



DE-FE0031522: Advance Syngas Cleanup for Radically Engineered Modular Systems (REMS)

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Small-Scale Modularization of Gasification Technology Components for REMS – Objectives of the FOA

- DOE's Clean Coal Program is focused on developing advanced technologies that increase the performance, efficiency and availability of existing and new coal-fueled power generation
- Develop emerging gasification technologies that can be scaled down to modular small-scale (1-5 MW) via the Radically Engineered Modular Systems (REMS) concept
- Develop REMS process technologies that are cost effective relative to SOTA commercial technology, due to low cost fabrication via advanced manufacturing
- REMS-based combined heat and power or polygeneration system implemented in remote areas subjected to traditionally high energy costs

Project Objective: Develop modular sorbent-based warm syngas cleanup designs that will enable 1- to 5-MW REMS-based plants utilizing all of our abundant domestic coal reserves to be cost-competitive with large state-of-the-art commercial plants.

Project Objectives

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- Build on the extensive development work of RTI's Warm-gas Desulfurization Process (WDP)
- Study desulfurization performance of WDP sorbent for low-sulfur syngas streams
- Develop a fluid-bed regenerator for REMS application, especially with low-sulfur syngas
- Develop a fixed-bed sorbent and process for its inherent suitability for small-scale modularized systems
- Develop and optimize conceptual designs for desulfurization processes based on fluidized-bed and fixed-bed reactors

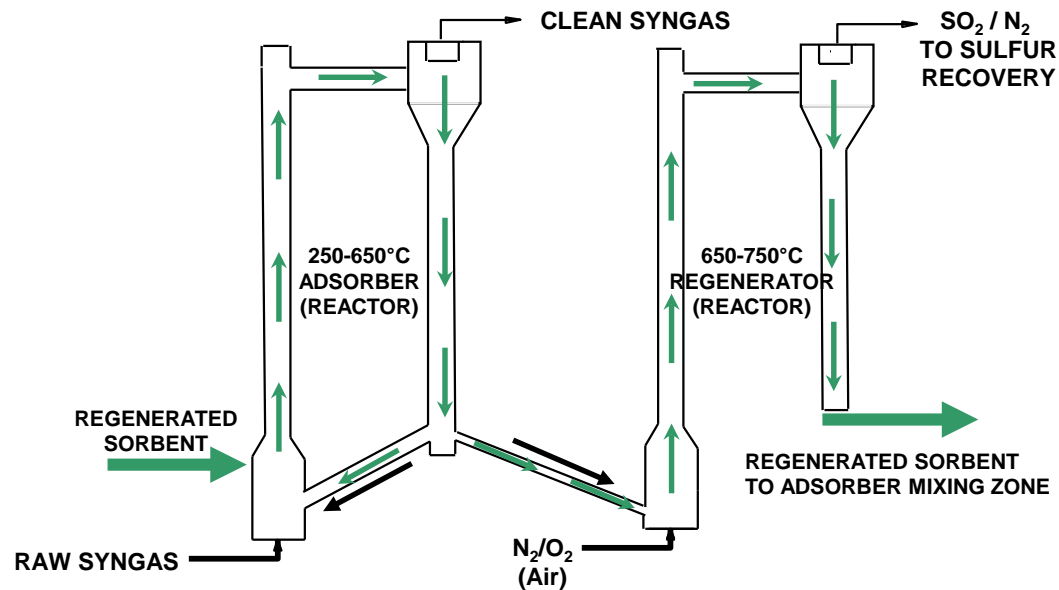
RTI Warm Gas Desulfurization Process (WDP) - Overview

Enables high removal of total sulfur ($\geq 99.9\%$) from syngas at temperatures as high as 650°C .

A unique process technology based on dual transport reactor loops (similar to FCC reactor designs)...



... and on a regenerable, high-capacity, rapid acting, attrition-resistant sorbent.



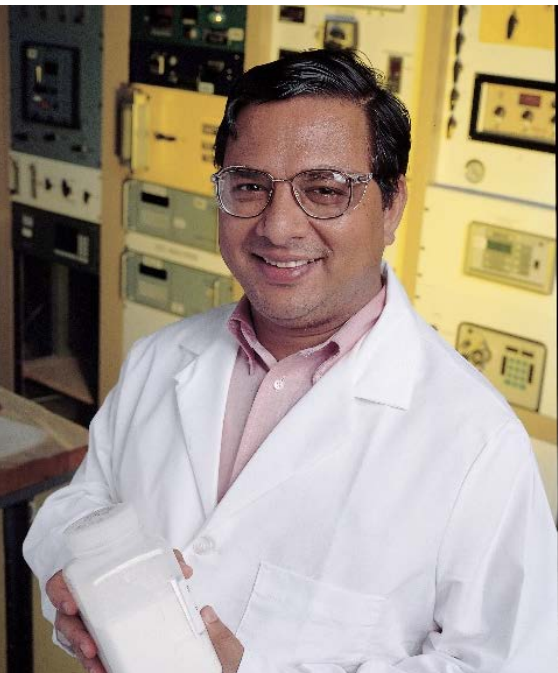
RTI Warm Gas Desulfurization Process (WDP)



RTI Proprietary Desulfurization Sorbent

- R&D 100 Award
- Unique highly-dispersed nanostructures
- Developed in long-term cooperation with Clariant (~100 tons to date)
- Covered by extensive US & International patents, including several recent improvements

Technology Development Timeline



**Invention
(2001)**



**Lab/Bench Testing
(2001-2003)**



**Pilot Testing
(2006-2008)**



**Demonstration at TECO, Tampa, FL
(2010-2016)**

WDP Potential to Address REMS FOA Objectives



How does this technology development apply to REMS & low-sulfur coals?

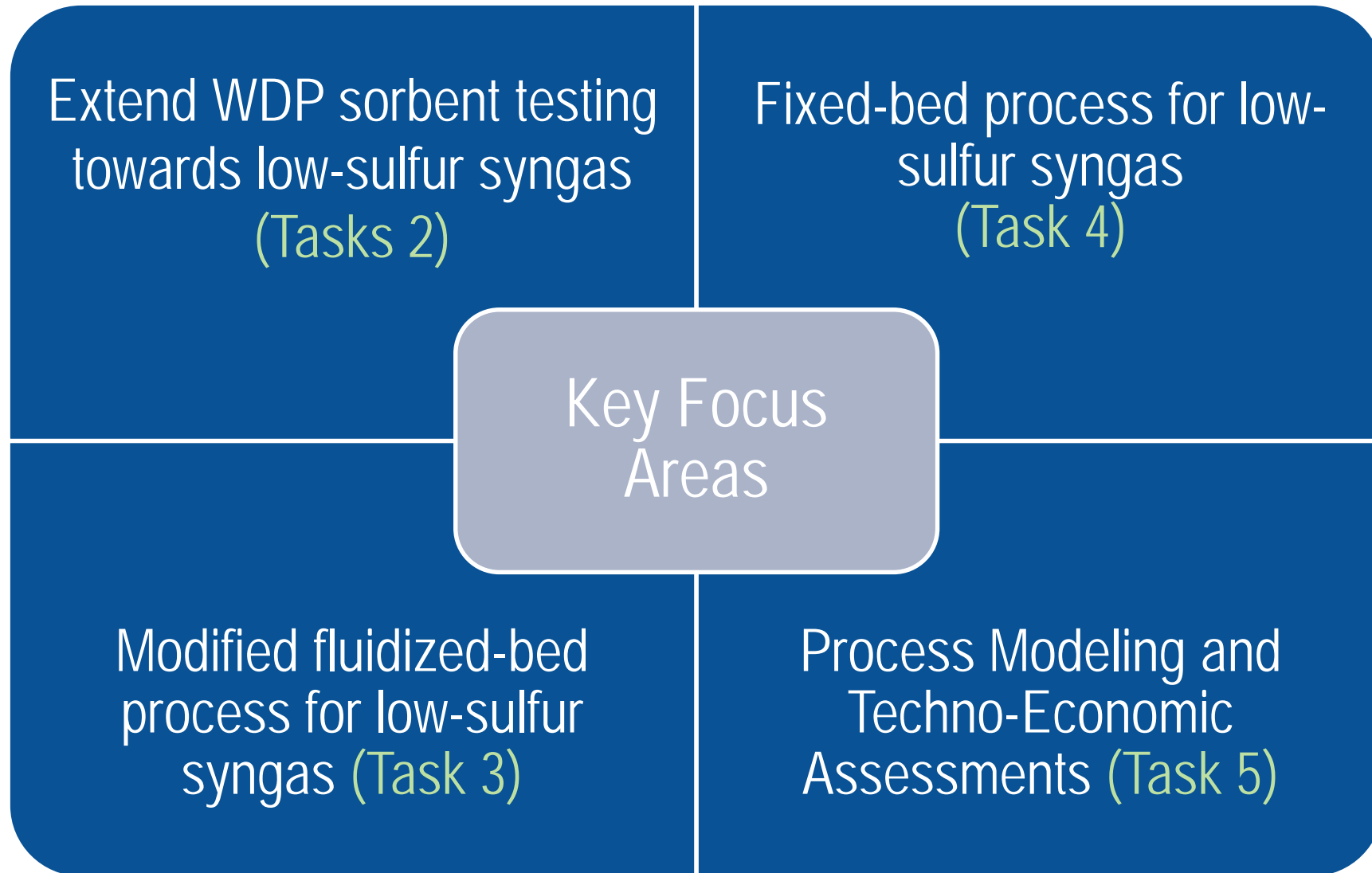
Key Strengths of WDP still apply

- Rapid reaction rates of desulfurization and regeneration
- Proven material chemistry and scale-up
- Fundamentally applicable to any sulfur concentration and pressure
- Modular design expected to reduce capital costs over other technologies
- Anticipate similar energy savings and GHG reductions as large-scale

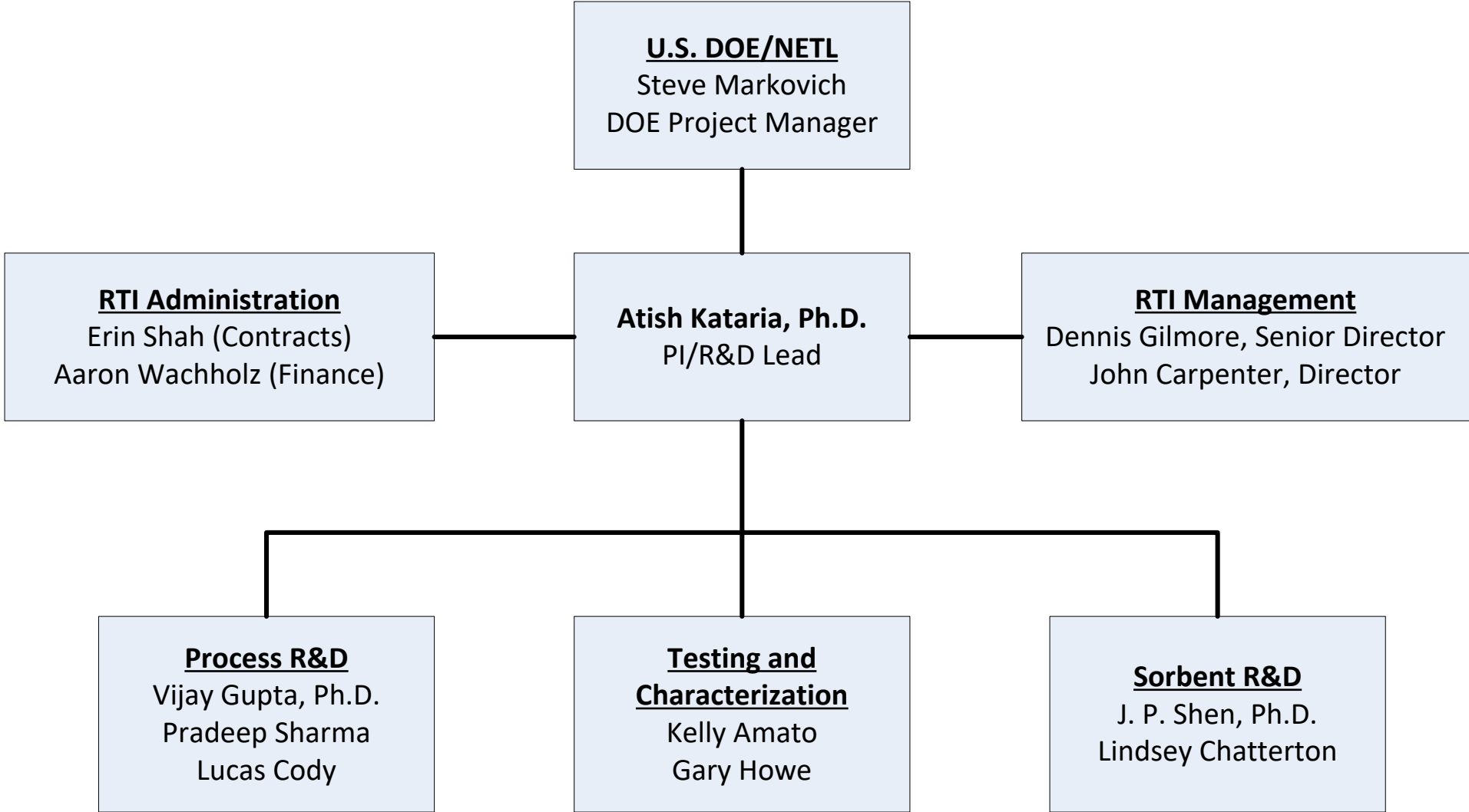
Knowledge gaps for application

- Expanded experimental data for low-sulfur syngas
- Identify modifications to the current process configurations to enable deployment of modular, cost-competitive cleanup systems
- Hydrodynamic data for fluid bed regenerator
- Processing steps to yield fixed-bed extrudate
- Performance of extrudates for fixed-bed
- Techno-economic assessment for REMS

Framework for Project



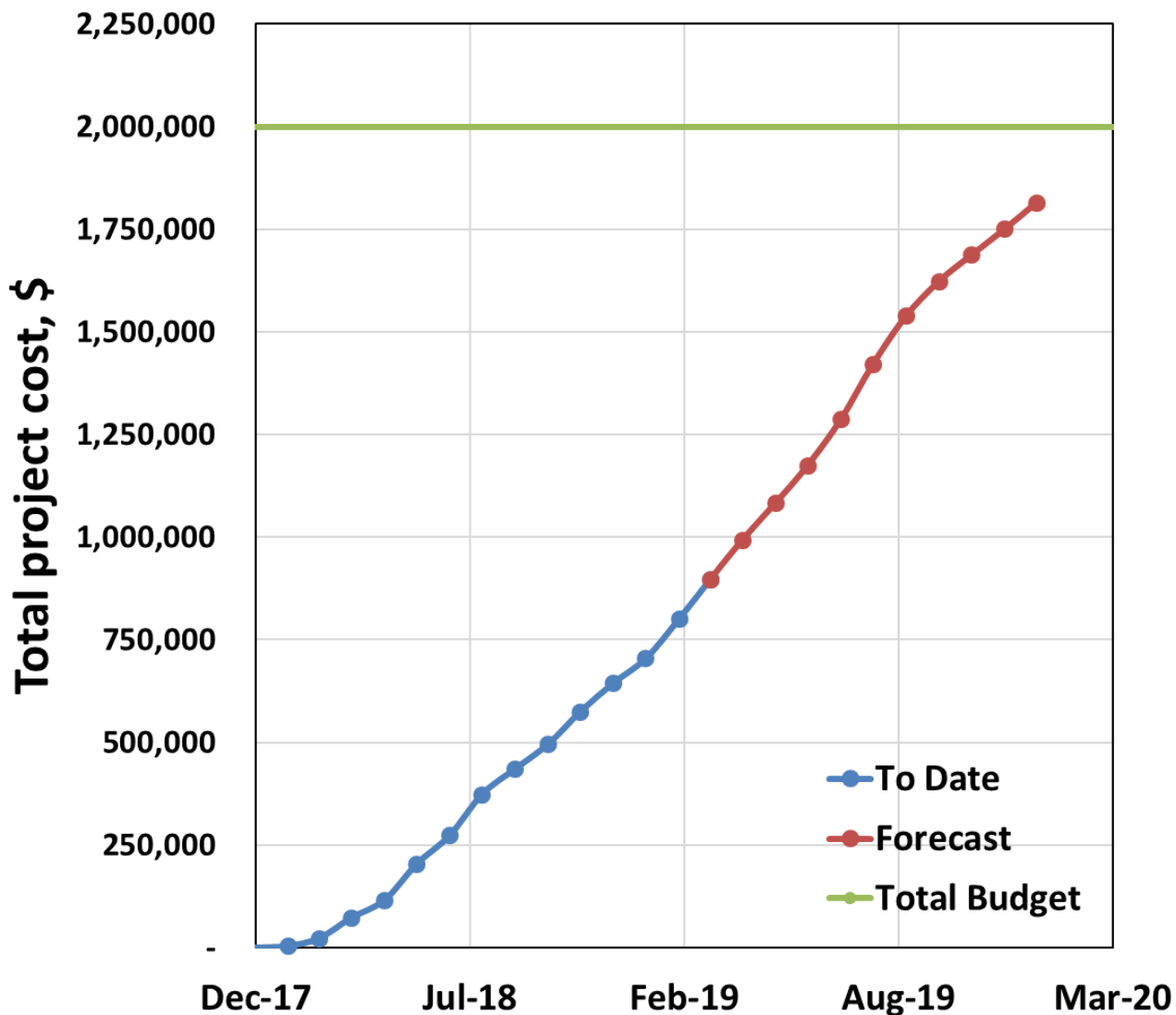
Task 1 – Project Management



Project Management Overview

- Project making good technical progress with all milestones on track
- All necessary resources available
- Project providing training opportunity to young engineers and chemists
- On track with all the technical and financial reporting requirements
- Made a presentation at the NETL Peer Review meeting in November 2018
 - Responded to Review Panel recommendations
 - Incorporated all four recommendations
- Investigating commercial interest in the fixed-bed process with varying sources for low sulfur

Project Budget Status and Forecast



Project Timeline

Task Name	Period of Performance																										
	J'8	F'8	M'8	A'8	M'8	J'8	J'8	A'8	S'8	O'8	N'8	D'8	J'9	F'9	M'9	A'9	M'9	J'9	J'9	A'9	S'9	O'9	N'9	D'9			
	Q1				Q2				Q3				Q4				Q5			Q6			Q7			Q8	
Task 1: Project Management	[Blue bar spanning all 24 months]																										
Task 2: Low-Sulfur Syngas Testing	[Orange bar from J'8 to D'8]																										
Task 3: Fluid-Bed Reactor Testing	[Blue bar from J'8 to J'9]																										
Subtask 3.1: Cold-flow testing	[Orange bar from J'8 to D'8]																										
Subtask 3.2: Pressurized and hot testing									[Blue bar from S'8 to J'9]																		
Subtask 3.3: Sulfur testing																				[Orange bar from J'9 to O'9]							
Task 4: Fixed-Bed Sorbent Development	[Blue bar spanning all 24 months]																										
Subtask 4.1: Sorbent production	[Orange bar in J'8]																										
Subtask 4.2: Sorbent development							[Blue bar from J'8 to J'9]																				
Subtask 4.3: Sorbent testing											[Orange bar from O'8 to O'9]																
Subtask 4.4: Extended multicycle testing																								[Blue bar in D'9]			
Task 5: Process Development	[Orange bar from J'8 to J'9]																										
Milestones	[Green diamond in J'8]				[Green diamond in A'8]					[Green diamond in J'8]	[Green diamond in A'8]													[Green diamond in O'9]	[Green diamond in N'9]	[Green diamond in D'9]	

Project Milestone Log

ID	Budget Period	Title	Completion Date	Actual Date
1	1	Submission of revised PMP to DOE	2/1/2018	2/16/2018
2	1	Pilot-scale sorbent wet cake delivered to RTI	4/30/2018	8/29/2018
3	1	Testing to generate a database for fluidized-bed sorbent desulfurization performance for low-sulfur syngas completed.	9/30/2018	9/30/2018
4	1	Hydrodynamic cold-flow testing supporting design of fluid-bed regenerator completed.	8/31/2018	9/5/2018
5	2	Demonstration testing of fluid-bed regenerator design at simulated operating conditions validating design for techno-economic analysis completed.	9/30/2019	-
6	2	Demonstration testing of fixed-bed sorbent and process at simulated operating conditions validating design for techno-economic analysis completed.	11/30/2019	-
7	2	Completion of techno-economic analyses for a full REMS plant incorporating fluid- and fixed-bed modular desulfurization systems, with goal of achieving a cost target of < \$90/MWh ¹ .	12/31/2019	-

¹ This value is based on values provided in DOE/NETL's "Cost and Performance Baseline for Fossil Energy Plant Volume 3a: Low Rank Coal to Electricity IGCC Cases (DOE/NETL2010/13990) which have been updated for 2016 costs.

Task 2.0: Low-Sulfur Testing

- Objective: Study desulfurization performance of WDP sorbent for low-sulfur syngas streams
- Commercially available fluidizable WDP sorbent was used for testing
- Testing performed in our existing Bench-Scale Fluidized-Bed Sorbent Testing System and atmospheric pressure TGA
- Parametric testing covered the typical operating conditions of temperature, pressure, syngas composition, and residence time
- Results validated the excellent performance of sorbent even under low-sulfur syngas conditions
- Task 2 and Milestone 3 completed

Atm-TGA and Bench-Scale Sorbent Testing System

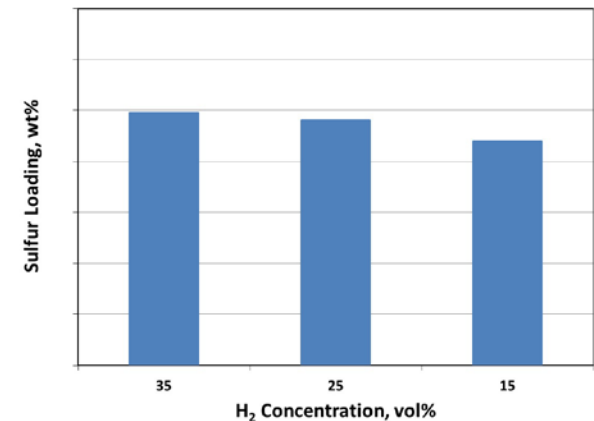
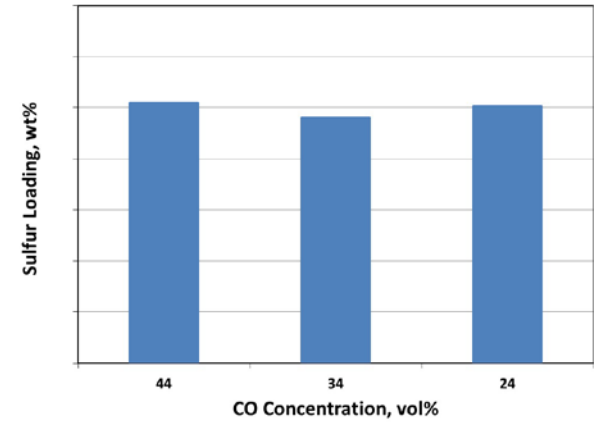
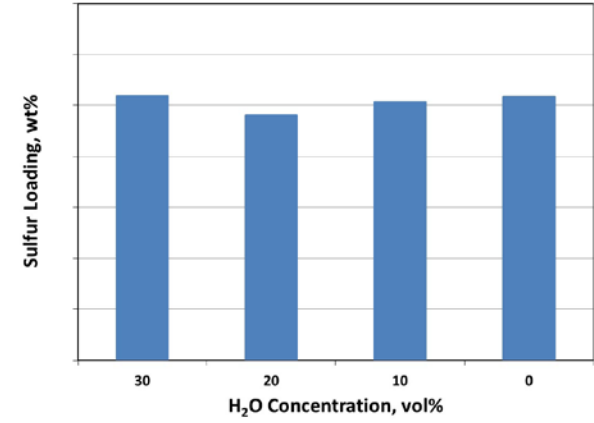
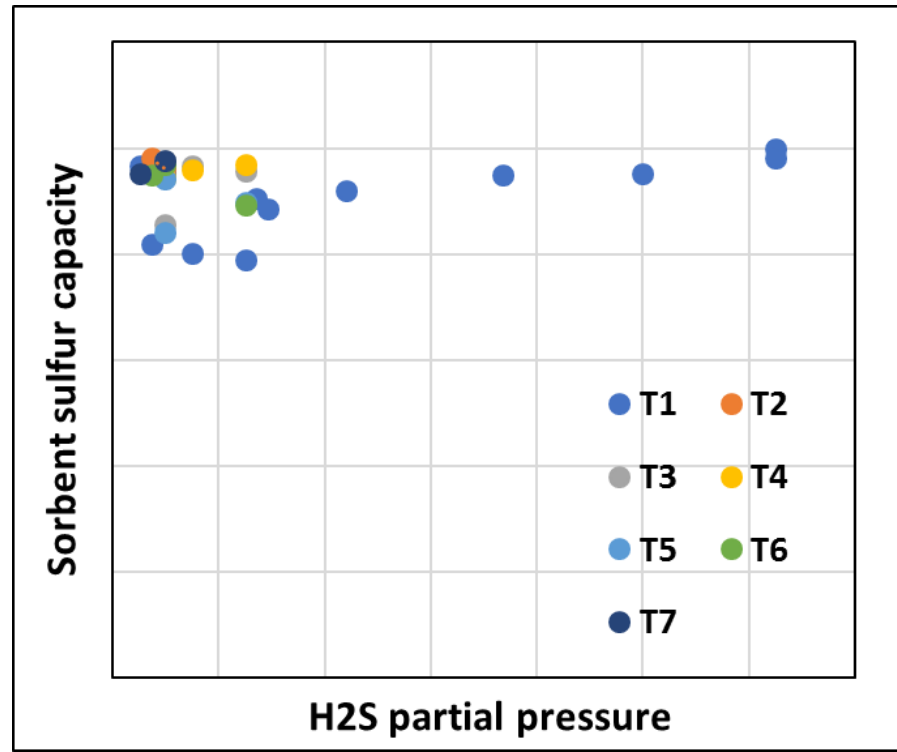
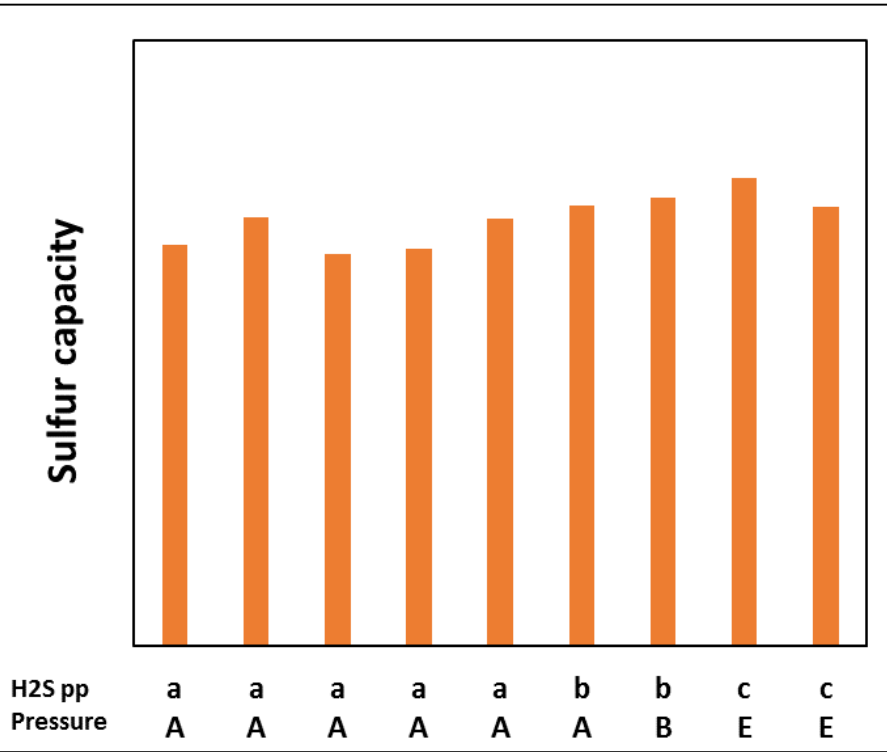


- Sorbent testing in simulated syngas and oxidation gases
- Operates at atmospheric pressure and up to 700°C
- Utilizes 5 to 20 mg of sorbent material
- Cross flow operation allows for kinetic measurements



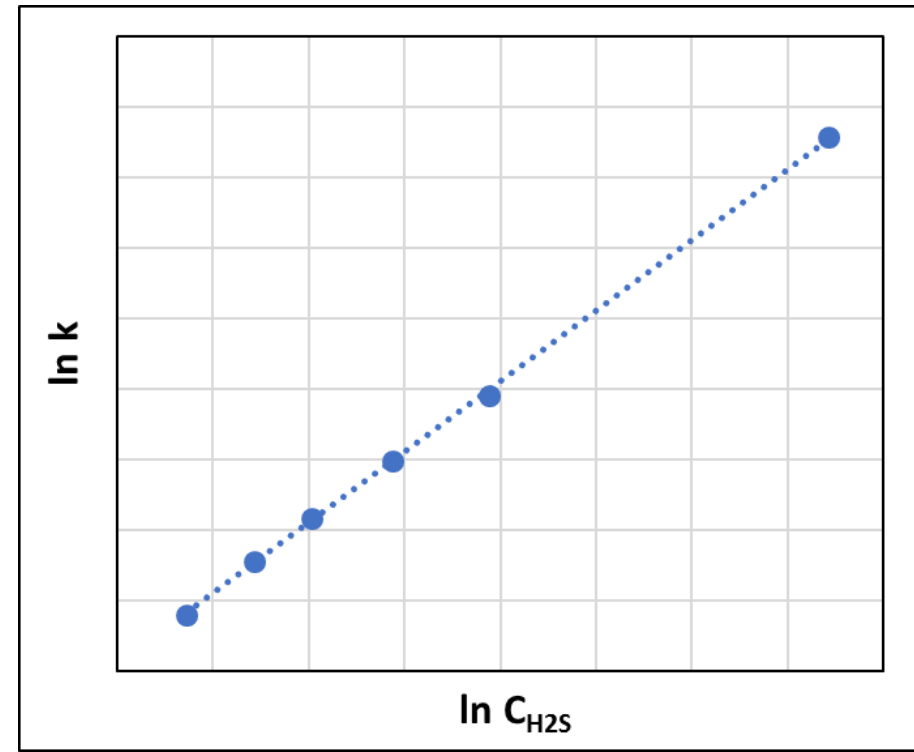
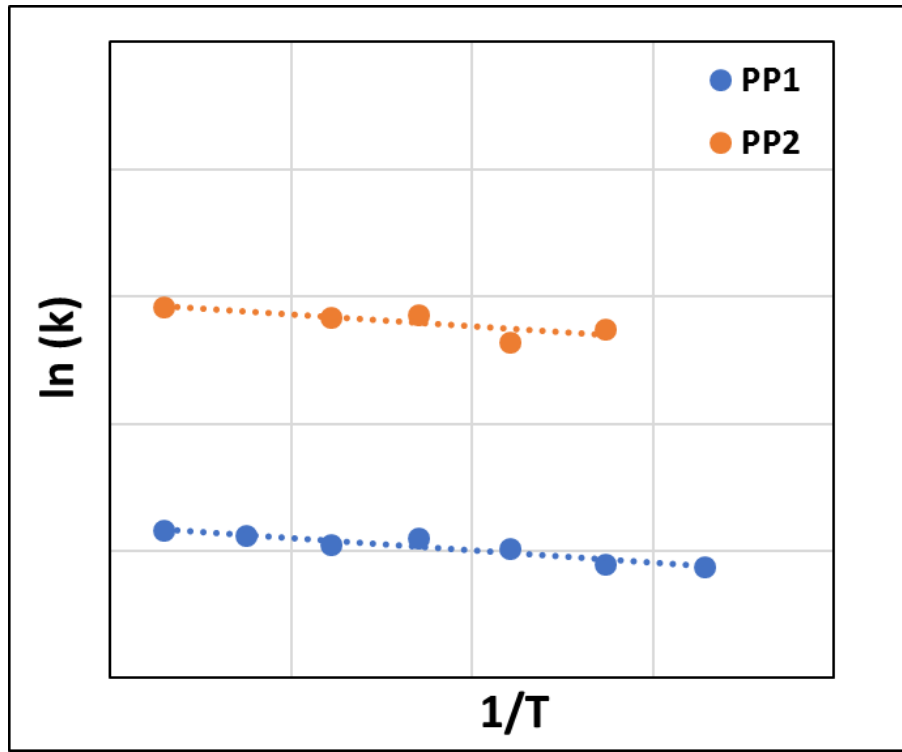
- Sorbent testing in simulated syngas and oxidation gases
- Operate up to 40 barg and 700°C
- Utilizes 100-300 g material
- Suspended quartz reactor inside stainless steel pressure vessel

Equilibrium Sorbent Sulfur Loading

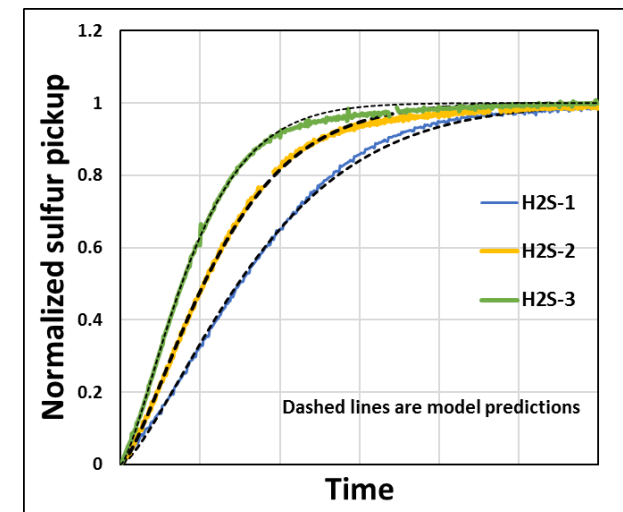


- Tested performance of fluidizable RTI-3 sorbent under varying operating conditions – temperature, pressure, H₂S concentration and syngas composition
- Generated the desired low-sulfur syngas sorbent performance database and quantified the variation in equilibrium sorbent capacity as a function of changing test conditions
- Sorbent remained stable over multiple cycles and varying test conditions

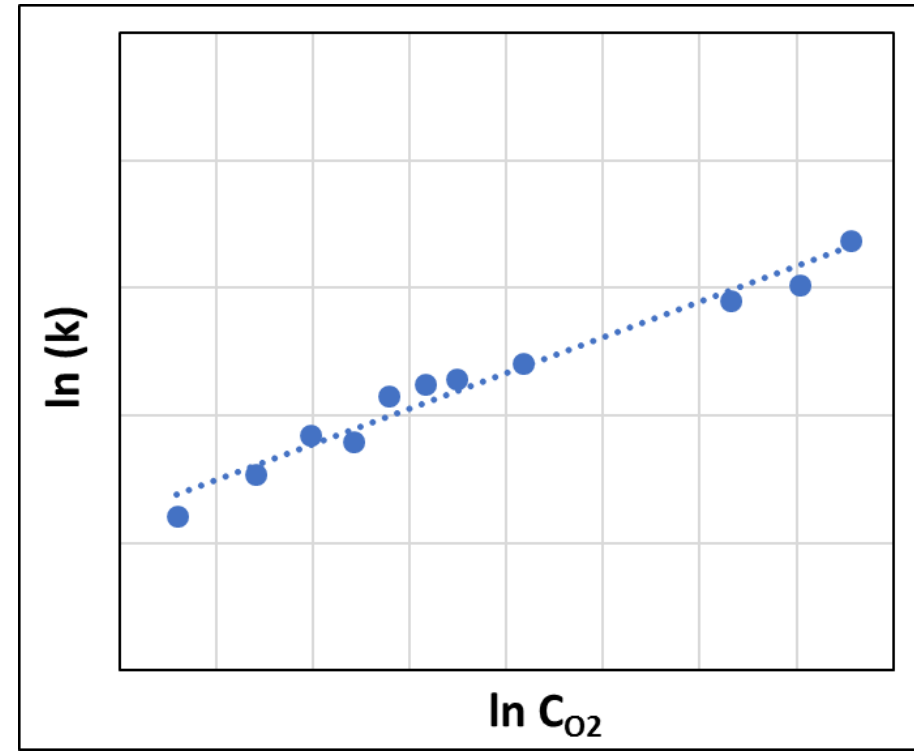
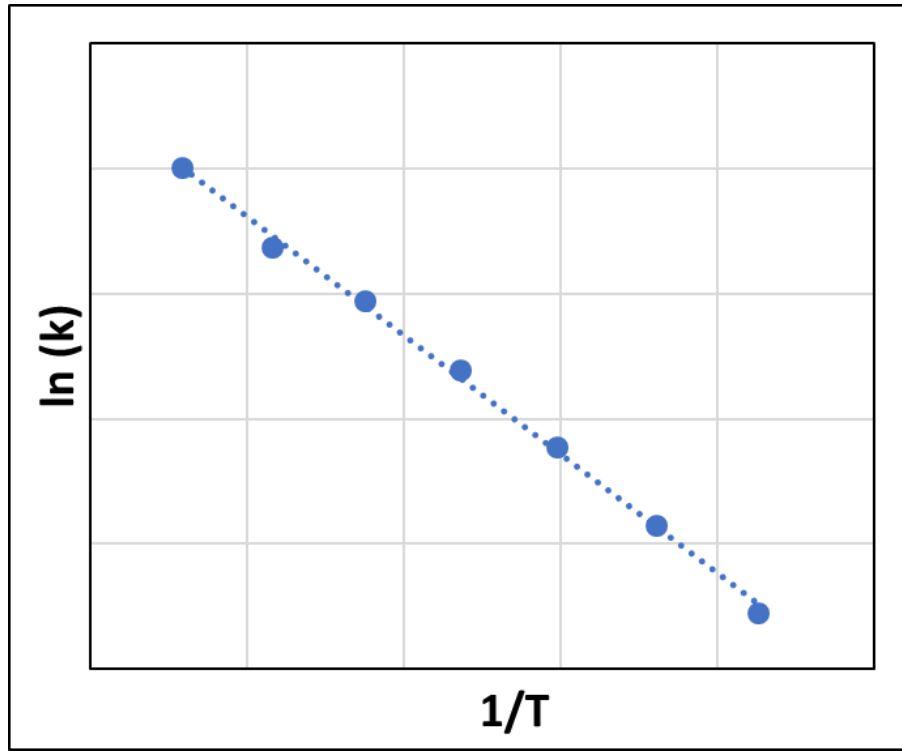
Adsorption Kinetics



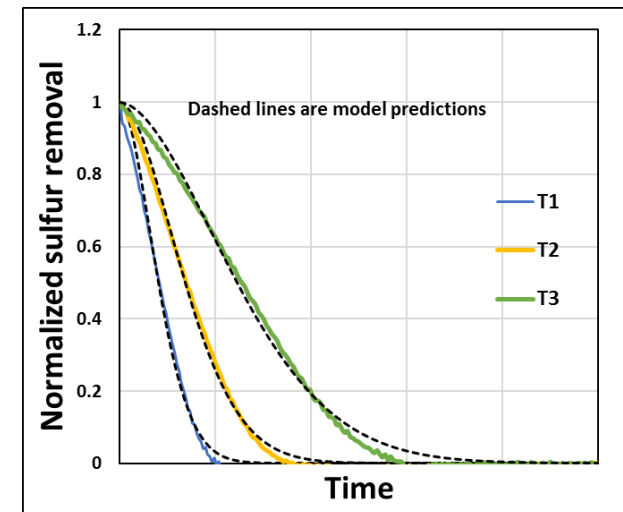
- A simplified kinetic expression was generated to incorporate the effect of adsorption operating parameters (temperature, H_2S partial pressure, etc.)
- Excellent agreement was observed between the experimental and model-predicted data



Desorption Kinetics



- A simplified kinetic expression was generated to incorporate the effect of regeneration operating parameters (temperature, O_2 partial pressure, etc.)
- Excellent agreement was observed between the experimental and model-predicted data

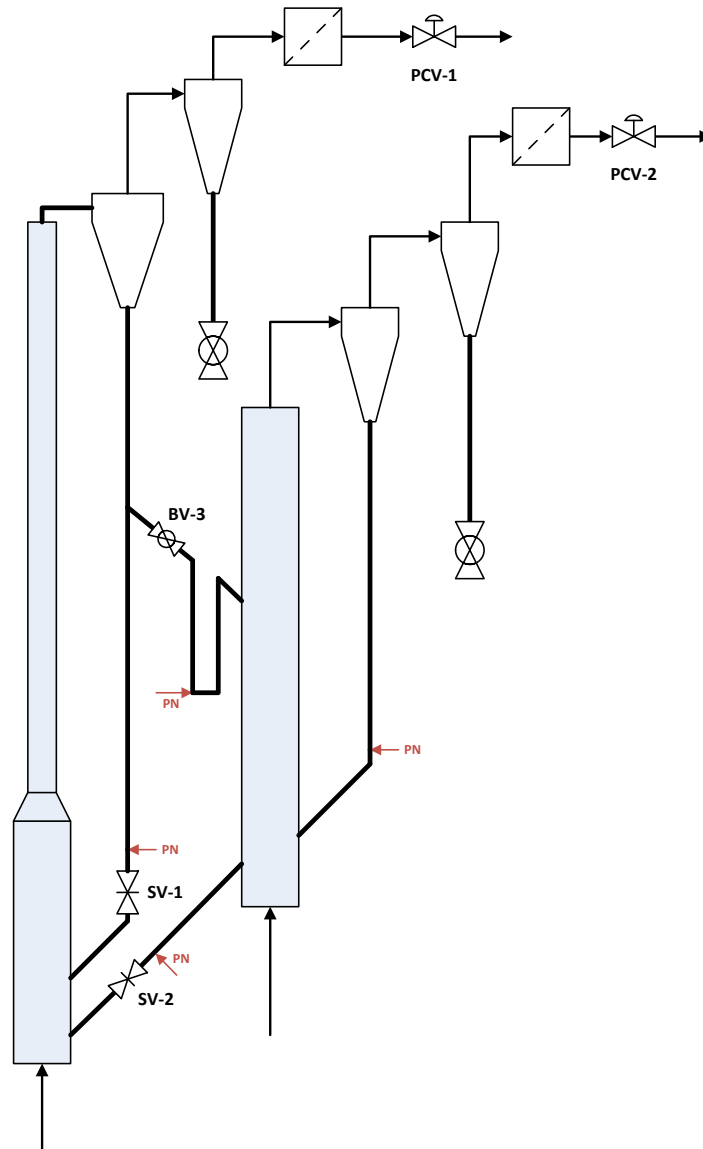


Task 3.0: Fluid-Bed Regenerator Development

- Objective: Development of a fluid-bed regenerator for REMS application, especially with low-sulfur syngas
- Completed acquiring hydrodynamic data for the sorbent at key regions within the fluid-bed reactor system using the existing cold-flow unit (Milestone 4)
- Additional hydrodynamic data will be collected in the hot-flow testing system at a combination of pressure and/or temperature to enable extending the application of the data to commercially relevant operating conditions
- Perform cyclic sorbent sulfur testing in the hot-flow unit under simulated operating conditions
- Hydrodynamic data generated at cold and hot/pressurized conditions will be used to develop sorbent hydrodynamic model

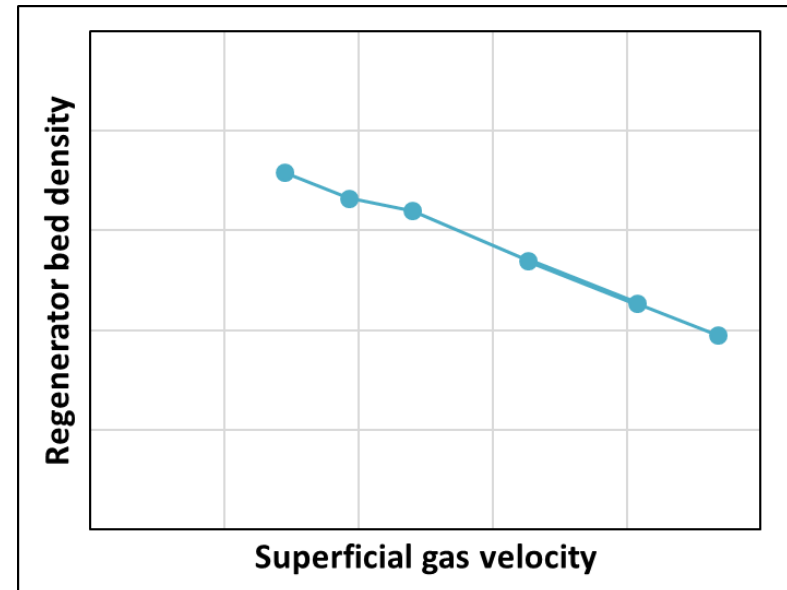
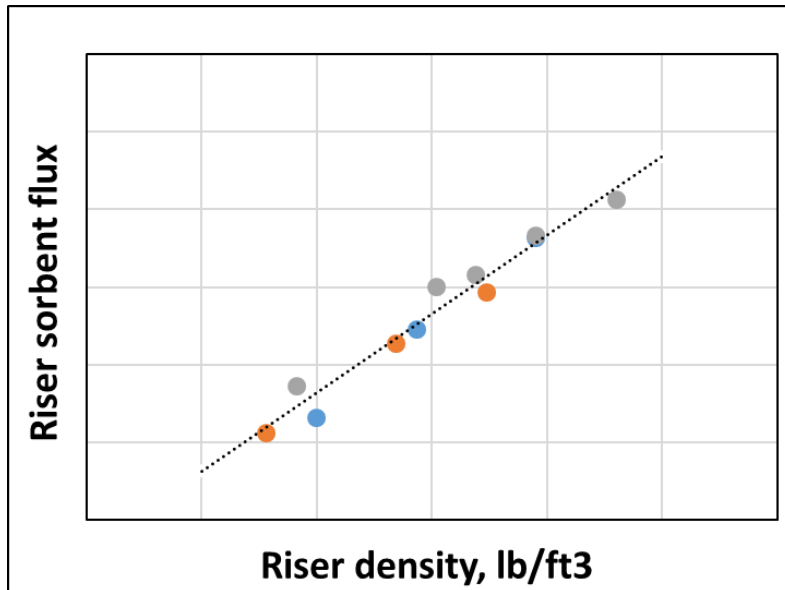
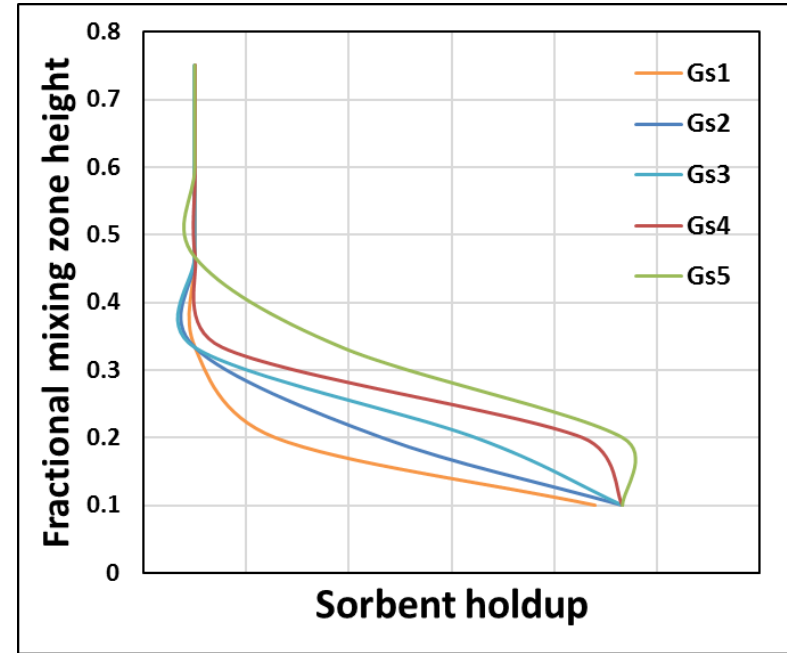
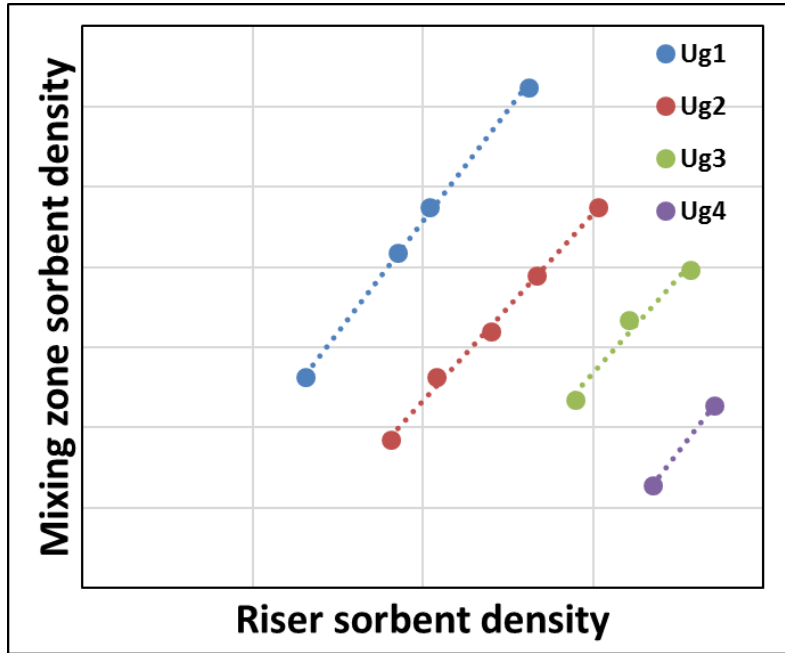
% Complete	50
Sub-task 3.1	100
Sub-task 3.2	50
Sub-task 3.3	NA

Subtask 3.1: Cold-Flow Testing

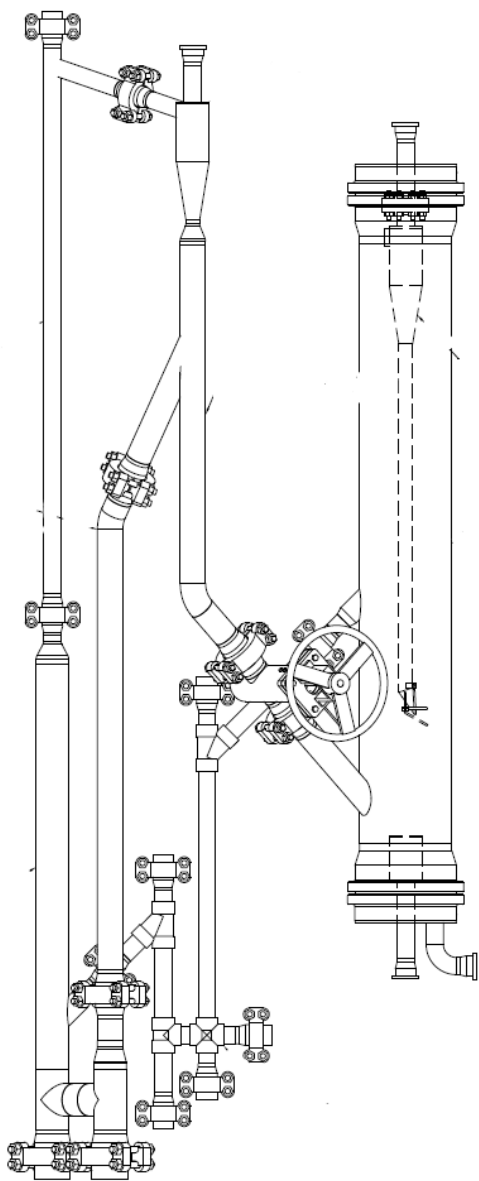


- Transport reactor absorber
 - Mixing zone-Riser Design
 - 8" mixing zone and 4" riser
- 6" fluidized bed regenerator
- 2" transfer lines
- Line size slide valves
 - Recirculation and transfer
- Two cyclones in series
- Extensively instrumented with dP transmitters

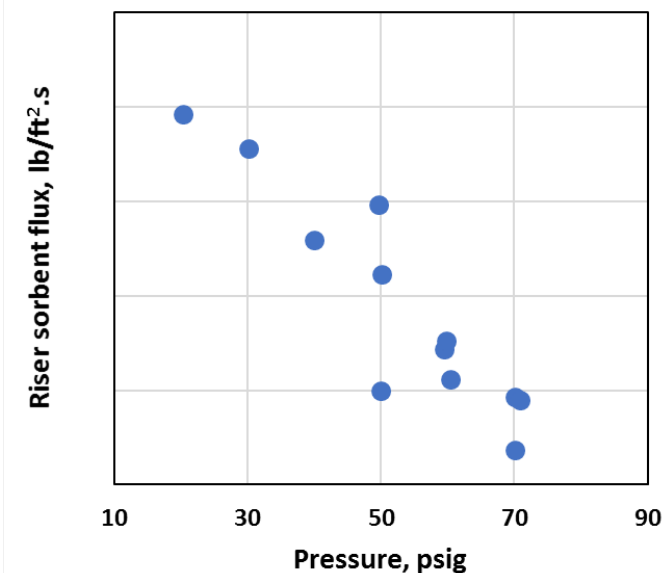
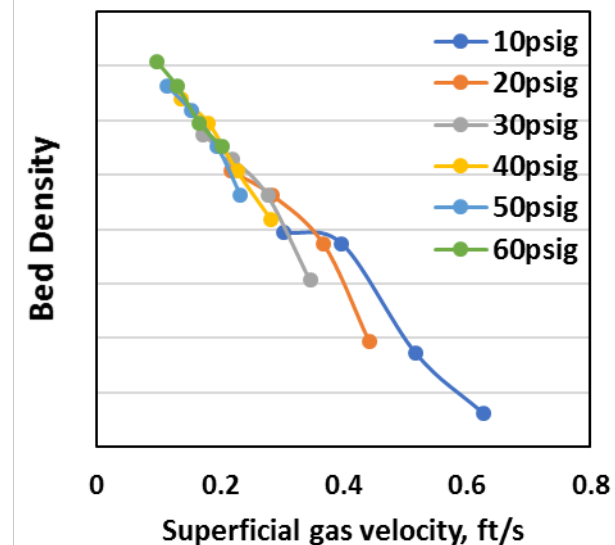
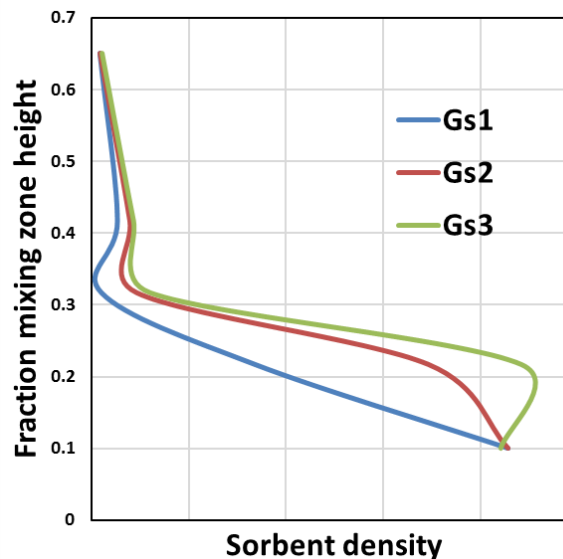
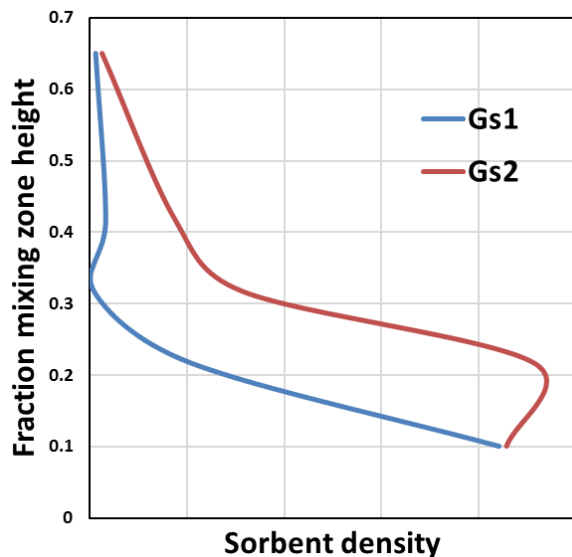
Milestone 4 Complete – Acquisition of Cold-Flow Hydrodynamic Data



Subtask 3.2 and 3.3: Hot-Flow Testing



- Design similar to the cold-flow unit
- Design limits of 150 psig and 650°C
- Completed commissioning and shake down
- Generated hydrodynamic data at ambient conditions and varying pressure
- Will study the effect of temperature in the next quarter
- Cyclic adsorption-regeneration testing in Q6-Q7



Task 4.0: Fixed-Bed Sorbent Development

- Objective: Develop a fixed-bed sorbent and process for its inherent suitability for small-scale modularized systems
- Proven chemistry of the fluidizable form will be leveraged by using co-precipitation wet cake to optimize the process of making extrudates
 - Received pilot-scale wet cake from Clariant (WDP sorbent licensed supplier) – Milestone 2 complete
 - Optimization parameters of interest are binder material and composition, and calcination temperature
- Physical properties of fresh and used sorbents will be tested for surface area, compositional analysis, XRD, and crush strength
- Parametric testing being used to optimize fixed bed process parameters (time sequences, regeneration conditions, purge, etc.)
- Optimized fixed-bed sorbent will be tested for extended stability for >50 cycles

% Complete	30
Sub-task 4.1	100
Sub-task 4.2	40
Sub-task 4.3	NA

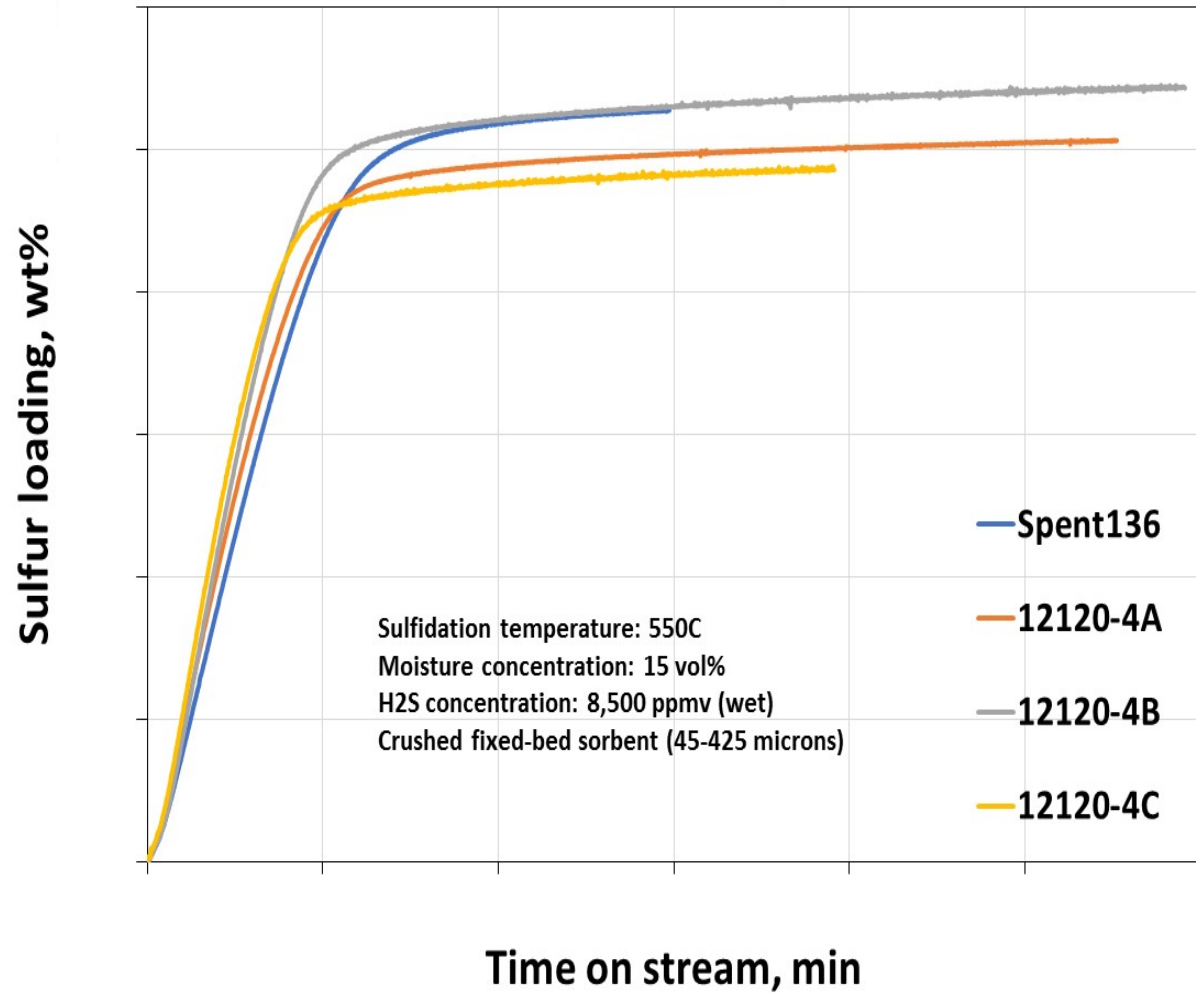
Promising Extrudates Synthesized

Sample ID	Synthesis of Extrudates		Characterization			
	Powder Source	Calcination Temp	Crush Strength, N/mm	Surface area, m ² /g	Pore size, A	Pore volume, cc/g
12120-4A	A	E	80.5	27.7	126	0.087
12120-4B	A	F	84.0	35.5	102	0.091
12120-4C	A	G	59.0	25.4	130	0.082
13768-186B	A	E	-	28.9	127	0.092
12120-13A	B	E	38.8	22.4	168	0.094
12120-14A	B	E	68.7	24.9	165	0.103

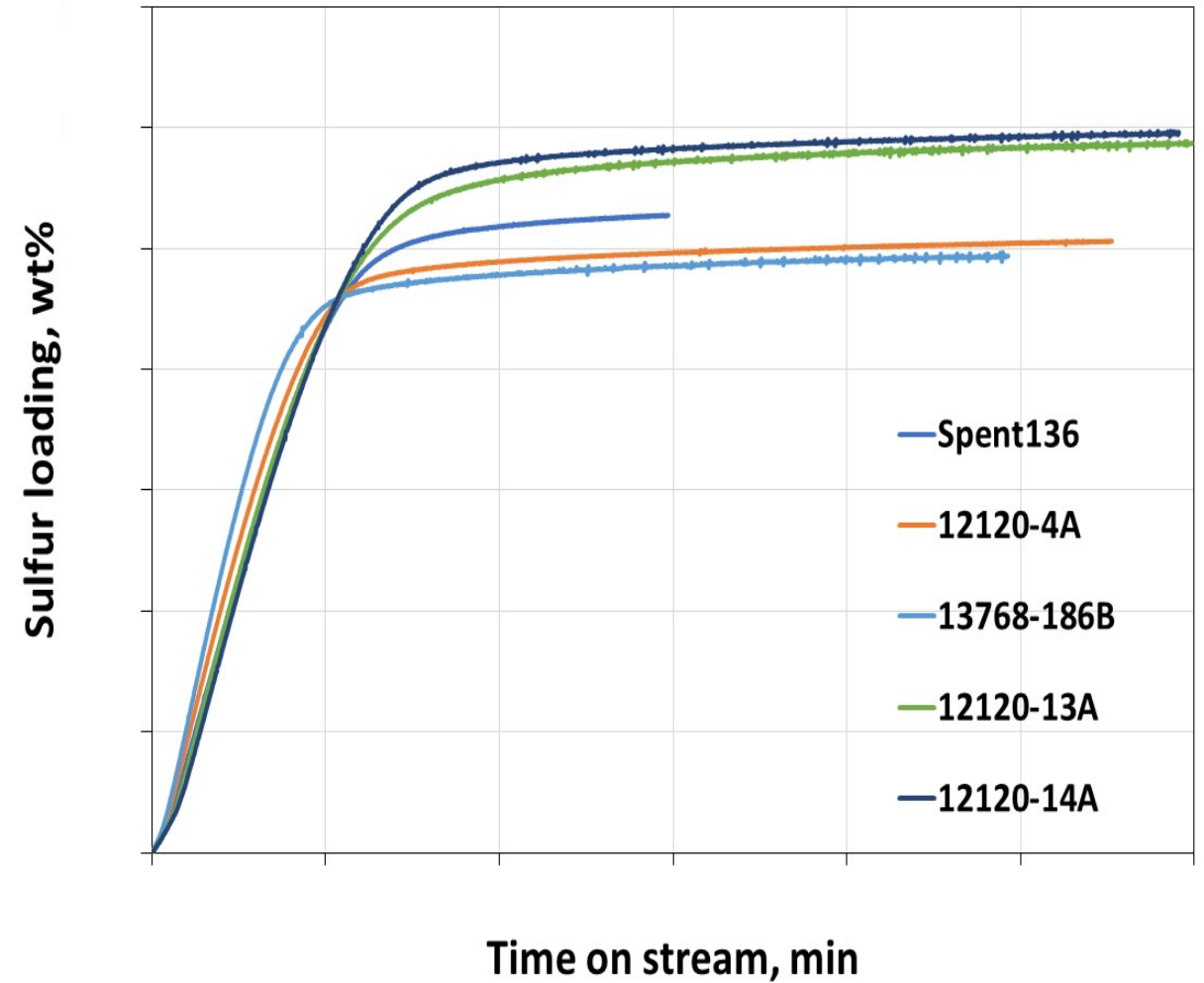
Steam reforming catalysts crush strengths in the range of 25 to 50 N/mm

Fixed-Bed Sorbent Performance – Effect of Synthesis Parameters

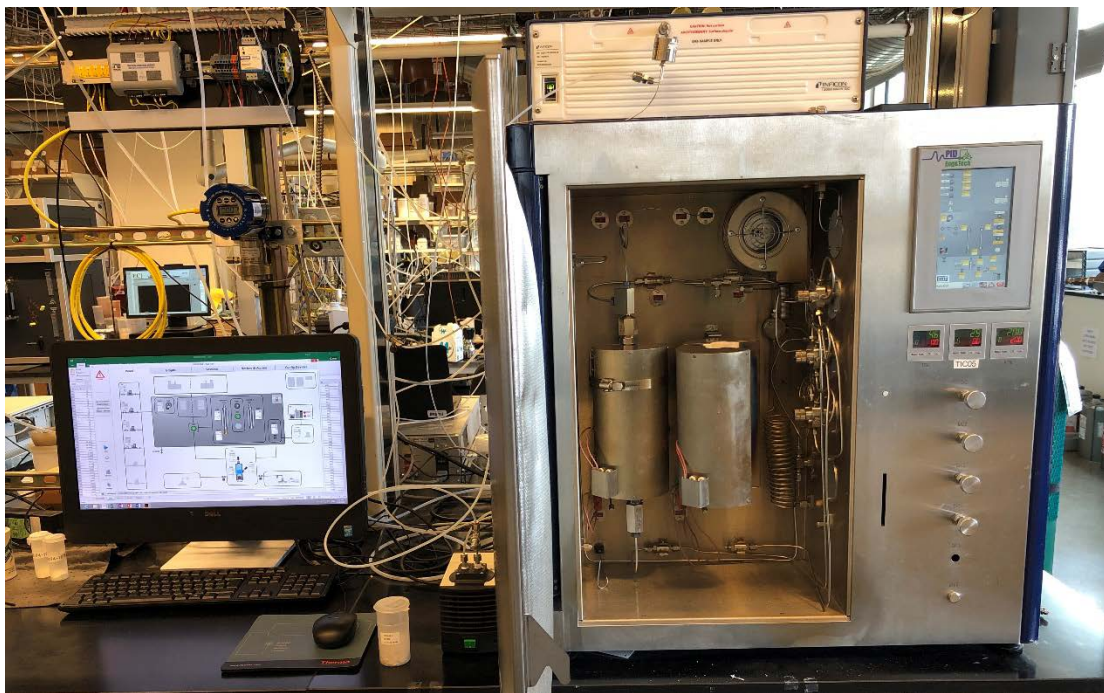
Effect of Calcination Temperature



Effect of Sorbent Source

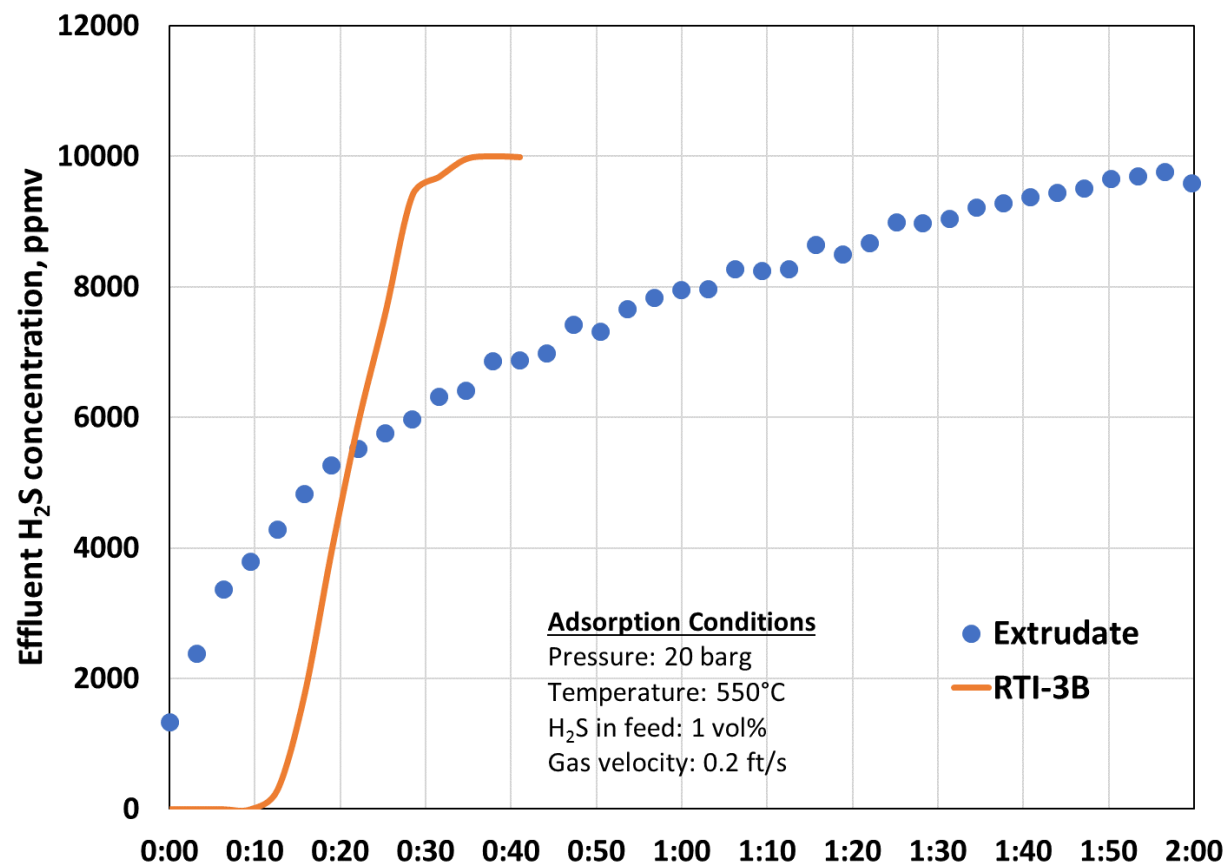


Fixed-Bed Sorbent Performance – Data for Optimization



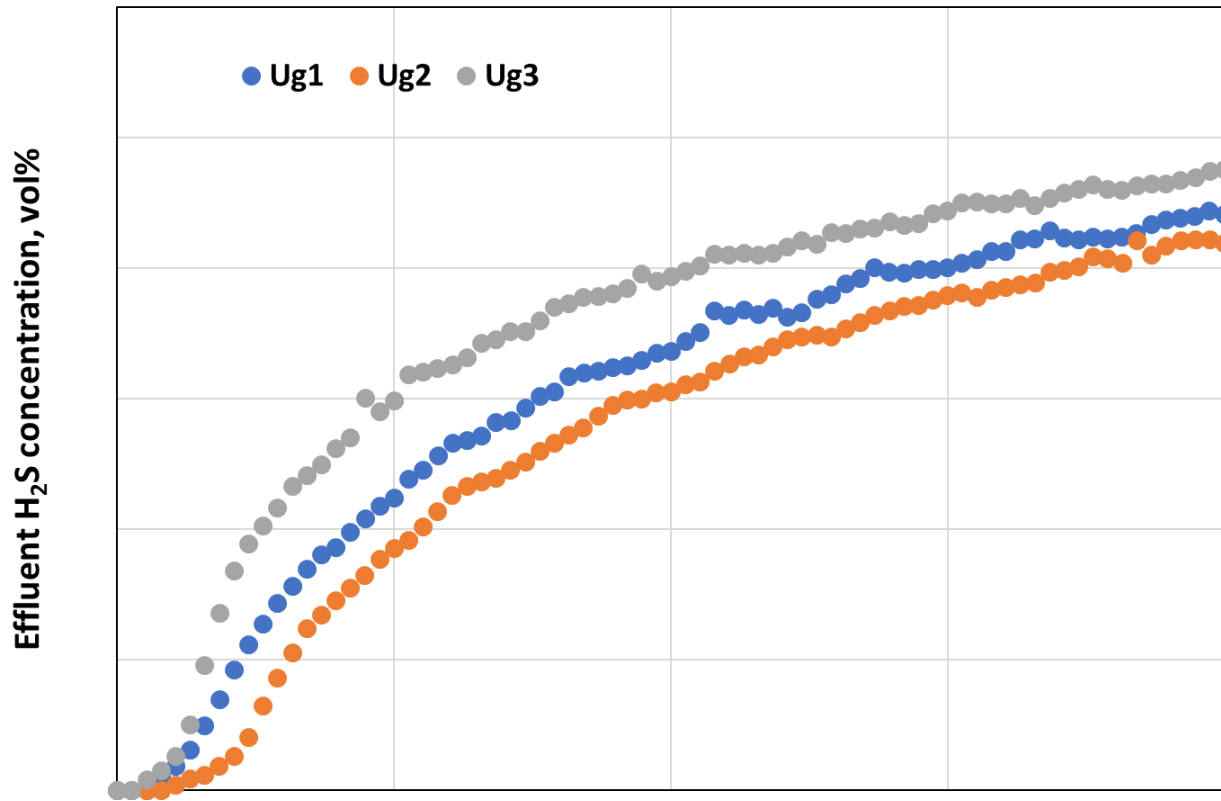
- Automated, computer controlled microreactor
- Operating limit – 100 bar and 790 C
- Standard 316 stainless steel reactor holds up to 3 mL of sorbent
- Four MFC gas feed channels
- On-line analysis of gas composition using Inficon Micro GC every 2.5 minutes
- Data logging for all instrument parameters

- Commissioned the automated system to collect data for sorbent and process optimization
- Experimental plan to study extrudate size and shape, and adsorption and desorption operating conditions

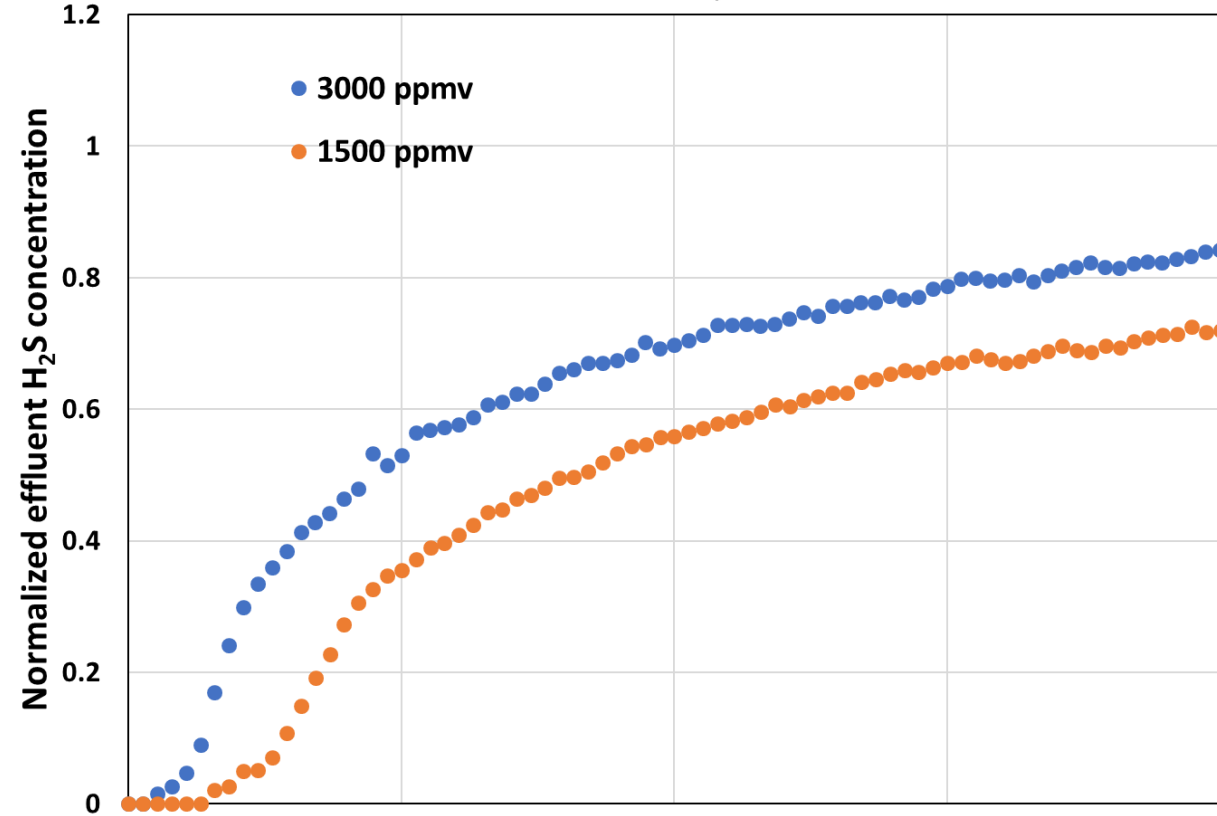


Fixed-Bed Sorbent – Parametric Testing Data

12120-14A



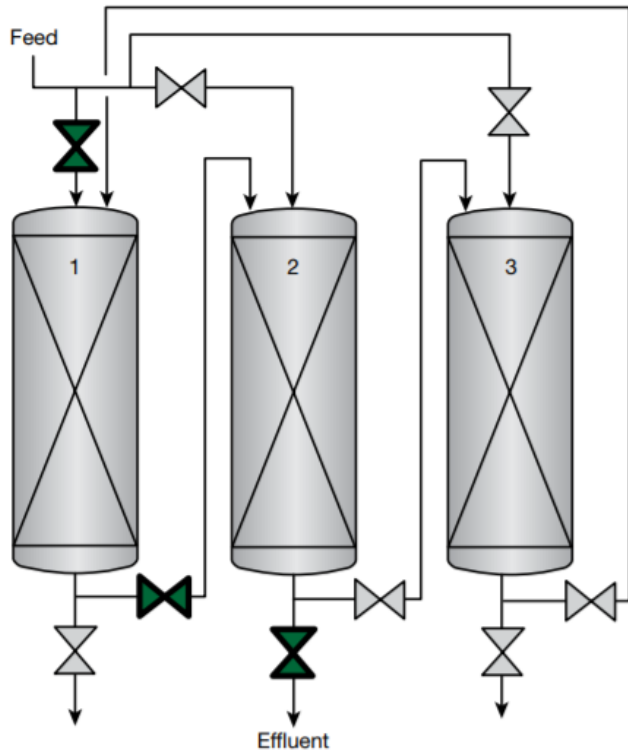
Fixed-Bed Sorbent Adsorption at 900 °F



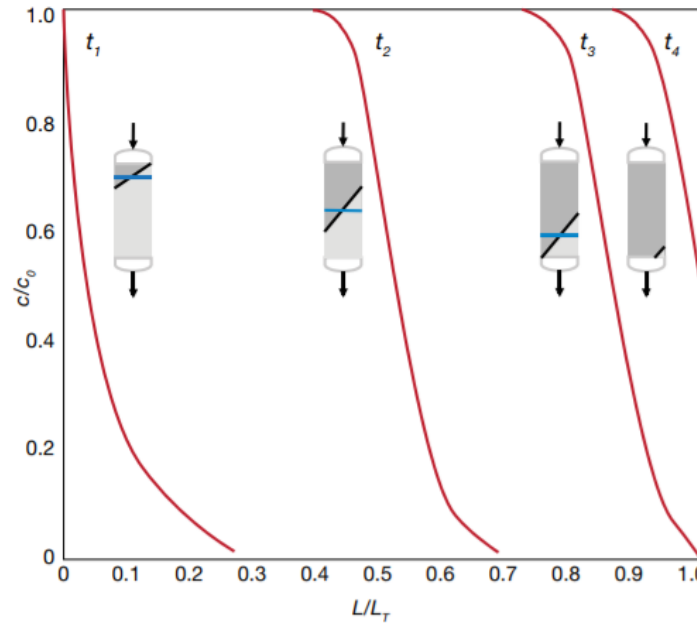
Task 5.0 Techno-Economic Analysis

- Objective: Develop and optimize conceptual designs for desulfurization processes based on fluidized-bed and fixed-bed reactors
- Data generated from Tasks 2, 3, and 4 will be used to develop and optimize fluidized-bed and fixed-bed processes
- Potential to reduce system cost through standardization, modular production and other advanced manufacturing techniques will be investigated
- The TEAs developed in this task will be developed for the overall plant from upstream gasification to syngas conversion
- Sensitivity analyses will be utilized to help optimize the overall system integration and to assess relative benefits of RTI's WDP
- Results from this task will be captured in a TEA report as a deliverable

Fixed Bed Process Development Parameters



An example three column arrangement where column 1 serves as the lead and column 3 serves as the guard with column 2 in regeneration mode



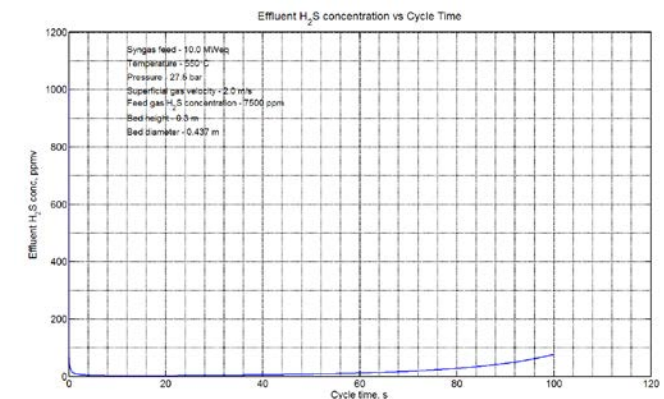
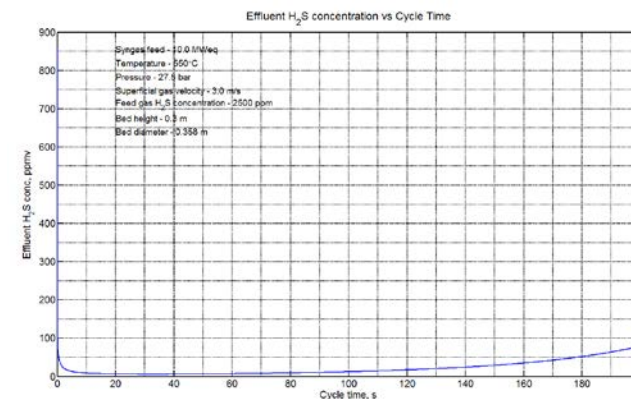
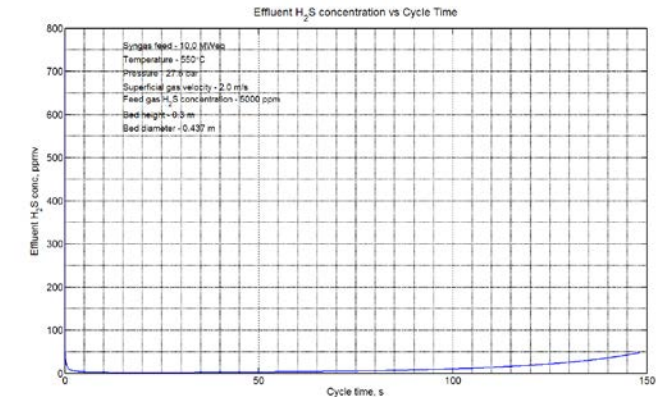
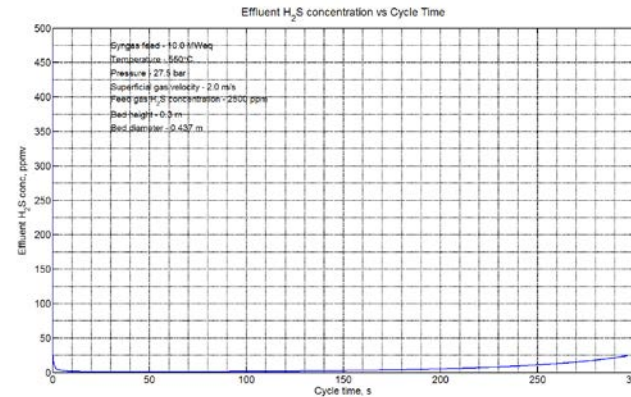
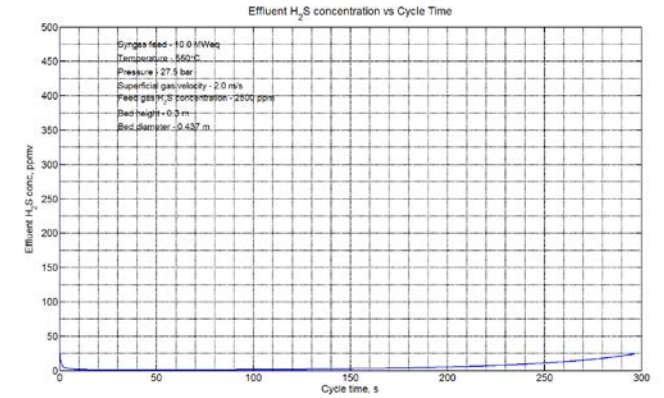
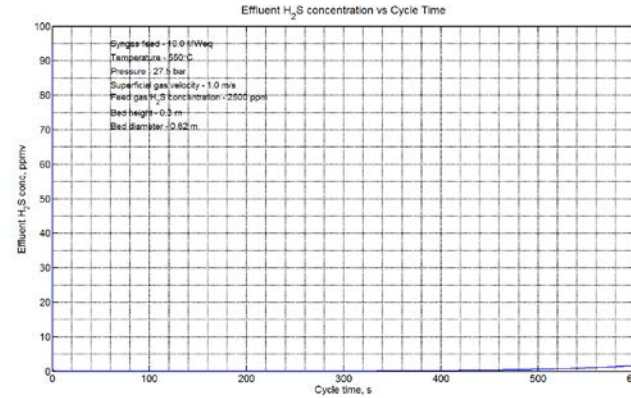
c = concentration of adsorbate
 c_0 = concentration of adsorbate in the incoming liquid
 L = length along the bed
 L_T = total bed length
 t = time

The mass transfer zone, indicated by the black diagonal line on each column, moves along the length of a fixed bed of adsorbent

- Iterative process of adsorption system design
- Adsorbent Particle Size
 - Smaller particle size lower mass transfer limitation but increase pressure drop
 - Preferred particle size is the smallest that still has a tolerable pressure drop
 - Common particle size range: 2-4 mm
- Superficial Gas Velocity
 - Length of MTZ increases with increasing gas velocity with a corresponding decrease in bed utilization
 - Typical velocity range: 0.15-0.45 m/s
- Bed Length
 - Longer bed allows for longer time-on-stream and higher bed utilization
 - However, it is more expensive and leads to higher pressure drop

Matlab Model to Simulate Fixed-Bed Reactors

- Developed a Matlab model to integrate:
 - Adsorption and desorption kinetics
 - WGS kinetics
 - Pressure drop
 - Heat transfer
 - Internal mass transfer diffusion
- Microreactor testing data will be used to estimate internal mass transfer diffusion coefficients
- Validated model will be used for reactor design, data for cycle development, and process optimization



Conclusions

- Proposed project builds on decades of effort invested in the development of RTI's Warm Syngas Cleanup technology
- Validated excellent performance of sorbent at low-sulfur syngas conditions extending its application to low-sulfur coals (Milestone 3)
- Completed generating ambient condition hydrodynamic data for the development of fluidized-bed regenerator at ambient conditions (Milestone 4)
- Currently working on studying the effect of pressure and temperature on sorbent hydrodynamics and optimizing fixed-bed sorbent extrudates and process
- Obtained pilot-scale fluidizable sorbent wet cake for the optimization of fixed-bed sorbent and process (Milestone 2)
- Currently optimizing fixed-bed sorbent and process
- Investigating commercial interest with varying sources for low sulfur, fixed-bed applications
- **Overall, the project is on track to meeting all project milestones and achieving the project objective of developing modular sorbent-based warm syngas cleanup designs that will be cost-competitive with large state-of-the-art commercial plants**

Acknowledgements

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- Steven Markovich – Project Manager



Questions?

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