gas sampling at 7 locations via mass spectrometer**
- **Voltage monitoring of individual cells**

Mass Spectrometer Sampling



- Capillary sampling lines:**
- anode in
 - anode out
 - cathode in
 - cathode out
 - pressure vessel

Gas sampling of up to 7 locations is possible

- Capillaries for processes:**
- < 30 psi: 0.010" ID x 1/16" OD
 - 30 psi < P < 50 psi: 0.007" ID x 1/16" OD

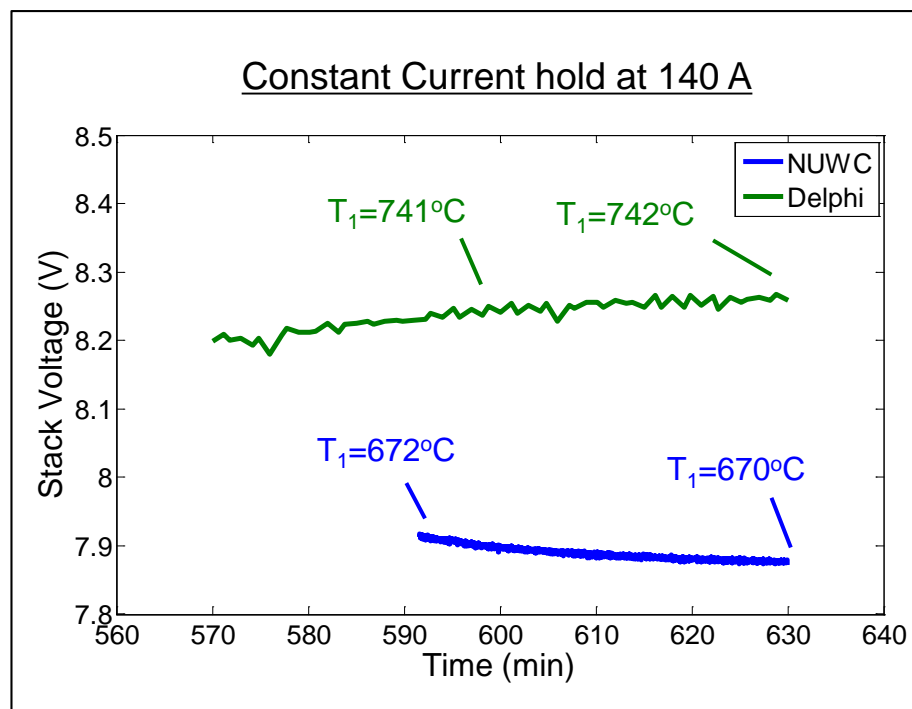


- Number of cells: 10
- Individual cell area: 403 cm²
- Stack Assembly
 - Laser-welded cassette
 - Glass ceramic seals
 - Stainless steel manifold
 - Co-flow gas design
- Test conditions
 - Gases:

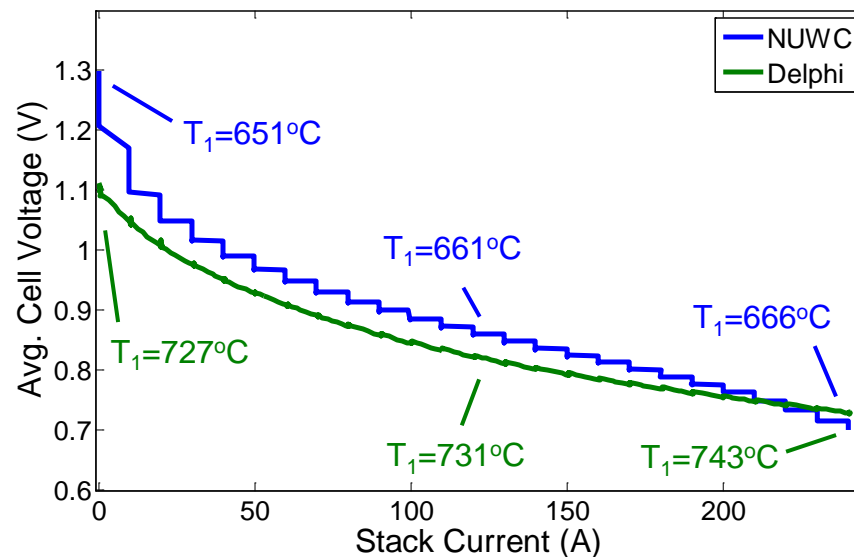
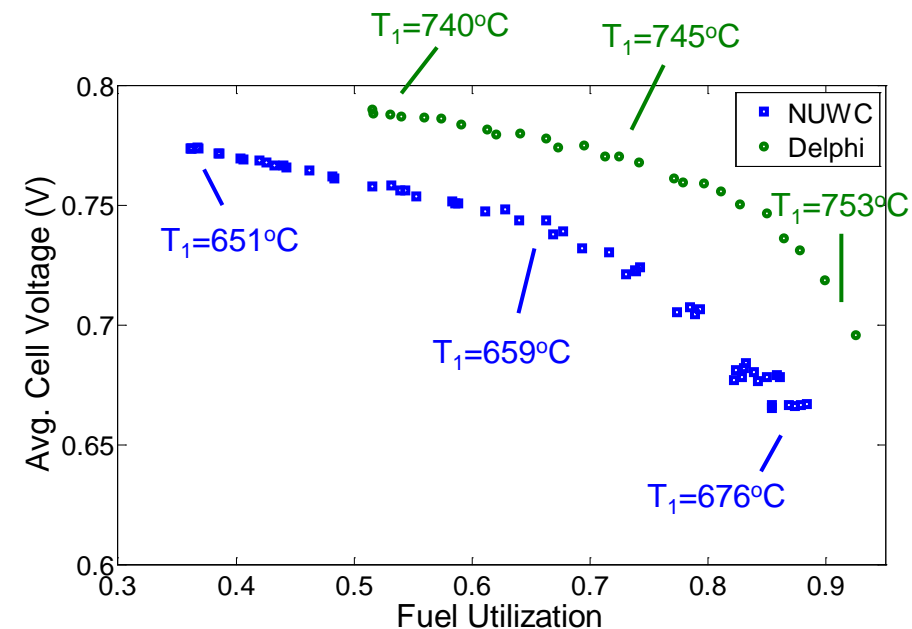
<u>Anode</u>	$x_{H_2} = 0.5, x_{N_2} = 0.5$ (dry)
<u>Cathode</u>	air / oxygen
 - Pressure: 1 to 3 atm
- Power output : 1.75 kW (240 A, 7.3 V) at 50% fuel utilization at 700°C with all zones at 45 psia



- Tests performed by Delphi prior to stack delivery and data provided to NUWC
 - Constant Current hold
 - Fuel utilization sweep
 - Polarization curve
- NUWC started operations by ramping current to 240 A, reaching an operating power level of 1.7 kW
- Current lowered and held at 140 A
- Stack temperature limited by inlet gas preheating
 - Lower air flows used to keep higher inlet gas temperatures
 - Lower stack temperature while under a load resulted in lower voltage
 - Stack temperature largely dependent on internal heat generation from load

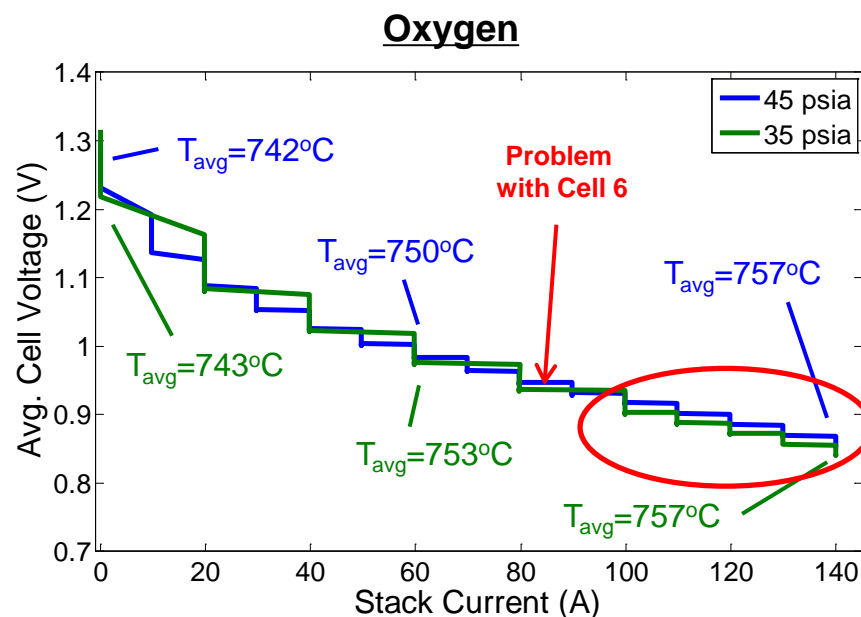
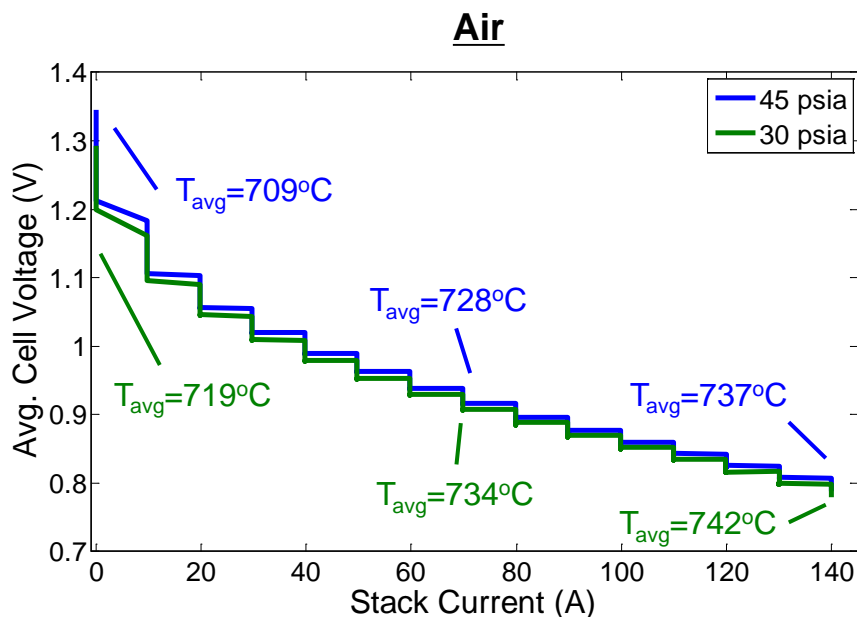


Ambient Test Results



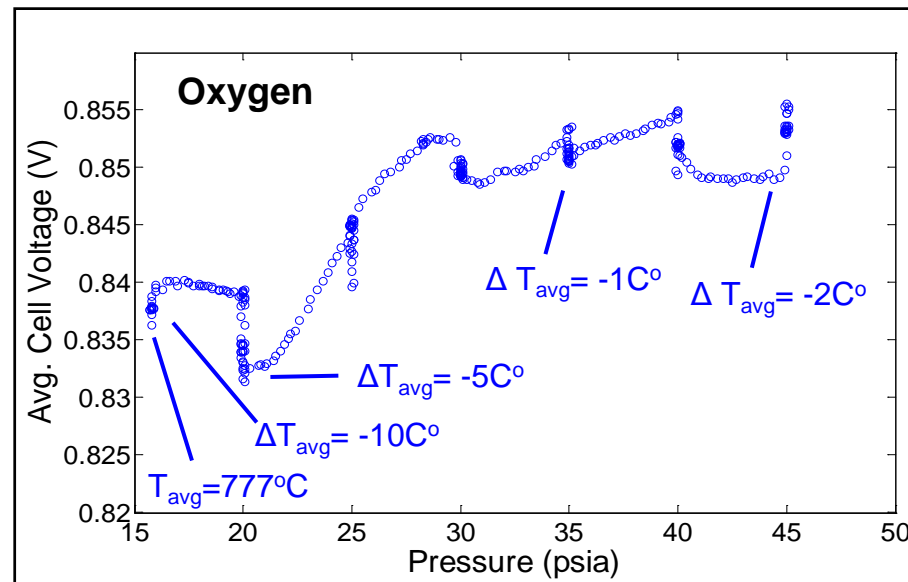
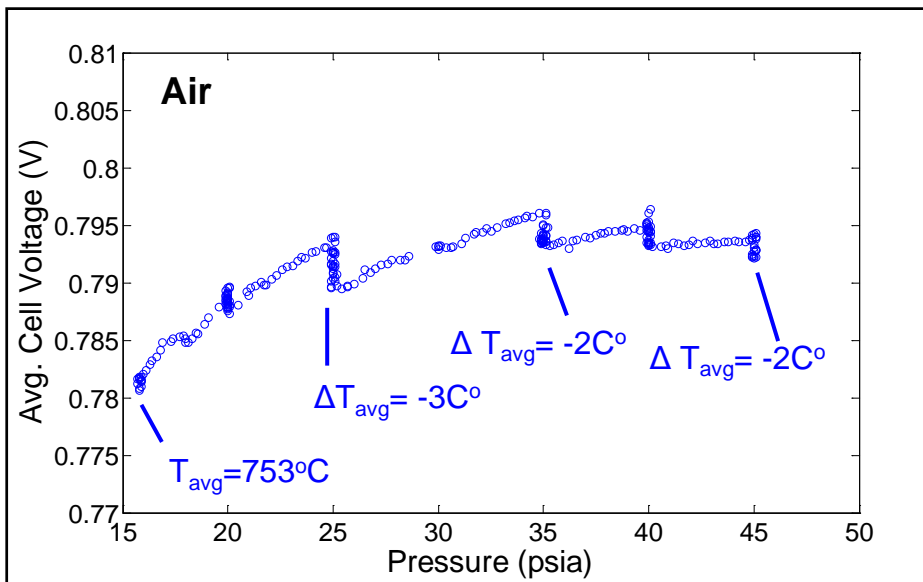
- **50% H₂: 50% N₂ flow lowered under constant 180 A load and constant air flow**
 - Results were comparable with offset due to lower operating temperature
 - Lower flow resulted in increase fuel utilization and stack heating
- **Polarization curve collected from 240 A decreasing 10 A per 30 sec**
 - Temperature change is inherent in SOFC polarization, but larger changes than expected were due to lower inlet temperature and flows

Pressurized Test Results



- Pressurized polarization curves collected after pressurization to 45 psia while held at 140 A and constant fuel and oxidant flows
- Higher pressure resulted in higher voltage (efficiency), even with a lower stack temperatures
- Temperature decreased with increase in pressure due to increase in gas density and specific heat, resulting in an increased cooling effect from the reactant gases

Pressurized Test Results



P (psia)	15-20	20-25	25-30	30-35	35-40	40-45	Total
$\Delta \epsilon$ (%)	0.64	0.48	0.16	0.16	0.16	0.08	1.68

P (psia)	15-20	20-25	25-30	30-35	35-40	40-45	Total
$\Delta \epsilon$ (%)	0.136	0.984	0.328	0.336	0.32	0.288	2.392

- **Constant current steady state operation**
 - 140 A load, constant gas flows
 - Pressurized at 0.5 psi / min
- Increase in voltage even with continuous decrease in stack temperature as pressure was increased (pre-heating of reactant gases insufficient)
- 30 minute hold every 5 psi resulted in further cooling and decrease in voltage
- Largest efficiency gains over first 10 psi increase, higher gain for oxygen

- **Delphi Gen IV 10-cell stack was tested at pressures up to 45 psia with both air and pure oxygen**
- **Efficiency gain of 2.4% and 1.7% demonstrated at 45 psia for oxygen and air, respectively**
- **Combined efficiency gain of almost 6% was observed for oxygen at 45 psia vs. air at 15 psia**
- **Limitations reaching and maintaining stack temperature due to insufficient capacity of inline gas heaters**
- **Fuel cell technology has the potential to greatly increase endurance of UUV missions over current battery technologies**
- **A minimum of 10-15 thermal cycles will make SOFCs economically competitive with Li-based battery systems**

Acknowledgements

National Energy Technology Laboratory (NETL)

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Efficiency = f (i, T, P, utilizations, reactant feeds, stack materials; significant increase in performance occurs at 3 to 4 atm

Relative Efficiency Gain

- Calculated by comparing operating voltage at elevated pressure vs. ambient pressure
- Difficult to make comparisons of stacks with different designs and operating conditions

Absolute Efficiency Gain

- Voltage gain vs. total fuel value entering the system
- Equate voltage to Lower Heating Value (LHV) of hydrogen (-241.8 kJ/mol)

$$E_{\text{LHV}} = -\Delta H_{\text{LHV}} / nF = 1.25 \text{ V}$$

- Gross SOFC efficiency (ε) with reference to LHV (H_2)

$$\varepsilon = V_{\text{cell}} / 1.25 \text{ V} * 100\%$$

- Absolute efficiency gain ($\Delta\varepsilon$)

$$\Delta\varepsilon = \Delta V_{\text{cell}} / 1.25 \text{ V} * 100\%$$

where ΔV_{cell} is the pressure-induced voltage change